# PERMIT APPLICATION FOR MODIFICATION OF THE BUCK COMBINED CYCLE FACILITY SALISBURY, NORTH CAROLINA Revision I

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#### **1.0 INTRODUCTION**

Duke Energy Carolinas, LLC (Duke Energy) is currently permitted (Air Permit No. 03786T34) to operate the Buck Steam Station located in Rowan County, North Carolina, which is currently attainment for all regulated pollutants. Duke Energy expanded this facility in 2011 by adding two (2) combustion turbine generators (CTGs) with supplemental duct firing operating in a 2x1 combined cycle mode with a nominal capacity of 620 MW. The combined cycle turbines are equipped with selective catalytic reduction (SCR) to minimize oxides of nitrogen (NO<sub>x</sub>) emissions and an oxidation catalyst to minimize carbon monoxide (CO) and volatile organic compounds (VOC) emissions. Three of the five coal-fired boilers were retired prior to initial operation of the new CTGs, and three existing simple cycle combustion turbines were retired in October 2012. The facility currently consists of the 2x1 combined cycle power island and ancillary equipment.

Duke Energy is proposing to install and operate a fly ash processing facility consisting of a Staged Turbulent Air Reactor (STAR<sup>®</sup>) plant and associated ancillary activities. To support this project, Duke Energy is submitting this application for a minor source construction permit.

North Carolina Department of Environmental Quality (NC DEQ) application forms and tables are located in Appendix A. Supporting emission calculations are presented in Appendix B. Supporting documents for the Prevention of Significant Deterioration (PSD) netting calculation are presented in Appendix C. A site plan, plot plan and process flow diagrams for the proposed project can be found in Appendix D. The toxic air dispersion modeling files are presented in Appendix E. The non-hazardous secondary material (NHSM) determination is provided in Appendix F. Reasonably Available Control Technology (RACT) analysis is presented in Appendix G. Compliance Assurance Monitoring (CAM) Plan is provided in Appendix H and Appendix I contains Zoning Commission documentation.



# 1.1 GENERAL APPLICATION INFORMATION

Following is the applicant's primary point of contact and the address and telephone number where he can be reached:

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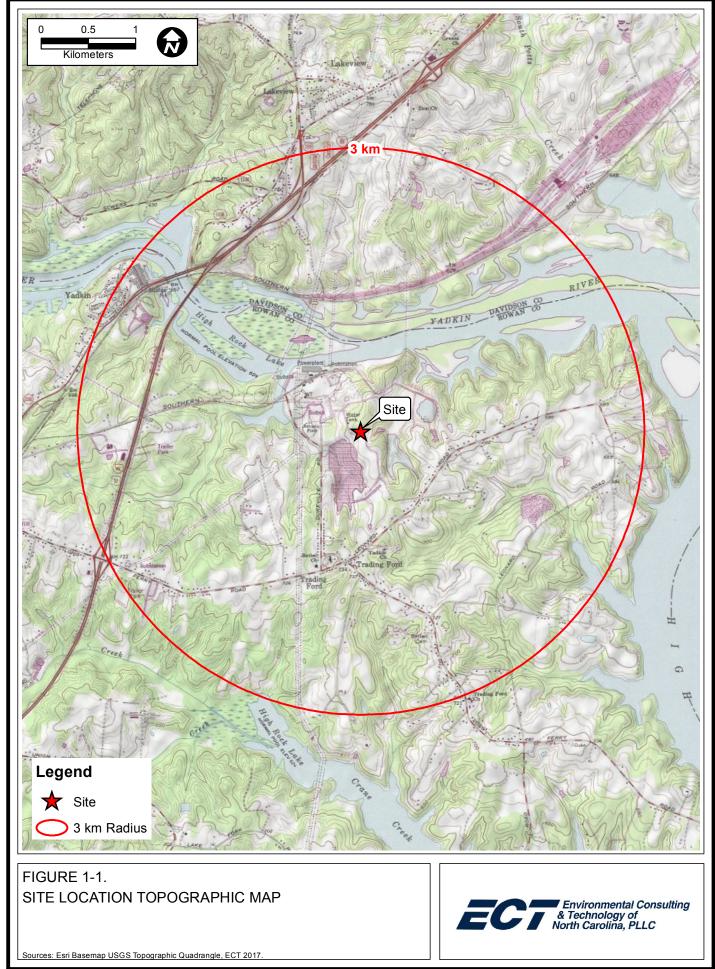
# 1.2 PROJECT LOCATION

The Buck STAR<sup>®</sup> facility will be located on the property associated with Duke Energy's Buck Combined Cycle facility, which is located at 1385 Dukeville Road, Salisbury, NC 28146. Figure 1-1 provides a regional topographic map showing the site location.

# 1.3 **PROJECT OVERVIEW**

The STAR<sup>®</sup> system is a patented technology developed by The SEFA Group Inc. (SEFA) to process feedstock (of any carbon content) like fly ash (wet or dry) along with other ingredient materials into a variety of commercial products. These products are used, not only for application as a partial cement replacement, but for many other commercial and industrial applications. For example, there are several products that SEFA is currently capable of producing because of the flexibility embodied in the STAR<sup>®</sup> process, including STAR<sup>®</sup> RP, Ultrix<sup>®</sup>, Spherix<sup>®</sup>, Fortimix<sup>®</sup>, and Permanix<sup>TM</sup>.





The associated sources of air emissions proposed to support the STAR<sup>®</sup> system includes the following:

- Ash Basin excavation.
- Ash Handling/Processing.
- Haul Roads.
- Screener.
- Crusher.
- Two diesel engines associated with a Screener and a Crusher.
- Wet ash receiving area and storage shed.
- Wet ash feed hopper.
- Wet ash unloading pile
- Two External heat exchangers (EHE) (with baghouses).
- Transfer silo filling and unloading (with bin vent product capture device).
- Feed silo filling and unloading (with bin vent product capture device).
- Storage dome filling and unloading (with bin vent product capture device).
- Loadout silo (with bin vent product capture device).
- Loadout silo chute 1A (with bin vent product capture device).
- Loadout silo chute 1B (with bin vent product capture device).
- FGD Byproduct Silo (with bin vent product capture device).
- FGD Absorbent Silo (with bin vent product capture device).

The facility will be designed to produce up to 400,000 tons of fly ash product annually. Figure 1-2 illustrates a general process flow diagram for proposed facility.

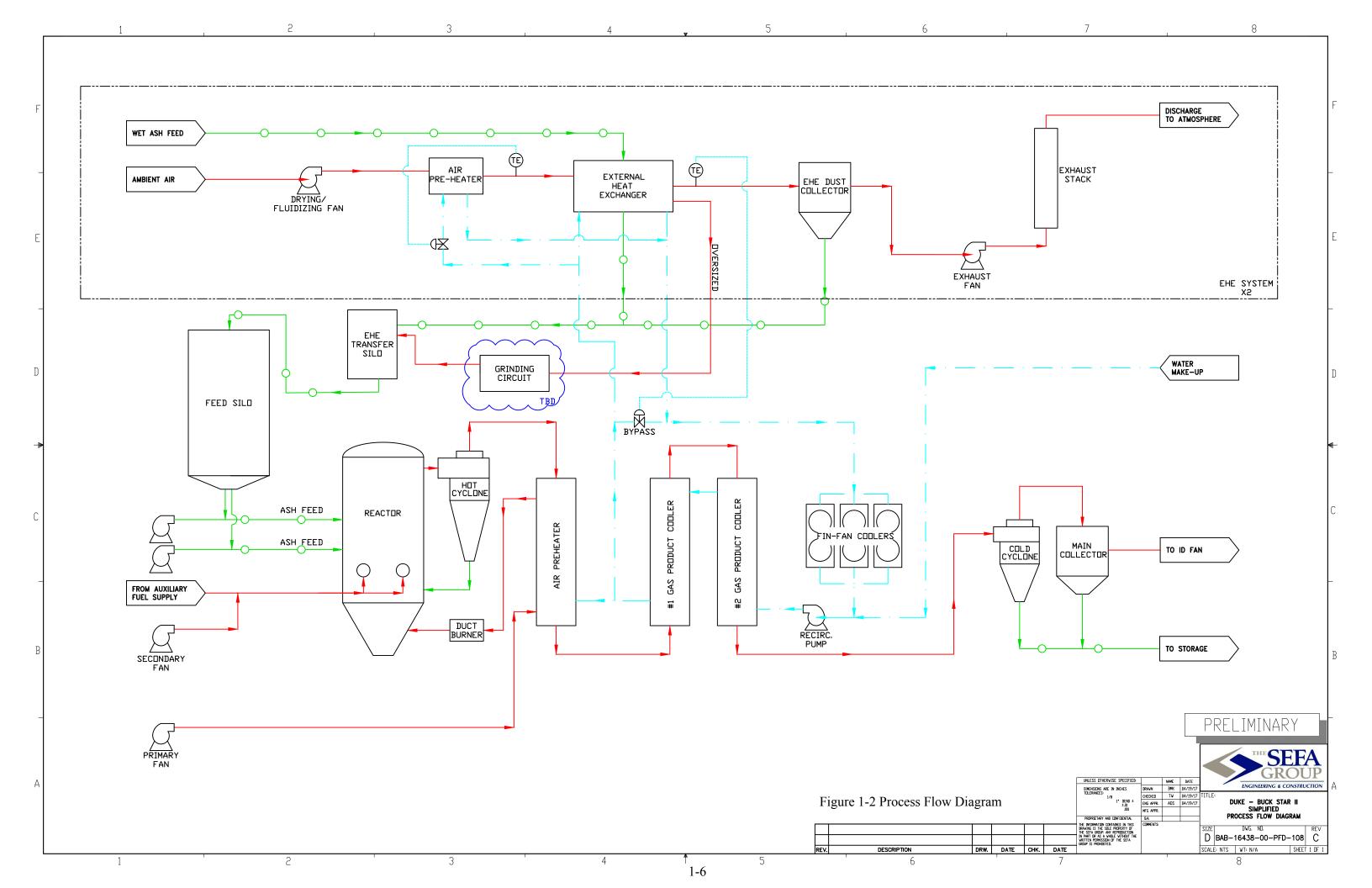
# 1.4 <u>CONTENTS OF THE MODIFICATION PERMIT APPLICATION</u>

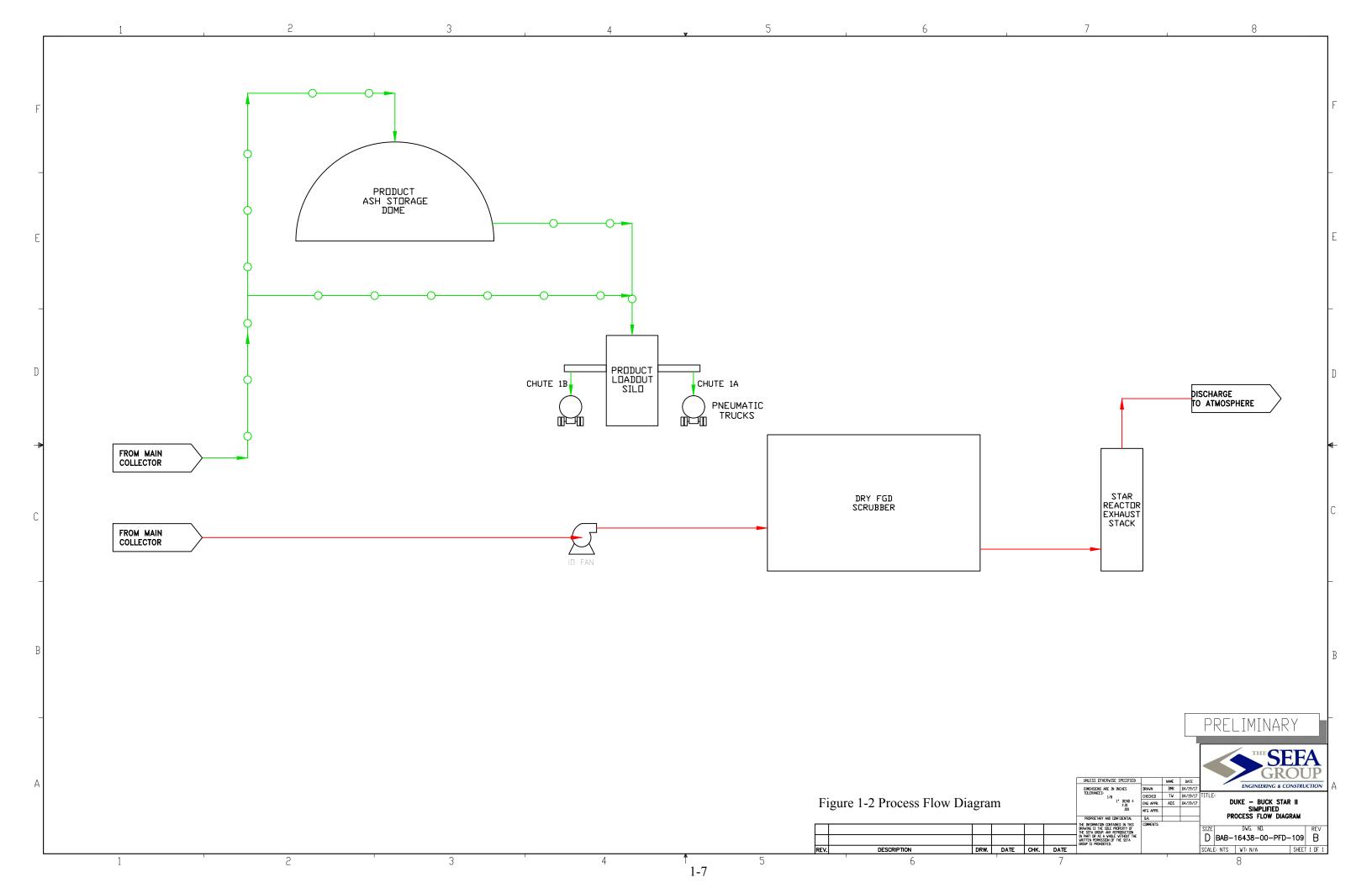
Section 2.0 of this document provides a source description of the facility. Section 3.0 presents the projected air emissions. Section 4.0 discusses the regulatory applicability, and Section 5.0 presents the air toxic dispersion modeling methodology and results. The appendices are organized as follows:



- Appendix A—Air Permit Application Forms.
- Appendix B—Supporting Emissions Calculations.
- Appendix C—PSD Netting Calculations and Support Documentation.
- Appendix D—Facility Drawings.
- Appendix E—Electronic Air Dispersion Modeling.
- Appendix F—NHSM Determination.
- Appendix G—RACT Analysis.
- Appendix H—CAM Plan.
- Appendix I—Zoning Commission Documentation.







#### 2.0 PROCESS DESCRIPTION

#### 2.1 PRE-REACTOR MATERIAL HANDLING EQUIPMENT

Excavation and processing of materials from the ash ponds to meet the STAR<sup>®</sup> system fly ash (ingredient) specifications will be under the control of the Duke Energy. All fly ash reclaimed from an ash pond delivered for use as an ingredient in the STAR<sup>®</sup> system must first undergo processing by the owner to be:

- A. Free of all, but minimal contaminants (e.g., organic debris, slag);
- B. Finely-divided and free-flowing,
- C. Have consistent moisture content of  $\leq 25\%$ ; and
- D. Have a consistent chemical composition, including organic content a measured by loss on ignition.

The processing sequence of events will include fly ash being excavated and staged to allow for dewatering (ensures moisture content of  $\leq 25\%$ ). Dewatered fly ash will then be screened to remove contaminants (organic debris, slag, etc.), to produce a consistent chemical composition and a finely divided free-flowing ingredient.

Wet fly ash nominal 15 percent by weight moisture (water) is delivered via trucks. The wet fly ash can be unloaded from the trucks into the storage shed, unloaded from the trucks to a pile that is then transferred to a storage shed by a front-end loader, or unloaded from the trucks directly into the feed hopper. The wet fly ash in the shed is transferred via front-end loader to a hopper at up to 70 wet "short" tons per hour (tph) (one "short" ton = 2,000 lb), which then conveys the wet fly ash to the mechanical conveyance equipment. The material is discharged from the mechanical conveyance equipment into a material delumper unit to reduce the "overs" material. The material discharged from the delumper unit is then introduced into the EHE by gravity, where it is continually fluidized using preheated air.

The fluidized material is dried by two heat transfer means: (1) intimate contact of the wet, fluidized material with the heated fluidizing air and (2) direct contact of the wet material



with hot water heat exchangers located in the EHE. By contact of the material with the outer surfaces of the heat exchanger tube, heating energy is transferred from the tube-side hot water (hot water that is a part of the facility's cooling loop at approximately 350 degrees Fahrenheit [°F] at 250 pounds per square inch gauge [psig]) to the material such that the material heats and, consequently, dries, while the supplied hot water temperature is reduced.

The material is discharged from the EHE units via two means. The primary method of material discharge from the unit is via the fixed-height overflow weir located at the discharge end of the unit. This overflow stream (comprising the majority of the material discharged from the unit) enters the integrally-constructed discharge box/chute of the unit. The second method of material discharge from the unit is via an integrally-constructed underflow discharge screw or rotary valve. The purpose of this underflow discharge stream is to discharge large or oversized material from the unit that, due to these particles' size, may not sufficiently fluidize to the point that they would reach the normal overflow weir height. The material is discharged from the unit at less than 2.0 percent by weight moisture and at a temperature range of 150 to 300°F to downstream material-handling equipment (transfer silos).

The exhaust air is discharged from each EHE through interconnecting ductwork to a highefficiency bag filter unit operation for feedstock recovery/exhaust air treatment. The moisture- and dust-laden exhaust air enters the unit, and, as the air passes through the filter media, dust is separated from the exhaust air stream with high fractional removal efficiency. The high-efficiency filter media used will be able to achieve a particulate matter (PM) exhaust rate of 0.025 grain per dry standard cubic foot (gr/dscf) of exhaust air (or less).

After the bag filter unit, the cleaned exhaust air stream passes through interconnecting ductwork to the exhaust air fan. The exhaust air volumetric rate is estimated at approximately 41,550 actual cubic feet per minute (acfm) at 10 inches in the water column (water



gauge) static pressure (atmospheric pressure) and at approximately between 150-300°F (and at or below the dust loading rate of 0.025 gr/dscf).

# 2.2 <u>STAR® TECHNOLOGY</u>

As discussed previously, the STAR<sup>®</sup> process is a patented technology developed by SEFA to process feedstock (of any carbon content) like fly ash (wet or dry) along with other ingredient materials into a variety of commercial products. These products are used not only for application as a partial cement replacement but also as an ingredient in many other commercial and industrial applications.

The STAR<sup>®</sup> process is inherently flexible in that operating parameters can be varied and different ingredients can be added to produce a desired product. The primary component of the STAR<sup>®</sup> is a cylindrical refractory-lined vessel in which the majority of the process reactions take place. These reactions can include a range of both chemical and physical reactions. Air required for pneumatic uplift of the solids and for the process reactions enters through the floor of the STAR<sup>®</sup> system as well as through the walls at multiple locations. The raw feedstock and any other ingredients are introduced through the walls of the STAR<sup>®</sup>. All of the solids and gases exit together at the top of the reactor. The gas/solids mixture enters a hot cyclone, where the majority of solids are separated from the gas and recycled back to the STAR<sup>®</sup> system. The high rate of hot recycle solids increases the operating flexibility of the process. The process reactions can occur through this reactor/hot cyclone loop. Due to the high gas velocity, multiple injection points, and recycle solids, there is a significant amount of turbulence created that enhances the mixing of the ingredients and optimizes the reactions. The gas and remaining solids not collected by the hot cyclone are passed over a heat exchanger, which can be designed to preheat the process air, used in heat recovery or to simply cool the gas/solids mixture. Once cooled, the solids are separated from the gas in a fabric filter recovery device. The STAR<sup>®</sup> system's integral design allows for solids to be removed from the bottom of the reactor or from the recycle loop ultimately to be combined with the solids/gas stream before the heat recovery equipment. By design the STAR<sup>®</sup> operates under a wide range of process parameters to produce



a high-quality class F fly ash for beneficial use in ready mix concrete or other specialty products.

During startup, the process air is heated with a startup burner firing auxiliary fuel (i.e., natural gas or propane) until reactor temperatures reach auto-ignition. At this point, the residual carbon in the fly ash reacts and becomes the heat source for the self-sustaining process. Under certain conditions, auxiliary fuel may be co-fired with the residual carbon in the fly ash. Process controls meter additional raw fly ash through a feeder into the reactor as necessary. As additional material is added to the reactor, processed fly ash is entrained in the exhaust and exits the top of the reactor.

After exiting the reactor, the fly ash entrained in the flue gas passes through a hot cyclone where solids are returned to the reactor for temperature control. The fly ash and flue gas leaving the hot cyclone is conveyed to the air preheater then passes through a gas cooler. The cooled flue gas and fly ash passes through a fabric filter baghouse, which is an integral part of the process for product capture, and then exhausts to a Dry Flue Gas Desulfurization (FGD) system (using hydrated lime as a reagent and an additional fabric filter control device) to reduce SO<sub>2</sub> emissions. The FGD exhaust is vented to the atmosphere through a stand-alone stack.

The Dry FGD system consist of a Circulating Dry Scrubbing System (CDS) and a Fabric Filter baghouse (FF). Flue gas, reagent (hydrated lime) and water are mixed homogenously in the CDS to absorb the acid gas, sulfur oxides, and is collected in the FF baghouse. The clean gas will then flow from the CDS-FF system to an Induced Draft (ID) fan which forces the clean exhaust gas up the stack where it discharges to atmosphere. The byproduct solids are discharged from the FF baghouse into a byproduct storage silo. The system is comprised of a three (3) day storage silo with vent filter, fluidizing air stones and dry unloading chutes. Dry dust unloading chutes are telescoping chutes equipped with small ventilation fans that recirculate displaced air back to the top of the byproduct storage silo.



# 2.3 POST-REACTOR MATERIAL HANDLING EQUIPMENT

Once the fly ash leaves the reactor, it is collected in the product recovery baghouse and pneumatically transferred to either the storage dome or the loadout silo, each equipped with a bin vent. The truck loadout station uses telescoping chutes and a negative pressure ventilation system to reduce fugitive emissions.



#### 3.0 EMISSIONS CALCULATIONS

This section contains the New Source Review (NSR) applicability determination for the proposed Project and discusses the basis and methodology for the calculation of air pollutant emission rates for the proposed sources. Per 40 CFR 51.166, the proposed project is subject to the provisions of PSD if the project will result in significant emissions increase and significant net emissions increase exceeding specified thresholds for each pollutant. Emissions increase analysis was prepared for each NSR pollutant to summarize the emissions increases and decreases associated with the proposed project. The results of this analysis were used to determine whether any pollutants are potentially subject to NSR applicability.

This section is organized to follow the steps in the project emissions increase analysis. A summary of the NSR applicability determination is provided first, with supporting documentation provided in the subsequent subsections. The NSR applicability determination was prepared in accordance with the provisions of 40 CFR 51.166, 15 NCAC 2D.0530 and 2D.0544.

For the emission sources to be added for the proposed Project, emission rates are based on process information developed and provided by SEFA, Duke Energy, manufacturers' data, and/or published emission factors such as those contained in the U.S. Environmental Protection Agency's (USEPA) Compilation of Air Pollutant Emission Factors, AP-42. Unit design parameters and operational practices have been incorporated into the analysis to make the emission estimates conservative and representative of on-site conditions. Emission estimates are provided for criteria pollutants, hazardous air pollutants (HAP) and toxic air pollutants (TAP).

The emissions impact of project-related sources is based on the potential emissions for all new sources that will be included in the project. Detailed emission calculation methodolo-



gies and throughput data for the emission sources specified in the PSD applicability analysis are presented in Appendix B. A summary of the results of the PSD applicability determination and project emissions increase analysis are provided in Appendix C.

#### 3.1 <u>NSR REVIEW APPLICABILITY DETERMINATION SUMMARY</u>

A NSR applicability determination was prepared for each applicable NSR pollutant specified in 40 CFR 51.166. These pollutants include NO<sub>x</sub>, SO<sub>2</sub>, PM, particulate matter with diameter less than 10 microns in diameter (PM<sub>10</sub>), particulate matter with diameter less than 2.5 microns in diameter (PM<sub>2.5</sub>), CO, ozone (as VOC), lead (Pb), sulfuric acid mist (H<sub>2</sub>SO<sub>4</sub>) and greenhouse gases (GHGs). The proposed project is deemed to be subject to PSD, if the sum of the increases and decreases associated with the project exceeds the pollutant-specific thresholds defined as a "significant emissions increase" in 40 CFR 51.165 and 40 CFR 51.166. A summary of the individual steps in preparing the NSR emissions increase analysis is as follows:

- Emissions increase associated with the project: The emissions increase equals the difference between the projected actual or potential emissions and the baseline actual emissions for each existing unit. If the modified units are new and therefore do not have 24 consecutive months of operating data, then the baseline actual emissions will equal the potential to emit.
- Emissions increase (or decrease) due to other permitted changes which occurred during the contemporaneous period for the proposed project.
- The project emissions increase equals the sum of the emissions increases (or decreases) for all new and existing sources associated with the project.

# 3.2 **PROJECT EMISSIONS**

# 3.2.1 STAR<sup>®</sup> SYSTEM

Emissions from the STAR<sup>®</sup> system, include PM/PM<sub>10</sub>/PM<sub>2.5</sub>, SO<sub>2</sub>, NO<sub>x</sub>, CO, VOCs, and GHGs from the auxiliary fuels and residual carbon in the fly ash. Emissions from the auxiliary fuels were estimated using the most recent emissions factors for natural gas- and propane-fired boilers contained in the U.S. Environmental Protection Agency's (EPA's)



Compilation of Air Pollutant Emissions Factors (AP-42). The auxiliary fuel burners are a low-NO<sub>x</sub> design intended to comply with North Carolina NO<sub>x</sub> control regulations.

Emissions of  $NO_x$  and CO from the processing of the residual carbon in the fly ash were estimated based on emissions estimates from other existing STAR<sup>®</sup> units. Particulate emissions for the STAR<sup>®</sup> are based on the baghouse manufacturer's data of 0.01 grain per actual cubic foot (gr/acf). The induced draft fan providing the motive force for the product transfer is rated at 56,846 acfm, at the expected process conditions of 350°F and nominal atmospheric pressure.

 $SO_2$  emissions are a function of the amount of fly ash processed through the reactor, the sulfur content of the fly ash, the amount of sulfur remaining in the product ash exiting the  $STAR^{(R)}$  reactor, and the  $SO_2$  air pollution control equipment removal efficiency, in this case the dry scrubber. Assuming ash sulfur content of 0.15 percent and 100-percent oxidation of the sulfur. The dry scrubber will be designed to provide 100-percent capture and can be operated with an  $SO_2$  control efficiency of 95 percent.

Fly ash generated from the combustion of coal may contain trace quantities of heavy metals. Duke Energy provided metals emission factors based on averages, ash analysis was used to calculate the emission rates for each metal.

The STAR<sup>®</sup> system will normally fire auxiliary fuels during system startup and will cut back on auxiliary fuel feed as the reactor reaches self-sustaining conditions. However, emissions have been estimated conservatively by combining the total emissions associated with firing the worst-case auxiliary fuel at full capacity with the total emissions from fly ash processing.

GHG emissions were also calculated from the STAR<sup>®</sup> reactor. GHG emissions were based on the annual natural gas and propane usages and emissions factors from Table C-1 of Chapter 40, Part 98, Code of Federal Regulations (CFR), Subpart C, along with the loss of



ignition of the fly ash. Appendix B provides detailed spreadsheets and example calculations.

# 3.2.2 MATERIAL HANDLING

The material handling system includes one wet ash raw feed unloading pile, one wet ash storage shed, one wet ash EHE feed hopper, two EHE's, raw feed silos, one loadout silo, two loadout chutes, transfer silos, a product storage dome, FGD byproduct silo, FGD absorbent silo, screener, crusher, ash basin and handling and haul roads. The silos are each equipped with a bin vent product capture device to minimize product losses associated with the pneumatic transfer process. The truck loadout station uses telescoping chutes and a negative pressure ventilation system to reduce fugitive emissions.

Particulate emissions from the silos were estimated using the maximum short- and long-term transfer rates and appropriate emissions factors from previous STAR<sup>®</sup> facilities.

Trace metal concentration data discussed previously for the STAR<sup>®</sup> system were used in conjunction with the calculated PM emissions rates to estimate emissions of trace metal from the material handling activities. Appendix B contains detailed spreadsheets and example calculations.

# 3.2.3 FUGITIVE EMISSIONS

Additional particulate emissions were also calculated for the wet ash receiving process, ash handling process (including screening and crushing activities) and haul roads. Windblown fugitive dust emissions were also calculated from the unloading pile. The emissions were calculated using the appropriate emissions factors from AP-42. Appendix B contains detailed spreadsheets and example calculations.

#### 3.2.4 FACILITYWIDE EMISSIONS

Table 3-1 presents a summary of the proposed project emissions and comparison to the respective Significant Emission Rate (SER).



Pollutant	Prop Project E	osed missions		
	lb/hr	tpy	SER (tpy)	Netting Required
РМ	12.05	49.14	25	Yes
$\mathbf{PM}_{10}$	10.75	43.59	15	Yes
PM <sub>2.5</sub>	6.42	24.64	10	Yes
$SO_2$	41.03	163.98	40	Yes
$NO_x^*$	30.34	117.66	40	Yes
CO	25.01	92.26	100	No
VOC	3.21	9.54	40	No
Lead	1.41E-03	6.17E-03	0.6	No
GHG (mass basis)		116,599		
GHG (CO <sub>2</sub> e basis)		116,604	75,000	Yes
Sulfuric acid mist	0.10	0.44	7	No

#### Table 3-1. Proposed Project Emissions and Comparison to the SER

\* NO<sub>x</sub> emissions from STAR<sup>®</sup> unit is based on NO<sub>x</sub> at 0.12 lb/MMBtu.

Note: lb/hr = pound per hour.

 $PM_{10}$  = particulate matter less than or equal to 10 micrometers.

 $PM_{2.5}$  = particulate matter less than or equal to 2.5 micrometers.

 $CO_2e =$  carbon dioxide equivalent.

Source: ECT, 2017.



#### 3.3 CONTEMPORANEOUS PROJECT EMISSIONS

Table 3-2 summarizes the contemporaneous increases and decreases based on data provided by Duke Energy and the existing air permit for the pollutants which have proposed project emissions above the SER. Contemporaneous project emissions include the creditable emissions increases and decreases which have occurred at the facility, which include the following:

- Shut down of coal boilers and associated coal handling equipment (contemporaneous decrease) – Per Duke Energy, for the emission decreases, the facility emission for the calendar years 2010 and 2011 represent the emission sources that have been removed from service. Therefore, emissions for these two years were averaged in order to represent the contemporaneous decrease. (See Appendix C)
- Combined cycle project (contemporaneous increase) The contemporaneous increase associated with the combined cycle project does take into account the PSD avoidance conditions with the existing permit. The emissions for the combine cycle project were taken from the current permit (03786T34), the Duct Burner Modification Application (Feb 2013), the BK Hot Gas Path Modification Application (May 2014), the BK ES-17EmGen Application (May 2016), and from the letter to NC DEQ for the addition of ash basin water pump (Feb 2017).

This information is provided in more detail in Appendix C.



Description of Emission	NO <sub>x</sub>	SO <sub>2</sub>	PM (TPY)	PM <sub>10</sub> (TPY)	PM <sub>2.5</sub> (TPY)	CO <sub>2</sub> e (TPY)
	(TPY)	(TPY)	(111)	(111)	(111)	(111)
PSD Avoidance CAP for ES11 and ES12 (Increases)	599.8	108.52	198.90	160.8	160.8	2,669,078
Non-Turbine Emissions, An- cillary Equipment (Increases)	5.71	0.23	8.05	8.04	8.04	0
Contemporaneous Decreases	(781.70)	(4724.45)	(290.26)	(257.94)	(220.84)	(0)

Note:

 $SO_2$ =sulfur dioxide PM = particulate matter  $PM_{10}$  =particulate matter less than or equal to 10 micrometers.  $PM_{2.5}$  =particulate matter less than or equal to 2.5 micrometers. CO = carbon monoxide  $H_2SO_4$  – sulfuric acid mist  $CO_2e$  =carbon dioxide equivalent.

Source: ECT, 2017.



# 3.4 PREVENTION OF SIGNIFICANT DETERIORATION NETTING ANALY-SIS

Duke Energy is applying to the NC DEQ for a revision to PSD avoidance conditions in Section 2.1.A.6.a and Section 2.1.A.7.a of Air Permit No. 03786T34 for sulfuric acid mist and VOCs. Specifically, Duke Energy is requesting the removal of VOC and sulfuric acid mist from these conditions, and the creation of a new PSD avoidance condition that addresses VOCs and sulfuric acid mist from the turbines (ES-11 and ES-12), the STAR<sup>®</sup> unit (proposed ES-74) and two proposed diesel engines associated with ash screening/crushing without change to the respective avoidance limits indicated in Section 2.1.A.6.a and Section 2.1.A.7.a of Air Permit No. 03786T34. As result of this request, VOCs and sulfuric acid mist are not subject to PSD review because no increase in these pollutants is requested.

As shown in Table 3-3 and considering the PSD avoidance condition requested in the previous paragraph, the project does not result in a significant increase in emissions of any PSD pollutant except for GHGs. Please note that GHG emissions are expected to increase by a value more than the Significant Emission Rate (SER) for GHG emissions. GHG emissions have been categorized as an "anyway" pollutant and require another PSD pollutant to be subject to PSD review before PSD review applies to GHG emissions. Therefore, GHG are not subject to PSD review for the proposed project. The emission calculation methodologies used to prepare the values are provided in Appendix B.



#### Table 3-3. PSD Netting Analysis

	NO <sub>x</sub>	$SO_2$	PM	$PM_{10}$	PM <sub>2.5</sub>	CO <sub>2</sub> e
Description of Emission	(TPY)	(TPY)	(TPY)	(TPY)	(TPY)	(TPY)
Proposed Project Emission (Increases)	117.66	163.98	49.14	43.59	24.64	116,604
PSD Avoidance CAP for ES11 and ES12 (Increases)	599.8	108.52	198.90	160.8	160.8	2,669,078
ES13 – 10 cell cooling tower (Increases)			7.00	7.00	7.00	
ES14 – Auxiliary Boiler (Increases)	1.80	0.22	0.40	0.40	0.40	
ES15 – Fuel oil fired emergency generator (Increases)	0.80	0.0009	0.028	0.023	0.023	
ES16 – Fuel oil fired fire water pump (Increases)	0.10	0.0001	0.004	0.004	0.004	
ES72 – Chiller cooling tower (Increases)			0.60	0.60	0.60	
Ash basin water management pump (Increases)	2.50	0.004	0.016	0.016	0.016	
ES17 – Fuel oil fired emergency generator, 762 hp (Increases)	0.513	0.0005	0.003	0.002	0.002	
Total Increases	723.17	272.73	256.09	212.43	193.48	2,785,682
Contemporaneous Decreases	(781.70)	(4724.45)	(290.26)	(257.94)	(220.84)	(0
Difference	-58.53	-4451.72	-34.17	-45.50	-27.35	2,785,68
PSD SERS	40	40	25	15	10	75,00
Significant Modification	No	No	No	No	No	Ye

Source: ECT, 2017.



# 3.5 TOXIC EMISSIONS

The toxic permitting emission rate (TPER) analysis was performed using the procedures outlined in 15A NCAC 2Q.0706.

The first step of the TPER analysis is to determine if the modification results in "a net increase in emissions of any toxic air pollutant that the facility was emitting before the modification" or if the modification results in "emissions of any toxic air pollutant that the facility was not emitting before the modification if such emissions exceed the levels contained in Rule .0711." The proposed modification is the installation of the STAR<sup>®</sup> unit and associated equipment. Table 3-4 presents the potential emissions of the toxic air pollutants (TAPs) from the proposed modification at the Buck STAR<sup>®</sup> facility. Please note that the diesel engines (ES-82B and ES-83B) were not included in the TPER analysis per 15A NCAC 2Q.0702 (a)(27). Additional calculation information is provided in Appendix B.

Using the list of TAPs determined from the first step of the TPER analysis, the emissions from the Buck STAR<sup>®</sup> facility, including the proposed modifications (Table 3-4) and the existing equipment, were compared to the TPERs, presented in Table 3-5, to identify the compounds exceeding their respective TPERs. The emissions for the existing turbines and auxiliary boiler were taken from the current permit (03786T34) limits and the Duct Burner Modification Application (February 15, 2013). Additional information is provided in Appendix B.

Once the compounds exceeding the TPERs were identified, an air dispersion modeling analysis was completed for the whole Buck STAR<sup>®</sup> facility including the existing combined cycle turbines and auxiliary boiler.



	Total Emissions				
Compound	lb/hr	lb/day	lb/yr		
Sulfuric acid	1.00E-01	2.4	-		
Benzene	-	-	3.34		
Formaldehyde	7.64E-03	-	-		
n-Hexane	-	2.54	-		
Toluene	1.32E-03	3.17E-02	-		
Arsenic	-	-	11.37		
Beryllium	-	-	2.34		
Cadmium	-	-	2.58		
Chromium VI (Soluble Chromate)	-	4.14E-03			
Manganese	-	6.70E-02	-		
Mercury	-	5.66E-04	-		
Nickel	-	4.06E-02	-		

# Table 3-4. Net Emission Increases – Proposed STAR<sup>®</sup> Project



		Total Emissions	5		TPER			Exceed TPER	
Compound	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr
Sulfuric acid	3.50	84.00		0.025	0.25		YES	YES	
Benzene			444.93			8.1			YES
Formaldehyde	0.91			0.04			YES		
n-Hexane		12.54			23.0			NO	
Toluene	0.26	62.15		14.4	98.0		NO	NO	
Arsenic			20.34			0.053			YES
Beryllium			2.89			0.28			YES
Cadmium			51.89			0.37			YES
Chromium VI (Sol- uble Chromate)		0.012			0.013			NO	
Manganese		0.117			0.630			NO	
Mercury		0.022			0.013			YES	
Nickel		0.302			0.013			YES	

#### Table 3-5. Summary of Potential TAP Emissions from the Buck Combined Cycle Facility and Comparison the TPERs

Note: Chromium VI total emission is less than TPER, but to be conservative it is still modeled because the emissions are very close to the threshold.



#### 4.0 REGULATORY ANALYSIS

Federal and state regulations were reviewed to determine their applicability to and implications for the various emissions sources at the Buck STAR<sup>®</sup> facility. The regulations that may apply only to the proposed emissions sources as a result of modification at the facility are discussed in the following subsections.

USEPA promulgated regulations that set NAAQS for seven criteria compounds: SO<sub>2</sub>, CO, NO<sub>x</sub>, PM<sub>10</sub>, PM<sub>2.5</sub>, Pb, and ozone (O<sub>3</sub>). Two classes of ambient air quality standards have been established: (1) primary standards defining levels of air quality that the USEPA has judged as necessary to protect public health; and (2) secondary standards defining levels for protecting soils, vegetation, wildlife, and other aspects of public welfare. Table 4-1 lists the national primary and secondary and state ambient air quality standards in micrograms per cubic meter ( $\mu$ g/m<sup>3</sup>). The NC DEQ ambient air quality standards are also included in Table 4-1.

According to 40 CFR §81.334, the current attainment status for the project area Rowan County for each of the criteria pollutants is provided in Table 4-2. The proposed facility is located in an area that is in attainment of the national ambient air quality standards (NAAQS).

#### 4.1 PSD (40 CFR 52.21)/ 15A NCAC 02D .0530

The proposed modification (addition of STAR<sup>®</sup> unit) to the operating limits in the Buck Combined Cycle facility air permit does not result in a significant increase of emissions for any PSD pollutant and is therefore not subject to PSD review.



Pollutant	Averaging Period*	NAAQS (µg/m <sup>3</sup> †)		NC DEQ Regulation Standards $(\mu g/m^3 \dagger)$	
		Primary	Secondary	Primary	Secondary
SO <sub>2</sub>	Annual‡	80	—§	80	—§
	24-hour‡	365	—§	365	—§
	1-hour	196	—§	196	<u> </u> §
	3-hour	—§	1,300	—§	1,300
$PM_{10}$	24-hour	150	150	150	150
PM <sub>2.5</sub>	Annual	12	15	12	15
	24-hour	35	35	35	35
СО	8-hour	10,000	—§	10,000	—§
	1-hour	40,000	—§	40,000	—§
Ozone	8-hour	0.070 ppm	0.070 ppm	0.075 ppm	0.075 ppm
NO <sub>2</sub>	Annual	100	100	100	100
	1-hour	188	—§	188	—§
Lead	3-month£	0.15	0.15	0.15	0.15

#### Table 4-1. Ambient Air Quality Standards

Note: ppm = part per million.

ppb = part per billion.  $NO_2 = nitrogen dioxide$ .

\*National short-term ambient standards may be exceeded once per year; annual standards may never be exceeded. North Carolina short-term standards may be exceeded once per year, annual standards may never be exceeded. Ozone standard is attained when the expected number of days of an exceedance is equal to or less than one.

†Standards expressed in micrograms per cubic meter ( $\mu g/m^3$ ) unless otherwise noted.

<sup>‡</sup>Final rule signed June 2, 2010. The 1971 annual and 24-hour SO<sub>2</sub> standards were revoked in this rulemaking. However, these standards remain in effect until one year after an area is designated for the 2010 standard, except in areas designated nonattainment for the 1971 standards, where the 1971 standards remain in effect until implementation plans to attain or maintain the 2010 standard are approved.

§No ambient standard for this pollutant and/or averaging period.

 $\pounds$ The rule signed October 15, 2008, finalized a new lead standard. The 1978 lead standard of 1.5  $\mu$ g/m<sup>3</sup> as a quarterly average remains in effect until one year after an area is designated for the 2008 standard, except in areas designated nonattainment for the 1978 standard, where, the 1978 standard remains in effect until implementation plans to attain or maintain the 2008 standard are approved.

Sources: 40 CFR 50. 15A NCAC 2D .0400.



Pollutant	Attainment Status
СО	Unclassifiable/attainment
$SO_2$	Attainment
$NO_2$	Unclassifiable/attainment
$PM_{10}$	Unclassifiable/attainment
PM <sub>2.5</sub>	Unclassifiable/attainment
Ozone (8-hour)	Attainment
Lead	Unclassifiable/attainment

Table 4-2. Attainment Status for Rowan County, North Carolina

Source: 40 CFR 81.334.



Duke Energy is applying to the NC DEQ for a revision to PSD avoidance conditions in Section 2.1.A.6.a and Section 2.1.A.7.a of Air Permit No. 03786T34 for sulfuric acid mist and VOCs. Specifically, Duke Energy is requesting the removal of VOC and sulfuric acid mist from these conditions, and the creation of a new PSD avoidance condition that addresses VOCs and sulfuric acid mist from the turbines (ES-11 and ES-12), the STAR<sup>®</sup> unit (proposed ES-74) and two proposed diesel engines associated with ash screening/crushing without change to the respective avoidance limits indicated in Section 2.1.A.6.a and Section 2.1.A.7.a of Air Permit No. 03786T34. Detailed explanation is provided in Section 3.4 earlier.

# 4.2 NORTH CAROLINA AMBIENT AIR QUALITY STANDARDS

#### 4.2.1 15A NCAC 2Q .0101 - REQUIRED AIR QUALITY PERMITS

This regulation requires the owner or operator of all sources for which there is an ambient air quality or emission control standard, which is not exempted from permit requirements, to apply for an air quality permit. The owner or operator of a source required to have a permit shall not begin construction or operation of the source without first obtaining a permit. The STAR<sup>®</sup> unit and the material handling equipment's listed in Section 1.3 are not categorically exempt from permitting. Thus, Duke Energy is submitting this air permit application to obtain a permit prior to any construction or change in method of operation of these sources. Duke Energy will submit a separate Title V permit application within 12 months after the initial start-up of the proposed project.

#### 4.2.2 15A NCAC 2D .0400. AMBIENT AIR QUALITY STANDARDS

The purpose of the ambient air quality standards is to establish certain maximum limits on parameters of air quality considered desirable for the preservation and enhancement of the quality of the State's air resources. The ambient air quality standards for North Carolina are the same as those promulgated by the EPA. All standards promulgated by the EPA as of June 22, 1988, have been adopted and incorporated by reference as the official ambient air quality standards of the State of North Carolina. Duke Energy expects that the proposed project will be in compliance with the applicable air quality standards.



#### 4.2.3 15A NCAC 2D .0515 – PARTICULATES FROM MISCELLANEOUS IN-DUSTRIAL PROCESSES

Allowable emissions of particulate matter from any industrial process for which no other emission control standards are applicable shall not exceed the amounts calculated by the following equation:

 $E=4.10 \ x \ P^{0.67}$  for  $P \leq 30$  tons per hour or  $E=55.0 \ x \ P^{0.11} \text{-} 40 \ \text{for } P > 30 \ \text{tons per hour}$ 

where: E = allowable emission rate in pounds per hour

P =process weight in tons per hour

Solid fuels charged are considered as part of the process weight, liquid and gaseous fuels and combustion air are not.

Table 4-3 presents the process weight rates and associated allowable emissions for the equipment onsite. Compliance with this requirement is expected and appropriate monitoring and recordkeeping will be performed to verify this expectation.



Emissions Source	Process Rate (tph)	Allowable PM (lb/hr)	
EHE (Units1 and 2)	70	47.8	
Feed silo filling	125	53.5	
Feed silo unloading	75	48.4	
FGD Byproduct Silo	TBD	TBD	
FGD Absorbent Silo	TBD	TBD	
STAR <sup>®</sup> Reactor	75	48.4	
Storage dome filling	75	48.4	
Storage dome unloading	275	62.02	
Transfer silo filling	125	53.5	
Transfer silo unloading	75	48.4	
Loadout	75	48.4	
Loadout chute 1A	100	51.3	
Loadout chute 1B	100	51.3	
Screener	165	56.4	
Crusher	7	15.1	

Table 4-3. 15A NCAC 2D .0515 Allowable Emissions

Note: lb/hr = pound per hour.

Source: 15A NCAC 2D .0515.



## 4.2.4 15A NCAC 02D .0516 – SULFUR DIOXIDE EMISSIONS FROM COM-BUSTION SOURCES

Emission of sulfur dioxide from any source of combustion that is discharged from any vent, stack, or chimney shall not exceed 2.3 pounds of sulfur dioxide per million BTU input. Sulfur dioxide formed by the combustion of sulfur in fuels, wastes, ores, and other substances shall be included when determining compliance with this standard. Sulfur dioxide formed or reduced as a result of treating flue gases with sulfur trioxide or other materials shall also be accounted for when determining compliance with this standard.

A source subject to an emission standard for sulfur dioxide in Rules 2D .0524, .0527, .1110, .1111, .1205, .1206, .1210, or .1211 of 15A NCAC shall meet the standard in that particular rule instead of the standard in the above paragraph.

The STAR<sup>®</sup> unit is not subject to any sulfur dioxide standards; therefore, it is subject to the requirements in 2D .0516. Compliance with the emission standard of 2.3 lb/million Btu is expected based on the conceptual design of the SO<sub>2</sub> device. Appropriate monitoring and recordkeeping will be performed to verify this expectation.

## 4.2.5 15A NCAC 2D .0521 – CONTROL OF VISIBLE EMISSIONS

The intent of this Rule is to prevent, abate and control emissions generated from fuel burning operations and industrial processes where visible emissions can be reasonably expected to occur, except during startup, shutdowns, and malfunctions approved as such according to procedures approved under 15A NCAC 2D .0535.

This Rule shall apply to all fuel burning sources and to other processes that may have a visible emission. However, sources subject to a visible emission standard in Rules .0506, .0508, .0524, .0543, .0544, .1110, .1111, .1205, .1206, .1210, .1211, or .1212 of this Subchapter shall meet that standard instead of the standard contained in this Rule.



For sources manufactured after July 1, 1971, visible emissions shall not be more than 20 percent opacity when averaged over a six-minute period. However, except for sources required to install, operate, and maintain continuous opacity monitoring systems (COMS), compliance with the 20 percent opacity limit shall be determined as follows:

- i. No six-minute period exceeds 87 percent opacity;
- ii. No more than one six-minute period exceeds 20 percent opacity in any hour; and
- iii. No more than four six-minute periods exceed 20 percent opacity in any 24-hour period.

Duke Energy assumes all proposed sources will be subject to this rule. Compliance will be achieved through the use of the proposed emission control equipment.

## 4.2.6 15A NCAC 02D .0530 PREVENTION OF SIGNIFICANT DETERIORA-TION

The Project will not result in a significant increase in emissions, and therefore the PSD review provisions of this rule do not apply, subject to the specific provisions in 15A NCAC 2D.0544 for GHG sources.

## 4.2.7 15A NCAC 2D .0535 - EXCESS EMISSIONS REPORTING AND MAL-FUNCTIONS

This regulation applies to all permitted facilities and outlines the procedures of reporting excess emissions as a result of malfunctions or operational upsets. The facility owner/operator must notify the appropriate regional office of any excess emissions that last for greater than four hours. This report must be made by 9:00 a.m. Eastern time of the Division's next business day of becoming aware of the occurrence. Notify the Director or his designee immediately when the corrective measures have been accomplished. Submit a written report to the Director within 15 days after the request.



## 4.2.8 15A NCAC 02D .0540 - PARTICULATES FROM FUGITIVE DUST EMIS-SION SOURCES

This rule requires that fugitive dust emissions not cause or contribute to substantive complaints, excessive fugitive dust emissions at the property boundary, or NAAQS violations. Dust emissions from the Ash handling and Loading/Unloading sources are expected to be in compliance. Appropriate monitoring and recordkeeping will be performed to verify this expectation.

## 4.2.9 15A NCAC 02D .0544 - PREVENTION OF SIGNIFICANT DETERIORA-TION REQUIREMENTS FOR GREENHOUSE GASES

This rule indicates that a major stationary source or major modification shall not be required to obtain a PSD permit on the sole basis of its greenhouse gases emissions. All other new source review pollutants are below the PSD major source thresholds. Thus, PSD review for GHGs does not apply.

## 4.2.10 15A NCAC 02D .1100 - CONTROL OF TOXIC AIR POLLUTANTS

This rule applies to all facilities that emit a toxic air pollutant that are required to have a permit under 15A NCAC 2Q .0700. NC DEQ requires any facility that emits a regulated Toxic Air Pollutant (TAP) at a rate greater than the TAP Permitting Emission Rate (TPER), as listed in the 15A NCAC 2Q .0711, demonstrate through air dispersion modeling that emissions from the facility are not resulting in the exceedance of the Acceptable Ambient Level (AAL) for that pollutant, as listed in 15A NCAC 2D .1104. Per 2Q.0700, the Duke Buck Combined Cycle facility has the potential to emit TAPs in excess of de minimis thresholds. Detailed explanation of toxic modeling analyses is presented in Section 5 of this application.

## 4.2.11 15A NCAC 02D .1200 - CONTROL OF EMISSIONS FROM INCINERA-TORS

Fly ash is not a waste material; instead, it is a feedstock (or an ingredient) for the Buck STAR<sup>®</sup> facility. The coal fly ash is a raw material for the proposed Buck STAR<sup>®</sup> facility. It is required to produce beneficiated product as per the standard of the American Society for Testing and Materials (ASTM) Standard C618, and American Association of State



Highway and Transportation Officials (AASHTO) Standard M 295 for pozzolan-grade fly ash.

Based on the determination that fly ash as proposed to be used is not a waste material, the Buck STAR<sup>®</sup> facility is not subject to this requirement. NC DEQ's concurrence with this conclusion is supported by the documentation included in Appendix F.

## 4.2.12 15A NCAC 02D .1400 - NITROGEN OXIDES

This rule applies to facilities with potential emissions of  $NO_x$  equal to or greater than 100 tons per year or 560 pounds per calendar day beginning May 1 through September 30 of any year in the following areas: (1) Cabarrus County; (2) Gaston County; (3) Lincoln County; (4) Mecklenburg County; (5) Rowan County; (6) Union County; and (7) Davidson Township and Coddle Creek Township in Iredell County.

Buck STAR<sup>®</sup> facility is located in Rowan county, but according to Rule .1402 (h), regardless of any statement of applicability, this rule is not applicable to incinerator or thermal or catalytic oxidizer used primarily for the control of air pollution. The STAR<sup>®</sup> process does not meet the definition of a fuel-burning operation. The combustion of natural gas or propane during startup is direct-fired with all of the STAR<sup>®</sup> ingredients, including fly ash. The proposed emission unit is subject to the NO<sub>x</sub> RACT requirements listed in 15A 02D.1413 – Sources Not Otherwise Listed in this Section. Detailed RACT analysis is presented in Appendix G.



## 4.3 FEDERAL REGULATIONS

Federal regulations were reviewed to determine their applicability to the proposed Buck STAR<sup>®</sup> facility. The federal regulations that were found to be potentially applicable only to the proposed STAR<sup>®</sup> are discussed as follows:

## 4.3.1 NEW SOURCE PERFORMANCE STANDARDS (NSPS)

## 4.3.1.1 <u>NSPS for Commercial and Industrial Solid Waste Incineration Units</u> (40 CFR 60, Subpart CCCC)

Unless exempt, combustion of a NHSM as defined in 40 C.F.R. Part 241 would subject an emissions unit to 40 CFR 60 Subpart CCCC-Standards Of Performance For Commercial And Industrial Solid Waste Incineration Units (CISWI). In accordance with 40 CFR 241.3(b)(3), "non-hazardous secondary materials used as an ingredient in a combustion unit that meet the legitimacy criteria..." are not solid wastes. Additionally, in accordance with 40 CFR 241.3(b)(4), "...ingredient products that are used in a combustion unit and are produced from the processing of discarded non-hazardous secondary materials and that meet the legitimacy criteria" are not solid wastes. Based on this it is determined that use of fly ash is not a waste but an ingredient therefore; the Buck STAR<sup>®</sup> unit is not subject to CISWI.

## 4.3.1.2 NSPS for Large Municipal Waste Combustors (40 CFR 60, Subpart Eb)

These standards apply to large municipal waste combustor units with a combustion capacity greater than 250 tons per day of municipal solid waste that initiated construction after September 20, 1994. According to 40 CFR 60.51b, a municipal waste combustor means "any equipment that combusts solid, liquid, or gasified municipal solid waste." Municipal solid waste means household, commercial, retail, or institutional waste and specifically excludes "industrial process or manufacturing wastes." Even if the raw fly ash were considered a solid waste, it does not meet the definition of municipal solid waste. The proposed Buck STAR<sup>®</sup> unit, therefore, is not subject to the NSPS codified under 40 CFR 60, Subpart Eb.



## 4.3.1.3 <u>NSPS Subpart IIII—Standards of Performance for Stationary Compres</u> <u>sion Ignition Internal Combustion Engines</u>

Per 40 CFR 60.4200(a)(2), the provisions of this subpart are applicable to, "Owners and operators of stationary compression ignition internal combustion engines that commence construction after July 11, 2005, where the stationary compression ignition internal combustion engines are:

- (i) Manufactured after April 1, 2006, and are not fire pump engines, or
- (ii) Manufactured as a certified National Fire Protection Association fire pump engine after July 1, 2006."

The diesel-fired engines will commence construction (be ordered) after July 11, 2005, and be manufactured after April 1, 2006; therefore, are subject to 40 CFR 60, Subpart IIII, Standards of Performance for Stationary Compression Ignition Internal Combustion Engines. Per 40 CFR 60.4201(a), Stationary CI internal combustion engine manufacturers must certify their 2007 model year and later non-emergency stationary CI ICE with a maximum engine power less than or equal to 2,237 kilowatt (KW) (3,000 horsepower (HP)) and a displacement of less than 10 liters per cylinder to the certification emission standards for new nonroad CI engines in 40 CFR 89.112, 40 CFR 89.113, 40 CFR 1039.101, 40 CFR 1039.102, 40 CFR 1039.104, 40 CFR 1039.105, 40 CFR 1039.107, and 40 CFR 1039.115, as applicable, for all pollutants, for the same model year and maximum engine power. Proposed diesel engines (ES-39B and ES-40B) have displacement less than 10 liters per cylinder to the certification is rule are applicable. Duke Energy will comply with all applicable Subpart IIII emissions limitation, monitoring, recordkeeping, and reporting requirements.

## 4.3.2 NATIONAL EMISSION STANDARD FOR HAZARDOUS AIR POLLU-TANT (NESHAP)

NESHAP are standards for HAPs from stationary sources. The Buck Combined Cycle facility has potential emissions of an individual HAP below 10 tpy or more and potential emissions of total HAPs below 25 tpy or more. Therefore, the Buck Combined Cycle facility is a minor source of HAP emissions. The applicability of relevant NESHAP is discussed in the following subsections.



## 4.3.2.1 <u>NESHAP for Stationary Reciprocating Internal Combustion Engines (40</u> <u>CFR 63, Subpart ZZZZ)</u>

The engines associated with the screening and crushing are subject to Subpart ZZZZ, because this standard is applicable to area sources of HAPs as well. Since the engines are new and located at an area source, the requirements of 40 CFR 60, Subpart IIII, must be met to meet the requirements of Subpart ZZZZ. The engines will meet applicable NSPS requirements.

### 4.3.2.2 <u>NESHAP for Industrial, Commercial and Institutional Boilers and Process</u> <u>Heaters (40 CFR 63, Subpart DDDDD)</u>

40 CFR 63 Subpart DDDDD, establishes national emission limitations and work practice standards for HAP emitted from industrial, commercial, and institutional boilers and process heaters located at major sources of HAP. The Buck Combined Cycle facility is an area source of HAPs. Therefore, the STAR<sup>®</sup> system is not subject to the NESHAP codified under 40 CFR 63, Subpart DDDDD.

## 4.3.2.3 <u>NESHAP for Industrial, Commercial and Institutional Boilers Area</u> <u>Sources (40 CFR 63, Subpart JJJJJJ)</u>

These standards apply to industrial, commercial, and institutional boilers at an area source of HAP. The Buck Combined Cycle facility is an area source of HAPs. However, no proposed units at the facility meet the definition of a boiler under 40 CFR 63.11237. Therefore, the STAR<sup>®</sup> system is not subject to the NESHAP codified under 40 CFR 63, Subpart JJJJJJ.

## 4.3.3 40 CFR 64 - COMPLIANCE ASSURANCE MONITORING REGULA-TIONS

On October 27, 1997, EPA promulgated the CAM Rule, 40 CFR Part 64, which addresses monitoring for certain emission units at major sources, thereby assuring that facility owners and operators conduct effective monitoring of their air pollution control equipment. In order to be subject to CAM, the following criteria must be met:



- The unit is subject to an emissions limitation or standard for the pollutant of concern;
- An "active" control device is used to achieve compliance with the emission limit; and
- The emission unit's pre-control potential-to-emit is greater than the applicable major source threshold.

For emissions of SO<sub>2</sub> from the STAR® system (ES-74), Duke Energy is subject to CAM requirements for the state SO<sub>2</sub> standard, i.e., 2.3 lb/MMBtu per 15A NCAC 02D .0516. A preliminary draft of a CAM plan is included in Appendix H for the agency's review.



## 5.0 AIR QUALITY IMPACT ASSESSMENT

## 5.1 MODEL SELECTION

For this modeling analysis, the American Meteorological Society (AMS)/EPA Regulatory Model Improvement Committee (AERMIC) model (AERMOD) system components were used. These include the existing regulatory components (AERMOD, AERMOD meteorological preprocessor program [AERMET], AERMOD terrain preprocessor program [AER-MAP], and Building Profile Input Program [BPIP] for Plume Rise Model Enhancement [PRIME] [BPIPPRM]), AERSURFACE and AERMINUTE. AERMOD (Version 16216r) was used in the refined modeling analyses for flat, elevated, and complex terrain.

The procedures used in conducting the air quality modeling analyses followed the requirements outlined in the 40 CFR 51, Appendix W, Guidelines on Air Quality Models; NC DEQ Air Toxic Quality Modeling Guidelines, February 2014; and direction received from the NC DEQ Modeling Section. Supporting information for the air quality modeling study included building downwash analyses, meteorological data, and terrain data.

## 5.1.1 PHYSICAL SOURCE GEOMETRY/GOOD ENGINEERING PRACTICE STACK HEIGHT ANALYSIS

A good engineering practice (GEP) stack height/building wake effect analysis was conducted to identify which building structures influence plume dispersion from each emissions source. Based on the formula, GEP stack height and region of influence, the Building Profile Input Program (BPIP) PRIME program was run for the point source emissions points and related building structures. Figure 5-1 shows the Buck Combined Cycle facility layout (including the modeled sources) and property lines. The BPIP PRIME (Version 04274 dated September 30, 2004) program was used to calculate the GEP height and wind direction-specific building dimensions for input to the air dispersion model.

The GEP analysis was used to identify critical buildings and to determine wind directionspecific building dimensions for use in the modeling analysis. GEP was also used to



demonstrate compliance with applicable state and federal stack height regulations. Following the Guideline for Determination of GEP Stack Height (Technical Document for the Stack Height Regulation), GEP height was calculated using the following equation:

```
Hg = H + 1.5 L
```

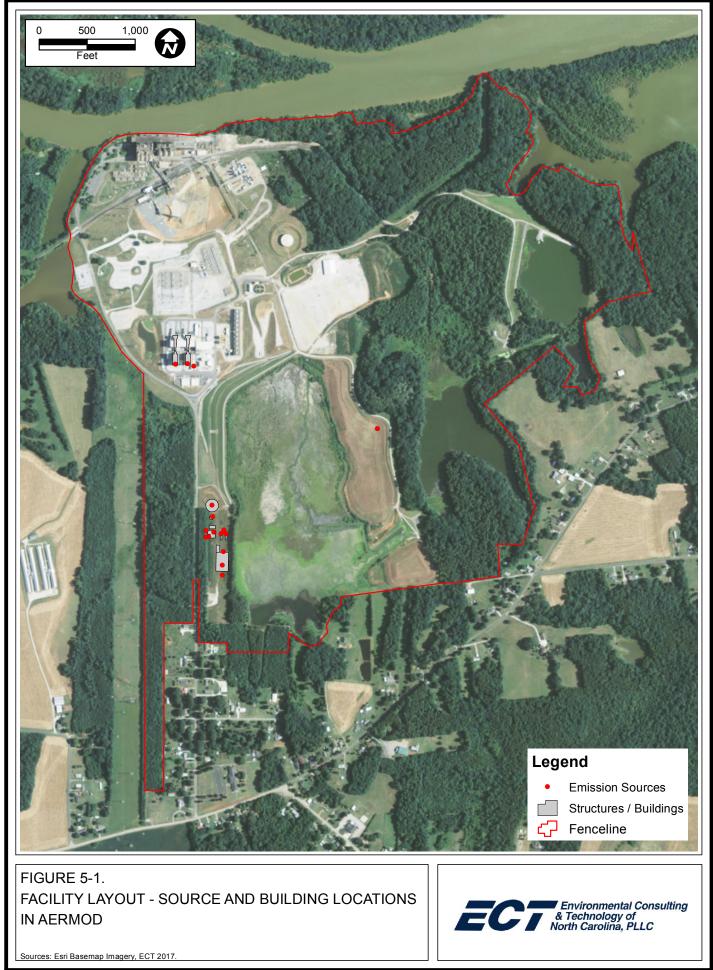
where: Hg = good engineering practice stack height.

- H = height of the structure or nearby structure.
- L = lesser dimension (height or projected width of the structure or nearby building).

In a situation where a nearby structure consists of multiple tiers or there are several structures nearby, the GEP height was calculated for each tier or structure, and the one resulting in the greatest calculated GEP height determined both the GEP height and the wind direction-specific building dimension used when modeling a stack that is lower than the GEP height.

The direction-specific building dimensions obtained from the BPIP PRIME analysis were put into the air dispersion model to simulate the effects of building-induced downwash. The BPIP files are included with the air dispersion modeling files on the DVD included in Appendix E.





## 5.1.2 LOCAL TOPOGRAPHY

Local topography played an important role in the selection of the appropriate dispersion model. Available dispersion models can be divided into two general categories: those applicable to terrain that is below stack top (simple terrain) and above stack top (complex terrain). The terrain near the Buck Combined Cycle facility can be described as generally flat terrain. A model that simulated both simple and complex terrain was used.

## 5.2 AERMOD MODEL APPLICATION

The AERMOD modeling system consists of two preprocessors and the dispersion model. AERMET is the meteorological preprocessor component, and AERMAP is the terrain preprocessor component that characterizes the terrain and generates receptor elevations along with critical hill heights for those receptors.

AERMOD has the following capabilities applicable to this study:

- Handles all terrain features.
- Simulates PRIME aerodynamic building downwash.
- Simulates both short- and long-term averaging periods.
- Handles large numbers of receptors.
- Calculates concentrations within the building cavity and within 5L of the stack.

## 5.2.1 METEOROLOGICAL DATA

For this project, refined modeling analyses were conducted using a data set downloaded from the NC DEQ Website that consisted of 5 years (2011 through 2015) of hourly meteorological data from Charlotte, North Carolina (surface), and Greensboro, North Carolina (upper air). This data set was processed by NC DEQ.

## 5.2.2 RECEPTORS AND TOPOGRAPHY FOR AERMOD

A single nested Cartesian receptor grid was generated for use in the AERMOD refined modeling. Receptors were spaced 100 meters apart along the property boundary, except where a source was within 100 meters, receptors were spaced 25 meters apart. Receptors



were spaced 100 meters apart extending from the property boundary out to 1,000 meters. Receptors were spaced 500 meters apart extending from 1,000 meters out to 10,000 meters. The receptor grid used in the modeling analysis was based on North American Datum of 1983 (NAD 83) and in Zone 17. The AERMAP (Version 11103) processor program was used to calculate terrain elevations and critical hill heights for the receptor grid (NAD 83 and Zone 17) using National Elevation Data (NED). The NED dataset was downloaded from the Multi-Resolution Land Characteristics Consortium (MRLC) website.

The base elevation for the buildings and emissions sources was also obtained from the NED. The base elevation for each building and emission source was then manually adjusted to be the lowest elevation for the buildings and sources in a particular area.

## 5.2.3 PHYSICAL SOURCE AND EMISSIONS DATA

The air dispersion modeling analysis was conducted with emissions rates and exhaust characteristics (flow rate and temperature) that are expected to represent the worst-case parameters for this project.

Tables 5-1 through 5-3 provide summaries of the exhaust data. Tables 5-4 through 5-5 present summaries of emissions rates for the air pollutants addressed in this modeling analysis.



Source ID and Description	Stack Height (ft)	Stack Diameter (ft)	Temperature (°F)	Exit Velocity (fps)
ES-11 – Existing CT 1	160	19	200	52.79
ES-12 – Existing CT 2	160	19	200	52.79
ES-14 – Existing Auxiliary Boiler	40	4	325	60.00
ES-73 – Feed Silo (1500 ton)	111	1.5	70	0.003281
ES-74 – STAR <sup>®</sup> Reactor (Exhaust	140	4	155	43.02
Stack)				
ES-77 – EHE – 1 (Dust Collector)	65	4	187	55.11
ES-78 – EHE – 2 (Dust Collector)	65	4	187	55.11
ES-79 – Transfer Silo (300 Ton)	100	0.667	70	0.003281
ES-80 – Storage Dome (Ash)	125	1.5	70	0.003281
ES-81 – Loadout Silo (1500 Ton)	111	1.5	70	0.003281
ES-81A – Loadout Silo Chute 1A	111	1.5	70	0.003281
ES-81B – Loadout Silo Chute 1B	111	1.5	70	0.003281

Table 5-1. Source Parameters—Point Sources

Note:  ${}^{\circ}F =$  degree Fahrenheit. fps = foot per second. ft = foot.

\*Horizontal exhaust orientation is represented as 0.003281 fps.



Source ID and Description	Release Height (ft)	Initial Horizontal Dimension (ft)	Initial Vertical (ft)
F-1 - wet ash receiving, transfer to storage shed	5	29.76	13.94
F-2 wet ash receiving, transfer to hopper	10	6.98	6.98

#### Table 5-2. Source Parameters—Volume Sources

Note: ft = foot.



Source ID and Description	Release Height (ft)	Easterly Length (ft)	Northerly Length (ft)	Angle from North (degree)
F-3 – Unloading Pile (secondary off-	4	35.00	Default	Default
loading zone)				
F-4 – Ash Basin/Ash Handling	10	660.0	Default	Default

Table 5-3.	Source	Parameters-	-Area Sources
------------	--------	-------------	---------------

Note: ft = foot.



	Averaging	Emissions Rates (lb/hr)											
Pollutant	Period	ES-11	ES-12	ES-14	ES-73	ES-74	ES-77	ES-78	ES-79	ES-80	ES-81	ES-81A	ES-81B
Sulfuric Acid Mist	1-HR	1.70	1.70			0.10							
Sulfuric Acid Mist	24-HR	1.70	1.70			0.10							
Benzene	Annual	2.51E-02	2.51E-02	2.35E-05		1.24E-04							
Formaldehyde	1-HR	4.46E-01	4.46E-01	3.68E-03		4.41E-03							
Arsenic	Annual	5.10E0-4	5.10E0-4	2.24E-06	5.27E-07	5.89E-04	6.35E-04	6.35E-04	5.27E-07	5.27E-07	2.63E-07	1.32E-07	1.32E-07
Beryllium	Annual	3.08E-05	3.08E-05	1.35E-07	1.09E-07	1.20E-04	1.32E-04	1.32E-04	1.09E-07	1.09E-07	5.46E-08	2.74E-08	2.74E-08
Cadmium	Annual	2.81E-03	2.81E-03	1.23E-05	9.41E-08	1.68E-04	1.13E-04	1.13E-04	9.41E-08	9.41E-08	4.70E-08	2.35E-08	2.35E-08
Chromium VI (Soluble Chromate)	24-HR	1.43E-04	1.43E-04	6.27E-07	1.54E-07	7.71E-05	8.48E-05	8.48E-05	1.54E-07	2.70E-07	5.78E-08	7.71E-08	7.71E-08
Mercury	24-HR	4.11E-04	4.11E-04	1.27E-05	7.40E-09	1.90E-05	4.07E-06	4.07E-06	7.40E-09	1.30E-08	2.78E-09	3.70E-09	3.70E-09
Nickel	24-HR	5.38E-03	5.38E-03	1.03E-04	1.40E-06	8.25E-04	7.71E-04	7.71E-04	1.40E-06	2.45E-06	5.26E-07	7.01E-07	7.01E-07

Table 5-4. Modeled Emissions Rates—Point Sources



	Averaging		Emissions Rates (lb/hr)					
Pollutant	Period	F-1	F-2	F-3	F-4			
Sulfuric Acid Mist	1-HR							
Sulfuric Acid Mist	24-HR							
Benzene	Annual							
Formaldehyde	1-HR							
Arsenic	Annual	1.96E-07	3.93E-07	5.81E-07	7.08E-05			
Beryllium	Annual	4.06E-08	8.13E-08	1.20E-07	1.47E-05			
Cadmium	Annual	3.52E-08	7.01E-08	1.04E-07	1.26E-05			
Chromium VI (Soluble Chromate)	24-HR	4.02E-08	8.04E-08	7.76E-08	9.76E-06			
Mercury	24-HR	1.94E-09	3.86E-09	3.73E-09	4.68E-07			
Nickel	24-HR	3.66E-07	7.31E-07	7.06E-07	8.87E-05			

#### Table 5-5. Modeled Emissions Rates—Volume and Area Sources



## 5.3 MODELING RESULTS

This section presents the results of the air quality impact analyses performed for Buck STAR<sup>®</sup> facility. The air quality analyses were conducted using the inputs and methodologies described previously. Methodologies and protocols adhere to the EPA and NC DEQ Guidelines. In accordance with NC DEQ requirements, Appendix E contains a DVD containing the modeling input and output files.

The emissions from the equipment were modeled with AERMOD to estimate the maximum concentrations for the pollutants and corresponding averaging period for each year of meteorological data. Table 5-6 provides a summary of the AERMOD modeling results for each pollutant and averaging period for the Cartesian grid and fenceline receptors discussed in Section 5.2.2.

Based on the results, the Buck STAR<sup>®</sup> facility demonstrates compliance with 15A NCAC 02Q .0700.



Table 5-6. Results for AERMOD Dispersion Modeling-

	Averaging		Modeled Impact (µg/m <sup>3</sup> )			Maximum Impact	Maximum Allowable Concentration	Complies		
Chemical	Period	Rank	2012	2013	2014	2015	2016	(µg/m <sup>3</sup> )	(µg/m <sup>3</sup> )	(Yes/No)
Sulfuric Acid Mist	1-HR	Н	0.66	0.65	0.68	0.92	0.71	0.92	100.00	Yes
Sulfuric Acid Mist	24-HR	Н	0.17	0.18	0.19	0.47	0.20	0.47	12.00	Yes
Benzene	Annual	Н	2.50E-04	1.70E-04	2.20E-04	1.70E-04	2.50E-04	2.50E-04	1.20E-01	Yes
Formaldehyde	1-HR	Н	0.17	0.17	0.18	0.25	0.19	0.25	150.00	Yes
Arsenic	Annual	Н	3.80E-04	3.70E-04	4.00E-04	4.50E-04	3.70E-04	4.50E-04	2.10E-03	Yes
Beryllium	Annual	Н	8.00E-05	8.00E-05	8.00E-05	9.00E-05	8.00E-05	9.00E-05	4.10E-03	Yes
Cadmium	Annual	Н	9.00E-05	8.00E-05	9.00E-05	1.00E-04	9.00E-05	1.00E-04	5.50E-03	Yes
Chromium VI (Soluble Chromate)	24-HR	Н	5.30E-04	4.90E-04	5.60E-04	5.80E-04	5.60E-04	5.80E-04	6.20E-04	Yes
Mercury	24-HR	Н	5.00E-05	5.00E-05	5.00E-05	1.30E-04	5.00E-05	1.30E-04	0.60	Yes
Nickel	24-HR	Н	4.92E-03	4.53E-03	5.17E-03	5.51E-03	5.14E-03	5.51E-03	0.60	Yes

Note:  $\mu g/m^3 =$  microgram per cubic meter. H = highest.

APPENDIX A

AIR PERMIT APPLICATION FORMS



## FORM A

#### **GENERAL FACILITY INFORMATION**

REVISED 09/22/16 NCDEQ/Division of Air Quality - Application NOTE- APPLICATION WILL NOT BE PROCE						
Local Zoning Consistency Determination (new or	_					
Local Zoning Consistency Determination (new or Appropriation only)	e Number of Copies of Application            Image: Application Image: Application Fee (if required)					
Responsible Official/Authorized Contact Signature P.E. Seal	(if required)					
GENERAL INFOR	MATION					
Legal Corporate/Owner Name: Duke Energy Carolinas LLC						
Site Name: Buck Combined Cycle Facility						
Site Address (911 Address) Line 1: 1385 Dukeville Road						
Site Address Line 2:						
City: Salisbury	State: NC					
Zip Code: 28146-8613	County: Rowan					
CONTACT INFOR	MATION					
Responsible Official/Authorized Contact:	Invoice Contact:					
Name/Title: Henry Botkins Jr. / General Manager, Buck Combined Cycle Facility	Name/Title: Cynthia Winston/ Manager, Permitting & Compliance, Carolinas					
Mailing Address Line 1: 1385 Dukeville Road	Mailing Address Line 1: 410 S. Wilmington Street					
Mailing Address Line 2:	Mailing Address Line 2:					
City: Salisbury State: NC Zip Code: 28146	City: Raleigh State: NC Zip Code: 27601					
Primary Phone No.: (704)-630-3019 Fax No.: (704)- 630-3021	Primary Phone No.: (919)-546-5538 Fax No.:					
Secondary Phone No.:	Secondary Phone No.:					
Email Address: <u>henry.botkins@duke-energy.com</u>	Email Address: Cynthia.Winston@duke-energy.com					
Facility/Inspection Contact:	Permit/Technical Contact:					
Name/Title: Dale Wooten/ Environmental Coordinator	Name/Title: Dan Markley/ Lead Environmental Specialist					
Mailing Address Line 1: 1385 Dukeville Road	Mailing Address Line 1: 526 South Church St.					
Mailing Address Line 2:	Mailing Address Line 2:					
City: Salisbury State: NC Zip Code: 28146	City: Charlotte State: NC Zip Code: 28202					
Primary Phone No.: (704)-630-3086 Fax No.: (704)-630-3021	Primary Phone No.: (704)-382-0696 Fax No.: (704)-382-0249					
Secondary Phone No.:	Secondary Phone No.:					
Email Address: <u>dale.wooten@duke-energy.com</u>	Email Address: <u>dan.markley@duke-energy.com</u>					
APPLICATION IS BEIN	G MADE FOR					
New Non-permitted Facility/Greenfield	Renewal Title V     Renewal Non-Title V					
Name Change Ownership Change Administrative Amendment	Renewal with Modification					
FACILITY CLASSIFICATION AFTER AF						
	ibitory Small Synthetic Minor Ititle V					
FACILITY (Plant Site) I						
Describe nature of (plant site) operation(s): Buck Combined Cycle Facility- Generation of electricity for s	are.					
	Facility ID No. 8000004					
Primary SIC/NAICS Code: 4911	Current/Previous Air Permit No. 03786T31 Expiration Date: 1/31/2020					
Facility Coordinates: Latitude: 35º 12' 55"	Longitude: 81º 45' 46"					
Does this application contain confidential data? YES V NO application	blease contact the DAQ Regional Office prior to submitting this on.*** (See Instructions)					
PERSON OR FIRM THAT PRE	PARED APPLICATION					
Person Name: Thomas 0. Pritcher	Firm Name: Environmental Consulting & Technology, Inc.					
Mailing Address Line 1: 7208 Falls of Neuse Road, Suite 102	Mailing Address Line 2:					
City: Raleigh State: NC	Zip Code: 27615 County: Wake					
Phone No.: (919) 861-8888 Fax No.:	Email Address: tpritcher@ectinc.com					
SIGNATURE OF RESPONSIBLE OFFIC						
Name (typed): Henry Botkins Jr.	Title: General Manager, Buck Combined Cycle Facility					
X Signature(Blue Ink):	Date:					

## FORM A (continued, page 2 of 2) GENERAL FACILITY INFORMATION

REVISED 09/2	22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate	Α
	SECTION AA1 - APPLICATION FOR NON-TITLE V PERMIT RENEWAL	
	(Company Name) hereby formally requests renewal of Air Permit No.	
There have be	een no modifications to the originally permitted facility or the operations therein that would require an air permit since the last permit was issued.	-
Is your facility	subject to 40 CFR Part 68 "Prevnetion of Accidental Releases" - Section 112(r) of the Clean Air Act?	
lf yes, have yo	ou already submitted a Risk Manage Plan (RMP) to EPA?	_
-	a current emissions inventory?	
lf no, did you s	submit the inventory via AERO or by mail? U Via AERO Mailed Date Mailed:	-
	SECTION AA2- APPLICATION FOR TITLE V PERMIT RENEWAL	
In accordance	with the provisions of Title 15A 2Q .0513, the responsible official of (Company Name)	
-	y requests renewal of Air Permit No. (Air Permit No.) and further certifies that:	
(1)	The current air quality permit identifies and describes all emissions units at the above subject facility, except where such units are exempted under the	
(2)	North Carolina Title V regulations at 15A NCAC 2Q .0500; The current air quality permit cits all applicable requirements and provides the method or methods for determing compliance with the applicable	
(2)	requirements;	
(3)	The facility is currently in compliance, and shall continue to comply, with all applicable requiremetns. (Note: As provided under 15A NCAC 2Q .0512	
	compliance with the conditions of the permit shall be deemed compliance with the applicable requirements specifically identified in the permit);	
(4)	For applicable requirements that become effective during the term of the renewed permit that the facility shall comply on a timely basis;	
(5)	The facility shall fulfill applicable enhanced monitoring requirements and submit a compliance certification as required by 40 CFR Part 64.	
	le official (signature on page 1) certifies under the penalty of law that all information and statements provided above, based on information and belief	
formed after re	easonable inquiry, are true, accurate, and complete.	
	SECTION AA3- APPLICATION FOR NAME CHANGE	
New Eacility N		
New Facility N		
Former Facility	/ Name:	
An official facili	ity name change is requested as described above for the air permit mentioned on page 1 of this form. Complete the other sections if there have been	
	to the originally premitted facility that would requie an air quality permit since the last permit was issued and if ther has been an ownership change	
associated with	h this name change.	
	SECTION AA4- APPLICATION FOR AN OWNERSHIP CHANGE	
By this applica	tion we hereby request transfer of Air Quality Permit No. from the former owner to the new owner as described below.	
	f permit responsibility, coverage and liability shall be effective (immediately or insert date.) The legal ownership of the	
facility describe	ed on page 1 of this form has been or will be transferred on (date). There have been no modifications to the originally	
permitted facili	ity that would require an air quality permit since the last permit was issued.	
Signature of N	lew (Buyer) Responsible Official/Authorized Contact (as typed on page 1):	
X Signature (B	Blue Ink):	
Date:		
New Facility N	ame:	
Former Facility		
I OITTEL LACING		
Signature of F	ormer (Seller) Responsible Official/Authorized Contact:	
Name (typed o	or print):	
Title:		
X Signature (B	Blue Ink):	
Date:		
Former Legal	Corporate/Owner Name:	
	In lieu of the seller's signature on this form, a letter may be submitted with the seller's signature indicating the ownership change	
	SECTION AA5- APPLICATION FOR ADMINISTRATIVE AMENDMENT	
Describe the re	equested administrative amendment here (attach additional documents as necessary):	

## FORMs A2, A3 EMISSION SOURCE LISTING FOR THIS APPLICATION - A2

112r APPLICABILITY INFORMATION - A3

REVISED 09/22/16	NCDEQ/Division of Air Quality - Appli			A2
	EMISSION SOURCE LISTING: New, Modi	ied, Previously Unpe	ermitted, Replaced, Deleted	
EMISSION SOURCE	EMISSION SOURCE	CONTROL DEVICE	CONTROL DEVICE	
ID NO.	DESCRIPTION	ID NO.	DESCRIPTION	
l	Equipment To Be ADDED By This Application	on (New, Previously	Unpermitted, or Replacement)	
ES-73A	Feed Silo Filling	CD-73	Bin Vent	
ES-73B	Feed Silo Unloading	CD-73	Bin Vent	
ES-74	STAR® Reactor	CD-74A & CD-74B	Scrubber and Baghouse	
ES-75	FGD Byproduct Silo	CD-75	Bin Vent	
ES-76	FGD Absorbent Silo	CD-76	Bin Vent	
ES-77	EHE- External Heat Exchanger 1	CD-77	Baghouse	
ES-78	EHE- External Heat Exchanger 2	CD-78	Baghouse	
ES-79A	Transfer Silo Filling	CD-79	Bin Vent	
ES-79B	Transfer Silo Unloading	CD-79	Bin Vent	
ES-80A	Storage Dome Filling	CD-80	Bin Vent	
ES-80B	Storage Dome Unloading	CD-80	Bin Vent	
ES-81	Loadout Silo	CD-81	Bin Vent	
ES-81A	Loadout Silo Chute 1A	CD-81A	Bin Vent	
ES-81B	Loadout Silo Chute 1B	CD-81B	Bin Vent	
ES-82A	Screener	N/A	N/A	
ES-82B	Screener-Diesel Engine	N/A	N/A	
ES-83A	Crusher	N/A	N/A	
ES-83B	Crusher-Diesel Engine	N/A	N/A	
F-1	Wet Ash Receiving-Transfer to Shed	N/A	N/A	
F-2	Wet Ash Receiving-Transfer to Hopper	N/A	N/A	
-2 F-3	Wet Ash Receiving-Indiate to hopper	N/A	N/A	
F-4	Ash Basin	N/A	N/A	
F-5	Ash Handling	N/A	N/A	
F-5 F-6	Haul Roads	N/A N/A	N/A N/A	
r-0				
1	Existing Permitted Equipment 1		/ This Application	
	Equipment To Be DE	LETED By This App	lication	
		1		
			1	

112(r	) APPLICABIL	LITY INFORMATION		A 3					
Is your facility subject to 40 CFR Part 68 "Prevention of Accidental Releases" - Section 112(r) of the Federal Clean Air Act? 🛛 Yes 🗹									
If No, please specify in detail how your facility avoided applicabilit	ly:	Facility does not use, store or handles any of the reguths rule above their respective threshold quantity.	lated substance	es listed under					
If your facility is Subject to 112(r), please complete the following: A. Have you already submitted a Risk Management Plan (RN	IP) to EPA Pursuant	to 40 CFR Part 68.10 or Part 68.150?							
Yes No Specify required RMP su B. Are you using administrative controls to subject your facilit     Yes No If yes, please specify: C. List the processes subject to 112(r) at your facility:	bmittal date:	If submitted, RMP submittal date:		-					
PROCESS DESCRIPTION	HAZARDOUS CHEMICAL	-	INTENDED DRY (LBS)						

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of A	Air Quality - Applica	ation for Air	Permit to	Construct/	Operate		В
EMISSION SOURCE DESCRIPTION:	Feed Silo Filling			EMISSION	SOURCE I	D NO: ES-7	'3A	
				CONTROL		NO(S): CD	)-73	
OPERATING SCENARIO1	OF	11				. ,	D(S): EP-73	
DESCRIBE IN DETAILTHE EMISSION Ash feed silo filled pneumatically at the		•			t capture de	evice.		
TYPE OF EMISSION SOUR	RCE (CHECK A	ND COMPLETE AP	PROPRIAT	E FORM B	1-B9 ON TH	IE FOLLOV	VING PAGE	S):
Coal,wood,oil, gas, other burner (Fellow)	orm B1)	Woodworking	(Form B4)		🗌 Man	uf. of chemi	cals/coating	ıs/inks (Form E
Int.combustion engine/generator (F	orm B2)	Coating/finishi	<b>.</b> .	,		eration (For	,	
Liquid storage tanks (Form B3)		Storage silos/b	oins (Form B	6)	□ Othe	er (Form B9)		
START CONSTRUCTION DATE: TBD			DATE MAN	NUFACTUR	ED: TBD			
MANUFACTURER / MODEL NO.: TBD			EXPECTER				DAY/WK 5	2 WK/YR
IS THIS SOURCE SUBJECT $\Box$ N	SPS (SUBPAR	ΓS?):			SHAP (SUB	PARTS?):_		
PERCENTAGE ANNUAL THROUGHP	( )		-MAY 25		JN-AUG	25	SEP-NOV	25
CRITERIA A	IR POLLUTA	ANT EMISSION	S INFOR	MATION	FOR TH	S SOUR	CE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONT	ROLS / LIMITS	SEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Manufacturer	6.09E-03	9.74E-03	N/A	N/A	6.09E-03	9.74E-03
PARTICULATE MATTER<10 MICRONS	(PM <sub>10</sub> )	Manufacturer	2.88E-03	4.60E-03	N/A	N/A	2.88E-03	4.60E-03
PARTICULATE MATTER<2.5 MICRONS	(PM <sub>2.5</sub> )	Manufacturer	2.88E-03	4.60E-03	N/A	N/A	2.88E-03	4.60E-03
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (	/OC)		N/A	N/A	N/A	N/A	N/A	N/A
LEAD		Ash Analysis	7.73E-07	1.24E-06	N/A	N/A	7.73E-07	1.24E-06
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS	AIR POLLU	TANT EMISSIC	NS INFO	RMATIO	N FOR T	his sou	RCE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION			BEFORE CONT			ITROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis				N/A	7.21E-07	1.15E-06
Beryllium	7440-41-7	Ash Analysis		2.39E-07	N/A	N/A	1.49E-07	2.39E-07
Cadmium	7440-43-9	Ash Analysis		2.06E-07	N/A	N/A	1.29E-07	2.06E-07
Chromium	7440-47-3	Ash Analysis				N/A		1.40E-06
Chromium VI Cobalt	18540-29-9	Ash Analysis			N/A	N/A	9.64E-08 3.50E-07	1.54E-07
	7440-48-4	Ash Analysis		5.61E-07	N/A	N/A	3.50E-07 1.55E-06	5.61E-07
Manganese Mercury	7439-96-5	Ash Analysis Ash Analysis				N/A N/A	1.55E-06 4.63E-09	2.47E-06 7.40E-09
Nickel	7439-97-6	Ash Analysis Ash Analysis		1.40E-09		N/A N/A	4.63E-09 8.76E-07	1.40E-08
Selenium	7782-49-2	Ash Analysis		3.79E-07	N/A	N/A	2.37E-07	3.79E-07
		IT EMISSIONS						5.79⊑-07
		SOURCE OF	1					
TOXIC AIR POLLUTANT	CAS NO.	EMISSION FACTOR	lb/	/hr	lb/	day	-	lb/yr
Arsenic	7440-38-2	Ash Analysis				E-05		31E-03
Beryllium	7440-41-7	Ash Analysis				E-06		78E-04
Cadmium	7440-43-9	Ash Analysis				E-06		2E-04
Chromium VI	18540-29-9	Ash Analysis				E-06		)8E-04
Manganese	7439-96-5	Ash Analysis				E-05		95E-03
Mercury	7439-97-6	Ash Analysis				E-07		18E-05
Nickel	7440-02-0	Ash Analysis				E-05		30E-03
Attachments: (1) emissions calculations and	currenting docum	ontation: (2) indicate a	ll requested s	tate and fed	aral enforceal	ole nermit lim	ite (e.a. bour	of operation

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

 MPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

 Attach Additional Sheets As Necessary

## EMISSION SOURCE (STORAGE SILO/BINS)

REVISED 09/22/16	NCDEQ/Divis	sion of Air Quality - Ap	plication	n for Air Permit to	o Construct/Operate	<b>;</b>	B6
EMISSION SOURCE DESCRIPT	TION: Feed Silo Filling	I		EMISSIO	N SOURCE ID NO: E	ES-73A	
				CONTRO	L DEVICE ID NO(S)	: CD-73	
OPERATING SCENARIO:	1	OF1		EMISSIO	N POINT(STACK) ID	NO(S): EP-73	
DESCRIBE IN DETAIL THE PRC Ash feed silo filled pneumatically			with bin v	vent product captu	re device.		
MATERIAL STORED: Fly Ash				DENSITY OF MA	TERIAL (LB/FT3): 6	0 bulk, 90 structural	
	CUBIC FEET: 76,000	)		TONS:			
DIMENSIONS (FEET)	HEIGHT: 97	DIAMETER: 41	(OR)	LENGTH:	WIDTH:	HEIGHT:	
ANNUAL PRODUCT THRO	UGHPUT (TONS)	ACTUAL: 400,000		MAXIMUN	I DESIGN CAPACIT	'Y: 400,000	
PNEUMATICALLY FIL	LLED	MECHANIC	ALLY FI	LLED		FILLED FROM	
BLOWER		SCREW CONVEYOR				CAR	
		BELT CONVEYOR				ж	
OTHER:		BUCKET ELEVATOR				RAGE PILE	
		OTHER:				:R:	
NO. FILL TUBES: 3							
MAXIMUM ACFM: 6600							
MATERIAL IS UNLOADED TO: N/A							
BY WHAT METHOD IS MATERI N/A	AL UNLOADED FROI	M SILO?					
MAXIMUM DESIGN FILLING RA	TE OF MATERIAL (T	ONS/HR): 125					
MAXIMUM DESIGN UNLOADIN	G RATE OF MATERIA	AL (TONS/HR): N/A					
COMMENTS: This form is for Feed Silo Filling.	Unloading data is pro	vided in Form B6 for ES	S-73B.				

## SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCI	DEQ/Division of /	Air Quality - Applica	tion for Air	Permit to (	Construct/C	Operate		В	
EMISSION SOURCE DESCRIPTION:	EMISSION SOURCE ID NO: ES-73B								
				CONTROL DEVICE ID NO(S): CD-73					
OPERATING SCENARIO	1 OF _	1		EMISSION	POINT (ST	ACK) ID NO	D(S): EP-73		
DESCRIBE IN DETAILTHE EMISSIO	N SOURCE PRO	CESS (ATTACH FLO	OW DIAGR	AM):					
Ash feed silo unloaded at the rate of 7	′5 ton/hr and equi	pped with bin vent pr	oduct captu	ire device.					
TYPE OF EMISSION SO	URCE (CHECK A	ND COMPLETE API	PROPRIATI	E FORM B1	-B9 ON TH	E FOLLOW	/ING PAGE	S):	
Coal,wood,oil, gas, other burner (		Woodworking (F	<sup>-</sup> orm B4)					gs/inks (Form B	
□ Int.combustion engine/generator	,	Coating/finishing	01 01	,		eration (For	,		
Liquid storage tanks (Form B3)		Storage silos/bir	•	,		er (Form B9)	)		
START CONSTRUCTION DATE: TBI	)			NUFACTUR					
MANUFACTURER / MODEL NO.: TB			EXPECTED		EDULE: 24		DAY/WK 5	2 WK/YR	
	NSPS (SUBPAR	,			SHAP (SUBI	7 =			
PERCENTAGE ANNUAL THROUGH					N-AUG	25	SEP-NOV	25	
CRITERIA	AIR POLLUT	ANT EMISSIONS			FOR THI				
		SOURCE OF	EXPECTE				L EMISSIO		
				ROLS / LIMITS)	BEFORE CONT	ROLS / LIMITS		ITROLS / LIMITS)	
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	
PARTICULATE MATTER (PM)		Manufacturer	3.65E-03		N/A	N/A	3.65E-03	9.74E-03	
PARTICULATE MATTER<10 MICRON	( 10/	Manufacturer	1.73E-03		N/A	N/A	1.73E-03	4.60E-03	
PARTICULATE MATTER<2.5 MICRON	IS (PM <sub>2.5</sub> )	Manufacturer	1.73E-03		N/A	N/A	1.73E-03	4.60E-03	
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A	
			N/A	N/A	N/A	N/A	N/A	N/A	
			N/A	N/A	N/A	N/A	N/A	N/A	
VOLATILE ORGANIC COMPOUNDS	(VOC)	Anti-Analysia	N/A	N/A	N/A	N/A	N/A	N/A	
LEAD		Ash Analysis	4.64E-07	1.24E-06	N/A	N/A	4.64E-07	1.24E-06	
		TANT EMISSIO	N/A	Ν/Α	N/A	N/A	N/A	N/A	
					r				
		SOURCE OF EMISSION							
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	Ib/hr	tons/yr	BEFORE CONT	tons/yr	Ib/hr	tons/yr	
Arsenic	7440-38-2	Ash Analysis		1.15E-06	N/A	N/A	4.33E-07	1.15E-06	
Beryllium	7440-38-2	Ash Analysis			N/A	N/A	4.33E-07 8.97E-08	2.39E-07	
Cadmium	7440-41-7	Ash Analysis		2.39E-07 2.06E-07	N/A	N/A	7.73E-08	2.39E-07 2.06E-07	
Chromium	7440-43-9	,	5.26E-07	1.40E-06		N/A	5.26E-07	1.40E-06	
Chromium VI	18540-29-9	Ash Analysis	5.78E-08	1.54E-07	N/A	N/A	5.78E-08	1.54E-07	
Cobalt	7440-48-4	Ash Analysis	2.10E-07	5.61E-07	N/A	N/A	2.10E-07	5.61E-07	
Manganese	7439-96-5	Ash Analysis	9.28E-07	2.47E-06		N/A	9.28E-07	2.47E-06	
Mercury	7439-97-6	Ash Analysis	2.78E-09	7.40E-09		N/A	2.78E-09	7.40E-09	
Nickel	7440-02-0	Ash Analysis		1.40E-06		N/A	5.26E-07	1.40E-06	
Selenium	7782-49-2	Ash Analysis		3.79E-07	N/A	N/A	1.42E-07	3.79E-07	
		NT EMISSIONS I						-	
		SOURCE OF						LIMITATION	
TOXIC AIR POLLUTANT	CAS NO.	EMISSION FACTOR	lb/	/hr	lb/c	day	[	lb/yr	
Arsenic	7440-38-2	Ash Analysis	4.33E-07			E-05		31E-03	
Beryllium	7440-41-7	Ash Analysis	8.97E-08		2.15	E-06	4.7	78E-04	
Cadmium	7440-43-9	Ash Analysis				2E-04			
	19540.20.0	Ash Analysis			1.39	E-06	3.0	)8E-04	
Chromium VI	18540-29-9					-			
Chromium VI Manganese	7439-96-5	Ash Analysis	9.28E-07		2.23	E-05	4.9	95E-03	
						E-05 E-08		95E-03 18E-05	
Manganese	7439-96-5	Ash Analysis	2.78E-09		6.66		1.4		

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

 WPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOUL

 Attach Additional Sheets As Necessary

## EMISSION SOURCE (STORAGE SILO/BINS)

REVISED 09/22/16	NCDEQ/Divis	sion of Air Quality - Ap	pplicatior	n for Air Pern	mit to Cons	truct/O	perate		B6
EMISSION SOURCE DESCRIPT	FION: Feed Silo Unloa	ading		EMIS	SSION SOU	RCE ID	0 NO: ES-73B		
				CON	ITROL DEVI	ICE ID	NO(S): CD-73		
OPERATING SCENARIO:	1	OF1		EMIS	SSION POIN	NT(STA	CK) ID NO(S): EP-73		
DESCRIBE IN DETAIL THE PRC Ash feed silo unloaded at the rate			duct capti	ure device.					
MATERIAL STORED: Fly Ash				DENSITY OF	F MATERIA	L (LB/F	T3): 60 bulk, 90 structu	Iral	
	CUBIC FEET: 76,000	)		TONS:			,,,,		
	HEIGHT: 97	DIAMETER: 41	(OR)	LENGTH:	V	NIDTH:	: HEIGHT:		
ANNUAL PRODUCT THRO	UGHPUT (TONS)	ACTUAL: 400,000		MAX	IMUM DESI	IGN CA	PACITY: 400,000		
PNEUMATICALLY FIL	LED	MECHANIC	CALLY FI	LLED			FILLED FR	ОМ	
BLOWER		SCREW CONVEYOR	۲				RAILCAR		
		BELT CONVEYOR					TRUCK		
OTHER:		BUCKET ELEVATOR	ł				STORAGE PILE		
		OTHER:					OTHER:		
NO. FILL TUBES: N/A									
MAXIMUM ACFM: 6600									
MATERIAL IS UNLOADED TO:									
STAR® Reactor									
BY WHAT METHOD IS MATERI N/A									
MAXIMUM DESIGN FILLING RA	TE OF MATERIAL (T	ONS/HR): N/A							
MAXIMUM DESIGN UNLOADING	G RATE OF MATERIA	AL (TONS/HR): 75							
COMMENTS: This form is for Feed Silo Unload	ling. Filling data is pro	vided in Form B6 for ES	3-73A.						

#### FORM C1 CONTROL DEVICE (FABRIC FILTER)

REVISED 09/22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate										
CONTROL DEVICE ID NO: CD-73	CONTROLS EMISSI	NTROLS EMISSIONS FROM WHICH EMISSION SOURCE ID NO(S): ES-73A & ES-73B								
EMISSION POINT (STACK) ID NO(S): EP-73	POSITION IN SERIE	SITION IN SERIES OF CONTROLS NO. 1 OF 1 UNIT								
OPERATING SCENARIO:										
1OF1		P.E. SEAL REQUIR	ED (PE	ER 2q .0112)?		V	YES		NO	
DESCRIBE CONTROL SYSTEM: A bin vent for particulate c	ontrol on the feed silo.									
POLLUTANTS COLLECTED:		PM (Filling)		PM10/PM2.5 (Filling)		PM (Unloading)		PM10/PM2.5 (Unloading)		
BEFORE CONTROL EMISSION RATE (LB/HR):		0.0061		0.00287		0.00365		0.00173		
CAPTURE EFFICIENCY:		<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	
CONTROL DEVICE EFFICIENCY:		N/A	%	N/A	%	N/A	%	N/A	%	
CORRESPONDING OVERALL EFFICIENCY:		N/A	%	N/A	%	N/A	%	N/A	%	
		2		2		2		2		
TOTAL AFTER CONTROL EMISSION RATE (LB/HR):		0.0061		0.00287		0.00365		0.00173		
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: Avg: 10-15 wg	GAUGE?	2 YES		] NO						
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25		INLET TEMPERATU	JRE (°F	F): Contract	MIN		MAX			
POLLUTANT LOADING RATE: N/A 🛛 LB/HR 🛛	] GR/FT <sup>3</sup>	OUTLET TEMPERA	TURE	(°F) Contract	MIN		MAX			
INLET AIR FLOW RATE (ACFM): 1300		FILTER OPERATIN	G TEM	P (°F): Contract						
NO. OF COMPARTMENTS: 1 NO. OF BAGS F	PER COMPARTMENT:	Contract			LENG	TH OF BAG (IN.): 2	20-30			
NO. OF CARTRIDGES: FILTER SURFA	CE AREA PER CARTI	RIDGE (FT <sup>2</sup> ):			DIAME	TER OF BAG (IN.)	: 5-15			
TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ):	AIR TO CLOTH RAT	IO: 1 to 4 : 1								
DRAFT TYPE: INDUCED/NEGATIVE	FORCED/POSITIVE			FILTER MATERIAL: Ca	artridge	Style	WOVE	N 🗆	FELTED	
DESCRIBE CLEANING PROCEDURES:						F	PARTIC	LE SIZE DISTRIBUTION		
☑ AIR PULSE	SONIC					SIZE		WEIGHT %	CUMULATIVE	
REVERSE FLOW	SIMPLE BAG COLLA	APSE				(MICRONS)		OF TOTAL	%	
	RING BAG COLLAPS			-		0-1				
OTHER:	KING BAG COLLAF	JE .				1-10				
DESCRIBE INCOMING AIR STREAM: Air stream will contain	fly ash									
	ny dom			-		10-25				
				-		25-50				
				-		50-100				
				-		>100				
				-	Suppli	er specific, 94% pa	eeina 2	TOTAL = 100		
					ouppin	n apconto, 0470 pa	Song o			
ON A SEPARATE PAGE, ATTACH A DIAGRAM SHOWING			EVICE	TO ITS EMISSION SO	URCE	S):				
COMMENTS:						0).				

Attach Additional Sheets As Necessary

		FO	RM B					
SPECIFIC EMISSION	SOURC		IATION	(REQUI	RED FO	OR ALL	SOUR	CES)
REVISED 09/22/1 NCDEQ/I	Division of Air	Quality - Appl	ication for	Air Permit t	o Construc	:t/Operate		В
EMISSION SOURCE DESCRIPTION: S	TAR® Reactor	r		EMISSION	SOURCE I	D NO: ES-7	4	
				CONTROL	DEVICE ID	NO(S): CD	-74	
OPERATING SCENARIO1_	OF	1		EMISSION	POINT (ST	ACK) ID NO	D(S): EP-74	
DESCRIBE IN DETAILTHE EMISSION The STAR® Reactor will process feedst variety of commercial products.	ock (of any car	bon content) like	e flyash (we	t or dry) alor		-		
TYPE OF EMISSION SOURCE Coal,wood,oil, gas, other burner (Fo Int.combustion engine/generator (Fi Liquid storage tanks (Form B3) START CONSTRUCTION DATE: TBD	orm B1)	<ul><li>Woodworl</li><li>Coating/fir</li></ul>	king (Form E hishing/printi ilos/bins (Fo	34) ing (Form B	☐ Mar ☐ Inci ☑ Oth		nicals/coating form B8)	<b>3ES):</b> gs/inks (Form
MANUFACTURER / MODEL NO.: TBD				D OP. SCHE		וד עאח/פר		
_	SPS (SUBPAR	TS?)			HAP (SUBI		CALLAR D	- 7117 117
	,	/	MAR-MAY	25 NES	JUN-AUG	, –	SEP-	NOV 25
CRITERIA AIR								NUV 25
CRITERIA AIR	PULLUTA	1			V FOR II			
		SOURCE OF					L EMISSIO	
		EMISSION		ROLS / LIMITS)				TROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		-	4.87	21.34	N/A	N/A	4.87	21.34
PARTICULATE MATTER<10 MICRONS (	10/	Sum of	4.48	19.63	N/A	N/A	4.48	19.63
PARTICULATE MATTER<2.5 MICRONS	PM <sub>2.5</sub> )	(NG+Propane	2.58	11.31	N/A	N/A	2.58	11.31
SULFUR DIOXIDE (SO2)		) AP-42+Fly	40.23	163.63	804.63	3272.57	40.23	163.63
NITROGEN OXIDES (NOx) 0.12 lb/MM	/IBtu	Ash (Manufacturer	18.22	112.29	N/A	N/A	18.22	112.29
CARBON MONOXIDE (CO)		(Manulacturer )	22.40	91.10	N/A	N/A	22.40	91.10
VOLATILE ORGANIC COMPOUNDS (V	OC)	,	2.24	9.11	N/A	N/A	2.24	9.11
LEAD			6.48E-04	2.84E-03	N/A	N/A	6.48E-04	2.84E-03
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS A	R POLLUT	ANT EMISS	IONS INF	ORMATI	ON FOR	THIS SO	URCE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	(AFTER CONT	ROLS / LIMITS)	EFORE CONT	ROLS / LIMITS	(AFTER CON	TROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Benzene	71-43-2		1.24E-04		N/A	N/A	1.24E-04	5.41E-04
Formaldehyde	50-00-0	1	4.41E-03		N/A	N/A		1.93E-02
Hexane	110-54-3	1	1.06E-01	4.64E-01	N/A	N/A	1.06E-01	4.64E-01
Naphthalene	91-20-3	1	3.59E-05		N/A	N/A		1.57E-04
Toluene	108-88-3	1	2.00E-04	8.76E-04	N/A	N/A	2.00E-04	8.76E-04
Arsenic	7440-38-2		5.89E-04	2.58E-03	N/A	N/A	5.89E-04	2.58E-03
Beryllium	7440-41-7	Sum of (NG) AP-42+Fly	1.20E-04	5.27E-04	N/A	N/A	1.20E-04	5.27E-04
Cadmium	7440-43-9	Ash	1.68E-04	7.35E-04	N/A	N/A	1.68E-04	7.35E-04
Chromium	7440-47-3	(Manufacturer	7.84E-04	3.43E-03	N/A	N/A	7.84E-04	3.43E-03
Chromium VI	18540-29-9	)	7.71E-05	3.38E-04	N/A	N/A	7.71E-05	3.38E-04
Cobalt	7440-48-4		2.85E-04	1.25E-03	N/A	N/A	2.85E-04	1.25E-03
Manganese	7439-96-5		1.26E-03	5.52E-03	N/A	N/A	1.26E-03	5.52E-03
Mercury	7439-97-6		1.90E-05	8.32E-05	N/A	N/A	1.90E-05	8.32E-05
Nickel	7440-02-0		8.25E-04	3.61E-03	N/A	N/A	8.25E-04	3.61E-03
Selenium	7782-49-2		1.91E-04	8.37E-04	N/A	N/A	1.91E-04	8.37E-04
TOXIC AIR P		T EMISSION						2.0.2.01
		SOURCE OF EMISSION						LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb	/hr	lb/	day		b/yr
Sulfuric Acid Mist		Stack Test	0.1			E+00		876
Benzene	71-43-2		1.24E-04			E-03		8E+00
Formaldehyde	50-00-0		4.41E-03			E-00		6E+01
Hexane	110-54-3		1.06E-01			E+00		8E+02
					2.07			

operation, emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source. PLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOL

2.00E-04

5.89E-04

1.20E-04

1.68E-04

7.71E-05

1.26E-03

1.90E-05

8.25E-04

108-88-3

7440-38-2

7440-41-7

7440-43-9

18540-29-9

7439-96-5

7439-97-6

7440-02-0

Attachments: (1) emissions calculations and supporting documentation: (2) indicate all requested state and fe

Sum of (NG)

AP-42+Fly

Ash

(Manufacturer

)

Toluene

Arsenic

Beryllium

Cadmium

Chromium VI

Manganese

Mercury Nickel 4.80E-03

1.41E-02

2.89E-03

4.03E-03

1.85E-03

3.02E-02

4.56E-04

1.98E-02

eral enforceable permit limits (e.g. hours of

1.75E+00

5.16E+00

1.05E+00

1.47E+00

6.76E-01

1.10E+01

1.66E-01

7.23E+00

Attach Additional Sheets As Necessary

# FORM B9 EMISSION SOURCE (OTHER)

REVISED 09/22/16 NCDEQ/Division of Air Quality - Ap	plication for A	Air Permit to Construct/Operate		B9
EMISSION SOURCE DESCRIPTION: STAR® Reactor		EMISSION SOURCE ID NO: ES-7	74	
		CONTROL DEVICE ID NO(S): CE	)-74	
OPERATING SCENARIO:1 OF1		EMISSION POINT (STACK) ID NO	O(S): EP-74	
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): The STAR ingredient materials into a variety of commercial products. The fly ash is not a fuel to maintain temperature in the reactor should the fly ash not contain enough carbor British thermal units per hour and are low-NOx burners.	and does not u	ndergo combustion. The natural gas	/propane burners are	only used for startup or
MATERIALS ENTERING PROCESS - CONTINUOUS PROCESS		MAX. DESIGN	REQUEST	ED CAPACITY
ТҮРЕ	UNITS	CAPACITY (UNIT/HR)		N(UNIT/HR)
Reactor- Feed Ash	MMBtu	140	-	140
MATERIALS ENTERING PROCESS - BATCH OPERATION		MAX. DESIGN	REQUEST	ED CAPACITY
ТҮРЕ	UNITS	CAPACITY (UNIT/BATCH)	LIMITATION	(UNIT/BATCH)
MAXIMUM DESIGN (BATCHES / HOUR):				
REQUESTED LIMITATION (BATCHES / HOUR):	(BATCHES/Y	/R):		
FUEL USED: Natural Gas/Propane	TOTAL MAX	IMUM FIRING RATE (MILLION BTU	J/HR): 140	
MAX. CAPACITY HOURLY FUEL USE: NG-58,824 scf/hr & Propane- 663 gal/hr	REQUESTE	D CAPACITY ANNUAL FUEL USE:	NG-58,824 scf/hr & Pr	opane- 663 gal/hr
COMMENTS:				

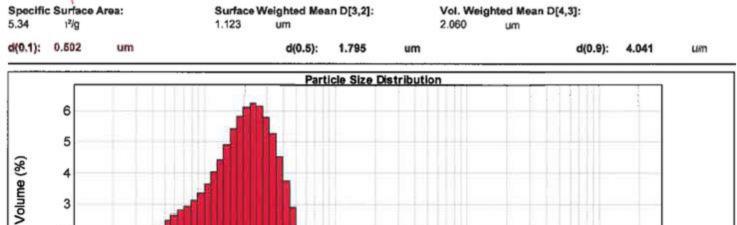
# FORM C9 CONTROL DEVICE (OTHER)

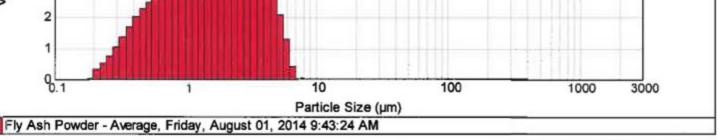
REVISED 09/22/16	NCDEQ/Divisi	on of Air Qualit	ty - Application	on for Air Permit to	Construct/Oper	ate	C9			
CONTROL DEVICE ID NO: CD-74A		CON	ITROLS EMIS	ROLS EMISSIONS FROM WHICH EMISSION SOURCE ID NO(S): ES-74						
EMISSION POINT (STACK) ID NO(S	): EP-74	POS	POSITION IN SERIES OF CONTROLS: NO. 1 OF 2 UNITS							
OPERAT	ING SCENARIO:									
1	OF1		P.E	. SEAL REQUIRED	(PER 2Q .0112)	? 🗸 YES	□ NO			
DESCRIBE CONTROL SYSTEM: Dr	y scrubber for $SO_2$	removal.								
POLLUTANT(S) COLLECTED:			SO <sub>2</sub>							
BEFORE CONTROL EMISSION RAT	F (I B/HR).		804.63							
CAPTURE EFFICIENCY:	_ (/).		N/A %		%	%	%			
CONTROL DEVICE EFFICIENCY:			95 %		%	%	<u> </u>			
CORRESPONDING OVERALL EFFI	CIENCY:		N/A %		%	%	<u> </u>			
EFFICIENCY DETERMINATION COI			2							
TOTAL AFTER CONTROL EMISSIO			40.23							
PRESSURE DROP (IN. H <sub>2</sub> 0):	10MIN	15 MAX	BU	LK PARTICLE DEN	SITY (LB/FT <sup>3</sup> ) Us	e gypsum as surrogat	e.			
INLET TEMPERATURE (°F):		MAX		ITLET TEMPERATU		150 MIN	225 MAX			
INLET AIR FLOW RATE (ACFM): 63			OU	ITLET AIR FLOW R	ATE (ACFM): 58,					
INLET AIR FLOW VELOCITY (FT/SE	:C):		OU	ITLET AIR FLOW VI	ELOCITY (FT/SE	C):				
INLET MOISTURE CONTENT (%): 1	6		[	FORCED AIR		AIR				
COLLECTION SURFACE AREA (FT	²): N/A		FU	EL USED: N/A		FUEL USAGE R	ATE: N/A			
DESCRIBE ANY AUXILIARY MATER	IALS INTRODUCE	D INTO THE CO	DNTROL SYS	TEM: None						
DESCRIBE ANY MONITORING DEV										
ATTACH A DIAGRAM OF THE RELA	TIONSHIP OF TH	E CONTROL DE	EVICE TO ITS	EMISSION SOURC	CE(S):					
COMMENTS:										
Attach manu	ufacturer's specifie	cations, schem	atics, and all	other drawings ne	cessary to desc	ribe this control.				

#### FORM C1 CONTROL DEVICE (FABRIC FILTER)

REVISED 09/22/16	NCDEQ/Division of Ai	ir Quality - Application for Ai	ir Permit to Construct/	Operate		C1
CONTROL DEVICE ID NO: CD-74B	CONTROLS EMISSI	IONS FROM WHICH EMISSIO	ON SOURCE ID NO(S):	ES-74		_
EMISSION POINT (STACK) ID NO(S): EP-74	POSITION IN SERIE	S OF CONTROLS		NO.	2 OF 2	UNITS
OPERATING SCENARIO:						
1 OF1		P.E. SEAL REQUIRED (PEF	R 2q .0112)?	<b>v</b>	YES	□ NO
DESCRIBE CONTROL SYSTEM: A baghouse for particula	te control on the STAR	reactor.				
POLLUTANTS COLLECTED:		PM	PM10	PM2.5		
BEFORE CONTROL EMISSION RATE (LB/HR):		4.87	4.48	2.58		
CAPTURE EFFICIENCY:		100 %	100 9	% 100	%	%
CONTROL DEVICE EFFICIENCY:		> 99.9 %	> 99.9	% > 99.9	%	%
CORRESPONDING OVERALL EFFICIENCY:		> 99.9 %	> 99.9	% > 99.9	%	%
EFFICIENCY DETERMINATION CODE:		2	2	2		
TOTAL AFTER CONTROL EMISSION RATE (LB/HR):		4.87	4.48	2.58		
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: Avg: 4-12 wc	GAUGE?	YES	NO			
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25	- 00/573 407	INLET TEMPERATURE (°F)			MAX 350	
POLLUTANT LOADING RATE: LB/HR	☑ GR/FT <sup>3</sup> 437	OUTLET TEMPERATURE (°		MIN 165	MAX 350	
INLET AIR FLOW RATE (ACFM): 58,218		FILTER OPERATING TEMP				
	PER COMPARTMENT	-		ENGTH OF BAG (		
	ACE AREA PER CART			DIAMETER OF BAC	3 (IN.): 6	
TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ): 26,790	AIR TO CLOTH RAT					
	FORCED/POSITIVE	F	FILTER MATERIAL:			FELTED
DESCRIBE CLEANING PROCEDURES:				1	TICLE SIZE DISTRIB	
☑ AIR PULSE	SONIC			SIZE	WEIGHT %	CUMULATIVE
REVERSE FLOW	SIMPLE BAG COLL		=	(MICRONS)	OF TOTAL	%
	RING BAG COLLAP	SE	_	0-1		
OTHER: DESCRIBE INCOMING AIR STREAM: The fly ash entraine	d in the flue are process	through header of particul	lata control	1-10		
DESCRIBE INCOMING AIR STREAM. THE IIY ash entraine	a in the lide gas passes	through baghouse for particul		10-25		
			-	25-50		
			-	50-100		
			-	>100		
				See attached jpeg.	TOTAL	. = 100
				see allached jpeg.		
ON A SEPARATE PAGE, ATTACH A DIAGRAM SHOWING	G THE RELATIONSHIP	OF THE CONTROL DEVICE	TO ITS EMISSION SOL	JRCE(S):		
COMMENTS:						

Attach Additional Sheets As Necessary





Size (µm)	Vol Under %	Size (µm)	Vol Under %	Size (um)	Vol Under %	Size (um)	Vol Under %	Size (µm)	Vol Under %	Size (µm)	Vol Under %
0.020		0.142	0.00	1.002	27.29	7.098	99.98	50.238	100.00	355.656	100.00
0.022	0.00	0.159	0.00	1.125	30.92	7.952	100.00	56.368	100.00	399.052	100.00
0.025	0.00	0.178	0.00	1.262	34.91	8.934	100.00	63.246	100.00	447.744	100.00
0.028	0.00	0.200	0.02	1.416	39.35	10.000	100.00	70.963	100.00	502.377	100.00
0.032	0.00	0.224	0.33	1.589	44.27	11.247	100.00	79.621	100.00	583.677	100.00
0.036	0.00	0.252	0.85	1.783	49.67	12.619	100.00	89.337	100.00	632.456	100.00
0.040	0.00	0.283	1.60	2.000	55.49	14.159	100.00	100.237	100.00	709.627	100.00
0.045	0.00	0.317	2.63	2.244	61.62	15.887	100.00	112.468	100.00	796.214	100.00
0.050	0.00	0.356	3.98	2.518	67.86	17.825	100.00	128.191	100.00	893.357	100.00
0.050	0.00	0.399	5.69	2.825	73.99	20.000	100.00	141.589	100.00	1002.374	100.00
0.063	0.00	0.448	7.72	3.170	79.78	22.440	100.00	158.866	100.00	1124.683	100.00
0.071	0.00	0.502	10.02	3.557	85.03	25.179	100.00	178.250	100.00	1261.915	100.00
0.080	0.00	0.564	12.51	3.991	89.55	28.251	100.00	200,000	100.00	1415.892	100.00
0.089	0.00	0.632	15.16	4.477	93.27	31.698	100.00	224.404	100.00	1588.656	100.00
0.100	0.00	0.710	17.94	5.024	98.16	35.586	100.00	251.785	100.00	1782.502	100.00
0.112	0.00	0.796	20.87	5.637	98.26	39.905	100.00	282.508	100.00	2000.000	100.00
0.126	0.00	0.893	23.97	6.325	99.55	44.774	100.00	316.979	100.00	1000000000	

## SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE EMISSION SOURCE DESCRIPTION:		ir Quality - Applic				•		В
EMISSION SOURCE DESCRIPTION:	FGD Byproduc	1 5110			SOURCE			
			CONTROL DEVICE ID NO(S): CD-75					
	1 OF				I POINT (ST	TACK) ID N	O(S): EP-7	5
DESCRIBE IN DETAILTHE EMISSIO The byproduct solids from the dry FGI		•		•	nto a bypro	duct storage	e silo.	
TYPE OF EMISSION SOUR	RCE (CHECK AN	ND COMPLETE AF	PROPRIA	TE FORM E	81-B9 ON T	HE FOLLO	WING PAG	ES):
Coal,wood,oil, gas, other burner (I	Form B1)	□ Woodworking	(Form B4)		🗆 Mani	uf. of chemi	cals/coating	gs/inks (Form
□ Int.combustion engine/generator (	Form B2)	Coating/finish	ing/printing	(Form B5)	🗌 Incin	eration (For	rm B8)	
Liquid storage tanks (Form B3)		Storage silos/	bins (Form	B6)	□ Othe	r (Form B9)	)	
START CONSTRUCTION DATE: TBE	)		DATE MAI	NUFACTUR	ED: TBD			
MANUFACTURER / MODEL NO.: TB	D		EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	52 WK/YR
IS THIS SOURCE SUBJECT	NSPS (SUBPAR	TS?):			SHAP (SUB	PARTS?):_		
PERCENTAGE ANNUAL THROUGH	. ,			-	JUN-AUG	25		OV 25
CRITERIA A	IR POLLUTA	ANT EMISSION	IS INFOR	<b>MATION</b>	FOR TH	IS SOUR	CE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIC	NS
		EMISSION	AFTER CONT	ROLS / LIMITS)	BEFORE CONT	ROLS / LIMITS	(AFTER CON	TROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Vendor	0.06	0.24	N/A	N/A	0.06	0.24
PARTICULATE MATTER<10 MICRONS	6 (PM <sub>10</sub> )	Vendor	0.05	0.22	N/A	N/A	0.05	0.22
PARTICULATE MATTER<2.5 MICRON	S (PM <sub>2.5</sub> )	Vendor	0.03	0.13	N/A	N/A	0.03	0.13
JLFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N//
			N/A	N/A	N/A	N/A	N/A	N//
ARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N//
VOLATILE ORGANIC COMPOUNDS	(VOC)		N/A	N/A	N/A	N/A	N/A	N/#
LEAD			N/A	N/A	N/A	N/A	N/A	N//
OTHER			N/A	N/A	N/A	N/A	N/A	N/#
HAZARDOUS	AIR POLLU	TANT EMISSIC						
		SOURCE OF	-	D ACTUAL				
HAZARDOUS AIR POLLUTANT	CAS NO.	EMISSION FACTOR	Ib/hr		BEFORE CONT	tons/yr	Ib/hr	tons/yr
HAZARDOUS AIR FOLLUTANT	CAS NO.	FACTOR	10/11	tons/yr	ID/TII	toris/yi	10/11	toris/yr
N/A								
TOXIC AII	R POLLUTAN	IT EMISSIONS	INFORM	ATION F	OR THIS	SOURC	E	
		SOURCE OF	EVDENTE					/ LIMITATION
	EMISSION	EXPECTE	JACTUAL	EIVIISSIONS	SAFIER	UNTROLS		
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb	/hr	lb/d	day		lb/yr
N/A								
	1							

 WPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

 Attach Additional Sheets As Necessary

## EMISSION SOURCE (STORAGE SILO/BINS)

REVISED 09/22/16	NCDEQ/Divi	sion of Air Quality - Ap	plicatio	n for Ai	r Permit to Con	struct/Operate		B6
EMISSION SOURCE DESCRIPTI	ION: FGD Byproduct	Silo			EMISSION SO	URCE ID NO: ES	S-75	
					CONTROL DE	VICE ID NO(S): (	CD-75	
OPERATING SCENARIO:	1	OF1			EMISSION PO	INT(STACK) ID N	NO(S): EP-75	
DESCRIBE IN DETAIL THE PRO			Filter ba	ghouse	into a byproduc	ct storage silo.		
MATERIAL STORED: Byproducts	from FGD			DENSI	TY OF MATERI	AL (LB/FT3): Us	e gypsum as surrogate.	
	CUBIC FEET: TBD			TONS:			gypean ae ean egater	
	HEIGHT: TBD	DIAMETER: TBD	(OR)	LENG		WIDTH:	HEIGHT:	
ANNUAL PRODUCT THROU	JGHPUT (TONS)	ACTUAL: TBD			MAXIMUM DE	SIGN CAPACITY	: TBD	
PNEUMATICALLY FILI	LED	MECHANIC	ALLY FI	LLED			FILLED FROM	
BLOWER		SCREW CONVEYOR				RAILCA	AR	
		BELT CONVEYOR					< colored and set of the set of t	
OTHER:		BUCKET ELEVATOR					GE PILE	
		OTHER:				OTHER	R: Dry Scrubber	
NO. FILL TUBES: 1								
MAXIMUM ACFM: 1300								
MATERIAL IS UNLOADED TO: Trucks								
BY WHAT METHOD IS MATERIA Gravity unloading to trucks.	AL UNLOADED FRO	M SILO?						
MAXIMUM DESIGN FILLING RAT	TE OF MATERIAL (1	ONS/HR): TBD						
MAXIMUM DESIGN UNLOADING	G RATE OF MATERI	AL (TONS/HR): TBD						
COMMENTS:								

REVISED 09/22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate C1										
CONTROL DEVICE ID NO: CD-75		CONTROLS EMISSI	ONS FROM WHICH	EMISSIC	ON SOURCE ID NO(S	): ES-7	5			
EMISSION POINT (STACK) ID NO(S):	P-75	POSITION IN SERIE	S OF CONTROLS				NO.	1	OF 1	UNITS
OPERATING SCE	NARIO:									
1OF			P.E. SEAL REQUIR	ED (PEF	R 2q .0112)?		7	YES		□ NO
DESCRIBE CONTROL SYSTEM: A bin vent f	or particulate	control on the FGD By	product Silo.							
POLLUTANTS COLLECTED:			PM		PM10		PM2.5			
				-						
BEFORE CONTROL EMISSION RATE (LB/HF	२):		0.06	_	0.05		0.03			
CAPTURE EFFICIENCY:			<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%		%
CONTROL DEVICE EFFICIENCY:			N/A	%	N/A	%	N/A	%		%
				<i>,</i> ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	1071			70		<i>,</i> ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
CORRESPONDING OVERALL EFFICIENCY:			N/A	%	N/A	%	N/A	%		%
EFFICIENCY DETERMINATION CODE:			2	_	2		2			
TOTAL AFTER CONTROL EMISSION RATE (	(I B/HR)·		0.06		0.05		0.03			
							0.05			
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: A	vg: 10-15 wg	GAUGE?	YES							
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25	LB/HR	GR/FT <sup>3</sup>	INLET TEMPERATU			MIN		MAX MAX		
			OUTLET TEMPERA			IVIIIN		IVIAA		
INLET AIR FLOW RATE (ACFM): 1300 NO. OF COMPARTMENTS: 1 N				GILIVIF				20		
		PER COMPARTMENT	-				TH OF BAG (IN.): 20			
NO. OF CARTRIDGES: FI TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ):	ILTER SURF	AIR TO CLOTH RAT				DIAIVIE	TER OF BAG (IN.):	5-15		
DRAFT TYPE: INDUCED/NEGATI	IVE 🗹	FORCED/POSITIVE			FILTER MATERIAL: C	ortriday	Stulo	WOVE	N D	FELTED
DESCRIBE CLEANING PROCEDURES:	VE 🗹	FORCED/POSITIVE		<u>г</u>	TETER MATERIAL. C	annuge				
	_									
		SONIC	DOF				SIZE		VEIGHT %	CUMULATIVE
		SIMPLE BAG COLLA					(MICRONS)	(	OF TOTAL	%
		RING BAG COLLAP	SE				0-1			
DESCRIBE INCOMING AIR STREAM:							1-10			
DESCRIBE INCOMING AIR STREAM.							10-25			
							25-50			
							50-100			
							>100			
						Cuppli	er specific, 94% pass		TOTAL	= 100
						Suppli	er specific, 94 % pass	any 52	5 mesn	
ON A SEPARATE PAGE, ATTACH A DIAGRA	M SHOWING	THE RELATIONSHIP	OF THE CONTROL	DEVICE	TO ITS EMISSION S	OURCE	E(S):			
COMMENTS:										
1										

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate								В	
EMISSION SOURCE DESCRIPTION:	FGD Absorber	nt Silo		EMISSION	SOURCE	ID NO: ES-	76		
				CONTROL	DEVICE ID	0 NO(S): C	D-76		
OPERATING SCENARIO	1 OF	1		EMISSION	I POINT (ST	FACK) ID N	O(S): EP-7	6	
DESCRIBE IN DETAILTHE EMISSIO Storage of absorbent (hydrated lime)		•	I FLOW DIA	(GRAM):					
TYPE OF EMISSION SOUR	CE (CHECK AN	ID COMPLETE A	PPROPRIA	TE FORM I	B1-B9 ON 1		WING PAG	SES):	
□ Coal,wood,oil, gas, other burner (	Form B1)		g (Form B4)	)	🗆 Manı	uf. of chemi	cals/coating	gs/inks (Form	
□ Int.combustion engine/generator (	Form B2)	Coating/finis	hing/printing	g (Form B5)		eration (Fo			
Liquid storage tanks (Form B3)		✓ Storage silos	s/bins (Form	n B6)	□ Othe	er (Form B9	)		
START CONSTRUCTION DATE: TBE	)		DATE MAN	NUFACTUR	ED: TBD				
MANUFACTURER / MODEL NO.: TB	D		EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	52 WK/YR	
IS THIS SOURCE SUBJECT	NSPS (SUBPAR	:TS?):			SHAP (SUB	PARTS?):_			
PERCENTAGE ANNUAL THROUGH	( )			25	JUN-AUG		SEP-I	NOV 25	
CRITERIA A	IR POLLUTA	NT EMISSIOI	NS INFOR	RMATION	I FOR TH	IIS SOUF	RCE		
		SOURCE OF	EXPECTE				L EMISSIC	NS	
		EMISSION	AFTER CONT	ROLS / LIMITS)	BEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)	
AIR POLLUTANT EMITTED	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr		
PARTICULATE MATTER (PM)		Vendor	0.06	0.24	N/A	N/A	0.06	0.24	
PARTICULATE MATTER<10 MICRON		Vendor	0.05	0.22	N/A	N/A	0.05	0.22	
PARTICULATE MATTER<2.5 MICRON	S (PM <sub>2.5</sub> )	Vendor	0.03	0.13	N/A	N/A	0.03	0.13	
SULFUR DIOXIDE (SO2)		-	N/A	N/A	N/A	N/A	N/A	N/A	
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A	
	(1/20)		N/A	N/A	N/A	N/A	N/A	N/A	
VOLATILE ORGANIC COMPOUNDS	(VOC)		N/A	N/A	N/A	N/A	N/A	N/A	
LEAD			N/A	N/A	N/A	N/A	N/A	N/A	
OTHER HAZARDOUS			N/A		N/A		N/A	N/A	
NAZARDO03	AIR POLLUI		T						
		SOURCE OF EMISSION	EXPECTE		POTENTIAL EMISSIONS BEFORE CONTROLS / LIMITS (AFTER CONTROLS /				
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	Ib/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	
	CAUNO.	TACTOR	10/11	10113/ yi	10/11	t0113/ y1	10/111	ton 3/ yr	
N/A									
TOXIC AIR	POLLUTAN	T EMISSIONS	<b>INFORM</b>	ATION P	OR THIS	S SOURC	E		
		SOURCE OF	EVDECTEI					LIMITATION	
		EMISSION		5 NOTONE					
TOXIC AIR POLLUTANT	NT CAS NO. FACTOR Ib/hr Ib/day						lb/yr		
		ļ							
		ļ							
		ļ							
N/A		ļ							
		ļ							
		1	1		1				

 IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

 Attach Additional Sheets As Necessary

REVISED 09/22/16	NCDEQ/Div	vision of Air Quality - Ap	plicatio	n for Ai	r Permit to Co	nstruct/Op	perate		B6
EMISSION SOURCE DESCRIP	TION: FGD Absorbe	nt Silo			EMISSION SC	OURCE ID	NO: ES-7	76	
					CONTROL DE	VICE ID N	IO(S): CE	0-76	
OPERATING SCENARIO:	1	OF1			EMISSION PC	DINT(STAC	K) ID NC	D(S): EP-76	
DESCRIBE IN DETAIL THE PRO									
MATERIAL STORED: FGD Abso	orbent			DENS	TY OF MATER	IAL (LB/FT	ГЗ): Use ł	hydrated lime as surrog	jate.
CAPACITY	CUBIC FEET: TBD			TONS:		<b>`</b>	,	<u>,                                     </u>	
DIMENSIONS (FEET)	DIMENSIONS (FEET) HEIGHT: TBD DIAMETER: TBD (OF			LENG	TH:	WIDTH:		HEIGHT:	
ANNUAL PRODUCT THRO	DUGHPUT (TONS)	ACTUAL: TBD			MAXIMUM DE	SIGN CAP	PACITY: 1	TBD	
PNEUMATICALLY FI	LLED	MECHANIC	ALLY FI	LLED				FILLED FROM	
BLOWER		SCREW CONVEYOR					RAILCAR	R	
		BELT CONVEYOR				-	TRUCK		
OTHER:		BUCKET ELEVATOR					STORAG	E PILE	
		OTHER:					OTHER:		
NO. FILL TUBES: 1									
MAXIMUM ACFM: 1300									
MATERIAL IS UNLOADED TO:									
Material is sent to dry scrubber. BY WHAT METHOD IS MATERI									
N/A									
MAXIMUM DESIGN FILLING RA	ATE OF MATERIAL	(TONS/HR): TBD							
MAXIMUM DESIGN UNLOADIN	G RATE OF MATER	RIAL (TONS/HR): TBD							
COMMENTS:									

REVISED 09/22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate C1									C1	
CONTROL DEVICE ID NO: CD-76	CONTROLS EMISSI	ONS FROM WHICH	EMISSIC	ON SOURCE ID NO(S	6): ES-7	6				
EMISSION POINT (STACK) ID NO(S): EP-76	POSITION IN SERIE	S OF CONTROLS				NO.	1	OF 1	UNITS	
OPERATING SCENARIO:										
1 OF1		P.E. SEAL REQUIR	ED (PER	R 2q .0112)?		<	YES		□ NO	
DESCRIBE CONTROL SYSTEM: A bin vent for particulate co	ontrol on the FGD Abs	sorbent Silo.								
POLLUTANTS COLLECTED:		PM		PM10	_	PM2.5			-	
BEFORE CONTROL EMISSION RATE (LB/HR):		0.06	_	0.05	-	0.03			-	
CAPTURE EFFICIENCY:		<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%		%	
		<= 0.003 gi/d3ci	/0	<= 0.005 gi/daci		<= 0.003 gi/daci	70		- 70	
CONTROL DEVICE EFFICIENCY:		N/A	%	N/A	%	N/A	%		%	
					-				•	
CORRESPONDING OVERALL EFFICIENCY:		N/A	%	N/A	%	N/A	%		%	
EFFICIENCY DETERMINATION CODE:		2		2	-	2			-	
				0.05						
TOTAL AFTER CONTROL EMISSION RATE (LB/HR):		0.06	-	0.05	-	0.03			<u> </u>	
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: Avg: 10-15 wg	GAUGE?	] YES		-						
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25	2	INLET TEMPERATU			MIN		MAX			
POLLUTANT LOADING RATE: N/A	GR/FT <sup>3</sup>	OUTLET TEMPERA			MIN		MAX			
INLET AIR FLOW RATE (ACFM): 1300		FILTER OPERATIN	G TEMP	(°F): Contract						
	ER COMPARTMENT:	_				TH OF BAG (IN.): 20				
	CE AREA PER CARTI				DIAME	TER OF BAG (IN.):	5-15			
	AIR TO CLOTH RAT	IO: 1 to 4 : 1				~				
DRAFT TYPE: INDUCED/NEGATIVE I DESCRIBE CLEANING PROCEDURES:	FORCED/POSITIVE		F	ILTER MATERIAL: C	annage		WOVE		FELTED	
	SONIC	205				SIZE		VEIGHT %	CUMULATIV	/E
	SIMPLE BAG COLLA					(MICRONS)	(	OF TOTAL	%	
	RING BAG COLLAPS	SE				0-1			<u> </u>	
DESCRIBE INCOMING AIR STREAM:						1-10			<u> </u>	
						10-25 25-50			<u> </u>	
						50-100				
						>100			<u> </u>	
						100		TOTAL	= 100	
					Supplie	er specific, 94% pass	sing 32		. = 100	
ON A SEPARATE PAGE, ATTACH A DIAGRAM SHOWING T COMMENTS:	THE RELATIONSHIP	OF THE CONTROL	DEVICE	TO ITS EMISSION S	OURCE	(S):				
COMMENTS.										

#### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDEC	ED 09/22/1 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate								
EMISSION SOURCE DESCRIPTION: EH	HE- External H	eat Exchanger 1 &	2	EMISSION SOURCE ID NO: ES-77 and ES-7					
					DEVICE ID				
OPERATING SCENARIO 1	OF	1			POINT (ST	. ,			
DESCRIBE IN DETAILTHE EMISSION S Process heat exchanger. Total operation the lb/hr of a single unit * 8760 hours per	of unit 1 and 2	2 combined will not	exceed 876	RAM): 0 hours per	years. The	refore annu	al emission	are based on	
TYPE OF EMISSION SOUR	CE (CHECK A	ND COMPLETE AP	PROPRIAT	E FORM B	1-B9 ON TH	IE FOLLOV	VING PAGE	S):	
Coal,wood,oil, gas, other burner (For	m B1)		(Form B4)		🗆 Man	uf. of chemi	cals/coating	s/inks (Form B	
Int.combustion engine/generator (Fo	rm B2)	Coating/finishi	ng/printing (	Form B5)	🗌 Incin	eration (For	m B8)		
Liquid storage tanks (Form B3)		Storage silos/b	oins (Form E	36)	⊡ Othe	r (Form B9)			
START CONSTRUCTION DATE: TBD			DATE MAN	NUFACTUR	ED: TBD				
MANUFACTURER / MODEL NO.: TBD			EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR	
IS THIS SOURCE SUBJECT 🛛 NS	PS (SUBPAR	rs?):			SHAP (SUB	PARTS?):_			
PERCENTAGE ANNUAL THROUGHPU	. ,		R-MAY 25		JN-AUG	25	SEP-NO\	/ 25	
CRITERIA Ali	R POLLUTA	NT EMISSION	S INFOR	MATION	FOR TH	IS SOUR	CE		
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS	
		EMISSION	AFTER CONT	ROLS / LIMITS	BEFORE CONT	ROLS / LIMITS	(AFTER CON	TROLS / LIMITS)	
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	
PARTICULATE MATTER (PM)		Vendor	5.36	23.46	N/A	N/A	5.36	23.46	
PARTICULATE MATTER<10 MICRONS (I	10/	Vendor	4.93	21.59	N/A	N/A	4.93	21.59	
PARTICULATE MATTER<2.5 MICRONS (	PM <sub>2.5</sub> )	Vendor	2.84	12.44	N/A	N/A	2.84	12.44	
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A	
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A	
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A	
VOLATILE ORGANIC COMPOUNDS (V	C)		N/A	N/A	N/A	N/A	N/A	N/A	
LEAD		Ash Analysis			N/A	N/A	6.80E-04	2.98E-03	
OTHER			N/A	N/A	N/A	N/A	N/A	N/A	
HAZARDOUS A					N FUR I			-	
		SOURCE OF EMISSION			BEFORE CONT			NS	
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	Ib/hr	tons/yr	
Arsenic	7440-38-2	Ash Analysis			N/A	N/A	6.35E-04	2.78E-03	
Beryllium	7440-41-7	Ash Analysis			N/A	N/A	1.32E-04	5.76E-04	
Cadmium	7440-43-9	Ash Analysis			N/A	N/A	1.13E-04	4.97E-04	
Chromium	7440-47-3	Ash Analysis			N/A	N/A	7.71E-04	3.38E-03	
Chromium VI	18540-29-9	Ash Analysis			N/A	N/A	8.48E-05	3.71E-04	
Cobalt	7440-48-4	Ash Analysis			N/A	N/A	3.08E-04	1.35E-03	
Manganese	7439-96-5	Ash Analysis	1.36E-03	5.96E-03	N/A	N/A	1.36E-03	5.96E-03	
Mercury	7439-97-6	Ash Analysis	4.07E-06	1.78E-05	N/A	N/A	4.07E-06	1.78E-05	
Nickel	7440-02-0	Ash Analysis	7.71E-04	3.38E-03	N/A	N/A	7.71E-04	3.38E-03	
Selenium	7782-49-2	Ash Analysis	2.09E-04	9.14E-04	N/A	N/A	2.09E-04	9.14E-04	
TOXIC AIR	POLLUTAN	IT EMISSIONS	INFORM	ATION F	OR THIS	SOURC	E		
		SOURCE OF	EXPECTE	D ACTUAL	EMISSION	6 AFTER C	ONTROLS /	LIMITATIONS	
TOXIC AIR POLLUTANT	CAS NO.	EMISSION FACTOR	lb/	/hr	lb/o	day		b/yr	
Arsenic	7440-38-2	Ash Analysis				E-02		6E+00	
Beryllium	7440-41-7	Ash Analysis				E-03		5E+00	
Cadmium	7440-43-9	Ash Analysis				E-03		3E-01	
Chromium VI	18540-29-9	Ash Analysis				E-03		3E-01	
Manganese	7439-96-5	Ash Analysis				E-02		9E+01	
Mercury	7439-97-6	Ash Analysis				E-05		7E-02	
Nickel	7440-02-0	Ash Analysis	7.71E-04		1.85	E-02	6.7	5E+00	
Nickel         7440-02-0         Ash Analysis         7.71E-04         1.85E-02         6.75E+00           Attachments: (1) emissions calculations and supporting documentation; (2) indicate all requested state and federal enforceable permit limits (e.g. hours of operation,									

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

# FORM B9 EMISSION SOURCE (OTHER)

REVISED 09/22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate									
EMISSION SOURCE DESCRIPTION: EHE- External Heat Exchanger 1 &	2	EMISSION SOURCE ID NO: ES-77	7 and ES-78						
		CONTROL DEVICE ID NO(S): CD-	77 and CD-78						
OPERATING SCENARIO:1 OF1		EMISSION POINT (STACK) ID NO(S): EP-77 and EP-78							
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): Pro	icess neat excr	nanger							
MATERIALS ENTERING PROCESS - CONTINUOUS PROCE	ESS	MAX. DESIGN	REQUESTED CAPACITY						
TYPE	UNITS	CAPACITY (UNIT/HR)	LIMITATION(UNIT/HR)						
Heat Exchanger	Tons	70	70						
MATERIALS ENTERING PROCESS - BATCH OPERATIO	N	MAX. DESIGN	REQUESTED CAPACITY						
TYPE	UNITS	CAPACITY (UNIT/BATCH)	LIMITATION (UNIT/BATCH)						
			· · ·						
MAXIMUM DESIGN (BATCHES / HOUR):									
REQUESTED LIMITATION (BATCHES / HOUR):	(BATCHES/Y	′R):							
FUEL USED: N/A		MUM FIRING RATE (MILLION BTU/	(HR): N/A						
MAX. CAPACITY HOURLY FUEL USE: N/A	1	CAPACITY ANNUAL FUEL USE: N							
COMMENTS:									

NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate         C1									
CONTROL DEVICE ID NO: CD-77 & CD-78	CONTROLS EMISSI	ONS FROM WHICH	EMIS	SION SOURCE ID NO(S	): ES-7	7 & ES-78			
EMISSION POINT (STACK) ID NO(S): EP-77 & EP-78	POSITION IN SERIE	S OF CONTROLS				NO.	1 OF	1 UNITS	
OPERATING SCENARIO:									
1OF1		P.E. SEAL REQUIR	ED (P	FR 2g (112)?		~	YES	□ NO	
DESCRIBE CONTROL SYSTEM: A baghouse for particulate c					for one		.20		
POLLUTANTS COLLECTED:		PM		PM10	-	PM2.5			
BEFORE CONTROL EMISSION RATE (LB/HR):		5.36		4.93	-	2.84			
CAPTURE EFFICIENCY:		99.95	%	99.95	%	99.95	%	%	
CONTROL DEVICE EFFICIENCY:		N/A	%	N/A	%	N/A	%	%	
CORRESPONDING OVERALL EFFICIENCY:		N/A	%	N/A	%	N/A	%	%	
		2		2	-	2	·		
TOTAL AFTER CONTROL EMISSION RATE (LB/HR):		5.36		4.93		2.84			
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: Avg: 10"	GAUGE?	YES	C	NO					
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 60		INLET TEMPERATI	JRE (⁰	F):	MIN 18	0	MAX 325		
POLLUTANT LOADING RATE:  U LB/HR	GR/FT <sup>3</sup>	OUTLET TEMPERA	ATURE	(°F)	MIN 150 MAX 300				
INLET AIR FLOW RATE (ACFM): 42,000 FILTER OPERATING TEMP (°F): 250									
NO. OF COMPARTMENTS: 1 NO. OF BAGS PE	R COMPARTMENT: N	N/A			LENGT	H OF BAG	(IN.): N/A		
NO. OF CARTRIDGES: N/A FILTER SURFACE AREA PER CARTRIDGE (FT <sup>2</sup> ): N/A DIAMETER OF BAG (IN.): 6									
TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ): N/A	AIR TO CLOTH RAT	10: 3:1							
DRAFT TYPE: INDUCED/NEGATIVE	FORCED/POSITIVE			FILTER MATERIAL:			WOVEN	FELTED	
DESCRIBE CLEANING PROCEDURES:						PAR	TICLE SIZE DIS	TRIBUTION	
☑ AIR PULSE	SONIC				5	SIZE	WEIGHT %	CUMULAT	IVE
REVERSE FLOW	SIMPLE BAG COLLA	APSE			(MIC	CRONS)	OF TOTAL	%	
□ MECHANICAL/SHAKER □	RING BAG COLLAPS	SE				0-1			
□ OTHER:						1-10			
DESCRIBE INCOMING AIR STREAM: Air stream will contain fly	/ ash.				1	0-25			
					2	5-50			
					50	0-100			
					;	>100			
							Т	OTAL = 100	
					Particle	Size Distrib	oution 0-100 micr	on with an average o	of 20
ON A SEPARATE PAGE, ATTACH A DIAGRAM SHOWING TH			EVICE	TO ITS EMISSION SOL		).			
COMMENTS:						).			

#### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate											
EMISSION SOURCE DESCRIPTION: T	ransfer Silo Fil	ling		EMISSION	MISSION SOURCE ID NO: ES-79A						
				CONTROL	DEVICE ID	NO(S): CD	)-79				
OPERATING SCENARIO1_	OF _	1		EMISSION	POINT (ST	ACK) ID NO	D(S): EP-79				
DESCRIBE IN DETAILTHE EMISSION S Transfer silo is filled at the rate of 125 to		•		,							
TYPE OF EMISSION SOUR	•	_		E FORM B							
Coal,wood,oil, gas, other burner (Fo								s/inks (Form B			
Int.combustion engine/generator (Fo	,	Coating/finishi	0. 0	,		eration (For	,				
Liquid storage tanks (Form B3)		Storage silos/t		•		er (Form B9)					
START CONSTRUCTION DATE: TBD				NUFACTUR							
MANUFACTURER / MODEL NO.: TBD			EXPECTE				DAY/WK 5	2 WK/YR			
		/			SHAP (SUB	, –					
	( )	eb 25 mar A <b>NT EMISSION</b>	R-MAY 25		JN-AUG	25	SEP-NO\	/ 25			
	<b>TOLLUIF</b>		EXPECTE					NC			
		SOURCE OF EMISSION	AFTER CONTI			1					
AIR POLLUTANT EMITTED		FACTOR	lb/hr					topo/ur			
PARTICULATE MATTER (PM)		Manufacturer		tons/yr 9.74E-03	lb/hr N/A	tons/yr N/A	lb/hr 6.09E-03	tons/yr 9.74E-03			
PARTICULATE MATTER (FM)	PM.)	Manufacturer			N/A	N/A	2.88E-03	4.60E-03			
PARTICULATE MATTER<2.5 MICRONS	107	Manufacturer			N/A	N/A	2.88E-03	4.60E-03			
SULFUR DIOXIDE (SO2)	1 1012.57	Mandiacturer	2.00L=03	4.00L-03	N/A	N/A	2.00L-03	4.00L-03			
NITROGEN OXIDES (NOX)			N/A	N/A	N/A	N/A	N/A	N/A			
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A			
VOLATILE ORGANIC COMPOUNDS (V	00)		N/A	N/A	N/A	N/A	N/A	N/A			
LEAD	00)	Ash Analysis		1.24E-06	N/A	N/A	7.73E-07	1.24E-06			
OTHER			N/A	N/A	N/A	N/A	N/A	N/A			
HAZARDOUS A	IR POLLU	TANT EMISSIC	NS INFO	RMATIO	N FOR T	HIS SOU	IRCE				
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS			
		EMISSION	AFTER CONTI	ROLS / LIMITS	SEFORE CONT	ROLS / LIMITS	(AFTER CON	R CONTROLS / LIMITS)			
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr			
Arsenic	7440-38-2	Ash Analysis	7.21E-07	1.15E-06	N/A	N/A	7.21E-07	1.15E-06			
Beryllium	7440-41-7	Ash Analysis	1.49E-07	2.39E-07	N/A	N/A	1.49E-07	2.39E-07			
Cadmium	7440-43-9	Ash Analysis	1.29E-07	2.06E-07	N/A	N/A	1.29E-07	2.06E-07			
Chromium	7440-47-3	Ash Analysis	8.76E-07	1.4E-06	N/A	N/A	8.76E-07	1.40E-06			
Chromium VI	18540-29-9	Ash Analysis	9.64E-08	1.54E-07	N/A	N/A	9.64E-08	1.54E-07			
Cobalt	7440-48-4	Ash Analysis	3.5E-07	5.61E-07	N/A	N/A	3.5E-07	5.61E-07			
Manganese	7439-96-5	Ash Analysis	1.55E-06	2.47E-06	N/A	N/A	1.55E-06	2.47E-06			
Mercury	7439-97-6	Ash Analysis	4.63E-09	7.4E-09	N/A	N/A	4.63E-09	7.40E-09			
Nickel	7440-02-0	,		1.4E-06	N/A	N/A	8.76E-07	1.40E-06			
Selenium	7782-49-2	Ash Analysis		3.79E-07	N/A	N/A	2.37E-07	3.79E-07			
	POLLUTAN	IT EMISSIONS	INFORM	ATION F	OR THIS	SOURC	E				
		SOURCE OF EMISSION	EXPECTE	D ACTUAL	EMISSION	S AFTER C	ONTROLS /	LIMITATIONS			
TOXIC AIR POLLUTANT	CAS NO.	FACTOR		/hr		day		b/yr			
Arsenic	7440-38-2	Ash Analysis				E-05		31E-03			
Beryllium	7440-41-7	Ash Analysis				E-06		'8E-04			
Cadmium	7440-43-9	Ash Analysis				E-06		2E-04			
Chromium VI	18540-29-9	Ash Analysis				E-06		08E-04			
Manganese	7439-96-5	Ash Analysis				E-05		95E-03			
Mercury	7439-97-6	Ash Analysis				E-07		8E-05			
Nickel	7440-02-0	Ash Analysis				E-05		0E-03			
Attachments: (1) emissions calculations and s	upporting docum	entation; (2) indicate a	all requested	state and fed	eral enforcea	ble permit lin	nits (e.g. hour	s of operation,			

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

REVISED 09/22/16	NCDEQ/Divis	sion of Air Quality - Ap	plicatior	n for Air Permit to Cor	nstruct/Operate		B6
EMISSION SOURCE DESCRIPT	ΓΙΟΝ: Transfer Silo Fil	ling		EMISSION SO	URCE ID NO: ES	5-79A	
				CONTROL DE	VICE ID NO(S): C	C-79	
OPERATING SCENARIO:	1	OF1		EMISSION PO	NNT(STACK) ID N	IO(S): EP-79	
DESCRIBE IN DETAIL THE PRO			ict captur	e device.			
MATERIAL STORED: Fly Ash				DENSITY OF MATER	IAL (LB/FT3): 60 I	bulk, 90 structural	
CAPACITY	CUBIC FEET: N/A	-		TONS: 300			
DIMENSIONS (FEET)	HEIGHT: 100	DIAMETER: 41	(OR)	LENGTH:	WIDTH:	HEIGHT:	
ANNUAL PRODUCT THRO		ACTUAL: 400,000			SIGN CAPACITY		
PNEUMATICALLY FIL	LED	MECHANIC	ALLY FI	LLED	T	FILLED FROM	
BLOWER		SCREW CONVEYOR	<u>.</u>			١R	
		BELT CONVEYOR					
OTHER:		BUCKET ELEVATOR			_	GE PILE	
		OTHER:				:	
NO. FILL TUBES: 3							
MAXIMUM ACFM: 9000							
MATERIAL IS UNLOADED TO:							
N/A BY WHAT METHOD IS MATERI							
N/A							
MAXIMUM DESIGN FILLING RA	TE OF MATERIAL (T	ONS/HR): 125					
MAXIMUM DESIGN UNLOADING	G RATE OF MATERIA	AL (TONS/HR): N/A					
COMMENTS: This form is for Transfer Silo Filli	ng. Unloading data is	provided in Form B6 for	ES-79B.				

#### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE		В						
EMISSION SOURCE DESCRIPTION: T	ransfer Silo Un	loading		EMISSION	SOURCE I	D NO: ES-7	'9B	
				CONTROL	DEVICE ID	NO(S): CD	0-79	
OPERATING SCENARIO1_	OF	1			POINT (ST	. ,		
DESCRIBE IN DETAILTHE EMISSION S Transfer silo unloaded at the rate of 75 to		-		-				
TYPE OF EMISSION SOUR			PROPRIATE	E FORM B1	_			•
Coal,wood,oil, gas, other burner (Fo	=.,	Woodworking (Fe	,				0	s/inks (Form B
□ Int.combustion engine/generator (Fo	,	Coating/finishing		,		eration (For	,	
Liquid storage tanks (Form B3)		Storage silos/bin	is (Form B6	)	□ Othe	r (Form B9)		
START CONSTRUCTION DATE: TBD			DATE MAN	NUFACTUR	ED: TBD			
MANUFACTURER / MODEL NO.: TBD			EXPECTER		EDULE: 24		DAY/WK 5	2 WK/YR
IS THIS SOURCE SUBJECT	SPS (SUBPART	ſS?):			SHAP (SUB	PARTS?):		
PERCENTAGE ANNUAL THROUGHPU	( )				N-AUG	-	SEP-NOV	25
CRITERIA A	R POLLUT	ANT EMISSIONS	S INFORM	NATION	FOR THIS	S SOURC	æ	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONT	ROLS / LIMITS	SEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Manufacturer	0.00365	0.00974	N/A	N/A	0.00365	0.00974
PARTICULATE MATTER<10 MICRONS (	PM <sub>10</sub> )	Manufacturer	0.00173	0.00460	N/A	N/A	0.00173	0.00460
PARTICULATE MATTER<2.5 MICRONS	(PM <sub>2.5</sub> )	Manufacturer	0.00173	0.00460	N/A	N/A	0.00173	0.00460
SULFUR DIOXIDE (SO2)					N/A	N/A		
NITROGEN OXIDES (NOx)		[]			N/A	N/A		
CARBON MONOXIDE (CO)		[]			N/A	N/A		
VOLATILE ORGANIC COMPOUNDS (V	OC)	· · · · ·			N/A	N/A		
LEAD		Ash Analysis	4.64E-07	1.24E-06	N/A	N/A	4.64E-07	1.24E-06
OTHER		[]		<u> </u>	N/A	N/A		
HAZARDOUS	AIR POLLU	ITANT EMISSION	NS INFOI	RMATIO	N FOR TH	IIS SOUF	RCE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
					SEFORE CONT			ITROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis				N/A		1.15E-06
Beryllium	7440-41-7	Ash Analysis			N/A	N/A		2.39E-07
Cadmium	7440-43-9	Ash Analysis			N/A	N/A		2.06E-07
Chromium	7440-47-3	-		1.4E-06		N/A		1.40E-06
Chromium VI	18540-29-9	Ash Analysis		1.54E-07	N/A	N/A	5.78E-08	1.54E-07
Cobalt	7440-48-4	Ash Analysis		5.61E-07	N/A	N/A	2.1E-07	5.61E-07
Manganese	7439-96-5	Ash Analysis		2.47E-06	N/A	N/A	9.28E-07	2.47E-06
Mercury	7439-97-6	Ash Analysis			N/A	N/A	2.78E-09	7.40E-09
Nickel	7440-02-0	Ash Analysis		1.4E-06	N/A	N/A	5.26E-07	1.40E-06
Selenium	7782-49-2	Ash Analysis		3.79E-07	N/A	N/A	1.42E-07	3.79E-07
		NT EMISSIONS I				-		
		SOURCE OF EMISSION						LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb/	/hr	lb/c	day		lb/yr
Arsenic	7440-38-2	Ash Analysis	4.33E-07		1.04	E-05	2.3	31E-03
Beryllium	7440-41-7	Ash Analysis	8.97E-08		2.15	E-06	4.7	78E-04
Cadmium	7440-43-9	Ash Analysis	7.73E-08		1.85	E-06	4.1	2E-04
Chromium VI	18540-29-9	Ash Analysis	5.78E-08		1.39	E-06	3.0	)8E-04
Manganese	7439-96-5	Ash Analysis		i	2.23	E-05	4.9	95E-03
Mercury	7439-97-6	Ash Analysis				E-08		48E-05
Nickel	7440-02-0	Ash Analysis				E-05		30E-03
Attachments: (1) emissions calculations and s	upporting docum	entation: (2) indicate all	requested sta	ate and feder	al enforceable	e permit limits	s (e.a. hours (	of operation

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

MPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOUI

REVISED 09/22/16	NCDEQ/Divis	sion of Air Quality - Ap	plication	n for Air Permit to Co	onstruct/Operate		B6
EMISSION SOURCE DESCRIPT	ION: Transfer Silo Un	loading		EMISSION SO	OURCE ID NO: ES	;-79B	
				CONTROL DI	EVICE ID NO(S): C	CD-79	
OPERATING SCENARIO:	1	OF1		EMISSION PO	OINT(STACK) ID N	JO(S): EP-79	
DESCRIBE IN DETAIL THE PRO Transfer silo unloaded at the rate			uct captu	ure device.			
MATERIAL STORED: Fly Ash				DENSITY OF MATER	RIAL (LB/FT3): 60	bulk 90 structural	
	CUBIC FEET: N/A			TONS: 300			
	HEIGHT: 100	DIAMETER: 41		LENGTH:	WIDTH:	HEIGHT:	
ANNUAL PRODUCT THROU		ACTUAL: 400,000		•	ESIGN CAPACITY		
PNEUMATICALLY FIL	. ,	MECHANIC	ALLY FI			FILLED FROM	
□ BLOWER		SCREW CONVEYOR					
		BELT CONVEYOR				•	
OTHER:		BUCKET ELEVATOR	ŗ		□ STORA	GE PILE	
		OTHER:					
NO. FILL TUBES: N/A							
MAXIMUM ACFM: 9000							
MATERIAL IS UNLOADED TO:							
N/A							
BY WHAT METHOD IS MATERIA Gravity MAXIMUM DESIGN FILLING RA							
MAXIMUM DESIGN UNLOADING	RATE OF MATERIA	L (TONS/HR): 75					
COMMENTS: This form is for Transfer Silo Unlo	ading. Filling data is p	provided in Form B6 for	<sup>•</sup> ES-79A.				

REVISED 09/22/16	REVISED 09/22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate C1								
CONTROL DEVICE ID NO: CD-79	CONTROLS EMISSI	ONS FROM WHICH	EMISS	ION SOURCE ID NO(S)	: ES-79	A & ES-79B			
EMISSION POINT (STACK) ID NO(S): EP-79	POSITION IN SERIE	S OF CONTROLS				NO.	1	OF 1 U	JNITS
OPERATING SCENARIO:									
1 OF1		P.E. SEAL REQUIR	ED (PE	R 2q .0112)?		V	YES		NO
DESCRIBE CONTROL SYSTEM: A bin vent for particulate of	ontrol on the transfer s	ilo.							
POLLUTANTS COLLECTED:		PM (Filling)		PM10/PM2.5 (Filling)		PM (Unloading)		PM10/PM2.5 (Unloading)	
BEFORE CONTROL EMISSION RATE (LB/HR):		0.0061		0.0029		0.0037		0.0017	
CAPTURE EFFICIENCY:		<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%
CONTROL DEVICE EFFICIENCY:		N/A	%	N/A	%	N/A	%	N/A S	%
CORRESPONDING OVERALL EFFICIENCY:		N/A	%	N/A	%	N/A	%	N/A S	%
		2		2		2		2	
TOTAL AFTER CONTROL EMISSION RATE (LB/HR):		0.0061		0.0029		0.0037		0.0017	
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: Avg: 10-15 wg	GAUGE?	YES		NO					
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25		INLET TEMPERATU			MIN		MAX		
POLLUTANT LOADING RATE: N/A 🛛 LB/HR 🗌	] GR/FT <sup>3</sup>	OUTLET TEMPERA	TURE	(°F) Contract	MIN		MAX		
INLET AIR FLOW RATE (ACFM): 1300		FILTER OPERATIN	G TEM	P (°F): Contract					
NO. OF COMPARTMENTS: 1 NO. OF BAGS P	PER COMPARTMENT:	Contract			LENG	TH OF BAG (IN.): 2	20-30		
NO. OF CARTRIDGES: FILTER SURFAC	CE AREA PER CARTE	RIDGE (FT <sup>2</sup> ):			DIAME	TER OF BAG (IN.)	: 5-15		
TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ):	AIR TO CLOTH RAT	IO: 1 to 4 : 1							
DRAFT TYPE: INDUCED/NEGATIVE	FORCED/POSITIVE			FILTER MATERIAL: Ca	artridge	Style	WOVE	N 🗆 F	ELTED
DESCRIBE CLEANING PROCEDURES:						F	PARTIC	LE SIZE DISTRIBUTION	
☑ AIR PULSE	SONIC					SIZE		WEIGHT %	CUMULATIVE
REVERSE FLOW	SIMPLE BAG COLLA	APSE				(MICRONS)		OF TOTAL	%
	RING BAG COLLAPS	SF				0-1			
				•		1-10			
DESCRIBE INCOMING AIR STREAM: Air stream will contain	fly ash.					10-25			
	,			-		25-50			
				-					
				4		50-100 >100			
				4		>100		TOTAL 100	
				-	Supplié	er specific, 94% pa	ssina 2	TOTAL = 100	
ON A SEPARATE PAGE, ATTACH A DIAGRAM SHOWING	THE RELATIONSHIP	OF THE CONTROL D	DEVICE	TO ITS EMISSION SO	URCE(	S):			
COMMENTS:					(				
				ata An Nanana					

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDEC	/Division of A	ir Quality - Applica	ation for Ai	r Permit to	Construct/	Operate		В
EMISSION SOURCE DESCRIPTION: S	torage Dome F	Filling		EMISSION	SOURCE I	D NO: ES-8	30A	
				CONTROL	DEVICE ID	NO(S): CE	0-80	
OPERATING SCENARIO1_	OF	1				. ,	D(S): EP-80	
DESCRIBE IN DETAILTHE EMISSION S Storage Dome silo is filled at the rate of 7		-		-	ice.			
	CE (CHECK AI		PROPRIAT	E FORM B				
□ Coal,wood,oil, gas, other burner (For	,		(Form B4)					s/inks (Form B
<ul> <li>Int.combustion engine/generator (Fo</li> <li>Liquid storage tanks (Form B3)</li> </ul>	/	<ul> <li>Coating/finishi</li> <li>Storage silos/t</li> </ul>	0. 0.			eration (For r (Form B9)	,	
START CONSTRUCTION DATE: TBD			DATE MAN	UFACTUR	ED: TBD			
MANUFACTURER / MODEL NO.: TBD			EXPECTE	O OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
IS THIS SOURCE SUBJECT	PS (SUBPAR	FS?):			SHAP (SUB	PARTS?):		
PERCENTAGE ANNUAL THROUGHPU	T (%): DEC-F	EB 25 MAR	R-MAY 25		JN-AUG	25	SEP-NO\	/ 25
CRITERIA AIF	R POLLUTA	NT EMISSION	S INFOR	MATION	FOR TH	IS SOUR	CE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONT	ROLS / LIMITS	BEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Manufacturer	0.0037	0.0097	N/A	N/A	0.0037	0.0097
PARTICULATE MATTER<10 MICRONS (F	PM <sub>10</sub> )	Manufacturer	0.0017	0.0046	N/A	N/A	0.0017	0.0046
PARTICULATE MATTER<2.5 MICRONS (	PM <sub>2.5</sub> )	Manufacturer	0.0017	0.0046	N/A	N/A	0.0017	0.0046
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (VO	C)		N/A	N/A	N/A	N/A	N/A	N/A
LEAD		Ash Analysis	4.64E-07	1.24E-06	N/A	N/A	4.64E-07	1.24E-06
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS A	IR POLLU	TANT EMISSIC	NS INFO	RMATIO	N FOR T	HIS SOU	IRCE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONT	ROLS / LIMITS	SEFORE CONT	ROLS / LIMITS	(AFTER CON	TROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis	4.33E-07	1.15E-06	N/A	N/A	4.33E-07	1.15E-06
Beryllium	7440-41-7	Ash Analysis	8.97E-08	2.39E-07	N/A	N/A	8.97E-08	2.39E-07
Cadmium	7440-43-9	Ash Analysis	7.73E-08	2.06E-07	N/A	N/A	7.73E-08	2.06E-07
Chromium	7440-47-3	Ash Analysis	5.26E-07	1.4E-06	N/A	N/A	5.26E-07	1.40E-06
Chromium VI	18540-29-9	Ash Analysis	5.78E-08	1.54E-07	N/A	N/A	5.78E-08	1.54E-07
Cobalt	7440-48-4	Ash Analysis	2.1E-07	5.61E-07	N/A	N/A	2.1E-07	5.61E-07
Manganese	7439-96-5	Ash Analysis	9.28E-07	2.47E-06	N/A	N/A	9.28E-07	2.47E-06
Mercury	7439-97-6	Ash Analysis	2.78E-09	7.4E-09	N/A	N/A	2.78E-09	7.40E-09
Nickel	7440-02-0	Ash Analysis	5.26E-07	1.4E-06	N/A	N/A	5.26E-07	1.40E-06
Selenium	7782-49-2	Ash Analysis		3.79E-07	N/A	N/A	1.42E-07	3.79E-07
TOXIC AIR I	POLLUTAN	IT EMISSIONS	INFORM	ATION F	OR THIS	SOURC	E	
		SOURCE OF EMISSION	EXPECTE	O ACTUAL	EMISSION	SAFTER C	ONTROLS /	LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	FACTOR		/hr	lb/d	day		b/yr
Arsenic	7440-38-2	Ash Analysis	4.33E-07		1.04	E-05	2.3	31E-03
Beryllium	7440-41-7	Ash Analysis	8.97E-08		2.15	E-06	4.7	'8E-04
Cadmium	7440-43-9	Ash Analysis	7.73E-08		1.85	E-06	4.1	2E-04
Chromium VI	18540-29-9	Ash Analysis	5.78E-08		1.39	E-06	3.0	8E-04
Manganese	7439-96-5	Ash Analysis	9.28E-07		2.23	E-05	4.9	95E-03
Mercury	7439-97-6	Ash Analysis	2.78E-09			E-08		8E-05
Nickel	7440-02-0	Ash Analysis	5.26E-07		1.26	E-05	2.8	80E-03
Attachments: (1) emissions calculations and se	upporting docum	entation; (2) indicate a	all requested	state and fed	eral enforcea	ble permit lin	nits (e.g. hour	s of operation,

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for full source.

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

REVISED 09/22/16	NCDEQ/Divis	sion of Air Quality - Ap	plicatior	n for Air Permit to Co	nstruct/Operate		B6		
EMISSION SOURCE DESCRIPT	FION: Storage Dome F	Filling		EMISSION SC	OURCE ID NO: ES	S-80A			
				CONTROL DE	EVICE ID NO(S): C	CD-80			
OPERATING SCENARIO:	1	OF1		EMISSION PC	DINT(STACK) ID N	IO(S): EP-80			
DESCRIBE IN DETAIL THE PRC Storage Dome is filled at the rate			uct captu	re device.					
MATERIAL STORED: Fly Ash				DENSITY OF MATER	IAL (LB/FT3): 60	bulk, 90 structural			
CAPACITY	CUBIC FEET: N/A	-		TONS: 30,000					
DIMENSIONS (FEET)	HEIGHT: 125	DIAMETER: 41	(OR)	LENGTH:	WIDTH:	HEIGHT:			
ANNUAL PRODUCT THRO		ACTUAL: 400,000		: 400,000					
PNEUMATICALLY FIL	LED	MECHANIC	ALLY FI	LLED		FILLED FROM			
BLOWER		SCREW CONVEYOR				NR			
		BELT CONVEYOR							
OTHER:		BUCKET ELEVATOR			_	GE PILE			
		OTHER:				:			
NO. FILL TUBES: 1									
MAXIMUM ACFM: 7600									
MATERIAL IS UNLOADED TO:									
N/A BY WHAT METHOD IS MATERI									
N/A									
MAXIMUM DESIGN FILLING RA	TE OF MATERIAL (T	ONS/HR): 75							
MAXIMUM DESIGN UNLOADING	G RATE OF MATERIA	AL (TONS/HR): N/A							
COMMENTS: This form is for Storage Dome Fi	lling. Unloading data is	s provided in Form B6 f	or ES-80	В.					

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of A	Air Quality - Applica	ation for Ai	r Permit to	Construct/	Operate		В
EMISSION SOURCE DESCRIPTION:	Storage Dome L	Jnloading		EMISSION	SOURCE I	D NO: ES-8	30B	
			ŀ	CONTROL	DEVICE ID	NO(S): CD	0-80	
OPERATING SCENARIO1_	OF	1			POINT (ST	. ,		
DESCRIBE IN DETAILTHE EMISSION Storage Dome is unloaded at the rate o		•			evice.			
TYPE OF EMISSION SOUR	CE (CHECK AN	ND COMPLETE AF	PROPRIAT	E FORM B	1-B9 ON TH	HE FOLLOW	WING PAGE	ES):
Coal,wood,oil, gas, other burner (Fo	orm B1)		(Form B4)		🗌 Manı	uf. of chemi	cals/coating	s/inks (Form B
<ul> <li>Int.combustion engine/generator (F</li> <li>Liquid storage tanks (Form B3)</li> </ul>	,	<ul><li>Coating/finishi</li><li>Storage silos/b</li></ul>	01 0	· · ·		eration (For r (Form B9)	,	
START CONSTRUCTION DATE: TBD			DATE MAN	NUFACTUR	ED: TBD			
MANUFACTURER / MODEL NO.: TBD			1		EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
	ISPS (SUBPART	rs?):			SHAP (SUBI			
PERCENTAGE ANNUAL THROUGHPU		,	R-MAY 25		UN-AUG	25	SEP-NO\	V 25
	. ,	ANT EMISSION						
	1	SOURCE OF		D ACTUAL				NS
	ļ				BEFORE CONT	-		NTROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Manufacturer		0.0097	N/A	N/A	0.0134	0.0097
PARTICULATE MATTER<10 MICRONS	(PM <sub>10</sub> )	Manufacturer		0.0046		N/A	0.0063	0.0046
PARTICULATE MATTER<2.5 MICRONS	107	Manufacturer		0.0046	N/A	N/A	0.0063	0.0046
SULFUR DIOXIDE (SO2)	(12.5)	in a contract of the second se	0.0000 N/A	0.0040 N/A	N/A	N/A	0.0000 N/A	0.0040 N/A
NITROGEN OXIDES (NOx)		ł	N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)		ł	N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (\	VOC)	ł	N/A	N/A N/A	N/A	N/A	N/A	N/A
LEAD	/00)	Ash Analysis				N/A N/A	1.70E-06	1.24E-06
OTHER		Plott / 11.00.7	N/A	1.24E-00 N/A	N/A	N/A	1.70E-06 N/A	1.24E-00
HAZARDOUS	AIR POLLU	TANT EMISSIC	-	-			-	
		SOURCE OF		D ACTUAL				INS
					BEFORE CONT			TROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis		1.15E-06		N/A		1.15E-06
Beryllium	7440-41-7	Ash Analysis		2.39E-07	N/A	N/A		2.39E-07
Cadmium	7440-43-9	Ash Analysis		2.06E-07	N/A	N/A		2.06E-07
Chromium	7440-47-3					N/A		1.40E-06
Chromium VI	18540-29-9	Ash Analysis	1	1.54E-07		N/A	2.12E-07	1.54E-07
Cobalt	7440-48-4	Ash Analysis		5.61E-07	N/A	N/A	7.71E-07	5.61E-07
Manganese	7439-96-5	Ash Analysis		2.47E-06		N/A	3.40E-06	2.47E-06
Mercury	7439-97-6	Ash Analysis		7.4E-09		N/A	1.02E-08	7.40E-09
Nickel	7440-02-0			1.4E-06		N/A	1.93E-06	1.40E-06
Selenium	7782-49-2	Ash Analysis				N/A	5.22E-07	3.79E-07
		IT EMISSIONS						
		SOURCE OF EMISSION						/ LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb	/hr	lb/c	day		lb/yr
Arsenic	7440-38-2	Ash Analysis				E-05		31E-03
	7440-41-7	Ash Analysis	1			E-06		78E-04
Beryllium		-				E-06		12E-04
,	7440-43-9	ASN ANAIYSIS	2.000-07					)8E-04
Cadmium	7440-43-9	Ash Analysis Ash Analysis	1			F-06	3.0	
Cadmium Chromium VI	18540-29-9	Ash Analysis	2.12E-07					
Cadmium Chromium VI Manganese	18540-29-9 7439-96-5	Ash Analysis Ash Analysis	2.12E-07 3.40E-06		8.16	E-05	4.9	95E-03
Cadmium Chromium VI	18540-29-9	Ash Analysis Ash Analysis	2.12E-07 3.40E-06 1.02E-08		8.16 2.44		4.9 1.4	

I IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): Storage Dome is unloaded at the rate of 275 ton/hr and equipped with bin vent product capture device.         MATERIAL STORED: Fly Ash       DENSITY OF MATERIAL (LB/FT3): 60 bulk, 90 structural         CAPACITY       CUBIC FEET: N/A         TONS: 30,000       TONS: 30,000         DIMENSIONS (FEET)       HEIGHT: 125         ANNUAL PRODUCT THROUGHPUT (TONS)       ACTUAL: 400,000         MAXIMUM DESIGN CAPACITY       HEIGHT: 25         ODMENSIONS (FEET)       HEIGHT: 25         NOL PNEUMATICALLY FILLED       FILLED FROM         BLOWER       SCREW CONVEYOR       RAILCAR         COMPRESSOR       BELT CONVEYOR       RAILCAR         BLOWER       BUCKET ELEVATOR       TRUCK         OTHER:       BUCKET ELEVATOR       OTHER:         NO. FILL TUBES: N/A       BUCKET ELEVATOR       OTHER:         MAXIMUM ACFM: 7600       MATERIAL IS UNLOADED TO:       N/A         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A       MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): 275	REVISED 09/22/16	NCDEQ/Divis	ion of Air Quality - Ap	plicatior	n for Air Permit to Con	struct/Operate	<b>;</b>	B6
OPERATING SCENARIO:      OF      EMISSION POINT(STACK) ID NO(S): EP-80         DESCRIBE: IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM):	EMISSION SOURCE DESCRIPT	ION: Storage Dome L	Jnloading		EMISSION SO	URCE ID NO: E		
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): Storage Dome is unloaded at the rate of 275 ton/hr and equipped with bin vent product capture device. MATERIAL STORED: Fly Ash CAPACITY CUBIC FEET: N/A DIMENSIONS (FEET) HEIGHT: 125 DIAMETER: 41 (OR) LENGTH: WIDTH: HEIGHT: ANNUAL PRODUCT THROUGHPUT (TONS) ACTUAL: 400,000 PNEUMATICALLY FILLED MECHANICALLY FILLED FILLED FROM BLOWER SCREW CONVEYOR RATECALLY FILLED FILLED FROM BLOWER BLOWER BELT CONVEYOR RATECALLY FILLED FILLED FROM DIMERSION CONVEYOR STORAGE PILE OTHER: BLOWER SCREW CONVEYOR STORAGE PILE NO. FILL TUBES: N/A MAXIMUM ACFM: 7600 MATERIAL IS UNLOADED TO: N/A					CONTROL DE	VICE ID NO(S):	: CD-80	
Storage Dome is unloaded at the rate of 275 ton/hr and equipped with bin vent product capture device.         MATERIAL STORED: Fly Ash       DENSITY OF MATERIAL (LB/FT3): 60 bulk, 90 structural         CAPACITY       CUBIC FEET: N/A       TONS: 30,000         DIMENSIONS (FEET)       HEIGHT: 125       DIAMETER: 41       (OP)       LENGITY         ANNUAL PRODUCT THROUGHPUT (TONS)       ACTUAL: 400,000       MAXIMUM DESIGN CAPACITY: 400,000       FILLED FROM         ANNUAL PRODUCT THROUGHPUT (TONS)       ACTUAL: 400,000       MAXIMUM DESIGN CAPACITY: 400,000       FILLED FROM         OTHER:       SCREW CONVEYOR       RAILCAR       TRUCK         OTHER:       SCREW CONVEYOR       TRUCK       STORAGE PILE         NO. FILL TUBES: N/A       BUCKET ELEVATOR       STORAGE PILE       OTHER:         NO. FILL TUBES: N/A       MAXIMUM ACFM: 7600       OTHER:       OTHER:         NO. FILL TUBES: N/A       MAXIMUM ACFM: 7600       OTHER:       OTHER:         NO.       FUNCAL TRUCK       OTHER:       OTHER:       OTHER:	OPERATING SCENARIO:	1	OF1		EMISSION PO	INT(STACK) ID	NO(S): EP-80	
CAPACITY         CUBIC FEET: N/A         TONS: 30,000           DIMENSIONS (FEET)         HEIGHT: 125         DIAMETER: 411         (0R)         LENGTH:         WIDTH:         HEIGHT:           ANNUAL PRODUCT THROUGHPUT (TONS)         ACTUAL: 400,000         MAXIMUM DESIGN CAPACITY: 400,000         MAXIMUM DESIGN CAPACITY: 400,000           PNEUMATICALLY FILLED         MECHANICALLY FILLED         MECHANICALLY FILLED         MAXIMUM DESIGN CAPACITY: 400,000           ONDERSSOR         Isocretion         Isocretion         Isocretion         Isocretion         Isocretion           Isocretion         Isocretion         Isocretion         Isocretion <thisocretion< th="">         Isocretion         Isocretion         Isocretion           Isocretion         <thisocretion< th=""> <thisocretion< th=""> <thi< th=""><th></th><th></th><th></th><th>: product</th><th>capture device.</th><th></th><th></th><th></th></thi<></thisocretion<></thisocretion<></thisocretion<>				: product	capture device.			
CAPACITY         CUBIC FEET: N/A         TONS: 30,000           DIMENSIONS (FEET)         HEIGHT: 125         DIAMETER: 411         (0R)         LENGTH:         WIDTH:         HEIGHT:           ANNUAL PRODUCT THROUGHPUT (TONS)         ACTUAL: 400,000         MAXIMUM DESIGN CAPACITY: 400,000         MAXIMUM DESIGN CAPACITY: 400,000           PNEUMATICALLY FILLED         MECHANICALLY FILLED         MECHANICALLY FILLED         MAXIMUM DESIGN CAPACITY: 400,000           ONDERSSOR         Isocretion         Isocretion         Isocretion         Isocretion         Isocretion           Isocretion         Isocretion         Isocretion         Isocretion <thisocretion< th="">         Isocretion         Isocretion         Isocretion           Isocretion         <thisocretion< th=""> <thisocretion< th=""> <thi< td=""><td>MATERIAL STORED: Flv Ash</td><td></td><td></td><td></td><td>DENSITY OF MATERI</td><td>AL (LB/FT3): 6</td><td>0 bulk. 90 structural</td><td></td></thi<></thisocretion<></thisocretion<></thisocretion<>	MATERIAL STORED: Flv Ash				DENSITY OF MATERI	AL (LB/FT3): 6	0 bulk. 90 structural	
ANNUAL PRODUCT THROUGHPUT (TONS)       ACTUAL: 400,000       MAXIMUM DESIGN CAPACITY: 400,000         PNEUMATICALLY FILLED       MECHANICALLY FILLED       FILLED FROM         BLOWER       SCREW CONVEYOR       RAILCAR         COMPRESSOR       BELT CONVEYOR       TRUCK         OTHER:       BUCKET ELEVATOR       STORAGE PILE         OTHER:       OTHER:       OTHER:         NO. FILL TUBES:       N/A         MAXIMUM ACFM: 7600       TOTHER:         NATERIAL IS UNLOADED TO:       N/A         N/A       SUCKET ELEVATOR         BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?       N/A         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A       MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275         COMMENTS:       COMMENTS:       SCREW CONS/HR): 275		CUBIC FEET: N/A						
ANNUAL PRODUCT THROUGHPUT (TONS)       ACTUAL: 400,000       MAXIMUM DESIGN CAPACITY: 400,000         PNEUMATICALLY FILLED       FILLED FROM         BLOWER       SCREW CONVEYOR       RAILCAR         COMPRESSOR       BELT CONVEYOR       TRUCK         OTHER:       BUCKET ELEVATOR       STORAGE PILE         NO. FILL TUBES: N/A       OTHER:       OTHER:         MAXIMUM ACFM: 7600       OTHER:       OTHER:         NATERIAL IS UNLOADED TO:       N/A         N/A       BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A         MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275         COMMENTS:			DIAMETER: 41	(OR)		WIDTH:	HEIGHT:	
BLOWER       SCREW CONVEYOR       RAILCAR         COMPRESSOR       BELT CONVEYOR       TRUCK         OTHER:       BUCKET ELEVATOR       STORAGE PILE         OTHER:       OTHER:       OTHER:         NO. FILL TUBES: N/A       OTHER:       OTHER:         MAXIMUM ACFM: 7600       OTHER:       OTHER:         MATERIAL IS UNLOADED TO:       NA         BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?       NA         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A       MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275         COMMENTS:       COMMENTS:       Comments:		UGHPUT (TONS)	ACTUAL: 400,000		Y: 400,000			
COMPRESSOR BELT CONVEYOR TRUCK   OTHER: BUCKET ELEVATOR STORAGE PILE   OTHER: OTHER: OTHER:     NO. FILL TUBES: N/A OTHER:     MAXIMUM ACFM: 7600   MATERIAL IS UNLOADED TO:      NA        BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?                       MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A                    MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275								
OTHER: BUCKET ELEVATOR   OTHER: OTHER:     NO. FILL TUBES: N/A   MAXIMUM ACFM: 7600   MATERIAL IS UNLOADED TO:   NA   WHAT METHOD IS MATERIAL UNLOADED FROM SILO? NA MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275 COMMENTS:	BLOWER		SCREW CONVEYOR				CAR	
OTHER:     OTHER:     OTHER:     MAXIMUM ACFM: 7600     MATERIAL IS UNLOADED TO:     N/A     BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?     N/A     MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A     MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275   COMMENTS:			BELT CONVEYOR				ж	
NO. FILL TUBES: N/A MAXIMUM ACFM: 7600 MATERIAL IS UNLOADED TO: N/A BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275 COMMENTS:	OTHER:		BUCKET ELEVATOR				AGE PILE	
MAXIMUM ACFM: 7600 MATERIAL IS UNLOADED TO: N/A BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275 COMMENTS:			OTHER:				R:	
MATERIAL IS UNLOADED TO: N/A BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275 COMMENTS:	NO. FILL TUBES: N/A							_
N/A BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275 COMMENTS:	MAXIMUM ACFM: 7600							
BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275 COMMENTS:	MATERIAL IS UNLOADED TO:							
N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275 COMMENTS:	N/A							
MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 275 COMMENTS:	N/A							
COMMENTS:								
			L (ΤΟΝδ/ΠΚ): 215					
		nloading. Filling data is	s provided in Form B6 fo	эт ES-80	Α.			

CONTROL DEVICE ID NO: CD-80 EMISSION POINT (STACK) ID NO(S): EP-80 OPERATING SCENARIO: OF1	POSITION IN SERIES		EMISSI	ON SOURCE ID NO(S):	: ES-80	A & ES-80B NO.			
OPERATING SCENARIO:		S OF CONTROLS				NO			
							1 C	DF 1	UNITS
1 OF 1									
		P.E. SEAL REQUIRI	ED (PE	R 2a .0112)?			YES		NO
DESCRIBE CONTROL SYSTEM: A bin vent for particulate of			,	1 · /				_	
POLLUTANTS COLLECTED:		PM (Filling)		PM10/PM2.5 (Filling)	_	PM (Unloading)	_	PM10/PM2.5 (Unloading)	
BEFORE CONTROL EMISSION RATE (LB/HR):	-	0.0037	-	0.0017	-	0.0134		0.0063	
CAPTURE EFFICIENCY:		<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%
CONTROL DEVICE EFFICIENCY:		N/A	%	N/A	%	N/A	%	N/A	%
CORRESPONDING OVERALL EFFICIENCY:		N/A	%	N/A	%	N/A	%	N/A	%
EFFICIENCY DETERMINATION CODE:	-	2	-	2	-	2	_	2	
TOTAL AFTER CONTROL EMISSION RATE (LB/HR):		0.0037		0.0017	-	0.0134		0.0063	
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: Avg: 10-15 wg	GAUGE?								
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25	2	INLET TEMPERATU			MIN		MAX		
		OUTLET TEMPERA			MIN		MAX		
INLET AIR FLOW RATE (ACFM): 1300		FILTER OPERATING	3 TEM						
	PER COMPARTMENT:					H OF BAG (IN.): 2			
	CE AREA PER CARTR				DIAME	TER OF BAG (IN.)	5-15		
TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ):	AIR TO CLOTH RATIO	U: 1 to 4 : 1						_	
	FORCED/POSITIVE			FILTER MATERIAL: Ca	artridge		WOVEN		FELTED
DESCRIBE CLEANING PROCEDURES:				F			ARTICL	E SIZE DISTRIBUTION	
☑ AIR PULSE □	SONIC					SIZE		WEIGHT %	CUMULATIVE
	SIMPLE BAG COLLA			=	(	MICRONS)		OF TOTAL	%
MECHANICAL/SHAKER	RING BAG COLLAPS	E		-		0-1			
	0					1-10			
DESCRIBE INCOMING AIR STREAM: Air stream will contain	n fly asn.			-		10-25			
				-		25-50			
				-		50-100			
				-		>100			
				-	<u> </u>	r specific, 94% pas		TOTAL = 100	
					Supplie	n specific, 9476 pa	saing 520	, mean	
ON A SEPARATE PAGE, ATTACH A DIAGRAM SHOWING	THE RELATIONSHIP C	F THE CONTROL D	EVICE	TO ITS EMISSION SO	URCE(	S):			
COMMENTS:				note An Nonceso					

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of <i>I</i>	Air Quality - Applica	tion for Air	Permit to (	Construct/C	Operate		В
EMISSION SOURCE DESCRIPTION: L	oadout Silo			EMISSION	SOURCE I	D NO: ES-8	51	
				CONTROL	DEVICE ID	NO(S): CD	-81	
OPERATING SCENARIO 1	OF	1				ACK) ID NO		
DESCRIBE IN DETAILTHE EMISSION S Loadout silo is unloaded at the rate of 75	i ton/hr and eq	uipped with bin vent	product cap	ture device.		,		
TYPE OF EMISSION SOUR	•	_		E FORM B1				,
Coal,wood,oil, gas, other burner (For	,	☐ Woodworking (F 	Form B4)					gs/inks (Form B
Int.combustion engine/generator (Fo	,	Coating/finishin	<b>.</b> .	,		eration (For	,	
Liquid storage tanks (Form B3)		Storage silos/bi	,	,		r (Form B9)		
START CONSTRUCTION DATE: TBD				NUFACTUR				
MANUFACTURER / MODEL NO.: TBD			EXPECTE	D OP. SCH			DAY/WK 5	2 WK/YR
	PS (SUBPAR	, .			SHAP (SUB	7 =		
PERCENTAGE ANNUAL THROUGHPU	( )				N-AUG	25	SEP-NOV	25
CRITERIA AI	R POLLUT/	ANT EMISSION			FOR THI			
		SOURCE OF	EXPECTE			-	L EMISSIO	NS
				ROLS / LIMITS)			-	ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Manufacturer	0.0037	0.0097	N/A	N/A	0.0037	0.0097
PARTICULATE MATTER<10 MICRONS (I	10,	Manufacturer	0.0017	0.0046	N/A	N/A	0.0017	0.0046
PARTICULATE MATTER<2.5 MICRONS (	PM <sub>2.5</sub> )	Manufacturer	0.0017	0.0046	N/A	N/A	0.0017	0.0046
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (V	OC)		N/A	N/A	N/A	N/A	N/A	N/A
LEAD		Ash Analysis	4.64E-07	1.24E-06	N/A	N/A	4.64E-07	1.24E-06
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS	AIR POLLU	TANT EMISSIO			N FOR II			
		SOURCE OF EMISSION						
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	Ib/hr	ROLS / LIMITS) tons/yr	lb/hr	tons/yr	Ib/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis	4.33E-07	1.15E-06	N/A	N/A	4.33E-07	1.15E-06
Beryllium	7440-38-2	Ash Analysis	4.33L-07 8.97E-08		N/A	N/A	4.33Ľ-07 8.97E-08	2.39E-07
Cadmium	7440-43-9	Ash Analysis	7.73E-08	2.06E-07	N/A	N/A	7.73E-08	2.06E-07
Chromium	7440-47-3		5.26E-07	1.4E-06		N/A	5.26E-07	1.40E-06
Chromium VI	18540-29-9	Ash Analysis	5.78E-08	1.54E-07	N/A	N/A	5.78E-08	1.54E-07
Cobalt	7440-48-4	Ash Analysis	2.1E-07	5.61E-07	N/A	N/A	2.10E-07	5.61E-07
Manganese	7439-96-5	Ash Analysis	9.28E-07	2.47E-06	N/A	N/A	9.28E-07	2.47E-06
Mercury	7439-97-6	Ash Analysis	2.78E-09	7.4E-09	N/A	N/A	2.78E-09	7.40E-09
Nickel	7440-02-0	Ash Analysis	5.26E-07	1.4E-06	N/A	N/A	5.26E-07	1.40E-06
Selenium	7782-49-2	Ash Analysis	1.42E-07	3.79E-07	N/A	N/A	1.42E-07	3.79E-07
		NT EMISSIONS						
		SOURCE OF	EXPECTE	DACTUAL	EMISSIONS	S AFTER C	ONTROLS /	LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	EMISSION FACTOR	lb	/hr	lb/c	day		lb/yr
Arsenic	7440-38-2	Ash Analysis	4.33E-07			E-05		31E-03
Beryllium	7440-41-7	Ash Analysis				E-06		78E-04
Cadmium	7440-43-9	Ash Analysis	7.73E-08			E-06		12E-04
Chromium VI	18540-29-9	Ash Analysis	5.78E-08			E-06		08E-04
Manganese	7439-96-5	Ash Analysis				E-05		95E-03
Mercury	7439-97-6	Ash Analysis				E-08		18E-05
Nickel	7440-02-0	Ash Analysis				E-05		30E-03

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

WPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

REVISED 09/22/16	NCDEQ/Divisi	ion of Air Quality - Ap	oplication	for Air Permit to Co	onstruct/Operate	<b>B6</b>
EMISSION SOURCE DESCRIPT	ION: Loadout Silo			EMISSION S	OURCE ID NO: ES-81	
				CONTROL D	EVICE ID NO(S): CD-81	
OPERATING SCENARIO:	1	OF1		EMISSION P	OINT(STACK) ID NO(S): EP-81	
DESCRIBE IN DETAIL THE PRC Loadout silo is unloaded at the ra			oduct cap	ture device.		
MATERIAL STORED: Fly Ash CAPACITY	CUBIC FEET: N/A			DENSITY OF MATER TONS: N/A	RIAL (LB/F13): N/A	
	HEIGHT: 111	DIAMETER: 41	(OR)	LENGTH:	WIDTH: HEIGHT:	
ANNUAL PRODUCT THRO		ACTUAL: 400,000	(- )		ESIGN CAPACITY: 400,000	
PNEUMATICALLY FIL		MECHANIC	CALLY FI		FILLED FROM	
BLOWER		SCREW CONVEYOR	2			
COMPRESSOR	_	BELT CONVEYOR				
OTHER:		BUCKET ELEVATOR	1		STORAGE PILE	
		OTHER:			OTHER:	
NO. FILL TUBES: N/A						
MAXIMUM ACFM: 6000						
MATERIAL IS UNLOADED TO:						
Trucks						
BY WHAT METHOD IS MATERI	AL UNLOADED FROM	I SILO?				
MAXIMUM DESIGN FILLING RA	TE OF MATERIAL (TO	ons/hr): N/A				
MAXIMUM DESIGN UNLOADING	3 RATE OF MATERIA	L (TONS/HR): 75				
COMMENTS: This silo only unloads.						

REVISED 09/22/16	NCDEQ/Division of Air	Quality - Application	on for	Air Permit to Construct	/Operate				C1
CONTROL DEVICE ID NO: CD-81	CONTROLS EMISSI	ONS FROM WHICH	EMISS	SION SOURCE ID NO(S)	): ES-81				
EMISSION POINT (STACK) ID NO(S): EP-81	POSITION IN SERIE	S OF CONTROLS			NC	. 1	OF 1	UNITS	
OPERATING SCENARIO:									
10F1		P.E. SEAL REQUIR	ED (P	ER 2a .0112)?	1	YES		□ NO	
DESCRIBE CONTROL SYSTEM: A bin vent for particulate			(	1 - 7		-			
POLLUTANTS COLLECTED:		PM		PM10/PM2.5		_			
BEFORE CONTROL EMISSION RATE (LB/HR):		0.0037		0.0017		_			
		- 0.00E gr/doof	0/	- 0.00E gr/doof	0/	0/		%	
CAPTURE EFFICIENCY:		<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	70	%		70	
CONTROL DEVICE EFFICIENCY:		N/A	%	N/A	%	%		%	
				· · · · · · · · · · · · · · · · · · ·		_		•	
CORRESPONDING OVERALL EFFICIENCY:		N/A	%	N/A	%	%		%	
						_			
EFFICIENCY DETERMINATION CODE:		2		2		_			
TOTAL AFTER CONTROL EMISSION RATE (LB/HR):		0.0037		0.0017		_			
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: Avg: 10-15 wg	GAUGE?	YES		NO					
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25	_	INLET TEMPERATU	JRE (°	F): Contract	MIN	MAX			
POLLUTANT LOADING RATE: N/A	□ GR/FT <sup>3</sup>	OUTLET TEMPERA			MIN	MAX			
INLET AIR FLOW RATE (ACFM): 1300		FILTER OPERATIN	G TEN	IP (°F): Contract					
	PER COMPARTMENT:	-			LENGTH OF BAG				
	ACE AREA PER CART				DIAMETER OF BA	G (IN.):	5-15		
TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ):	AIR TO CLOTH RAT	O: 1 to 4 : 1							
DRAFT TYPE: INDUCED/NEGATIVE	FORCED/POSITIVE			FILTER MATERIAL: C				FELTED	_
DESCRIBE CLEANING PROCEDURES:					PAF	TICLE	SIZE DISTRIB	UTION	
AIR PULSE	SONIC				SIZE	N	/EIGHT %	CUMULA	ATIVE
REVERSE FLOW	SIMPLE BAG COLLA	PSE			(MICRONS)	C	OF TOTAL	%	
□ MECHANICAL/SHAKER □	RING BAG COLLAPS	SE			0-1				
OTHER:					1-10				
DESCRIBE INCOMING AIR STREAM: Air stream will contain	n fly ash.				10-25				
					25-50				
					50-100				
					>100				
								L = 100	
							sina 325 mesh		
					Supplier specific, 9	4% pas			
					Supplier specific, 9	4% pas			
					Supplier specific, 9	4% pas			
					Supplier specific, 9	4% pas:			
ON A SEPARATE PAGE, ATTACH A DIAGRAM SHOWING	THE RELATIONSHIP	DF THE CONTROL I	DEVIC	E TO ITS EMISSION SO		4% pas			
ON A SEPARATE PAGE, ATTACH A DIAGRAM SHOWING COMMENTS:	THE RELATIONSHIP (	OF THE CONTROL L	DEVIC	E TO ITS EMISSION SO		4% pas			
	THE RELATIONSHIP	DF THE CONTROL I	DEVIC	e to its emission so		4% pas			
	THE RELATIONSHIP	DF THE CONTROL I	DEVIC	e to its emission so		4% pas:			
	B THE RELATIONSHIP (	DF THE CONTROL I	DEVIC	e to its emission so		4% pas			
	B THE RELATIONSHIP (	DF THE CONTROL I	DEVIC	e to its emission so		4% pas:			
	THE RELATIONSHIP	OF THE CONTROL L	DEVIC	E TO ITS EMISSION SO		4% pas			
	THE RELATIONSHIP	OF THE CONTROL I	DEVIC	E TO ITS EMISSION SO		4% pas			
	THE RELATIONSHIP	OF THE CONTROL I	DEVIC	E TO ITS EMISSION SO		4% pas:			
	THE RELATIONSHIP	OF THE CONTROL I	DEVIC	E TO ITS EMISSION SO		4% pas			

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of A	Air Quality - Applica	ation for Ai	r Permit to	Construct/	Operate		В
EMISSION SOURCE DESCRIPTION:	Loadout Silo Ch	ute 1A	· · · · ·	EMISSION	SOURCE I	D NO: ES-8	31A	
			ŀ	CONTROL	DEVICE ID	0 NO(S): CD	)-81A	
OPERATING SCENARIO1	OF _	1				( )	D(S): EP-81	A
DESCRIBE IN DETAILTHE EMISSION Loadout silo chute 1A is unloaded at the		-		-	oture device	۰. 		
TYPE OF EMISSION SOUR	CE (CHECK A	ND COMPLETE AP	PROPRIAT	E FORM B				•
Coal,wood,oil, gas, other burner (Fo	orm B1)	U Woodworking	(Form B4)		🗆 Manı	uf. of chemi	cals/coating	js/inks (Form B
<ul> <li>Int.combustion engine/generator (F</li> <li>Liquid storage tanks (Form B3)</li> </ul>	,	Coating/finishin	<b>0</b> . <b>0</b> .	. ,		eration (For er (Form B9)	,	
START CONSTRUCTION DATE: TBD	-		DATE MAN	NUFACTUR	ED: TBD			
MANUFACTURER / MODEL NO.: TBD			EXPECTE	D OP. SCHE	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
	ISPS (SUBPART	TS?):	L=		SHAP (SUB			
PERCENTAGE ANNUAL THROUGHPU		,	R-MAY 25		JN-AUG	25	SEP-NOV	/ 25
		ANT EMISSION					CE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
	ļ			ROLS / LIMITS)	BEFORE CONT			ITROLS / LIMITS)
AIR POLLUTANT EMITTED	ļ	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Manufacturer			N/A	N/A	0.00487	0.00487
ARTICULATE MATTER<10 MICRONS (PM <sub>10</sub> )		Manufacturer			N/A	N/A	0.0023	0.0023
PARTICULATE MATTER<2.5 MICRONS	100	Manufacturer			N/A	N/A	0.0023	0.0023
SULFUR DIOXIDE (SO2)	(* 2.0,		N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)	i	ł	N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)	;	ł	N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (	VOC)	ł	N/A	N/A	N/A	N/A	N/A	N/A
LEAD	100,	Ash Analysis			N/A	N/A	6.18E-07	6.18E-07
OTHER	;		N/A		N/A	N/A	0.102 07 N/A	0.10E 0/
	AIR POLLU	TANT EMISSIO	-			-		
	T 1	SOURCE OF		D ACTUAL			L EMISSIO	NS
	/	EMISSION		ROLS / LIMITS)	EFORE CONT			ITROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis	5.77E-07		N/A	N/A		5.77E-07
Beryllium	7440-41-7	Ash Analysis			N/A	N/A		1.20E-07
Cadmium	7440-43-9	Ash Analysis			N/A	N/A		1.03E-07
Chromium	7440-47-3				N/A	N/A		7.01E-07
Chromium VI	18540-29-9	Ash Analysis			N/A	N/A	7.71E-08	7.71E-08
Cobalt	7440-48-4	Ash Analysis			N/A	N/A	2.80E-07	2.80E-07
Manganese	7439-96-5	Ash Analysis	1.24E-06	1.24E-06	N/A	N/A	1.24E-06	1.24E-06
Mercury	7439-97-6				N/A	N/A	3.70E-09	3.70E-09
Nickel	7440-02-0	Ash Analysis	7.01E-07	7.01E-07	N/A	N/A	7.01E-07	7.01E-07
Selenium	7782-49-2	Ash Analysis			N/A	N/A	1.90E-07	1.90E-07
		T EMISSIONS		ATION F	OR THIS	SOURC		
		SOURCE OF EMISSION	EXPECTE	D ACTUAL	EMISSIONS	S AFTER C	ONTROLS /	LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb	/hr	lb/o	day	ļ	lb/yr
Arsenic	7440-38-2	Ash Analysis	5.77E-07			E-05		5E-03
Beryllium	7440-41-7	Ash Analysis			2.87	'E-06		39E-04
Cadmium	7440-43-9	Ash Analysis				'E-06		)6E-04
	18540-29-9	Ash Analysis				E-06		54E-04
Chromium VI		· · · ·						17E-03
	7439-96-5	Ash Analysis	1.24E-06	1.24E-06 2.97E-05 2				
Manganese	7439-96-5 7439-97-6	Ash Analysis Ash Analysis				E-08		10E-06
			3.70E-09		8.88		7.4	

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): Laadout silo chute 1A is unloaded at the rate of 100 ton/hr and equipped with bin vent product capture device.         MATERIAL STORED: Fly Ash CAPACITY       DENSITY OF MATERIAL (LB/FT3): N/A         CAPACITY       CUBIC FEET: N/A         DIMENSIONS (FEET)       HEIGHT: 111         DIMENSIONS (FEET)       HEIGHT: 111         DIMENSIONS (FEET)       HEIGHT: 111         DIMENSIONS (FEET)       HEIGHT: 200,000         MAXIMUM DESIGN CAPACITY       CUBIC FEET: N/A         OMENSIONS (FEET)       HEIGHT: 111         DIMENSIONS (FEET)       HEIGHT: 111         DIMENSIONS (FEET)       HEIGHT: 200,000         MAXIMUM LENDOUCT THROUGHPUT (TONS)       ACTUAL: 200,000         PNEUMATICALLY FILLED       FILLED FROM         BLOWER       SCREW CONVEYOR       RAILCAR         COMPRESSOR       BELT CONVEYOR       RAILCAR         BLOWER       BUCKET ELEVATOR       STORAGE PILE         OTHER:       BUCKET ELEVATOR       STORAGE PILE         NO. FILL TUBES: N/A       MAXIMUM ACFM: 6000         MATERIAL IS UNLOADED TO:       MAX         NA       MAXERIAL SUNLOADED TO:         NA       MAXERIAL UNLOADED FROM SILO?         N/A       MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A	REVISED 09/22/16	NCDEQ/Divis	ion of Air Quality -	· Applicatior	n for Air Permit to Co	onstruct/Operate		B6
OPERATING SCENARIO:	EMISSION SOURCE DESCRIPT	FION: Loadout Silo Ch	ute 1A		EMISSION S	OURCE ID NO: ES-8	1A	
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): Loadout silo chute 1A is unloaded at the rate of 100 ton/hr and equipped with bin vent product capture device. MATERIAL STORED: Fly Ash CAPACITY CUBIC FEET: NA TONS: N/A DIMENSIONS (FEET) HEIGHT: 111 DIAMETER: 41 (07) LENGTH: WIDTH: HEIGHT: ANNUAL PRODUCT THROUGHPUT (TONS) ACTUAL: 200,000 MAXIMUM DESIGN CAPACITY: 200,000 PNEUMATICALLY FILLED SCREW CONVEYOR RAILCAR BLOWER BLOWER BELT CONVEYOR RAILCAR 0 OTHER: BLOWEYOR STRUCK 0 OTHER: STRUCK 0 OTHER 0					CONTROL DI	EVICE ID NO(S): CD-	-81A	
MATERIAL STORED: Fly Ash       DENSITY OF MATERIAL (LB/FT3): N/A         CAPACITY       CUBIC FEET: N/A       TONS: N/A         DIMENSIONS (FEET)       HEIGHT: 111       DIAMETER: 41       (OR)       LENGTH:       WIDTH:       HEIGHT:         ANNUAL PRODUCT THROUGHPUT (TONS)       ACTUAL: 20,000       MAXIMUM DESIGN CAPACITY: 200,000       MAXIMUM DESIGN CAPACITY: 200,000         PNEUMATICALLY FILLED       MECHANICALLY FILLED       FILLED FROM         BLOWER       SCREW CONVEYOR       RAILCAR         OTHER:       BLIC CONVEYOR       TRUCK         NO. FILL TUBES: N/A       BLIC CONVEYOR       OTHER:         NO. FILL TUBES: N/A       MAXIMUM ACFM: 6000         MATERIAL IS UNLOADED TO:       NA         N/A       BUY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?         N/A       SMATERIAL UNLOADED FROM SILO?         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A         MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100       COMMENTS:	OPERATING SCENARIO:	1	OF^	1	EMISSION P	OINT(STACK) ID NO	(S): EP-81A	
CAPACITY         CUBIC FEET: N/A         TONS: N/A           DIMENSIONS (FEET)         HEIGHT: 111         DIAMETER: 411         (0R)         LENGTH:         WIDTH:         HEIGHT:           ANNUAL PRODUCT THROUGHPUT (TONS)         ACTUAL: 200,000         MAXIMUM DESIGN CAPACITY: 200,000           PNEUMATICALLY FILLED         MECHANICALLY FILLED         MAXIMUM DESIGN CAPACITY: 200,000           PNEUMATICALLY FILLED         MECHANICALLY FILLED         MAXIMUM DESIGN CAPACITY: 200,000           ONDERSSOR         BELT CONVEYOR         Indicating Rate of MATERIAL (TONS/HR): N/A           MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A         Indicating Rate of MATERIAL (TONS/HR): 100				<i>i</i> ith bin vent p	product capture device	Э.		
CAPACITY         CUBIC FEET: N/A         TONS: N/A           DIMENSIONS (FEET)         HEIGHT: 111         DIAMETER: 411         (0R)         LENGTH:         WIDTH:         HEIGHT:           ANNUAL PRODUCT THROUGHPUT (TONS)         ACTUAL: 200,000         MAXIMUM DESIGN CAPACITY: 200,000           PNEUMATICALLY FILLED         MECHANICALLY FILLED         MAXIMUM DESIGN CAPACITY: 200,000           PNEUMATICALLY FILLED         MECHANICALLY FILLED         MAXIMUM DESIGN CAPACITY: 200,000           OMECHANICALLY FILLED         MECHANICALLY FILLED         FILLED FROM           BLOWER         SCREW CONVEYOR         RAILCAR           COMPRESSOR         BELT CONVEYOR         TRUCK           OTHER:         BUCKET ELEVATOR         STORAGE PILE           OTHER:         OTHER:         OTHER:         OTHER:           NO. FILL TUBES: N/A         BUCKAT ELEVATOR         STORAGE PILE           MAXIMUM ACFM: 6000         OTHER:         OTHER:         OTHER:           N/A         MAXIMUM DESIGN SINCORNAL UNLOADED TO:         MAXIMUM DESIGN SINCORNAL UNLOADED FROM SILO?           N/A         MAXIMUM DESIGN VILOADING RATE OF MATERIAL (TONS/HR): N/A         MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100           MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100         COMMENTS:         MAXIMUM DESIGN UNLOADING RATE O	MATERIAL STORED: Fly Ash				DENSITY OF MATE	RIAL (LB/FT3): N/A		
ANNUAL PRODUCT THROUGHPUT (TONS)       ACTUAL: 200,000       MAXIMUM DESIGN CAPACITY: 200,000         PNEUMATICALLY FILLED       MECHANICALLY FILLED       FILLED FROM         BLOWER       SCREW CONVEYOR       RAILCAR         COMPRESSOR       BELT CONVEYOR       TRUCK         OTHER:       BUCKET ELEVATOR       STORAGE PILE         NO. FILL TUBES: N/A       OTHER:       OTHER:         MAXIMUM ACFM: 6000       OTHER:       OTHER:         NO. FILL TUBES: N/A       NAXIMUM ACFM: 6000         MAXIMUM ACFM: 6000       MAXIMUM ACFM: 6000         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A         MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100         COMMENTS:       COMMENTS:		CUBIC FEET: N/A						
PNEUMATICALLY FILLED       MECHANICALLY FILLED       FILLED FROM         BLOWER       SCREW CONVEYOR       RAILCAR         COMPRESSOR       BELT CONVEYOR       TRUCK         OTHER:       BUCKET ELEVATOR       STORAGE PILE         NO. FILL TUBES: N/A       OTHER:       OTHER:         MAXIMUM ACFM: 6000       OTHER:       OTHER:         NA       STORAGE DILE       STORAGE PILE         BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?       N/A         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A       MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100         COMMENTS:       SCOMMENTS:       STORAGE PILE	DIMENSIONS (FEET)	HEIGHT: 111	DIAMETER: 41	(OR)	LENGTH:	WIDTH:	HEIGHT:	
BLOWER       SCREW CONVEYOR       RAILCAR         COMPRESSOR       BELT CONVEYOR       TRUCK         OTHER:       BUCKET ELEVATOR       STORAGE PILE         OTHER:       OTHER:       OTHER:         NO. FILL TUBES: N/A       OTHER:       OTHER:         MAXIMUM ACFM: 6000       MATERIAL IS UNLOADED TO:       N/A         BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?       N/A         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A       MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100         COMMENTS:       COMMENTS:       COMMENTS:		UGHPUT (TONS)	ACTUAL: 200,000	<u>с</u>	MAXIMUM DI	ESIGN CAPACITY: 2	200,000	
COMPRESSOR       BELT CONVEYOR       TRUCK         OTHER:       BUCKET ELEVATOR       STORAGE PILE         OTHER:       OTHER:       OTHER:         NO. FILL TUBES: N/A       MAXIMUM ACFM: 6000       OTHER:         MATERIAL IS UNLOADED TO:       MATERIAL IS UNLOADED TO:       Image: Comparison of the comparis	PNEUMATICALLY FIL	LED	MECHA	NICALLY FI	LLED		FILLED FROM	
OTHER:       BUCKET ELEVATOR       STORAGE PILE         OTHER:       OTHER:       OTHER:         NO. FILL TUBES: N/A       MAXIMUM ACFM: 6000       OTHER:         MAXIMUM ACFM: 6000       MATERIAL IS UNLOADED TO:       N/A         N/A       BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?       N/A         MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A       MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): 100         COMMENTS:       E       E	BLOWER		SCREW CONVEY	′OR		□ RAILCAR		
NO. FILL TUBES: N/A   MAXIMUM ACFM: 6000   MATERIAL IS UNLOADED TO:   N/A   BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO?   N/A   MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100 COMMENTS:			BELT CONVEYOF	२				
NO. FILL TUBES: N/A MAXIMUM ACFM: 6000 MATERIAL IS UNLOADED TO: N/A BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100 COMMENTS:	OTHER:		BUCKET ELEVAT	OR			E PILE	
MAXIMUM ACFM: 6000 MATERIAL IS UNLOADED TO: N/A BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100 COMMENTS:			OTHER:			OTHER:		
MATERIAL IS UNLOADED TO: N/A BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100 COMMENTS:	NO. FILL TUBES: N/A							
N/A BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100 COMMENTS:	MAXIMUM ACFM: 6000							
BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO? N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100 COMMENTS:	MATERIAL IS UNLOADED TO:							
N/A MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/HR): N/A MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100 COMMENTS:	N/A							
MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TONS/HR): 100 COMMENTS:	N/A							
COMMENTS:	MAXIMUM DESIGN FILLING RA	TE OF MATERIAL (TO	ONS/HR): N/A					
	MAXIMUM DESIGN UNLOADIN	G RATE OF MATERIA	L (TONS/HR): 100					

REVISED 09/22/16		NCDEQ/Division of Air	Quality - Applicatio	on for A	Air Permit to Construct	/Operate				C1
CONTROL DEVICE ID NO: CD-81A		CONTROLS EMISSI	ONS FROM WHICH	EMISS	SION SOURCE ID NO(S	): ES-81A				
EMISSION POINT (STACK) ID NO(S):	EP-81A	POSITION IN SERIE	S OF CONTROLS				NO.	1 OF	1 UNITS	
OPERATING SC	ENARIO:									
1OF	1		P.E. SEAL REQUIR	ED (PE	ER 2g .0112)?		$\checkmark$	YES	🗆 NO	
DESCRIBE CONTROL SYSTEM: A bin vent		control on the Loadout			. ,		_		_	
POLLUTANTS COLLECTED:			PM		PM10/PM2.5					
BEFORE CONTROL EMISSION RATE (LB/H	R):		0.005		0.002					
CAPTURE EFFICIENCY:			<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%		%	%	
CONTROL DEVICE EFFICIENCY:			N/A	%	N/A	%		%	%	
CORRESPONDING OVERALL EFFICIENCY:			N/A	%	N/A	%		%	%	
EFFICIENCY DETERMINATION CODE:			2		2					
TOTAL AFTER CONTROL EMISSION RATE	(LB/HR):		0.005		0.002					
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX: A	Avg: 10-15 wg	GAUGE?	YES		] NO					
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25			INLET TEMPERATU	JRE (°F	F): Contract	MIN		MAX		
POLLUTANT LOADING RATE: N/A	LB/HR	□ GR/FT <sup>3</sup>	OUTLET TEMPERA	TURE	(°F) Contract	MIN		MAX		
INLET AIR FLOW RATE (ACFM): 1300			FILTER OPERATIN	G TEM	P (°F): Contract					
NO. OF COMPARTMENTS: 1	NO. OF BAGS	PER COMPARTMENT:	Contract			LENGTH O	of BAG (I	N.): 20-30		
NO. OF CARTRIDGES:	FILTER SURF	ACE AREA PER CARTI	RIDGE (FT <sup>2</sup> ):			DIAMETER	R OF BAG	(IN.): 5-15		
TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ):		AIR TO CLOTH RAT	IO: 1 to 4 : 1							
DRAFT TYPE: 🗹 INDUCED/NEGAT	TIVE 🗹	FORCED/POSITIVE			FILTER MATERIAL: C	artridge Styl	le 🗌	WOVEN	FELTED	)
DESCRIBE CLEANING PROCEDURES:							PART	ICLE SIZE DIS	TRIBUTION	
AIR PULSE		SONIC				SIZ	E	WEIGHT	6 CUN	IULATIVE
REVERSE FLOW		SIMPLE BAG COLLA	APSE			(MICRO	ONS)	OF TOTA	L	%
MECHANICAL/SHAKER		RING BAG COLLAPS	SE			0-1	I			
OTHER:						1-1	0			
DESCRIBE INCOMING AIR STREAM: Air stre	eam will conta	in fly ash.				10-2	25			
						25-5	50			
						50-1	00			
						>10	0			
								-	TOTAL = 100	
						Supplier sp	ecific, 949	% passing 325	mesh	
ON A SEPARATE PAGE, ATTACH A DIAGRA	AM SHOWING	G THE RELATIONSHIP		DEVICE	E TO ITS EMISSION SO	URCE(S):				
COMMENTS:										

#### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCD	EQ/Division of	Air Quality - Applicat	ion for Air	Permit to C	onstruct/O	perate		В
EMISSION SOURCE DESCRIPTION:	Loadout Silo Ch	ute 1B		EMISSION	SOURCE I	D NO: ES-8	1B	
				CONTROL				
OPERATING SCENARIO1	OF	1		EMISSION		. ,		В
DESCRIBE IN DETAILTHE EMISSION Loadout silo chute 1B is unloaded at the		•			re device.			
TYPE OF EMISSION SOU	•			FORM B1	_			
Coal,wood,oil, gas, other burner (Fo		Woodworking (F	,					s/inks (Form B
Int.combustion engine/generator (F	,	Coating/finishing		,		eration (For		
Liquid storage tanks (Form B3)		Storage silos/bin	. ,			r (Form B9)		
START CONSTRUCTION DATE: TBD				IUFACTUR				
MANUFACTURER / MODEL NO.: TBD			EXPECTE	D OP. SCHE			DAY/WK 5	2 WK/YR
	SPS (SUBPART	,			HAP (SUB	,		
PERCENTAGE ANNUAL THROUGHP	. ,						SEP-NOV	25
	NR POLLUT	ANT EMISSIONS			-OR THIS			
		SOURCE OF		D ACTUAL			L EMISSIO	
		EMISSION		ROLS / LIMITS)				ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Manufacturer	0.00487	0.00487	N/A	N/A	0.00487	0.00487
PARTICULATE MATTER<10 MICRONS	107	Manufacturer	0.0023	0.0023	N/A	N/A	0.0023	0.0023
PARTICULATE MATTER<2.5 MICRONS	(PM <sub>2.5</sub> )	Manufacturer	0.0023	0.0023	N/A	N/A	0.0023	0.0023
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
			N/A	N/A	N/A	N/A	N/A	N/A
	(00)		N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (	/OC)		N/A	N/A	N/A	N/A	N/A	N/A
LEAD		Ash Analysis	6.18E-07	6.18E-07	N/A	N/A	6.18E-07	6.18E-07
OTHER		ITANT EMISSIOI	N/A		N/A	N/A	N/A	N/A
NAZARDO05								10
		SOURCE OF						
HAZARDOUS AIR POLLUTANT	CAS NO.	EMISSION FACTOR		ROLS / LIMITS)			Ib/hr	ITROLS / LIMITS)
	7440-38-2		lb/hr 5.77E-07	tons/yr 5.77E-07	lb/hr N/A	tons/yr N/A	5.77E-07	tons/yr 5.77E-07
Arsenic Beryllium	7440-38-2	Ash Analysis Ash Analysis	1.2E-07	1.2E-07	N/A	N/A	1.20E-07	1.20E-07
Cadmium	7440-41-7	Ash Analysis	1.03E-07		N/A	N/A	1.03E-07	1.03E-07
				1.00L-07		N/A		7.01E-07
			7 01E-07	7 01E-07	NI/A			
Chromium Chromium VI	7440-47-3	Ash Analysis			N/A		7.01E-07	
Chromium VI	18540-29-9	Ash Analysis	7.71E-08	7.71E-08	N/A	N/A	7.71E-08	7.71E-08
Chromium VI Cobalt	18540-29-9 7440-48-4	Ash Analysis Ash Analysis	7.71E-08 2.8E-07	7.71E-08 2.8E-07	N/A N/A	N/A N/A	7.71E-08 2.80E-07	7.71E-08 2.80E-07
Chromium VI Cobalt Manganese	18540-29-9 7440-48-4 7439-96-5	Ash Analysis Ash Analysis Ash Analysis	7.71E-08 2.8E-07 1.24E-06	7.71E-08 2.8E-07 1.24E-06	N/A N/A N/A	N/A N/A N/A	7.71E-08 2.80E-07 1.24E-06	7.71E-08 2.80E-07 1.24E-06
Chromium VI Cobalt Manganese Mercury	18540-29-9           7440-48-4           7439-96-5           7439-97-6	Ash Analysis Ash Analysis Ash Analysis Ash Analysis	7.71E-08 2.8E-07 1.24E-06 3.7E-09	7.71E-08 2.8E-07 1.24E-06 3.7E-09	N/A N/A N/A N/A	N/A N/A N/A N/A	7.71E-08 2.80E-07 1.24E-06 3.70E-09	7.71E-08 2.80E-07 1.24E-06 3.70E-09
Chromium VI Cobalt Manganese Mercury Nickel	18540-29-9           7440-48-4           7439-96-5           7439-97-6           7440-02-0	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07	N/A N/A N/A N/A	N/A N/A N/A N/A	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07
Chromium VI Cobalt Manganese Mercury Nickel Selenium	18540-29-9           7440-48-4           7439-96-5           7439-97-6           7440-02-0           7782-49-2	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07	N/A N/A N/A N/A N/A	N/A N/A N/A N/A N/A N/A	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07
Chromium VI Cobalt Manganese Mercury Nickel Selenium	18540-29-9           7440-48-4           7439-96-5           7439-97-6           7440-02-0           7782-49-2	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORMA</b>	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b>	N/A N/A N/A N/A N/A <b>DR THIS :</b>	N/A N/A N/A N/A N/A SOURCE	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07
Chromium VI Cobalt Manganese Mercury Nickel Selenium	18540-29-9           7440-48-4           7439-96-5           7439-97-6           7440-02-0           7782-49-2	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF EMISSION	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORMA</b> EXPECTEI	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b>	N/A N/A N/A N/A N/A DR THIS EMISSIONS	N/A N/A N/A N/A N/A SOURCE	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 / LIMITATIONS
Chromium VI Cobalt Manganese Mercury Nickel Selenium <b>TOXIC AIF</b>	18540-29-9 7440-48-4 7439-96-5 7439-97-6 7440-02-0 7782-49-2 <b>POLLUTAI</b>	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF EMISSION FACTOR	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORMA</b> EXPECTEI	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b> D ACTUAL	N/A N/A N/A N/A N/A DR THIS EMISSIONS	N/A N/A N/A N/A N/A SOURCE & AFTER C	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 4 LIMITATIONS
Chromium VI Cobalt Manganese Mercury Nickel Selenium <b>TOXIC AIR</b> <b>TOXIC AIR POLLUTANT</b>	18540-29-9         7440-48-4         7439-96-5         7439-97-6         7440-02-0         7782-49-2         POLLUTAI         CAS NO.	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF EMISSION FACTOR Ash Analysis	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORMA</b> EXPECTEI Ib/ 5.77E-07	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b> D ACTUAL	N/A N/A N/A N/A N/A DR THIS 3 EMISSIONS EMISSIONS	N/A N/A N/A N/A N/A SOURCE S AFTER C lay E-05	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 ONTROLS /	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 7 LIMITATIONS b/yr 5E-03
Chromium VI Cobalt Manganese Mercury Nickel Selenium <b>TOXIC AIR</b> TOXIC AIR POLLUTANT Arsenic	18540-29-9         7440-48-4         7439-96-5         7439-97-6         7440-02-0         7782-49-2         POLLUTAI         CAS NO.         7440-38-2	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF EMISSION FACTOR	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORMA</b> EXPECTEI Ib, 5.77E-07 1.20E-07	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b> D ACTUAL	N/A N/A N/A N/A N/A DR THIS EMISSIONS	N/A N/A N/A N/A N/A SOURCE S AFTER C day E-05 E-06	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 ONTROLS / 1.1 2.3	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 4 LIMITATIONS
Chromium VI Cobalt Manganese Mercury Nickel Selenium <b>TOXIC AIR POLLUTANT</b> Arsenic Beryllium	18540-29-9         7440-48-4         7439-96-5         7439-97-6         7440-02-0         7782-49-2         POLLUTAI         CAS NO.         7440-38-2         7440-41-7	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF EMISSION FACTOR Ash Analysis Ash Analysis	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORMA</b> EXPECTEI Ib/ 5.77E-07 1.20E-07 1.03E-07	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b> D ACTUAL	N/A N/A N/A N/A N/A N/A N/A EMISSIONS Ib/c 1.39 2.87 2.47	N/A N/A N/A N/A N/A SOURCE S AFTER C day E-05 E-06	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 ONTROLS / 1.1 2.3 2.0	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 4 LIMITATIONS 7 LIMITATIONS 7 SE-03 39E-04
Chromium VI Cobalt Manganese Mercury Nickel Selenium <b>TOXIC AIR POLLUTANT</b> Arsenic Beryllium Cadmium Chromium VI	18540-29-9         7440-48-4         7439-96-5         7439-97-6         7440-02-0         7782-49-2         POLLUTAI         CAS NO.         7440-38-2         7440-41-7         7440-43-9	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF EMISSION FACTOR Ash Analysis Ash Analysis Ash Analysis	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORMA</b> EXPECTEI Ib/ 5.77E-07 1.20E-07 1.20E-07 7.71E-08	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b> D ACTUAL	N/A N/A N/A N/A N/A N/A N/A EMISSIONS Ib/c 1.39 2.87 2.47	N/A N/A N/A N/A N/A SOURCE S AFTER C day E-05 E-06 E-06 E-06	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 ONTROLS / 1.1 2.3 2.0 1.5	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 / LIMITATIONS // LIMITATIONS // LIMITATIONS // LIMITATIONS // LIMITATIONS // LIMITATIONS
Chromium VI Cobalt Manganese Mercury Nickel Selenium <b>TOXIC AIR POLLUTANT</b> Arsenic Beryllium Cadmium	18540-29-9         7440-48-4         7439-96-5         7439-97-6         7440-02-0         7782-49-2 <b>POLLUTAI</b> CAS NO.         7440-38-2         7440-43-9         18540-29-9	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF EMISSION FACTOR Ash Analysis Ash Analysis Ash Analysis	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORMA</b> EXPECTEI Ib/ 5.77E-07 1.20E-07 1.03E-07 7.71E-08 1.24E-06	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b> D ACTUAL	N/A N/A N/A N/A N/A N/A N/A CR THIS S EMISSIONS EMISSIONS EMISSIONS 2.87 2.47 1.85	N/A N/A N/A N/A N/A SOURCE S AFTER C Jay E-05 E-06 E-06 E-06 E-06 E-06 E-05	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 0NTROLS / 0NTROLS / 1.1 2.3 2.0 1.5 2.4	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 / LIMITATIONS // LIMITATIONS
Chromium VI Cobalt Manganese Mercury Nickel Selenium <b>TOXIC AIR POLLUTANT</b> Arsenic Beryllium Cadmium Chromium VI Manganese	18540-29-9         7440-48-4         7439-96-5         7439-97-6         7440-02-0         7782-49-2 <b>POLLUTAI</b> CAS NO.         7440-38-2         7440-43-9         18540-29-9         7439-96-5	Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis Ash Analysis <b>NT EMISSIONS I</b> SOURCE OF EMISSION FACTOR Ash Analysis Ash Analysis Ash Analysis Ash Analysis	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>NFORM/</b> EXPECTEI Ib, 5.77E-07 1.20E-07 1.20E-07 1.03E-07 7.71E-08 1.24E-06 3.70E-09	7.71E-08 2.8E-07 1.24E-06 3.7E-09 7.01E-07 1.9E-07 <b>ATION FC</b> D ACTUAL	N/A N/A N/A N/A N/A DR THIS S EMISSIONS Ib/c 1.39 2.87 2.47 1.85 2.97	N/A N/A N/A N/A N/A SOURCE & AFTER C day E-05 E-06 E-06 E-06 E-06 E-06 E-06 E-06 E-06	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 ONTROLS / 0NTROLS / 1.1 2.3 2.0 1.5 2.4 7.4	7.71E-08 2.80E-07 1.24E-06 3.70E-09 7.01E-07 1.90E-07 7 1.90E-07 7 1.90E-07 8 9 5 E-03 8 9 E-04 9 6 E-04 9 6 E-04 9 7 E-03

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

MPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOUF

EMISSION SOURCE DESCRIPTION: Loadout Silo Chute 1E	В		EMISSION SOL		_	
			LIVIIO0ION 000	JRCE ID NO. ES-	81B	
			CONTROL DEV	/ICE ID NO(S): CI	D-81B	
OPERATING SCENARIO:1	OF1		EMISSION POIL	NT(STACK) ID NO	D(S): EP-81B	
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DI Loadout silo chute 1B is unloaded at the rate of 100 ton/hr at		n vent p	roduct capture device.			
MATERIAL STORED: Fly Ash			DENSITY OF MATERIA	AL (LB/FT3): N/A		
CAPACITY CUBIC FEET: N/A			TONS: N/A	(,		
	METER: 41			WIDTH:	HEIGHT:	
	TUAL: 200,000			SIGN CAPACITY:	200,000	
PNEUMATICALLY FILLED	MECHANICA	LLY FI			FILLED FROM	
□ BLOWER □ SCR	REW CONVEYOR			RAILCAF	2	
COMPRESSOR	BELT CONVEYOR			□ TRUCK		
OTHER: BUC	BUCKET ELEVATOR				E PILE	
П отн	HER:			OTHER:		
NO. FILL TUBES: N/A						
MAXIMUM ACFM: 6000						
MATERIAL IS UNLOADED TO:						
N/A						
BY WHAT METHOD IS MATERIAL UNLOADED FROM SILO						
MAXIMUM DESIGN FILLING RATE OF MATERIAL (TONS/H	HR): N/A					
MAXIMUM DESIGN UNLOADING RATE OF MATERIAL (TO	ONS/HR): 100					
COMMENTS: This silo only unloads.						

REVISED 09/22/16		NCDEQ/Division of Air	Quality - Applicatio	on for A	Air Permit to Construct	t/Operate			C1
CONTROL DEVICE ID NO: CD-81B		CONTROLS EMISSI	ONS FROM WHICH	EMISS	SION SOURCE ID NO(S	): ES-81B			
EMISSION POINT (STACK) ID NO(S):	EP-81B	POSITION IN SERIE	S OF CONTROLS			١	IO. ·	1 OF 1	UNITS
OPERATING SC	CENARIO:								
1OF _	1		P.E. SEAL REQUIR	ED (PE	ER 2g .0112)?	<b>√</b>	YES		□ NO
DESCRIBE CONTROL SYSTEM: A bin vent					. ,				
POLLUTANTS COLLECTED:			PM		PM10/PM2.5				-
BEFORE CONTROL EMISSION RATE (LB/H	HR):		0.005		0.002				-
CAPTURE EFFICIENCY:			<= 0.005 gr/dscf	%	<= 0.005 gr/dscf	%	%		_%
CONTROL DEVICE EFFICIENCY:			N/A	%	N/A	%	%		_%
CORRESPONDING OVERALL EFFICIENCY	<i>(</i> :		N/A	%	N/A	%	%		_%
EFFICIENCY DETERMINATION CODE:			2		2				-
TOTAL AFTER CONTROL EMISSION RATE	(LB/HR):		0.005		0.002		_		_
PRESSURE DROP (IN H <sub>2</sub> 0): MIN: MAX:	Avg: 10-15 wg	GAUGE?	YES		] NO				
BULK PARTICLE DENSITY (LB/FT <sup>3</sup> ): 25		-	INLET TEMPERATU	JRE (°F	F): Contract	MIN	MAX		
POLLUTANT LOADING RATE: N/A	] LB/HR	□ GR/FT <sup>3</sup>	OUTLET TEMPERA	TURE	(°F) Contract	MIN	MAX		
INLET AIR FLOW RATE (ACFM): 1300			FILTER OPERATIN	G TEM	P (°F): Contract				
NO. OF COMPARTMENTS: 1	NO. OF BAGS	PER COMPARTMENT:	Contract			LENGTH OF BA	G (IN.): 2	0-30	
NO. OF CARTRIDGES:	FILTER SURF	ACE AREA PER CARTE	RIDGE (FT <sup>2</sup> ):			DIAMETER OF E	BAG (IN.):	5-15	
TOTAL FILTER SURFACE AREA (FT <sup>2</sup> ):		AIR TO CLOTH RAT	IO: 1 to 4 : 1						
DRAFT TYPE: 🗹 INDUCED/NEGA	TIVE 🗹	FORCED/POSITIVE			FILTER MATERIAL: C	artridgeStyle	WOV	EN 🗌	FELTED
DESCRIBE CLEANING PROCEDURES:						P.	ARTICLE	SIZE DISTRIE	BUTION
AIR PULSE		SONIC				SIZE	v	VEIGHT %	CUMULATIVE
REVERSE FLOW		SIMPLE BAG COLLA	APSE			(MICRONS)	(	OF TOTAL	%
MECHANICAL/SHAKER		RING BAG COLLAPS	SE			0-1			
OTHER:						1-10			
DESCRIBE INCOMING AIR STREAM: Air stre	eam will contair	n fly ash.				10-25			
						25-50			
						50-100			
						>100			
							-	TOTA	L = 100
						Supplier specific	94% pas	sing 325 mesh	1
ON A SEPARATE PAGE, ATTACH A DIAGR	RAM SHOWING	THE RELATIONSHIP	OF THE CONTROL I	DEVICE	E TO ITS EMISSION SO	URCE(S):			
COMMENTS:									

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of A	Air Quality - Applic	ation for Ai	r Permit to	Construct/	Operate		В	
EMISSION SOURCE DESCRIPTION: \$	Screener			EMISSION	SOURCE IE	NO: ES-8	2A		
					DEVICE ID				
OPERATING SCENARIO1	OF	1			POINT (STA	. ,			
DESCRIBE IN DETAILTHE EMISSION		CESS (ATTACH F				101.7.1	·( <b>c</b> ): :		
The screening process will occur to pro		-		-	r.				
TYPE OF EMISSION SOUR	RCE (CHECK A	ND COMPLETE AF	PPROPRIAT	FE FORM B					
Coal,wood,oil, gas, other burner (Fe	orm B1)	Woodworking	(Form B4)		🗌 Manı	uf. of chemi	cals/coating	s/inks (Form B	
□ Int.combustion engine/generator (F	orm B2)	Coating/finishi	01 01	. ,		eration (For	,		
Liquid storage tanks (Form B3)		Storage silos/t	bins (Form E	36)	🚽 Othe	r (Form B9)	1		
START CONSTRUCTION DATE: TBD			DATE MAN	NUFACTURE	D: TBD			_	
MANUFACTURER / MODEL NO.: TBD	<u>,                                    </u>	_	EXPECTED	D OP. SCHE	DULE: 260	0 hours/yea	ır		
IS THIS SOURCE SUBJECT 🛛 N	ISPS (SUBPART	ſS?):		□ NES	HAP (SUBP	ARTS?):			
PERCENTAGE ANNUAL THROUGHP			R-MAY 25		JN-AUG	25	SEP-NOV	25	
CRITERIA A	IR POLLUTA	ANT EMISSION	IS INFOR	MATION	FOR THI	S SOUR	CE		
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	AL EMISSIO	NS	
		EMISSION	(AFTER CONT	ROLS / LIMITS)	BEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)	
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	
PARTICULATE MATTER (PM)		AP-42	0.015	0.020	N/A	N/A	0.015	0.020	
PARTICULATE MATTER<10 MICRONS	(PM <sub>10</sub> )	AP-42	0.005	0.007	N/A	N/A	0.005	0.007	
PARTICULATE MATTER<2.5 MICRONS	5 (PM <sub>2.5</sub> )	AP-42	0.0003	0.0004	N/A	N/A	0.0003	0.0004	
SULFUR DIOXIDE (SO2)		!	N/A	N/A	N/A	N/A	N/A	N/A	
NITROGEN OXIDES (NOx)		!	N/A	N/A	N/A	N/A	N/A	N/A	
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A	
VOLATILE ORGANIC COMPOUNDS (	VOC)		N/A	N/A	N/A	N/A	N/A	N/A	
LEAD		Ash Analysis	1.92E-06	2.50E-06	N/A	N/A	1.92E-06	2.50E-06	
OTHER		!	N/A	N/A	N/A	N/A	N/A	N/A	
HAZARDOUS	AIR POLLU	TANT EMISSIC	ONS INFO	RMATIO	N FOR T	HIS SOU	RCE		
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS	
		EMISSION	(AFTER CONT	ROLS / LIMITS)	IMITS)BEFORE CONTROLS / LIMITS (AFTE		(AFTER CON	R CONTROLS / LIMITS)	
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	
Arsenic	7440-38-2	Ash Analysis	1.79E-06	2.33E-06	N/A	N/A	1.79E-06	2.33E-06	
Beryllium	7440-41-7	Ash Analysis	3.71E-07	4.83E-07	N/A	N/A	3.71E-07	4.83E-07	
Cadmium	7440-43-9	Ash Analysis	3.20E-07	4.16E-07	N/A	N/A		4.16E-07	
Chromium	7440-47-3	Ash Analysis	2.18E-06	2.83E-06	N/A	N/A	2.18E-06	2.83E-06	
Chromium VI	18540-29-9	Ash Analysis	2.39E-07	3.11E-07	N/A	N/A	2.39E-07	3.11E-07	
Cobalt	7440-48-4	Ash Analysis	8.71E-07	1.13E-06	N/A	N/A	8.71E-07	1.13E-06	
Manganese	7439-96-5	Ash Analysis	3.84E-06	4.99E-06	N/A	N/A	3.84E-06	4.99E-06	
Mercury	7439-97-6	Ash Analysis	1.15E-08	1.49E-08	N/A	N/A	1.15E-08	1.49E-08	
Nickel	7440-02-0	Ash Analysis	2.18E-06	2.83E-06	N/A	N/A	2.18E-06	2.83E-06	
Selenium	7782-49-2	Ash Analysis	1 1		N/A	N/A	5.89E-07	7.66E-07	
TOXIC AIR	POLLUTAN	IT EMISSIONS	INFORM	ATION F	OR THIS	SOURC	E		
		SOURCE OF EMISSION	EXPECTE	D ACTUAL E	EMISSIONS	AFTER CO	ONTROLS /	LIMITATIONS	
TOXIC AIR POLLUTANT	CAS NO.	FACTOR		/hr	lb/c	lay		lb/yr	
Arsenic	7440-38-2	Ash Analysis	1.79E-06		4.30	E-05	4.6	6E-03	
Beryllium	7440-41-7	Ash Analysis	3.71E-07		8.91	E-06	9.6	65E-04	
Cadmium	7440-43-9	Ash Analysis	3.20E-07		7.68	E-06	8.3	32E-04	
	18540-29-9	Ash Analysis	2.39E-07		5.75	E-06	6.2	23E-04	
Chromium VI	10040-29-9	<u>````</u> `						99E-03	
Chromium VI Manganese	7439-96-5	Ash Analysis	3.84E-06		9.22	E-05	9.5	JJL-05	
		-			9.221 2.761			99E-05	

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

# FORM B9 EMISSION SOURCE (OTHER)

REVISED 09/22/16 NCDEQ/Division of Air Quality - A	Application for A	Air Permit to Construct/Operate		B9
EMISSION SOURCE DESCRIPTION: Screener		EMISSION SOURCE ID NO: ES-824	Ą	
		CONTROL DEVICE ID NO(S): N/A		
OPERATING SCENARIO:1 OF1		EMISSION POINT (STACK) ID NO(	S): EP-82	
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): The scree	ening process wil	l occur to produce free flowing feedsto	ck suitable for the STAR®	reactor
MATERIALS ENTERING PROCESS - CONTINUOUS PROCES	S	MAX. DESIGN	REQUESTED CAP	PACITY
ТҮРЕ	UNITS	CAPACITY (UNIT/HR)	LIMITATION(UNIT	T/HR)
Capacity	ton	165		165
MATERIALS ENTERING PROCESS - BATCH OPERATION		MAX. DESIGN	REQUESTED CAP	PACITY
TYPE	UNITS	CAPACITY (UNIT/BATCH)	LIMITATION (UNIT/E	BATCH)
MAXIMUM DESIGN (BATCHES / HOUR):				
REQUESTED LIMITATION (BATCHES / HOUR):	(BATCHES/Y	R):		
FUEL USED: N/A		MUM FIRING RATE (MILLION BTU/H	IR): N/A	
MAX. CAPACITY HOURLY FUEL USE: N/A		CAPACITY ANNUAL FUEL USE: N/		
COMMENTS:				

#### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of	Air Quality - Applicat	ion for Air	Permit to C	Construct/C	perate		В
EMISSION SOURCE DESCRIPTION: S	creener-Diese	I Engine		EMISSION	SOURCE I	D NO: ES-8	32B	
				CONTROL	DEVICE ID	NO(S): N/	4	
OPERATING SCENARIO1_	OF _	1		EMISSION	POINT (ST	ACK) ID N	D(S): EP-82	
DESCRIBE IN DETAILTHE EMISSION S	SOURCE PRO	CESS (ATTACH FLO)	V DIAGRA	M):				
Diesel Engine to run the Screener.								
TYPE OF EMISSION SOUR								s).
Coal,wood,oil, gas, other burner (Fo		Woodworking (Fo						ngs/inks (Form I
✓ Int.combustion engine/generator (For Comparison of Comparison)		Coating/finishing/	,	orm B5)	_	ineration (F		.9-,
Liquid storage tanks (Form B3)		Storage silos/bin	s (Form B6)	)	□ Oth	ner (Form B	9)	
START CONSTRUCTION DATE: TBD			DATE MAN	NUFACTUR	ED: TBD			
MANUFACTURER / MODEL NO.: TBD			EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
	PS (SUBPAR	1			SHAP (SUB			
	. ,	EB 25 MAR-M. TANT EMISSIONS					SEP-NOV	25
CRITERIA A								NC
		SOURCE OF EMISSION		D ACTUAL ROLS / LIMITS				ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		AP-42	2.00E-01	2.60E-01	N/A	N/A	2.00E-01	2.60E-01
PARTICULATE MATTER<10 MICRONS (F	PM <sub>10</sub> )	AP-42	2.00E-01		N/A	N/A	2.00E-01	2.60E-01
PARTICULATE MATTER<2.5 MICRONS (I	PM <sub>2.5</sub> )	AP-42	2.00E-01	2.60E-01	N/A	N/A	2.00E-01	2.60E-01
SULFUR DIOXIDE (SO2)		AP-42	0.187	0.243	N/A	N/A	0.187	0.243
NITROGEN OXIDES (NOx)		AP-42	2.821	3.667	N/A	N/A	2.821	3.667
CARBON MONOXIDE (CO)		AP-42	0.608	0.790	N/A	N/A	0.608	0.790
VOLATILE ORGANIC COMPOUNDS (VO	JC)	AP-42	0.225 N/A	0.292 N/A	N/A N/A	N/A N/A	0.225 N/A	0.292 N/A
OTHER			N/A N/A	N/A N/A	N/A N/A	N/A N/A	N/A N/A	N/A
HAZARDOUS AIR POLLUTANT EMISSIONS INFORMATION FOR THIS SOURCE						1070		
		SOURCE OF		D ACTUAL				NS
		EMISSION		ROLS / LIMITS	SEFORE CONT			ITROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Benzene	71-43-2	AP-42	5.94E-04	7.73E-04	N/A	N/A	5.94E-04	7.73E-04
Toluene	108-88-3	AP-42	2.61E-04		N/A	N/A	2.61E-04	3.39E-04
Xylenes	1330-20-7	AP-42	1.82E-04		N/A	N/A	1.82E-04	2.36E-04
1,3-Butadiene	106-99-0	AP-42	2.49E-05		N/A	N/A	2.49E-05	3.24E-05
Formaldehyde Acetaldehyde	50-00-0 75-07-0	AP-42 AP-42	7.52E-04 4.89E-04		N/A N/A	N/A N/A	7.52E-04 4.89E-04	9.77E-04 6.35E-04
Acrolein	107-02-8	AP-42 AP-42	5.89E-05		N/A	N/A	4.89E-04	7.66E-05
Total PAH		AP-42	1.07E-04	1.39E-04	N/A	N/A	1.07E-04	1.39E-04
Naphthalene	91-20-3	AP-42	5.40E-05	7.02E-05	N/A	N/A	5.40E-05	7.02E-05
Acenaphthalene	208-96-8	AP-42	3.22E-06	4.19E-06	N/A	N/A	3.22E-06	4.19E-06
Acenaphthene	83-32-9	AP-42	9.05E-07	1.18E-06	N/A	N/A	9.05E-07	1.18E-06
Fluorene	86-73-7	AP-42	1.86E-05	2.42E-05	N/A	N/A	1.86E-05	2.42E-05
Phenanthrene	85-01-8			2.43E-05	N/A	N/A		2.43E-05
Anthracene	120-12-7	AP-42 AP-42	1.19E-06		N/A	N/A	1.19E-06 4.85E-06	1.55E-06
Fluoranthene Pyrene	206-44-0 129-00-0	AP-42 AP-42	4.85E-06 3.04E-06	6.30E-06 3.96E-06	N/A N/A	N/A N/A	4.85E-06 3.04E-06	6.30E-06 3.96E-06
Benzo(a)anthracene	56-55-3	AP-42 AP-42	1.07E-06		N/A	N/A N/A	1.07E-06	1.39E-06
Chrysene	218-01-9	AP-42	2.25E-07		N/A	N/A	2.25E-07	2.92E-07
Benzo(b)fluoranthene	205-99-2	AP-42	6.31E-08		N/A	N/A	6.31E-08	8.21E-08
Benzo(k)fluoranthene	207-08-9	AP-42	9.87E-08	1.28E-07	N/A	N/A	9.87E-08	1.28E-07
Benzo(a)pyrene	50-32-8	AP-42	1.20E-07	1.56E-07	N/A	N/A	1.20E-07	1.56E-07
Indeno(1,2,3-cd)pyrene	193-39-5	AP-42	2.39E-07		N/A	N/A	2.39E-07	3.11E-07
Dibenz(a,h)anthracene	53-70-3	AP-42	3.71E-07		N/A	N/A	3.71E-07	4.83E-07
Benzo(g,h,l)perylene	191-24-2	AP-42	3.11E-07		N/A	N/A	3.11E-07	4.05E-07
	POLLUTA	NT EMISSIONS II						
			EXPECTE	D ACTUAL	EMISSION	S AFTER C	ONTROLS	LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	SOURCE OF EMISSION FACTOR	lb	/hr	lb/	day		lb/yr
Benzene	71-43-2	AP-42		E-04		E-02		5E+00
Toluene	108-88-3	AP-42	2.61	E-04	6.25	E-03	6.	7E-01
Xylenes	1330-20-7	AP-42	1.82	2E-04	4.36	E-03	4.	'2E-01
1,3-Butadiene	106-99-0	AP-42		E-05		E-04		18E-02
Formaldehyde	50-00-0	AP-42		2E-04		E-02		5E+00
Acetaldehyde	75-07-0	AP-42		E-04		E-02		7E+00
Acrolein	107-02-8	AP-42		E-05		E-03		53E-01
Attachments: (1) emissions calculations and so emission rates) and describe how these are me								

MPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOUR Attach Additional Sheets As Necessary

### EMISSION SOURCE (INTERNAL COMBUSTION ENGINES/TURBINES/GENERATORS)

REVISED 09/22/16	NCDEQ/Division of Air Qua	lity - Application for Air Perm	nit to Construct/Operate	B2			
EMISSION SOURCE DESCRIPTION: \$	Screener-Diesel Engine		EMISSION SOURCE ID NO: ES-82B				
			CONTROL DEVICE ID NO(S): N/A				
OPERATING SCENARIO:	1OFŕ		EMISSION POINT (STACK) ID NO(S): EP-82	2			
	EMERGENCY	SPACE HEAT					
(CHECK ALL THAT APPLY)	PEAK SHAVER	OTHER (DESCRIBE): To o					
GENERATOR OUTPUT (KW):		· · · · · ·	OPERATION (HRS/YR): 2600				
ENGINE OUTPUT (HP): 91	/ write						
	IE 🔽 DIESEL ENGINE U	P TO 600 HP 🔲 DIESE	L ENGINE GREATER THAN 600 HP	DUAL FUEL ENGINE			
			(complete below)	DOMETOLL ENGINE			
		GRETARD DREIG		OTHER			
OR STATIONARY GAS TURE		_	COMPRESSOR OR TURBINE (complete belo				
FUEL: A NATURAL GAS	_						
			_				
			I MODIFICATIONS (DESCRIBE):				
		EAN BURN AND PRECOMBL					
	LEAN-PREMIX			· 			
	FUEL USAGE	(INCLUDE STARTUP/B	ACKUP FUEL)				
		MAXIMUM DESIGN	IGN REQUESTED CAPACITY				
FUEL TYPE	UNITS	CAPACITY (UNIT/HF					
Diagol	gollono						
Diesel	gallons	3.75 @ 75 % load	2600 hr/yr				
	FUEL CHARACTERISTI						
FUEL TYPE	BTU/UNIT	UNITS	SULFUR CON (% BY WEIGH				
Diesel	6.40E+	05 Hour		0.0015%			
	r	ECIFIC EMISSION FAC					
POLLUTANT	NOX	CO PM	PM10 VOC	OTHER			
EMISSION FACTOR LB/UNIT							
UNIT							
COMMENTS:							

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of A	Air Quality - Applic	ation for Ai	ir Permit to	Construct/	Operate		В
EMISSION SOURCE DESCRIPTION: C	Crusher			EMISSION	SOURCE II	D NO: ES-8	3A	
					DEVICE ID			
OPERATING SCENARIO1_	OF	1		EMISSION		. ,		
DESCRIBE IN DETAILTHE EMISSION							/(O). LI -00	
Fly ash will be processed further by pas		-		-	oduce more	e fine and fr	ee flowing fe	edstock.
TYPE OF EMISSION SOUR	CE (CHECK A		PPROPRIA		1-B9 ON TH			S):
Coal,wood,oil, gas, other burner (Fo	•	Woodworking						s/inks (Form B
□ Int.combustion engine/generator (Fe	- ,	Coating/finishi	. ,	(Form B5)		eration (For	-	o/iiiiio (i c
Liquid storage tanks (Form B3)	,	Storage silos/	bins (Form E	B6)	⊡ Othe	er (Form B9)	,	
START CONSTRUCTION DATE: TBD			DATE MAN	NUFACTURE	ED: TBD			
MANUFACTURER / MODEL NO.: TBD			EXPECTED	D OP. SCHE	DULE: 365	hours/year		
IS THIS SOURCE SUBJECT	SPS (SUBPART	ΓS?):		□ NES	HAP (SUBF	PARTS?):		
PERCENTAGE ANNUAL THROUGHPU	( )		R-MAY 25		JN-AUG	25	SEP-NOV	25
CRITERIA AI	R POLLUTA	ANT EMISSION	IS INFOR	<b>MATION</b>	FOR TH	S SOUR	CE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	(AFTER CONTI	ROLS / LIMITS)	BEFORE CONT	ROLS / LIMITS	(AFTER CON	TROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		AP-42	0.008	0.002	N/A	N/A	0.008	0.002
PARTICULATE MATTER<10 MICRONS	(PM <sub>10</sub> )	AP-42	0.004	0.001	N/A	N/A	0.004	0.001
PARTICULATE MATTER<2.5 MICRONS	(PM <sub>2.5</sub> )	AP-42	0.0007	0.0001	N/A	N/A	0.0007	0.0001
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (\	VOC)		N/A	N/A	N/A	N/A	N/A	N/A
LEAD		Ash Analysis			N/A	N/A	1.05E-06	1.912E-07
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS	AIR POLLU	TANT EMISSIC						
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION		ROLS / LIMITS)	EFORE CONT			TROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis		-	N/A	N/A		1.78E-07
Beryllium	7440-41-7	Ash Analysis			N/A	N/A		3.70E-08
Cadmium	7440-43-9	Ash Analysis		3.19E-08	N/A	N/A		3.19E-08
Chromium	7440-43-3	Ash Analysis			N/A	N/A		2.17E-07
Chromium VI	18540-29-9	Ash Analysis		2.38E-08	N/A	N/A	1.31E-07	2.38E-08
Cobalt	7440-48-4	Ash Analysis		8.67E-08	N/A	N/A	4.75E-07	8.67E-08
Manganese	7439-96-5	Ash Analysis		3.82E-07	N/A	N/A	2.10E-06	3.82E-07
Mercury	7439-90-3	Ash Analysis		1.14E-09	N/A	N/A	6.27E-09	1.14E-09
Nickel	7440-02-0	Ash Analysis		2.17E-07	N/A	N/A	1.19E-06	2.17E-07
Selenium	7782-49-2	Ash Analysis		5.86E-08	N/A	N/A		5.86E-08
		IT EMISSIONS						J.00L-00
		SOURCE OF	1					LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	EMISSION FACTOR		/hr		day		b/yr
Arsenic	7440-38-2	Ash Analysis		/11		E-05		57E-04
Beryllium	7440-38-2					E-05		39E-05
Cadmium	7440-41-7	Ash Analysis						
						E-06		37E-05
Chromium VI	18540-29-9	Ash Analysis				E-06		7E-05
Manganese	7439-96-5	Ash Analysis				E-05		5E-04
	7400 07 0							9E-06
Mercury Nickel	7439-97-6	Ash Analysis Ash Analysis			1.50	E-05		3E-04

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

# FORM B9 EMISSION SOURCE (OTHER)

REVISED 09/22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate							
EMISSION SOURCE DESCRIPTION: Crusher		EMISSION SOURCE ID NO: ES	-83A				
		CONTROL DEVICE ID NO(S): N	/A				
OPERATING SCENARIO:1 OF1		EMISSION POINT (STACK) ID N	IO(S): EP-83				
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): Fly ash will i more fine and free flowing feedstock.	be processed f	urther by passing through a crushe	r to remove larger parti	cles and to produce			
MATERIALS ENTERING PROCESS - CONTINUOUS PROCESS		MAX. DESIGN	REQUEST	ED CAPACITY			
ТҮРЕ	UNITS	CAPACITY (UNIT/HR)		N(UNIT/HR)			
Capacity	ton	165 ton/day	165 ton/day				
MATERIALS ENTERING PROCESS - BATCH OPERATION	<u>.</u>	MAX. DESIGN	REQUEST	ED CAPACITY			
ТҮРЕ	UNITS	CAPACITY (UNIT/BATCH)	LIMITATION	(UNIT/BATCH)			
MAXIMUM DESIGN (BATCHES / HOUR):							
REQUESTED LIMITATION (BATCHES / HOUR):	(BATCHES/Y	R):					
FUEL USED: N/A	TOTAL MAXI	MUM FIRING RATE (MILLION BT	U/HR): N/A				
MAX. CAPACITY HOURLY FUEL USE: N/A	REQUESTED	CAPACITY ANNUAL FUEL USE	N/A				
COMMENTS:							

#### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate B						В		
EMISSION SOURCE DESCRIPTION: C	rusher-Diesel	Engine		EMISSION	SOURCE I	D NO: ES-8	33B	
				CONTROL	DEVICE ID	0 NO(S): N//	4	
OPERATING SCENARIO1_	OF _	1	-		POINT (ST	ACK) ID NO	O(S): EP-83	
DESCRIBE IN DETAILTHE EMISSION S	OURCE PRO	CESS (ATTACH FLO)	N DIAGRA	M):				
Diesel Engine to run the Crusher.								
TYPE OF EMISSION SOUR	CE (CHECK			FORM B1				s).
Coal,wood,oil, gas, other burner (Fo		Woodworking (Fo						ngs/inks (Form I
Int.combustion engine/generator (Fo	orm B2)	Coating/finishing	/printing (Fo	orm B5)	🗌 Inc	ineration (Fe	orm B8)	•
Liquid storage tanks (Form B3)		Storage silos/bin	s (Form B6)	)	□ Oth	ner (Form B	9)	
START CONSTRUCTION DATE: TBD	START CONSTRUCTION DATE: TBD DATE MANUFACTURED: TBD							
MANUFACTURER / MODEL NO.: TBD			EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
	PS (SUBPAR	,			SHAP (SUB	,		
PERCENTAGE ANNUAL THROUGHPUT	. ,						SEP-NOV	25
CRITERIA A	IR POLLUI	TANT EMISSIONS			-OR THIS			
		SOURCE OF		D ACTUAL			L EMISSIC	
AIR POLLUTANT EMITTED		EMISSION FACTOR		ROLS / LIMITS				ITROLS / LIMITS)
PARTICULATE MATTER (PM)		AP-42	lb/hr 6.60E-01	tons/yr 1.20E-01	lb/hr N/A	tons/yr N/A	lb/hr 6.60E-01	tons/yr 1.20E-01
PARTICULATE MATTER (PM) PARTICULATE MATTER<10 MICRONS (P	M)	AF-42 AP-42	6.60E-01	1.20E-01	N/A N/A	N/A	6.60E-01	1.20E-01
PARTICULATE MATTER<2.5 MICRONS (F		AP-42	6.60E-01	1.20E-01	N/A	N/A	6.60E-01	1.20E-01
SULFUR DIOXIDE (SO2)	2.3]	AP-42 AP-42	0.615	0.112	N/A	N/A	0.615	0.112
NITROGEN OXIDES (NOx)		AP-42	9.300	1.697	N/A	N/A	9.300	1.697
CARBON MONOXIDE (CO)		AP-42	2.004	0.366	N/A	N/A	2.004	0.366
VOLATILE ORGANIC COMPOUNDS (VO	C)	AP-42	0.741	0.135	N/A	N/A	0.741	0.135
LEAD			N/A	N/A	N/A	N/A	N/A	N/A
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS AIR POLLUTANT EMISSIONS INFORMATION FOR THIS SOURCE								
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA		NS
		EMISSION	AFTER CONT	ROLS / LIMITS	BEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Benzene	71-43-2	AP-42	1.96E-03		N/A	N/A	1.96E-03	3.58E-04
Toluene	108-88-3	AP-42	8.59E-04		N/A	N/A	8.59E-04	1.57E-04
Xylenes 1,3-Butadiene	1330-20-7 106-99-0	AP-42 AP-42	5.99E-04 8.21E-05		N/A N/A	N/A	5.99E-04 8.21E-05	1.09E-04 1.50E-05
Formaldehyde	50-00-0	AP-42 AP-42	2.48E-03		N/A	N/A	2.48E-03	4.52E-04
Acetaldehyde	75-07-0	AP-42	1.61E-03		N/A	N/A	1.61E-03	2.94E-04
Acrolein	107-02-8	AP-42	1.94E-04		N/A	N/A	1.94E-04	3.55E-05
Total PAH		AP-42	3.53E-04		N/A	N/A	3.53E-04	6.44E-05
Naphthalene	91-20-3	AP-42	1.78E-04	3.25E-05	N/A	N/A	1.78E-04	3.25E-05
Acenaphthalene	208-96-8	AP-42	1.06E-05	1.94E-06	N/A	N/A	1.06E-05	1.94E-06
Acenaphthene	83-32-9	AP-42	2.98E-06	5.44E-07	N/A	N/A	2.98E-06	5.44E-07
Fluorene	86-73-7	AP-42	6.13E-05	1.12E-05	N/A	N/A	6.13E-05	1.12E-05
Phenanthrene	85-01-8	AP-42	6.17E-05	1.13E-05	N/A	N/A	6.17E-05	1.13E-05
Anthracene	120-12-7	AP-42	3.93E-06		N/A	N/A	3.93E-06	7.17E-07
Fluoranthene	206-44-0	AP-42	1.60E-05		N/A	N/A	1.60E-05	2.92E-06
Pyrene	129-00-0	AP-42	1.00E-05	1.83E-06	N/A	N/A	1.00E-05	1.83E-06
Benzo(a)anthracene	56-55-3	AP-42	3.53E-06		N/A	N/A	3.53E-06	6.44E-07
Chrysene	218-01-9 205-99-2	AP-42 AP-42	7.41E-07 2.08E-07	1.35E-07 3.80E-08	N/A	N/A	7.41E-07 2.08E-07	1.35E-07 3.80E-08
Benzo(b)fluoranthene Benzo(k)fluoranthene	205-99-2	AP-42 AP-42	3.26E-07	5.94E-08	N/A N/A	N/A N/A	3.26E-07	5.94E-08
Benzo(a)pyrene	50-32-8	AP-42 AP-42	3.95E-07	7.21E-08	N/A	N/A	3.95E-07	7.21E-08
Indeno(1,2,3-cd)pyrene	193-39-5	AP-42	7.88E-07	1.44E-07	N/A	N/A	7.88E-07	1.44E-07
Dibenz(a,h)anthracene	53-70-3	AP-42	1.22E-06		N/A	N/A	1.22E-06	2.23E-07
Benzo(g,h,l)perylene	191-24-2	AP-42	1.03E-06		N/A	N/A	1.03E-06	1.87E-07
	POLLUTA	NT EMISSIONS II	NFORMA	TION FC	R THIS S	SOURCE		
			EXPECTE		EMISSION	S AFTER C		LIMITATIONS
		SOURCE OF		DACIOAL		SALIERO		LIMITATIONO
TOXIC AIR POLLUTANT	CAS NO.	EMISSION FACTOR	lb	/hr	lb/	day		lb/yr
Benzene	71-43-2	AP-42		E-03		E-02		I5E-01
Toluene	108-88-3	AP-42		E-04		E-02		13E-01
Xylenes	1330-20-7	AP-42		E-04		E-02		18E-01
1,3-Butadiene	106-99-0	AP-42		E-05		E-03		00E-02
Formaldehyde Acetaldehyde	50-00-0 75-07-0	AP-42 AP-42		E-03 E-03		E-02 E-02		04E-01 38E-01
Acrolein	107-02-8	AF-42 AP-42		E-03		E-02 E-03		09E-01
Attachments: (1) emissions calculations and su								
emission rates) and describe how these are mo								

MPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOUR Attach Additional Sheets As Necessary

### EMISSION SOURCE (INTERNAL COMBUSTION ENGINES/TURBINES/GENERATORS)

REVISED 09/22/16	NCDEQ/Division of Air Qua	ity - Application for Air Perm	it to Construct/Ope	erate	B2			
EMISSION SOURCE DESCRIPTION: 0	Crusher-Diesel Engine		EMISSION SOURC	E ID NO: ES-83B				
			CONTROL DEVICE	E ID NO(S): N/A				
OPERATING SCENARIO:	10F1			(STACK) ID NO(S): EP-83				
	EMERGENCY	SPACE HEAT						
(CHECK ALL THAT APPLY)	PEAK SHAVER	OTHER (DESCRIBE): To o						
GENERATOR OUTPUT (KW):		PATED ACTUAL HOURS OF	•	VR): 365				
ENGINE OUTPUT (HP): 300	7.0010			11().000				
	E 🔽 DIESEL ENGINE U	P TO 600 HP 🔲 DIESE	L ENGINE GREATE	R THAN 600 HP 🔲 DUAL F	UEL ENGINE			
			(complete b					
		RETARD D PREIG	NITION CHAMBER					
OR 🗌 STATIONARY GAS TURB				TURBINE (complete below)				
FUEL: A NATURAL GAS	_			4-CYCLE LEAN TURBIN	JE			
				OTHER (DESCRIBE):				
				DESCRIBE):				
		INSELECTIVE CATALYTIC R		SELECTIVE CATALYTIC REDU	CTION			
		EAN BURN AND PRECOMBL	_					
	LEAN-PREMIX							
OTHER (SPECIFY):								
	FUEL USAGE	INCLUDE STARTUP/B	ACKUP FUEL)					
	MAXIMUM DES			GN REQUESTED CAPACITY				
FUEL TYPE	UNITS	CAPACITY (UNIT/HF		LIMITATION (UNIT/HR)				
Diesel	gallons	11.71 @ 75% load		365 hr/yr				
Diesei	galions	11.71 @ 7576 load		505 m/yi				
	FUEL CHARACTERISTIC	S (COMPLETE ALL TH		CABLE)				
				SULFUR CONTENT				
FUEL TYPE	BTU/UNIT	UNITS		(% BY WEIGHT)				
					0.00450/			
Diesel	2.10E+	06 Hour			0.0015%			
	MANUFACTURER'S SP	ECIFIC EMISSION FAC	TORS (IF AVAIL	ABLE)				
POLLUTANT	NOX		PM10	,	OTHER			
EMISSION FACTOR LB/UNIT			1 1110					
UNIT								
GNIT								
DESCRIBE METHODS TO MINIMIZE \	ISIBLE EMISSIONS DURING ID	LING, OR LOW LOAD OPERA	ATIONS:					
COMMENTS:								

#### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of A	ir Quality - Applic	ation for Ai	r Permit to	Construct/	Operate		В
EMISSION SOURCE DESCRIPTION:	Wet Ash Receivi	ing-Transfer to She	d	EMISSION	SOURCE I	D NO: F-1		
				CONTROL	DEVICE ID	NO(S): N/	Ą	
OPERATING SCENARIO1	OF _	1		EMISSION	POINT (ST	ACK) ID NO	D(S): FUGIT	IVE FEP-1
DESCRIBE IN DETAILTHE EMISSION Transfer of materials to storage shed.	I SOURCE PRO	CESS (ATTACH F	LOW DIAG	RAM):				
TYPE OF EMISSION SOU	RCE (CHECK A	_		FE FORM B	_			•
Coal,wood,oil, gas, other burner (F	,							s/inks (Form B
Int.combustion engine/generator (F	Form B2)	Coating/finish	o. o	,		eration (For		
Liquid storage tanks (Form B3)		Storage silos/	bins (Form I	B6)	⊡ Othe	r (Form B9)		
START CONSTRUCTION DATE: TBD				NUFACTUR				
MANUFACTURER / MODEL NO.: TBE			EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
IS THIS SOURCE SUBJECT	ISPS (SUBPAR	rs?):			SHAP (SUB	PARTS?):_		
PERCENTAGE ANNUAL THROUGHP			R-MAY 25		UN-AUG	25	SEP-NO	/ 25
CRITERIA A	IR POLLUTA	NT EMISSION			FOR TH			
		SOURCE OF	-	D ACTUAL			L EMISSIO	NS
		EMISSION		ROLS / LIMITS)	SEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		AP-42	0.0025	0.0073	N/A	N/A	0.0025	0.0073
PARTICULATE MATTER<10 MICRONS	10/	AP-42	0.0012	0.0034	N/A	N/A	0.0012	0.0034
PARTICULATE MATTER<2.5 MICRON	S (PM <sub>2.5</sub> )	AP-42	0.0002	0.0005	N/A	N/A	0.0002	0.0005
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (VOC)			N/A	N/A	N/A	N/A	N/A	N/A
LEAD		Ash Analysis	3.23E-07	9.22E-07	N/A	N/A	3.23E-07	9.22E-07
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS	AIR POLLUT	TANT EMISSIC	ONS INFC	DRMATIO	N FOR T	HIS SOU	RCE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	
		EMISSION		· · ·		ROLS / LIMITS		ITROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis			N/A	N/A		8.60E-07
Beryllium	7440-41-7	Ash Analysis			N/A	N/A	6.24E-08	1.78E-07
Cadmium	7440-43-9	Ash Analysis			N/A	N/A		1.54E-07
Chromium	7440-47-3	,				N/A		1.04E-06
Chromium VI	18540-29-9 7440-48-4	Ash Analysis			N/A	N/A	4.02E-08	1.15E-07 4.18E-07
Cobalt	7440-48-4	Ash Analysis		4.18E-07	N/A	N/A	1.46E-07	
Manganese	7439-96-5	Ash Analysis Ash Analysis		1.84E-06 5.53E-09	N/A N/A	N/A N/A	6.45E-07 1.94E-09	1.84E-06 5.53E-09
Mercury Nickel	7439-97-6	,		1.04E-06	N/A N/A	N/A N/A	3.66E-07	1.04E-06
Selenium	7782-49-2	Ash Analysis Ash Analysis			N/A N/A	N/A	9.89E-08	2.83E-07
		T EMISSIONS						2.032-07
		SOURCE OF EMISSION						LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	FACTOR		/hr		day		b/yr
Arsenic	7440-38-2	Ash Analysis				E-06		'2E-03
Beryllium	7440-41-7	Ash Analysis				E-06		6E-04
Cadmium	7440-43-9	Ash Analysis				E-06		)7E-04
Chromium VI	18540-29-9	Ash Analysis				E-07		30E-04
Manganese	7439-96-5	Ash Analysis				E-05		9E-03
Mercury	7439-97-6	Ash Analysis				E-08		1E-05
Nickel	7440-02-0	Ash Analysis	3.66E-07		8.78	E-06	2.0	9E-03
Attachments: (1) emissions calculations and	supporting docum	entation; (2) indicate	all requested	state and fee	leral enforcea	able permit lin	nits (e.g. hou	rs of operation,

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

## FORM B9 EMISSION SOURCE (OTHER)

REVISED 09/22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate						
EMISSION SOURCE DESCRIP	TION: Wet Ash Receivi	ing-Transfer to Shed	EMISSION SOURCE ID NO: F-1			
			CONTROL DEVICE ID NO(S): N/A	L		
OPERATING SCENARIO:	1OF	1	EMISSION POINT (STACK) ID NO	0(S): FUGITIVE FEP-1		
DESCRIBE IN DETAIL THE PR						
			MAX. DESIGN	REQUESTED CAPACITY		
MATERIALS ENTERING PROCESS - CONTINUOUS PROCESS           TYPE         UNI		UNITS	CAPACITY (UNIT/HR)	LIMITATION(UNIT/HR)		
Transfer		Tons	70	70		
		10115	70	10		
	ERING PROCESS - B					
	TYPE	UNITS	MAX. DESIGN CAPACITY (UNIT/BATCH)	REQUESTED CAPACITY LIMITATION (UNIT/BATCH)		
		01113				
MAXIMUM DESIGN (BATCHES	S / HOUR):					
REQUESTED LIMITATION (BA	*	(BATCHES/	YR):			
FUEL USED: N/A		TOTAL MAX	KIMUM FIRING RATE (MILLION BTU	/HR): N/A		
MAX. CAPACITY HOURLY FUE	EL USE: N/A		D CAPACITY ANNUAL FUEL USE: N			
COMMENTS:						

# FORM B

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate								В		
EMISSION SOURCE DESCRIPTION: V	Vet Ash Receivi	ng-Transfer to Hopp	er	EMISSION	SOURCE I	D NO: F-2				
				CONTROL	DEVICE ID	NO(S): N/A	4			
OPERATING SCENARIO	1 OF _	1		EMISSION POINT (STACK) ID NO(S): FUGITIVE FEP-2						
DESCRIBE IN DETAILTHE EMISSION Transfer of materials to feed hopper.	SOURCE PRO	CESS (ATTACH FL	OW DIAGR	AM):						
TYPE OF EMISSION SOU	RCE (CHECK A	ND COMPLETE AP	PROPRIAT	E FORM B	I-B9 ON TH	E FOLLOW	ING PAGE	S):		
Coal,wood,oil, gas, other burner (Fo	orm B1)	Woodworking (	Form B4)		🗆 Man	uf. of chemi	cals/coating	s/inks (Form B		
<ul> <li>Int.combustion engine/generator (F</li> <li>Liquid storage tanks (Form B3)</li> </ul>	orm B2)	Coating/finishin	0. 0.	,		eration (For r (Form B9)	,			
START CONSTRUCTION DATE: TBD					Ľ	( /				
MANUFACTURER / MODEL NO.: TBD						HR/DAY 7	DAY/WK 5	2 WK/YR		
	SPS (SUBPAR	rs?):			SHAP (SUB		2,11,111 0			
PERCENTAGE ANNUAL THROUGHP	,	/	MAY 25		N-AUG	25	SEP-NOV	25		
		ANT EMISSION	-			-				
		SOURCE OF	EXPECTE				L EMISSIO	NS		
		EMISSION			EFORE CONT			TROLS / LIMITS)		
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr		
PARTICULATE MATTER (PM)		AP-42	0.0051	0.0145	N/A	N/A	0.0051	0.0145		
PARTICULATE MATTER<10 MICRONS	(PM <sub>10</sub> )	AP-42	0.0024		N/A	N/A	0.0024	0.0069		
PARTICULATE MATTER<2.5 MICRONS	(PM <sub>2.5</sub> )	AP-42	0.0004	0.0010	N/A	N/A	0.0004	0.0010		
SULFUR DIOXIDE (SO2)	,		N/A	N/A	N/A	N/A	N/A	N/A		
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A		
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A		
VOLATILE ORGANIC COMPOUNDS (	VOC)		N/A	N/A	N/A	N/A	N/A	N/A		
LEAD		Ash Analysis	6.45E-07	1.84E-06	N/A	N/A	6.45E-07	1.84E-06		
OTHER			N/A	N/A	N/A	N/A	N/A	N/A		
HAZARDOUS	AIR POLLU	TANT EMISSIO	NS INFO	RMATIO	N FOR T	HIS SOU	RCE			
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS		
		EMISSION	AFTER CONTI	ROLS / LIMITS	EFORE CONT	ROLS / LIMITS	(AFTER CON	TROLS / LIMITS)		
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr		
Arsenic	7440-38-2	Ash Analysis	6.02E-07	1.72E-06	N/A	N/A	6.02E-07	1.72E-06		
Beryllium	7440-41-7	Ash Analysis	1.25E-07	3.56E-07	N/A	N/A	1.25E-07	3.56E-07		
Cadmium	7440-43-9	Ash Analysis	1.08E-07	3.07E-07	N/A	N/A	1.08E-07	3.07E-07		
Chromium	7440-47-3	Ash Analysis	7.31E-07	2.09E-06	N/A	N/A	7.31E-07	2.09E-06		
Chromium VI	18540-29-9	Ash Analysis	8.04E-08	2.3E-07	N/A	N/A	8.04E-08	2.30E-07		
Cobalt	7440-48-4	Ash Analysis	2.93E-07	8.36E-07	N/A	N/A	2.93E-07	8.36E-07		
Manganese	7439-96-5	Ash Analysis	1.29E-06	3.69E-06	N/A	N/A	1.29E-06	3.69E-06		
Mercury	7439-97-6	Ash Analysis	3.86E-09	1.1E-08	N/A	N/A	3.86E-09	1.10E-08		
Nickel	7440-02-0	Ash Analysis	7.31E-07	2.09E-06	N/A	N/A	7.31E-07	2.09E-06		
Selenium	7782-49-2	Ash Analysis	1.98E-07		N/A	N/A	1.98E-07	5.65E-07		
TOXIC AIR	R POLLUTAN	T EMISSIONS	INFORM,	ATION F	OR THIS	SOURCE				
		SOURCE OF EMISSION	EXPECTE	D ACTUAL	EMISSION	S AFTER C	ONTROLS /	LIMITATIONS		
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb/	/hr	lb/o	day		b/yr		
Arsenic	7440-38-2	Ash Analysis	6.02E-07		1.45	E-05	3.4	4E-03		
Beryllium	7440-41-7	Ash Analysis	1.25E-07		2.99	E-06	7.1	3E-04		
Cadmium	7440-43-9	Ash Analysis	1.08E-07		2.58	E-06	6.1	4E-04		
Chromium VI	18540-29-9	Ash Analysis	8.04E-08		1.93	E-06	4.6	60E-04		
Manganese	7439-96-5	Ash Analysis	1.29E-06		3.10	E-05	7.3	7E-03		
Mercury	7439-97-6	Ash Analysis	3.86E-09		9.27E-08		2.21E-05			
Nickel	7440-02-0	Ash Analysis	7.31E-07		1.76	1.76E-05		4.18E-03		
Nickel Attachments: (1) emissions calculations and emission rates) and describe how these are	supporting docum	entation; (2) indicate al	I requested s		ral enforceab	le permit limi	ts (e.g. hours	of operation,		

L WPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

## FORM B9 EMISSION SOURCE (OTHER)

REVISED 09/22/16 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate							B9
EMISSION SOURCE DESCRI	PTION: Wet	Ash Receivin	g-Transfer to Hopper		EMISSION SOURCE ID NO: F-2		
					CONTROL DEVICE ID NO(S): N/	Ά	
OPERATING SCENARIO:	1	OF	1		EMISSION POINT (STACK) ID N	O(S): FUGITIVE FEP-	2
DESCRIBE IN DETAIL THE PF	(UCL33 (A			o materi			
MATERIALS ENTE		CESS - CONT	TINUOUS PROCESS		MAX. DESIGN	REQUESTED	CAPACITY
	TYPE			UNITS	CAPACITY (UNIT/HR)	LIMITATION(	UNIT/HR)
Transfer			Tor	าร	70		70
MATERIALS EN		OCESS - BA	ATCH OPERATION		MAX. DESIGN	REQUESTED	CAPACITY
	TYPE		l	JNITS	CAPACITY (UNIT/BATCH)	LIMITATION (U	NIT/BATCH)
MAXIMUM DESIGN (BATCHE			I				
REQUESTED LIMITATION (BA		OUR):	(BA	TCHES/Y	R):		
FUEL USED: N/A					MUM FIRING RATE (MILLION BT	U/HR) <sup>,</sup> N/A	
MAX. CAPACITY HOURLY FU	EL USE: N/	A			CAPACITY ANNUAL FUEL USE:		
COMMENTS:							

# FORM B

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate						В			
EMISSION SOURCE DESCRIPTION:	Net Ash Receiv	ing-Unloading Pile		EMISSION	SOURCE I	D NO: F-3			
				CONTROL DEVICE ID NO(S): N/A					
OPERATING SCENARIO	1 OF _	1		EMISSION	POINT (ST	ACK) ID NO	D(S): FUGIT	IVE FEP-3	
DESCRIBE IN DETAILTHE EMISSION Unloading Pile Windblown Fugitive Dus		CESS (ATTACH F	LOW DIAG	RAM):					
TYPE OF EMISSION SOUR	•			FE FORM B				•	
Coal,wood,oil, gas, other burner (F								∣s/inks (Form B	
Int.combustion engine/generator (F	form B2)	Coating/finish	0. 0	,		eration (For	,		
Liquid storage tanks (Form B3)		Storage silos/	•	-	Ľ	r (Form B9)			
START CONSTRUCTION DATE: TBD				NUFACTUR					
MANUFACTURER / MODEL NO.: TBD EXPECTED OP. SCHEDULE: 24 HR/DAY 7 DAY/WK 52 WK/YR							2 WK/YR		
	ISPS (SUBPAR	/			SHAP (SUB	, –			
	. ,	EB 25 MAR NT EMISSION	R-MAY 2		UN-AUG	25	SEP-NO	V 25	
	K POLLUTA	1	-					10	
		SOURCE OF	EXPECTE				L EMISSIO		
		EMISSION			BEFORE CONT			ITROLS / LIMITS)	
		FACTOR	lb/hr 0.0049	tons/yr 0.0215	lb/hr N/A	tons/yr	lb/hr 0.0049	tons/yr	
PARTICULATE MATTER (PM) PARTICULATE MATTER<10 MICRONS	(PM )	AP-42, Chapter	0.0049	0.0215	N/A N/A	N/A N/A	0.0049	0.0215	
PARTICULATE MATTER<2.5 MICRONS	10,	11.9	0.0023	0.0043	N/A N/A	N/A	0.0023	0.0043	
SULFUR DIOXIDE (SO2)	5 (1 1012.5)		0.0010 N/A	0.0043 N/A	N/A	N/A	0.0010 N/A	0.0043 N/A	
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A	
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A	
VOLATILE ORGANIC COMPOUNDS (VOC)			N/A	N/A	N/A	N/A	N/A	N/A	
LEAD		Ash Analysis		2.73E-06	N/A	N/A	6.23E-07	2.73E-06	
OTHER			N/A	N/A	N/A	N/A	N/A	N/A	
HAZARDOUS	AIR POLLU	TANT EMISSIC	ONS INFO	RMATIC	N FOR T	HIS SOU	IRCE		
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS	
		EMISSION			BEFORE CONT			ITROLS / LIMITS)	
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr	
Arsenic	7440-38-2	Ash Analysis	5.81E-07	2.55E-06	N/A	N/A	5.81E-07	2.55E-06	
Beryllium	7440-41-7	Ash Analysis	1.2E-07	5.27E-07	N/A	N/A	1.20E-07	5.27E-07	
Cadmium	7440-43-9	Ash Analysis	1.04E-07	4.54E-07	N/A	N/A	1.04E-07	4.54E-07	
Chromium	7440-47-3	Ash Analysis	7.06E-07	3.09E-06	N/A	N/A	7.06E-07	3.09E-06	
Chromium VI	18540-29-9	Ash Analysis	7.76E-08	3.4E-07	N/A	N/A	7.76E-08	3.40E-07	
Cobalt	7440-48-4	Ash Analysis	2.82E-07	1.24E-06	N/A	N/A	2.82E-07	1.24E-06	
Manganese	7439-96-5	Ash Analysis	1.25E-06	5.45E-06	N/A	N/A	1.25E-06	5.45E-06	
Mercury	7439-97-6	Ash Analysis	3.73E-09	1.63E-08	N/A	N/A	3.73E-09	1.63E-08	
Nickel	7440-02-0	Ash Analysis	7.06E-07	3.09E-06	N/A	N/A	7.06E-07	3.09E-06	
Selenium	7782-49-2	Ash Analysis		8.36E-07	N/A	N/A	1.91E-07	8.36E-07	
TOXIC AIR	POLLUTAN	IT EMISSIONS	INFORM	IATION F	OR THIS	SOURC	E		
		SOURCE OF EMISSION	EXPECTE	D ACTUAL	EMISSIONS	SAFTER C	ONTROLS /	LIMITATIONS	
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb.	/hr	lb/o	day		lb/yr	
Arsenic	7440-38-2	Ash Analysis	5.81E-07		1.39	E-05	5.0	)9E-03	
Beryllium	7440-41-7	Ash Analysis	1.20E-07		2.89	E-06	1.0	)5E-03	
Cadmium	7440-43-9	Ash Analysis	1.04E-07		2.49E-06		9.0	9E-04	
Chromium VI	18540-29-9	Ash Analysis			1.86E-06		6.8	80E-04	
Manganese	7439-96-5	Ash Analysis			2.99	E-05		)9E-02	
Mercury	7439-97-6	Ash Analysis			8.94		3.26E-05		
Nickel	7440-02-0	Ash Analysis	7.06E-07		1.69	E-05	6.1	8E-03	
Attachments: (1) emissions calculations and	supporting docum	entation; (2) indicate	all requested	state and fee	deral enforcea	able permit lir	nits (e.g. hou	rs of operation,	

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

## FORM B9 EMISSION SOURCE (OTHER)

REVISED 09/22/16	rate	B9				
EMISSION SOURCE DESCRI	PTION: Wet Ash	Receiving-Unloading Pile	9	EMISSION SOURCE ID NO: F-	3	
				CONTROL DEVICE ID NO(S):	N/A	
OPERATING SCENARIO:				EMISSION POINT (STACK) ID		3
		GITLEW DIAGRAM). U	nicading File v	/indblown Fugitive Dust Emission:		
MATERIALS ENTERING PROCESS - CONTINUOUS PROCESS				MAX. DESIGN	REQUESTED	CAPACITY
	TYPE		UNITS	CAPACITY (UNIT/HR)	LIMITATION(	
Area			Acres	0.03 Acres	N/A	,
MATERIALS EN	TERING PROCE	ESS - BATCH OPERATIO	ON	MAX. DESIGN	REQUESTED	CAPACITY
	TYPE		UNITS	CAPACITY (UNIT/BATCH)	LIMITATION (U	NIT/BATCH)
			-			
			-			
			-			
MAXIMUM DESIGN (BATCHE REQUESTED LIMITATION (B/		<u></u>	(BATCHES/	VD).		
``````````````````````````````````````		<u>.</u>				
FUEL USED: N/A MAX. CAPACITY HOURLY FU				(IMUM FIRING RATE (MILLION B D CAPACITY ANNUAL FUEL US		
COMMENTS:	JEE 03E. N/A		REQUESTE	D CAPACITY ANNOALT OLL US	N/A	

# FORM B

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDE	Q/Division of /	Air Quality - Applica	ation for Air	Permit to	Construct/0	Operate		В
EMISSION SOURCE DESCRIPTION: A	sh Basin			EMISSION SOURCE ID NO: F-4				
				CONTROL	DEVICE ID	NO(S): N/	4	
OPERATING SCENARIO1	OF _	1		EMISSION	POINT (ST	ACK) ID NO	D(S): FUGIT	IVE FEP-4
DESCRIBE IN DETAILTHE EMISSION Dust may be generated by wind erosion		•		AM):				
TYPE OF EMISSION SOUR	CE (CHECK A	ND COMPLETE AP	PROPRIAT	E FORM B	1-B9 ON TH	E FOLLOW	ING PAGE	S):
└ Coal,wood,oil, gas, other burner (Fo	rm B1)	Woodworking (	Form B4)					∣s/inks (Form B
□ Int.combustion engine/generator (Fo	orm B2)	Coating/finishin	<b>.</b> .	,		eration (For	,	
Liquid storage tanks (Form B3)		Storage silos/bi	ins (Form B	6)	✓ Othe	r (Form B9)		
START CONSTRUCTION DATE: N/A			DATE MAN	NUFACTUR	ED: N/A			
MANUFACTURER / MODEL NO.: N/A			EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
IS THIS SOURCE SUBJECT 🛛 NS	SPS (SUBPAR	ΓS?):			SHAP (SUBI	PARTS?):_		
PERCENTAGE ANNUAL THROUGHPL	. ,				N-AUG	25	SEP-NOV	25
CRITERIA AI	R POLLUT	ANT EMISSION	S INFOR	MATION	FOR THI	S SOUR	CE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONTI	ROLS / LIMITS)	SEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		AP-42	0.507	2.222	N/A	N/A	0.507	2.222
PARTICULATE MATTER<10 MICRONS (	PM <sub>10</sub> )	AP-42	0.254	1.111	N/A	N/A	0.254	1.111
PARTICULATE MATTER<2.5 MICRONS	(PM <sub>2.5</sub> )	AP-42	0.038	0.167	N/A	N/A	0.038	0.167
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (VOC)			N/A	N/A	N/A	N/A	N/A	N/A
LEAD		Ash Analysis	6.44E-05	2.82E-04	N/A	N/A	6.44E-05	2.82E-04
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS	AIR POLLU	TANT EMISSIO	NS INFO	RMATIO	N FOR TI	HIS SOU	RCE	
		SOURCE OF	EXPECTE				L EMISSIO	
	0.00.00	EMISSION			BEFORE CONT			ITROLS / LIMITS)
	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis			N/A	N/A	6.01E-05	2.63E-04
Beryllium	7440-41-7	Ash Analysis			N/A	N/A	1.25E-05	5.45E-05
Cadmium	7440-43-9	Ash Analysis	1.07E-05		N/A	N/A	1.07E-05	4.70E-05
Chromium	7440-47-3	,				N/A		3.20E-04
Chromium VI	18540-29-9	Ash Analysis			N/A	N/A	8.03E-06	3.52E-05
Cobalt	7440-48-4	Ash Analysis			N/A	N/A	2.92E-05	1.28E-04
Manganese	7439-96-5	Ash Analysis			N/A	N/A	1.29E-04	5.64E-04
Mercury Nickel	7439-97-6	Ash Analysis			N/A	N/A	3.86E-07 7.30E-05	1.69E-06
	7440-02-0 7782-49-2	Ash Analysis			N/A	N/A		3.20E-04
		Ash Analysis				N/A	1.98E-05	8.65E-05
	POLLUTAN	T ENIISSICINS				SUURCE		
		SOURCE OF EMISSION	EXPECTE	D ACTUAL	EMISSIONS	SAFTER C	ONTROLS	LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb/	/hr	lb/c	day		lb/yr
Arsenic	7440-38-2	Ash Analysis			1.44	E-03	5.2	27E-01
Beryllium	7440-41-7	Ash Analysis	1.25E-05		2.99	E-04	1.0	)9E-01
Cadmium	7440-43-9	Ash Analysis			2.58	E-04	9.4	0E-02
Chromium VI	18540-29-9	Ash Analysis	8.03E-06		1.93	E-04	7.(	)3E-02
Manganese	7439-96-5	Ash Analysis	1.29E-04		3.09	E-03	1.1	3E+00
Mercury	7439-97-6	Ash Analysis	3.86E-07		9.25	E-06	3.3	88E-03
Nickel	7440-02-0	Ash Analysis	7.30E-05		1.75	E-03	6.4	I0E-01
						le permit limi		

emission rates) and describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

WPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

## FORM B9 EMISSION SOURCE (OTHER)

REVISED 09/22/16			n of Air Quality -	Application	for Air Permit to Construct/Ope	rate	B9
EMISSION SOURCE DESCRI	PTION: Ash B	asin			EMISSION SOURCE ID NO: F-	4	
					CONTROL DEVICE ID NO(S):	N/A	
OPERATING SCENARIO: _	1	OF	1		EMISSION POINT (STACK) ID	NO(S): FUGITIVE FEP-	4
DESCRIBE IN DETAIL THE PI	ROCESS (AT	TACH FLOW	DIAGRAM). Du	st may be ger	nerated by wind erosion of expose		a facinty.
MATERIALS ENTI					MAX. DESIGN	REQUESTED	
MATERIALS ENT	TYPE			UNITS	CAPACITY (UNIT/HR)	LIMITATION	
Active Basin Area				Acres	67 Acres	N/A	
				, 10.00			
MATERIALS EN	TERING PRO	CESS - BA	TCH OPERATIO	N	MAX. DESIGN	REQUESTED	CAPACITY
	TYPE			UNITS	CAPACITY (UNIT/BATCH)	LIMITATION (U	NIT/BATCH)
MAXIMUM DESIGN (BATCHE	S / HOUR):			1			
REQUESTED LIMITATION (B	ATCHES / HO	UR):		(BATCHES/	YR):		
FUEL USED: N/A				TOTAL MAX	IMUM FIRING RATE (MILLION B	TU/HR): N/A	
MAX. CAPACITY HOURLY FL				REQUESTE	D CAPACITY ANNUAL FUEL US	E: N/A	
COMMENTS: Maximum ash	throughput = 4	130,000 ton/y	r				

# FORM B

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

		ir Quality - Applic	ation for Ai	r Permit to	Construct/	Operate		В
EMISSION SOURCE DESCRIPTION:	Ash Handling			EMISSION	SOURCE I	D NO: F-5		
				CONTROL	DEVICE ID	NO(S): N/	4	
OPERATING SCENARIO	1 OF _	1		EMISSION	POINT (ST	ACK) ID NO	D(S): FUGIT	IVE FEP-4
DESCRIBE IN DETAILTHE EMISSION Emissions from the handling of materia		•	LOW DIAG	RAM):				
TYPE OF EMISSION SOUR	RCE (CHECK AN	ND COMPLETE AP	PROPRIAT	E FORM B	1-B9 ON TH	HE FOLLO	WING PAGE	S):
Coal,wood,oil, gas, other burner (F	orm B1)	Woodworking	(Form B4)		🗌 Manu	uf. of chemi	cals/coating	s/inks (Form E
Int.combustion engine/generator (F	Form B2)	Coating/finish	ing/printing	(Form B5)	🗌 Incin	eration (For	m B8)	
Liquid storage tanks (Form B3)		Storage silos/	bins (Form	B6)	🗸 Othe	r (Form B9)		
START CONSTRUCTION DATE: N/A			DATE MAN	NUFACTUR	ED: N/A			
MANUFACTURER / MODEL NO.: N/A			EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
IS THIS SOURCE SUBJECT $\ \square$ N	ISPS (SUBPAR	rs?):			SHAP (SUBI	PARTS?):_		
PERCENTAGE ANNUAL THROUGHP	UT (%): DEC-FI	EB 25 MAI	R-MAY 2	5 J	UN-AUG	25	SEP-NO	V 25
CRITERIA A	IR POLLUTA	NT EMISSION	IS INFOR	MATION	FOR TH	IS SOUR	CE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONTI	ROLS / LIMITS)	BEFORE CONT	ROLS / LIMITS	(AFTER CON	TROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		AP-42	0.086	0.376	N/A	N/A	0.086	0.376
PARTICULATE MATTER<10 MICRONS	(PM <sub>10</sub> )	AP-42	0.041	0.178	N/A	N/A	0.041	0.178
PARTICULATE MATTER<2.5 MICRONS	6 (PM <sub>2.5</sub> )	AP-42	0.006	0.027	N/A	N/A	0.006	0.027
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (VOC)			N/A	N/A	N/A	N/A	N/A	N/A
LEAD		Ash Analysis	1.09E-05	4.77E-05	N/A	N/A	1.09E-05	4.77E-05
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS	AIR POLLUT	TANT EMISSIC	DNS INFC	ORMATIC	N FOR T	'HIS SOU	IRCE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONTI	ROLS / LIMITS)	BEFORE CONT	ROLS / LIMITS	(AFTER CON	TROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
Arsenic	7440-38-2	Ash Analysis	1.02E-05	4.45E-05	N/A	N/A	1.02E-05	4.45E-05
Beryllium	7440-41-7	Ash Analysis	2.11E-06	9.22E-06	N/A	N/A	2.11E-06	9.22E-06
Cadmium	7440-43-9	Ash Analysis	1.81E-06	7.95E-06	N/A	N/A	1.81E-06	7.95E-06
Chromium	7440-47-3	Ash Analysis	1.23E-05	5.41E-05	N/A	N/A	1.23E-05	5.41E-05
Chromium VI	18540-29-9	Ash Analysis	1.36E-06	5.95E-06	N/A	N/A	1.36E-06	5.95E-06
Cobalt	7440-48-4	Ash Analysis	4.94E-06	2.16E-05	N/A	N/A	4.94E-06	2.16E-05
Manganese	7439-96-5	Ash Analysis	2.18E-05	9.54E-05	N/A	N/A	2.18E-05	9.54E-05
Mercury	7439-97-6	Ash Analysis	6.52E-08	2.85E-07	N/A	N/A	6.52E-08	2.85E-07
Nickel	7440-02-0	Ash Analysis	1.23E-05	5.41E-05	N/A	N/A	1.23E-05	5.41E-05
Selenium	7782-49-2	Ash Analysis	3.34E-06	1.46E-05	N/A	N/A	3.34E-06	1.46E-05
TOXIC AIR	POLLUTAN	T EMISSIONS	INFORM	ATION F	OR THIS	SOURC	E	
		SOURCE OF EMISSION	EXPECTE	D ACTUAL	EMISSIONS	S AFTER C	ONTROLS /	LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	FACTOR	lb,	/hr	lb/c	day		b/yr
Arsenic	7440-38-2	Ash Analysis	1.02E-05		2.44	E-04	8.9	0E-02
Beryllium	7440-41-7	Ash Analysis	2.11E-06		5.05	E-05	1.8	4E-02
Cadmium	7440-43-9	Ash Analysis	1.81E-06		4.36	E-05	1.5	9E-02
Chromium VI	18540-29-9	Ash Analysis	1.36E-06		3.26E-05		1.1	9E-02
Manganese	7439-96-5	Ash Analysis	2.18E-05		5.23	E-04	1.9	1E-01
Mercury	7439-97-6	Ash Analysis	6.52E-08		1.56	E-06	5.7	1E-04

IPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOU

# FORM B9 EMISSION SOURCE (OTHER)

	n of Air Quality - Application f	or Air Permit to Construct/Operat	e	B9
EMISSION SOURCE DESCRIPTION: Ash Handling		EMISSION SOURCE ID NO: F-5		
		CONTROL DEVICE ID NO(S): N/A	ł	
OPERATING SCENARIO:1 OF	1	EMISSION POINT (STACK) ID NO		4
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW	DIAGRAM): Emissions from th	e handling of material at an industri	al site.	
MATERIALS ENTERING PROCESS - CONT	UNITS	MAX. DESIGN	REQUESTED	
TYPE		CAPACITY (UNIT/HR)		JNII/HK)
Ash throughput	Tons	49.09	N/A	
MATERIALS ENTERING PROCESS - BA	TCH OPERATION	MAX. DESIGN	REQUESTED	CAPACITY
ТҮРЕ	UNITS	CAPACITY (UNIT/BATCH)	LIMITATION (UN	NIT/BATCH)
MAXIMUM DESIGN (BATCHES / HOUR):				
REQUESTED LIMITATION (BATCHES / HOUR):	(BATCHES/Y	R):		
FUEL USED: N/A		MUM FIRING RATE (MILLION BTU	//HR): N/A	
MAX. CAPACITY HOURLY FUEL USE: N/A		CAPACITY ANNUAL FUEL USE: I		
COMMENTS: Maximum ash throughput = 430,000 ton/yr				

# FORM B

### SPECIFIC EMISSION SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 09/22/1 NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate						В		
EMISSION SOURCE DESCRIPTION: Ha	aul Roads			EMISSION SOURCE ID NO: F-6				
					DEVICE ID		Ą	
OPERATING SCENARIO1_	OF	1			POINT (ST	( )		IVE FEP-4
DESCRIBE IN DETAILTHE EMISSION S A portion of the ash will be moved by truc wheels on the road surface. This force ca wheels and the road surface is exposed to	k to an offsite auses pulveriz o strong air cu	location. Partic ation of the surf irrents, which ge	ulate emiss ace materia nerate airb	IAGRAM): ions are gen al. The parti orne particu	nerated from cles are lifte late emissio	n the haul ro ad and drop ons.	bads from the	e force of the e rolling
TYPE OF EMISSION SOURCE	•	_						
Coal,wood,oil, gas, other burner (For	,	U Woodwork	0 (	,			0	s/inks (Form B
<ul> <li>Int.combustion engine/generator (For</li> <li>Liquid storage tanks (Form B3)</li> </ul>	m B2)	0	ishing/printi os/bins (Fo	ing (Form B rm B6)		eration (For r (Form B9)	,	
START CONSTRUCTION DATE: N/A			DATE MAN	NUFACTUR	ED: N/A			
MANUFACTURER / MODEL NO.: N/A			EXPECTE	D OP. SCH	EDULE: 24	HR/DAY 7	DAY/WK 5	2 WK/YR
IS THIS SOURCE SUBJECT	PS (SUBPAR	TS?):			HAP (SUB	PARTS?):		
PERCENTAGE ANNUAL THROUGHPU	T (%): DEC-F	EB 25 M	/AR-MAY	25	JUN-AUG	25	SEP-I	NOV 25
CRITERIA AIR I	POLLUTAI	NT EMISSIO	NS INFO	RMATIO	N FOR T	HIS SOU	RCE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONT	ROLS / LIMITS	EFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)
AIR POLLUTANT EMITTED		FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
PARTICULATE MATTER (PM)		Section 13.2.2 (Unpaved	1.65E-01	-	N/A	N/A	1.65E-01	7.22E-01
PARTICULATE MATTER<10 MICRONS (P	'M <sub>10</sub> )	Roads) of the U.S. EPA's	4.26E-02	1.86E-01	N/A	N/A	4.26E-02	1.86E-01
PARTICULATE MATTER<2.5 MICRONS (F	PM <sub>2.5</sub> )	AP-42	4.26E-03	1.87E-02	N/A	N/A	4.26E-03	1.87E-02
SULFUR DIOXIDE (SO2)			N/A	N/A	N/A	N/A	N/A	N/A
NITROGEN OXIDES (NOx)			N/A	N/A	N/A	N/A	N/A	N/A
CARBON MONOXIDE (CO)			N/A	N/A	N/A	N/A	N/A	N/A
VOLATILE ORGANIC COMPOUNDS (VOC)			N/A	N/A	N/A	N/A	N/A	N/A
LEAD			N/A	N/A	N/A	N/A	N/A	N/A
OTHER			N/A	N/A	N/A	N/A	N/A	N/A
HAZARDOUS AIF	R POLLUT/	ANT EMISSI	ONS INF	ORMATI	ON FOR	THIS SO	URCE	
		SOURCE OF	EXPECTE	D ACTUAL		POTENTIA	L EMISSIO	NS
		EMISSION	AFTER CONT	ROLS / LIMITS	SEFORE CONT	ROLS / LIMITS	(AFTER CON	ITROLS / LIMITS)
HAZARDOUS AIR POLLUTANT	CAS NO.	FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	lb/hr	tons/yr
N/A								
TOXIC AIR PO	OLLUTANI	EMISSION	S INFOR	MATION	FOR TH	S SOUR	CE	
		SOURCE OF						LIMITATIONS
TOXIC AIR POLLUTANT	CAS NO.	EMISSION FACTOR	lb	/hr	lb/d	lay		lb/yr
N/A								
Attachments: (1) emissions calculations and su operation, emission rates) and describe how th								
				. ,		-		•

<sup>2</sup>LETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SO Attach Additional Sheets As Necessary

### FORM B9 EMISSION SOURCE (OTHER)

				<b>D</b> 0
	ity - Application for	or Air Permit to Construct/Opera	te	B9
EMISSION SOURCE DESCRIPTION: Haul Roads		EMISSION SOURCE ID NO: F-6		
		CONTROL DEVICE ID NO(S): N/	A	
OPERATING SCENARIO:1 OF1		EMISSION POINT (STACK) ID N		
DESCRIBE IN DETAIL THE PROCESS (ATTACH FLOW DIAGRAM): generated from the haul roads from the force of the wheels on the road and dropped from the rolling wheels and the road surface is exposed to	d surface. This for	ce causes pulverization of the surfa	ace material. The part	
MATERIALS ENTERING PROCESS - CONTINUOUS PRO	OCESS	MAX. DESIGN	REQUESTED	
TYPE	UNITS	CAPACITY (UNIT/HR)	LIMITATION(	
htt L				UNITIN
		+		
		++		
		+		
		+ +		
		+ +		
		1		
MATERIALS ENTERING PROCESS - BATCH OPERA	TION	MAX. DESIGN	REQUESTED	CAPACITY
ТҮРЕ	UNITS	CAPACITY (UNIT/BATCH)	LIMITATION (U	NIT/BATCH)
MAXIMUM DESIGN (BATCHES / HOUR):				
REQUESTED LIMITATION (BATCHES / HOUR):	(BATCHES/Y	R):		
FUEL USED: N/A	TOTAL MAXI	MUM FIRING RATE (MILLION BTU	J/HR): N/A	
MAX. CAPACITY HOURLY FUEL USE: N/A	REQUESTED	CAPACITY ANNUAL FUEL USE:	N/A	
COMMENTS: Haul Roads- Max loading throughput = 101,191 lbs and	Max unloading thr	roughput = 51,191 lbs.		

### FORM D1 FACILITY-WIDE EMISSIONS SUMMARY

	Division of Air Qualit						D1		
CRITERIA	A AIR POLLUTANT	EMISSIONS	<b>INFORMATI</b>	ON - FACILITY	WIDE				
		EMIS (AFTER C	ED ACTUAL SIONS ONTROLS / ATIONS)	POTENTIAL (BEFORE CO LIMITA	ONTROLS /	(AFTER C	L EMISSION ONTROLS / ATIONS)		
AIR POLLUTANT EMITTED			ns/yr	tons/yr			ns/yr		
PARTICULATE MATTER (PM)			6.09	N/	•		6.09		
PARTICULATE MATTER < 10 MICRONS ( $PM_{10}$ )		212.43		N/			2.43		
PARTICULATE MATTER < 2.5 MICRONS (PM <sub>2.5</sub> )			3.48	N/		19	3.48		
		272.73		N/		27	2.73		
NITROGEN OXIDES (NOx)			3.17	N/			3.17		
CARBON MONOXIDE (CO)			6.47	N/			6.47		
VOLATILE ORGANIC COMPOUNDS (VOC)			5.70	N/			5.70		
			.02	N/			.02		
GREENHOUSE GASES (GHG) (SHORT TONS)			5,682	N/			.02		
OTHER		2,70	5,002	11/	~	2,10	5,002		
	JS AIR POLLUTAN	NT EMISSION	NS INFORMA	LION - FACILIT	Y-WIDE				
			DACTUAL			1			
		EMIS (AFTER C	SIONS ONTROLS /	POTENTIAL (BEFORE CO LIMITA	ONTROLS /	(AFTER C	L <b>EMISSION</b> ONTROLS / ATIONS)		
HAZARDOUS AIR POLLUTANT EMITTED	CAS NO.	tor	ns/yr	tons	s/yr	to	ns/yr		
Benzene	71-43-2	2.22	2E-01	N/	A	2.2	2E-01		
Formaldehyde	50-00-0	3.97	'E+00	N/A		3.97E+00			
Hexane	110-54-3	2.29	)E+00	N/A		N/A		2.29E+	
Naphthalene	91-20-3	1.78E-03 N/A		N/A		1.7	3E-03		
Toluene	108-88-3	1.16E+00 N/A		1.16E+0					
Arsenic	7440-38-2	1.02E-02 N/A		1.0	2E-02				
Beryllium	7440-41-7	1.44E-03		N/	A	1.4	4E-03		
Cadmium	7440-43-9		9E-02	N/			9E-02		
Chromium	7440-47-3	7.20	)E-03	N/	A	7.2	DE-03		
Chromium VI	18540-29-9	2.24	4E-03	N/A		2.2	4E-03		
Cobalt	7440-48-4	2.76E-03		N/A		2.76E-03			
Manganese	7439-96-5		3E-02	N/A			3E-02		
Mercury	7439-97-6		9E-03	N/A		3.99E-03			
Nickel	7440-02-0	5.52E-02		N/A			2E-02		
Selenium	7782-49-2	1.86E-03		N/A		1.86E-03			
Xylene	1330-20-7		5E-04	N/		3.45E-			
1,3-Butadiene	106-99-0		4E-05	N/			4E-05		
Acetaldehvde	75-07-0		9E-04	N/			9E-04		
Acrolein	107-02-8		7E-02	N/			7E-02		
Total PAH (exclude Naphthalene)	101 02 0		IE-04	N/			1E-04		
	AIR POLLUTANT E								
NDICATE REQUESTED ACTUAL EMISSIONS AF	TER CONTROLS / LI	MITATIONS. I	EMISSIONS AB	OVE THE TOXIC	PERMIT EMIS	SION RATE (T	PER) IN 15A		
NCAC 2Q .0711 MAY REQUIRE AIR DISPERSION	MODELING. USE N	IETTING FORI	M D2 IF NECES	SARY.					
			-		Modeling	Required ?			
TOXIC AIR POLLUTANT EMITTED	CAS NO.	lb/hr	lb/day	lb/year	Yes	No			
Sulfuric Acid Mist	7664-93-9	3.50	84.00		Х				
Benzene	71-43-2			444.93	Х				
Formaldehyde	50-00-0	0.91			Х				
Hexane	110-54-3		12.538			Х			
Toluene	108-88-3	0.26	62.149			Х			
Arsenic	7440-38-2			20.34	Х				
Beryllium	7440-41-7			2.89	Х				
Cadmium	7440-43-9			51.89	Х				
Chromium VI	18540-29-9		0.012		Х				
Manganese	7439-96-5		0.117			Х			
	1		0.022		х		T		
Mercury	7439-97-6		0.022						

For modeling purposes toxic air pollutant facility wide emissions include emissions from the STAR facility and the Combined Cycle facility. TAPS from diesel engines (ES-82B and ES-83B) were not included in the TPER analysis per 15A NCAC 2Q.0702 (a)(27). Chromium VI total emission is less than TPER, but to be conservative it is still modeled because the emissions are very close to the threshold.

### AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

REVISED 09/22/16	NCDEQ/Division of Air Quality - A	pplication for Air Permit to Construct/C	Operate D2
PURPOSE OF NETTING: AIR TO	)XICS		
TOXIC AIR POLLUTANT:	Sulfuric Acid Mist	CAS NO.: 7664-93-9	
EMISSION SOURCE ID NOS .:	ES-74, ES-11, ES-12, ES-14		
SECTIO	ON A - EMISSION OFFSETTING	G ANALYSIS FOR MODIFIED/NI	EW SOURCES
Summarize in this section	EMI	ISSIONS - USE APPROPRIATE COLUM	NS ONLY
using the B forms	LB/YEAR	LB/DAY	LB/HR
MODIFICATION	N/A		
INCREASE	1973		
- MINUS -	- MINUS -	- MINUS -	- MINUS -
MODIFICATION	N/A	T	T
DECREASE	1		
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =
NET CHANGE	N/A		
FROM MODIFICATION			
	SECTION B - FACILITY-WI	DE EMISSION NETTING ANALY	'SIS
CREDITABLE			
INCREASE			
- MINUS -	- MINUS -	- MINUS -	- MINUS -
CREDITABLE		T	T
DECREASE			
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =
NET CREDITABLE		T	T
CHANGE			
	SECTION C - FA	CILITY-WIDE EMISSIONS	
TOTAL FACILITY	N/A	84	3.50
EMISSIONS			0.00
TPER LEVELS (2Q .0711)	N/A	0.25	0.25
Are the total facility-wide emissions	s less than the TPER levels?:	YES 🗹	NO
If YES, no further analysis is requir			
		on level is greater than the 2Q .0711 Toxic 15A NCAC 2Q .0702(a)(27) "Exemptions".	
	SION MODELING ANALYSIS IS REQU		
	is required, complete the stack paramet	lers section of Form D3-1 for each emission	on source that emits this TAP. Review the
modeling plan requirements. COMMENTS:			

### AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

REVISED 09/22/16	NCDEQ/Division of Air Quality - A	pplication for Air Permit to Construct/	/Operate D2			
PURPOSE OF NETTING: AIR TO	IXICS					
TOXIC AIR POLLUTANT:	Benzene	CAS NO.: 71-43-2				
EMISSION SOURCE ID NOS .:	ES-74, ES-11, ES-12, ES-14					
SECTIO	NA - EMISSION OFFSETTING	G ANALYSIS FOR MODIFIED/N	NEW SOURCES			
Summarize in this section	EMI	ISSIONS - USE APPROPRIATE COLUN	MNS ONLY			
using the B forms	LB/YEAR	LB/DAY	LB/HR			
MODIFICATION		N/A	N/A			
INCREASE	l	IW// \				
- MINUS -	- MINUS -	- MINUS -	- MINUS -			
MODIFICATION		N/A	N/A			
DECREASE						
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =			
NET CHANGE		N/A	N/A			
FROM MODIFICATION						
	SECTION B - FACILITY-WI	DE EMISSION NETTING ANAL	YSIS			
CREDITABLE		T				
INCREASE	l					
- MINUS -	- MINUS -	- MINUS -	- MINUS -			
CREDITABLE						
DECREASE	l					
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =			
NET CREDITABLE						
CHANGE						
	SECTION C - FAC	CILITY-WIDE EMISSIONS				
TOTAL FACILITY	445	N/A	N/A			
EMISSIONS	ى <del>ب</del> ت	IW// X				
TPER LEVELS (2Q .0711)	8.1	N/A	N/A			
Are the total facility-wide emissions	less than the TPER levels?:	YES 🗸	] NO			
If YES, no further analysis is require						
		on level is greater than the 2Q .0711 Tox 15A NCAC 2Q .0702(a)(27) "Exemptions	kic Air Pollutant Permitting Emissions Rate s".			
	SION MODELING ANALYSIS IS REQU					
If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.						
COMMENTS:						

### AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

REVISED 09/22/16	NCDEQ/Division of Air Quality - Ap	oplication for Air Permit to Construct/	Operate D2			
PURPOSE OF NETTING: AIR TO	XICS					
TOXIC AIR POLLUTANT:	Formaldehyde	CAS NO.: 50-00-0				
EMISSION SOURCE ID NOS .:	ES-74, ES-11, ES-12, ES-14					
SECTIC	NA - EMISSION OFFSETTING	G ANALYSIS FOR MODIFIED/N	IEW SOURCES			
Summarize in this section	EMI	SSIONS - USE APPROPRIATE COLUM	INS ONLY			
using the B forms	LB/YEAR	LB/DAY	LB/HR			
MODIFICATION	N/A	N/A				
INCREASE						
- MINUS -	- MINUS -	- MINUS -	- MINUS -			
MODIFICATION	N/A	N/A				
DECREASE	1977 5					
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =			
NET CHANGE	N/A	N/A				
FROM MODIFICATION						
	SECTION B - FACILITY-WI	DE EMISSION NETTING ANAL	YSIS			
CREDITABLE						
INCREASE						
- MINUS -	- MINUS -	- MINUS -	- MINUS -			
CREDITABLE						
DECREASE						
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =			
NET CREDITABLE		T				
CHANGE						
	SECTION C - FAC	CILITY-WIDE EMISSIONS				
TOTAL FACILITY	N/A	N/A	0.91			
EMISSIONS			· -			
TPER LEVELS (2Q .0711)	N/A	N/A	0.04			
Are the total facility-wide emissions	eless than the TPER levels?:	YES 🗹	NO			
If YES, no further analysis is requir						
		on level is greater than the 2Q .0711 Toxi I5A NCAC 2Q .0702(a)(27) "Exemptions"	ic Air Pollutant Permitting Emissions Rate ".			
	SION MODELING ANALYSIS IS REQU					
If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the						
modeling plan requirements. COMMENTS:						

### AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

REVISED 09/22/16	NCDEQ/Division of Air Quality - A	pplication for Air Permit to Construct/Operation	ate D2
PURPOSE OF NETTING: AIR TOXIC	CS		
TOXIC AIR POLLUTANT: Ar	rsenic	CAS NO.: 7440-38-2	
E EMISSION SOURCE ID NOS.:	S-11, ES-12, ES-14, ES-73A, ES-73	3B, ES-74, ES-77, ES-78, ES-79A, ES-79B, E ES-82A, ES-83A, F-1, F-2, F-3, F-4, F-5	S-80A, ES-80B, ES-81, ES-81A, ES-81B,
SECTION	NA - EMISSION OFFSETTI	NG ANALYSIS FOR MODIFIED/NEV	N SOURCES
Summarize in this section	E	MISSIONS - USE APPROPRIATE COLUMNS	ONLY
using the B forms	LB/YEAR	LB/DAY	LB/HR
MODIFICATION		N/A	N/A
INCREASE		N/A	N/A
- MINUS -	- MINUS -	- MINUS -	- MINUS -
MODIFICATION		N/A	N/A
DECREASE	_		
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =
NET CHANGE		N/A	N/A
FROM MODIFICATION			
	SECTION B - FACILITY-W	VIDE EMISSION NETTING ANALYS	IS
CREDITABLE		1	
INCREASE			
- MINUS -	- MINUS -	- MINUS -	- MINUS -
CREDITABLE		1	
DECREASE			
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =
NET CREDITABLE		1	
CHANGE			
	SECTION C - F/	ACILITY-WIDE EMISSIONS	
TOTAL FACILITY	20.34	N/A	N/A
EMISSIONS		4	
TPER LEVELS (2Q .0711)	0.053	N/A	N/A
Are the total facility-wide emissions le		YES IN	NO
If YES, no further analysis is required.		ion level is greater than the 2Q .0711 Toxic Air	Dill test Descritting Emissions Data
		ION level is greater than the 2Q .0711 Toxic Air 15A NCAC 2Q .0702(a)(27) "Exemptions".	Pollutant Permitting Emissions Rate
CHECK HERE IF AN AIR DISPERSIC			
		eters section of Form D3-1 for each emission s	source that emits this TAP. Review the
COMMENTS:			

### AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

PURPOSE OF NETTING: AIR TOXICS           TOXIC AIR POLLUTANT:         Berylium:         CAS NO: 7440-41-7           Existion SOURCE ID NO:         Existication Science State	REVISED 09/22/16	NCDEQ/Division of Air Quality - App	Dication for Air Permit to Construct/Ope	rate D2		
E8-11, ES-12, ES-14, ES-73B, ES-73B, ES-73B, ES-73B, ES-73B, ES-80B, ES-81, ES-81A, ES-81B ES-82A, ES-83B, F-1, F-2, F-3, F-4, F-5         SECTION A - EMISSION OFFSETTING ANALYSIS FOR MODIFIEDNEW SOURCES         Summarize in this section using the B forms       LB/YEAR       LB/DAY       LB/HR         MODIFICATION INCREASE       N/A       N/A       N/A         MODIFICATION INCREASE       N/A       N/A       N/A         MODIFICATION INCREASE       N/A       N/A       N/A         MODIFICATION INCREASE       N/A       N/A       N/A         MODIFICATION INCREASE       - MINUS MI	PURPOSE OF NETTING: AIR TO	XICS				
EMISSION SOURCE ID NOS:       ES-82A, ES-83A, F-1, F-2, F-3, F-4, F-5         SECTION A - EMISSION OFFSETTING ANALYSIS FOR MODIFICED/NEW SOURCES         Summarize in this section       EMISSIONS - USE APPROPRIATE COLUMNS ONLY         using the B forms       LB/YEAR       LB/DAY         MODIFICATION       N/A       N/A         MODIFICATION       N/A       N/A         MODIFICATION       N/A       N/A         DECREASE       N/A       N/A         MODIFICATION       N/A       N/A         DECREASE       N/A       N/A         FROM MODIFICATION       N/A       N/A         MET CHANGE       N/A       N/A         FROM MODIFICATION       N/A       N/A         SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS       CREDITABLE         INCREASE       N/A       N/A         - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -         CREDITABLE       E       EQUALS = <td colspan="5">TOXIC AIR POLLUTANT: Beryllium CAS NO.: 7440-41-7</td>	TOXIC AIR POLLUTANT: Beryllium CAS NO.: 7440-41-7					
Summarize in this section using the B forms         EMISSIONS - USE APPROPRIATE COLUMNS ONLY           MODIFICATION INCREASE         LB/YEAR         LB/DAY         LB/HR           MODIFICATION INCREASE         N/A         N/A         N/A           - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MODIFICATION DECREASE         N/A         N/A         N/A           = EQUALS =         = EQUALS =         = EQUALS =         = EQUALS =           NET CHANGE         N/A         N/A         N/A           SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS         - MINUS -         - MINUS -           CREDITABLE         INCREASE         -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MI	EMISSION SOURCE ID NOS.:	ES-11, ES-12, ES-14, ES-73A, ES-73E				
Summarize in this section using the B forms         EMISSIONS - USE APPROPRIATE COLUMNS ONLY           MODIFICATION INCREASE         LB/YEAR         LB/DAY         LB/HR           MODIFICATION INCREASE         N/A         N/A         N/A           - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MODIFICATION DECREASE         N/A         N/A         N/A           = EQUALS =         = EQUALS =         = EQUALS =         = EQUALS =           NET CHANGE         N/A         N/A         N/A           SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS         - MINUS -         - MINUS -           CREDITABLE         INCREASE         -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MI	SECTI	ON A - EMISSION OFFSETTING	G ANALYSIS FOR MODIFIED/NE	W SOURCES		
using the B forms         LBYEAR         LB/DAY         LB/HR           MODIFICATION NCREASE         N/A         N/A         N/A           - MINUS -         - MINUS -         - MINUS -         - MINUS -           - MINUS -         - MINUS -         - MINUS -         - MINUS -           MODIFICATION DECREASE         N/A         N/A         N/A           = EQUALS =         = EQUALS =         = EQUALS =         = EQUALS =           NET CHANCE FROM MODIFICATION         N/A         N/A         N/A           SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS         SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS           CREDITABLE INCREASE         -         -         MINUS -         -           - NINUS -         -         -         MINUS -         -         MINUS -           - NINUS -         -         -         -         MINUS -         -         MINUS -           - NINUS -         -         -         -         MINUS -         -         MINUS -         -         MINUS -           - MINUS -         -         -         -         MINUS -         -         MINU						
INCREASE       N/A       N/A         · MINUS ·       · MINUS ·       · MINUS ·       · MINUS ·         MODIFICATION       N/A       N/A       N/A         DECREASE       = EQUALS =       = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NA       N/A       N/A       N/A         MET CHANGE       N/A       N/A       N/A         FROM MODIFICATION       SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS       CREDITABLE         CREDITABLE       N/A       N/A       N/A         INCREASE       - MINUS ·       - MINUS ·       - MINUS ·         · MINUS ·       - MINUS ·       - MINUS ·       - MINUS ·         CREDITABLE	using the B forms					
INCREASE       - MINUS -       - MINUS -       - MINUS -       - MINUS -         MODIFICATION       N/A       N/A       N/A         DECREASE       - EQUALS =       = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CHANGE       N/A       N/A       N/A         FROM MODIFICATION       N/A       N/A       N/A         SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS         CREDITABLE       N/A       N/A         INCREASE       -       -       MINUS -         - MINUS -       - MINUS -       - MINUS -       -         CREDITABLE       -       -       -       MINUS -         OCREDITABLE       -       -       -       MINUS -         OCREDITABLE       -       -       -       MINUS -         TOTAL FACILITY       2.89       N/A       N/A         TOTAL FACILITY       2.89       N/A       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         Ard spersion modeling analysis is required.       -       YES       NO         If YES, no further analysis is required.       -       -       -     <	MODIFICATION					
MODIFICATION DECREASE       N/A       N/A         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CHANGE FROM MODIFICATION       N/A       N/A       N/A         SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS         CREDITABLE INCREASE         - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -         CREDITABLE DECREASE	INCREASE		N/A	N/A		
DECREASE       N/A       N/A         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CHANGE       N/A       N/A       N/A         FROM MODIFICATION       N/A       N/A       N/A         SECTION B - FACILITY-WIJE EMISSION NETTING ANALYSIS         CREDITABLE       N/A       N/A         INCREASE       - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -       - MINUS -         - CREDITABLE       DECREASE       -       = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CREDITABLE       -       -       -       -         DECREASE       -       -       -       -       -         - FOUALS =       = EQUALS =       = EQUALS =       = EQUALS =       -       -       -         - WHY       2.89       N/A       N/A       N/A       N/A       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       - <td>- MINUS -</td> <td>- MINUS -</td> <td>- MINUS -</td> <td>- MINUS -</td>	- MINUS -	- MINUS -	- MINUS -	- MINUS -		
DECREASE       = EQUALS =       = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CHANGE       N/A       N/A       N/A         FROM MODIFICATION       SECTION B - FACILITY-WIJE EMISSION NETTING ANALYSIS         CREDITABLE       NINCREASE       NINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -       - MINUS -         CREDITABLE       DECREASE       -       -         DECREASE       -       -       -         - EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CREDITABLE       -       -       -       -         DECREASE       -       -       -       -       -         MARE       -       EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CREDITABLE       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       - <td< td=""><td>MODIFICATION</td><td></td><td>N//A</td><td>N1/A</td></td<>	MODIFICATION		N//A	N1/A		
NET CHANGE       N/A       N/A         RED MODIFICATION       SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS         CREDITABLE       INCREASE       INCREASE         - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -         CREDITABLE       INCREASE       INCREASE         - MINUS -       - MINUS -       - MINUS -         CREDITABLE       INCREASE       INCREASE         DECREASE       = EQUALS =       = EQUALS =         RET CREDITABLE       INCREASE       INCREASE         CHANGE       SECTION C - FACILITY-WIDE EMISSIONS       INCREASE         TOTAL FACILITY       2.89       N/A       N/A         TPER LEVELS (20.0711)       0.28       N/A       N/A         TPER LEVELS (20.0711)       0.28       N/A       N/A         If YES, on further analysis is required.       If viewide emissions less than the TPER levels?:       YES       NO         If YES, on further analysis is required.       If dispersion modeling analysis is required.       If dispersion modeling analysis is required.         Air dispersion modeling analysis is required.       If air dispersion modeling analysis is required.       If air dispersion modeling analysis is required.         If air dispersion modeling anal	DECREASE		N/A	N/A		
FROM MODIFICATION       N/A       N/A         SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS         CREDITABLE       INCREASE       INCREASE         - MINUS -       - MINUS -       - MINUS -         - MINUS -       - MINUS -       - MINUS -         CREDITABLE       INCREASE       INCREASE         DECREASE       INCREASE       INCREASE         - EQUALS =       = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =       = EQUALS =         NET CREDITABLE       INCREASE       INCREASE         CHANGE       INCREASE       INCREASE         TOTAL FACILITY       2.89       N/A         MINISIONS       INCA       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         If YES, no further analysis is required.       INCA       INCA       INCA         Are the total facility-wide emissions less than the TPER levels?:       YES       NO       INCA         If YES, no further analysis is required.       INCA       INCA       INCA         Are the total facility-wide emissions less than the TPER levels?:       YES       NO       INCA         If YES, no further analysis is required.       INCA       INCA       INCA <td>= EQUALS =</td> <td>= EQUALS =</td> <td>= EQUALS =</td> <td>= EQUALS =</td>	= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =		
FROM MODIFICATION       SECTION B - FACILITY-WIDE EMISSION NETTING ANALYSIS         CREDITABLE       INCREASE         INCREASE       - MINUS -         - MINUS -       - MINUS -         CREDITABLE       - MINUS -         DECREASE       - MINUS -         DECREASE       - EQUALS =         = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =         NET CREDITABLE       -         CHANGE       -         TOTAL FACILITY       2.89         N/A       N/A         TPER LEVELS (2Q.0711)       0.28         Are the total facility-wide emissions less than the TPER levels?:       YES         YES, no further analysis is required.       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES         If YES, no further analysis is required.       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES         If version modeling analysis is required.       N/A         Are the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".         CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       I         If	NET CHANGE		NI/A	NI/A		
CREDITABLE INCREASE       CREDITABLE         - MINUS -       - MINUS -         CREDITABLE DECREASE       - MINUS -         = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =         NET CREDITABLE CHANGE	FROM MODIFICATION		N/A	N/A		
INCREASE       INCUS       INCUS       INCUS       INCUS         MINUS       · MINUS       · MINUS       · MINUS       · MINUS         CREDITABLE       DECREASE       -       -       -       MINUS         DECREASE       = EQUALS =         NET CREDITABLE       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -       -		SECTION B - FACILITY-WI	DE EMISSION NETTING ANALYS	SIS		
- MINUS -       - MINUS -       - MINUS -       - MINUS -         CREDITABLE       DECREASE       -       -         DECREASE       = EQUALS =       = EQUALS =       = EQUALS =         NET CREDITABLE       CHANGE       -       -         CHANGE       SECTION C - FACILITY-WIDE EMISSIONS       -       N/A         TOTAL FACILITY       2.89       N/A       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES       NO       N/A         If YES, no further analysis is required.       -       XIC dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".         CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: CHECK HERE	CREDITABLE					
CREDITABLE       CREDITABLE         DECREASE       = EQUALS =       = EQUALS =       = EQUALS =         = EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CREDITABLE       CHANGE            CHANGE       SECTION C - FACILITY-WIDE EMISSIONS            TOTAL FACILITY       2.89       N/A       N/A          TPER LEVELS (2Q.0711)       0.28       N/A       N/A          Are the total facility-wide emissions less than the TPER levels?:       YES       NO           If YES, no further analysis is required.               Air dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".            CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	INCREASE					
DECREASE       Image: Comparison of the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".         DECREASE       Image: Comparison of the total facility for the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	- MINUS -	- MINUS -	- MINUS -	- MINUS -		
= EQUALS =       = EQUALS =       = EQUALS =       = EQUALS =         NET CREDITABLE CHANGE            CHANGE       SECTION C - FACILITY-WIDE EMISSIONS          TOTAL FACILITY EMISSIONS       2.89       N/A       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES       NO         If YES, no further analysis is required.           Air dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".         CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: Complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	CREDITABLE					
NET CREDITABLE CHANGE       District         NET CREDITABLE CHANGE       SECTION C - FACILITY-WIDE EMISSIONS         TOTAL FACILITY EMISSIONS       2.89       N/A       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES       NO         If YES, no further analysis is required.       Air dispersion modeling analysis is required.         Air dispersion modeling analysis is required.       SECTION C - GAULY SIGNER CONTROL OF CONTRO	DECREASE					
CHANGE       SECTION C - FACILITY-WIDE EMISSIONS         TOTAL FACILITY EMISSIONS       2.89       N/A       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES       NO         If YES, no further analysis is required.       VIA       VIA         Air dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".         CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: Complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =		
SECTION C - FACILITY-WIDE EMISSIONS         TOTAL FACILITY EMISSIONS       2.89       N/A       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES       NO         If YES, no further analysis is required.       VES       NO         Air dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".         CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: Complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	NET CREDITABLE					
TOTAL FACILITY EMISSIONS       2.89       N/A       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES       NO         If YES, no further analysis is required.       YES       NO         Air dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".       CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: Complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	CHANGE					
EMISSIONS       2.89       N/A       N/A         TPER LEVELS (2Q.0711)       0.28       N/A       N/A         Are the total facility-wide emissions less than the TPER levels?:       YES       NO         If YES, no further analysis is required.       YES       NO         Ari dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions".         CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED       Image: Complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.		SECTION C - FA	CILITY-WIDE EMISSIONS			
Are the total facility-wide emissions less than the TPER levels?: YES NO If YES, no further analysis is required. Air dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q.0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q.0702(a)(27) "Exemptions". CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.		2.89	N/A	N/A		
If YES, no further analysis is required. Air dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q .0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q .0702(a)(27) "Exemptions". CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	TPER LEVELS (2Q .0711)	0.28	N/A	N/A		
Air dispersion modeling analysis is required if the total facility-wide emission level is greater than the 2Q .0711 Toxic Air Pollutant Permitting Emissions Rate (TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q .0702(a)(27) "Exemptions". CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	Are the total facility-wide emissions	less than the TPER levels?:	YES 🗸	NO		
(TPER) and the source emitting the toxic air pollutant is not exempted by 15A NCAC 2Q .0702(a)(27) "Exemptions". CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.	If YES, no further analysis is require	ed.				
If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the modeling plan requirements.				ir Pollutant Permitting Emissions Rate		
modeling plan requirements.						

## AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

REVISED 09/22/16	NCDEQ/Division of Air Quality - Ap	oplication for Air Permit to Construct/Ope	erate D2		
PURPOSE OF NETTING: AIR TO	XICS				
TOXIC AIR POLLUTANT:	Cadmium	CAS NO.: 7440-43-9			
EMISSION SOURCE ID NOS .:	ES-11, ES-12, ES-14, ES-73A, ES-73	B, ES-74, ES-77, ES-78, ES-79A, ES-79B, ES-82A, ES-83A, F-1, F-2, F-3, F-4, F-	ES-80A, ES-80B, ES-81, ES-81A, ES-81B, 5		
SECTI	ON A - EMISSION OFFSETTIN	IG ANALYSIS FOR MODIFIED/NE	EW SOURCES		
Summarize in this section	EN	IISSIONS - USE APPROPRIATE COLUMN	IS ONLY		
using the B forms	LB/YEAR	LB/DAY	LB/HR		
MODIFICATION		N//A	N/A		
INCREASE		N/A	N/A		
- MINUS -	- MINUS -	- MINUS -	- MINUS -		
MODIFICATION		NI/A	N/A		
DECREASE		N/A	N/A		
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =		
NET CHANGE		N//A	N//A		
FROM MODIFICATION		N/A	N/A		
	SECTION B - FACILITY-W	IDE EMISSION NETTING ANALY	SIS		
CREDITABLE					
INCREASE					
- MINUS -	- MINUS -	- MINUS -	- MINUS -		
CREDITABLE					
DECREASE					
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =		
NET CREDITABLE					
CHANGE					
	SECTION C - FA	CILITY-WIDE EMISSIONS			
TOTAL FACILITY	54.00	N1/A	N1/A		
EMISSIONS	51.89	N/A	N/A		
TPER LEVELS (2Q .0711)	0.37	N/A	N/A		
Are the total facility-wide emissions	s less than the TPER levels?:	YES 🗸	NO		
If YES, no further analysis is requir	ed.				
		on level is greater than the 2Q .0711 Toxic a 5A NCAC 2Q .0702(a)(27) "Exemptions".	Air Pollutant Permitting Emissions Rate		
CHECK HERE IF AN AIR DISPERSION MODELING ANALYSIS IS REQUIRED					
If air dispersion modeling analysis is required, complete the stack parameters section of Form D3-1 for each emission source that emits this TAP. Review the					
modeling plan requirements. COMMENTS:					

### AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

REVISED 09/22/16	NCDEQ/Division of Air Quality - App	lication for Air Permit to Construct/Ope	erate D2		
PURPOSE OF NETTING: AIR TO	XICS				
TOXIC AIR POLLUTANT:	TOXIC AIR POLLUTANT: Chromium VI CAS NO.: 18540-29-9				
EMISSION SOURCE ID NOS.:		ES-82A, ES-83A, F-1, F-2, F-3, F-4, F-			
	ON A - EMISSION OFFSETTING	S ANALYSIS FOR MODIFIED/NE	EW SOURCES		
Summarize in this section	EMIS	SSIONS - USE APPROPRIATE COLUMN			
using the B forms	LB/YEAR	LB/DAY	LB/HR		
MODIFICATION INCREASE	N/A		N/A		
- MINUS -	- MINUS -	- MINUS -	- MINUS -		
MODIFICATION DECREASE	N/A		N/A		
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =		
NET CHANGE FROM MODIFICATION	N/A		N/A		
	SECTION B - FACILITY-WIE	DE EMISSION NETTING ANALY	SIS		
CREDITABLE					
INCREASE					
- MINUS -	- MINUS -	- MINUS -	- MINUS -		
CREDITABLE					
DECREASE					
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =		
NET CREDITABLE					
CHANGE					
	SECTION C - FAC	CILITY-WIDE EMISSIONS			
TOTAL FACILITY EMISSIONS	N/A	0.012	N/A		
TPER LEVELS (2Q .0711)	N/A	0.013	N/A		
Are the total facility-wide emissions	less than the TPER levels?:	YES	NO		
If YES, no further analysis is requir	ed.				
	required if the total facility-wide emission e toxic air pollutant is not exempted by 15.	level is greater than the 2Q .0711 Toxic / A NCAC 2Q .0702(a)(27) "Exemptions".	Air Pollutant Permitting Emissions Rate		
CHECK HERE IF AN AIR DISPERS	SION MODELING ANALYSIS IS REQUIR	ED 🗹			
modeling plan requirements.		rs section of Form D3-1 for each emissior			
COMMENTS: Chromium VI total e	mission is less than TPER, but to be cons	servative it is still modeled because the er	nissions are very close to the threshold.		

### FORM D2 AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

REVISED 09/22/16	NCDEQ/Division of Air Quality -	Application for Air Permit to Construct	t/Operate D2
PURPOSE OF NETTING: AIR TO	DXICS		
TOXIC AIR POLLUTANT:	Mercury	CAS NO.: 7439-97-6	
EMISSION SOURCE ID NOS .:	ES-11, ES-12, ES-14, ES-73A, ES-	-73B, ES-74, ES-77, ES-78, ES-79A, ES-7 ES-82A, ES-83A, F-1, F-2, F-3, F-	79B, ES-80A, ES-80B, ES-81, ES-81A, ES-81B, 4, F-5
SECT	ION A - EMISSION OFFSETT	ING ANALYSIS FOR MODIFIED	NEW SOURCES
Summarize in this section		EMISSIONS - USE APPROPRIATE COLI	UMNS ONLY
using the B forms	LB/YEAR	LB/DAY	LB/HR
MODIFICATION	N/A		N/A
INCREASE	IN/A		N/A
- MINUS -	- MINUS -	- MINUS -	- MINUS -
MODIFICATION	N/A		N/A
DECREASE	IN/A		
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =
NET CHANGE	N/A		N/A
FROM MODIFICATION	N/A		
	SECTION B - FACILITY-	WIDE EMISSION NETTING ANA	ALYSIS
CREDITABLE			
INCREASE			
- MINUS -	- MINUS -	- MINUS -	- MINUS -
CREDITABLE			
DECREASE			
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =
NET CREDITABLE			
CHANGE			
	SECTION C -	FACILITY-WIDE EMISSIONS	
TOTAL FACILITY	N/A	0.022	N/A
EMISSIONS	IN/A	0.022	
TPER LEVELS (2Q .0711)	N/A	0.0013	N/A
Are the total facility-wide emission	is less than the TPER levels?:	YES -	NO NO
If YES, no further analysis is requi			
		ssion level is greater than the 2Q .0711 To y 15A NCAC 2Q .0702(a)(27) "Exemption	oxic Air Pollutant Permitting Emissions Rate ns".
CHECK HERE IF AN AIR DISPER	RSION MODELING ANALYSIS IS REC	QUIRED 🗹	
If air dispersion modeling analysis modeling plan requirements.	is required, complete the stack parar	neters section of Form D3-1 for each emis	ssion source that emits this TAP. Review the
COMMENTS:			

### AIR POLLUTANT NETTING WORKSHEET AND FACILITY-WIDE EMISSION SUMMARY

REVISED 09/22/16	NCDEQ/Division of Air Quality - A	pplication for Air Permit to Construct/Ope	erate D2
PURPOSE OF NETTING: AIR TO	XICS		
TOXIC AIR POLLUTANT:	Nickel	CAS NO.: 7440-02-0	
EMISSION SOURCE ID NOS.:	ES-11, ES-12, ES-14, ES-73A, ES-73	3B, ES-74, ES-77, ES-78, ES-79A, ES-79B, ES-82A, ES-83A, F-1, F-2, F-3, F-4, F-	
SECTI	ON A - EMISSION OFFSETTIN	NG ANALYSIS FOR MODIFIED/NE	EW SOURCES
Summarize in this section	E	MISSIONS - USE APPROPRIATE COLUMN	IS ONLY
using the B forms	LB/YEAR	LB/DAY	LB/HR
MODIFICATION	N/A		N/A
INCREASE	19/13		1977
- MINUS -	- MINUS -	- MINUS -	- MINUS -
MODIFICATION	N/A		N/A
DECREASE	1977		18/73
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =
NET CHANGE	N/A	T	N/A
FROM MODIFICATION			
	SECTION B - FACILITY-W	VIDE EMISSION NETTING ANALY	SIS
CREDITABLE			
INCREASE			
- MINUS -	- MINUS -	- MINUS -	- MINUS -
CREDITABLE			
DECREASE			
= EQUALS =	= EQUALS =	= EQUALS =	= EQUALS =
NET CREDITABLE			
CHANGE			
	SECTION C - F/	ACILITY-WIDE EMISSIONS	
TOTAL FACILITY	N/A	0.302	N/A
EMISSIONS	IV/7	0.302	
TPER LEVELS (2Q .0711)	N/A	0.13	N/A
Are the total facility-wide emissions	s less than the TPER levels?:	YES 7	NO
If YES, no further analysis is requir			
		ion level is greater than the 2Q .0711 Toxic A 15A NCAC 2Q .0702(a)(27) "Exemptions".	Air Pollutant Permitting Emissions Rate
CHECK HERE IF AN AIR DISPER	SION MODELING ANALYSIS IS REQU	JIRED 🔽	
If air dispersion modeling analysis modeling plan requirements.	is required, complete the stack parame	eters section of Form D3-1 for each emission	source that emits this TAP. Review the
COMMENTS:			

### FORM D5 TECHNICAL ANALYSIS TO SUPPORT PERMIT APPLICATION

RE	VISED 09/22/16	NCDEQ/Division of Air Quality - Application for	· · · · · · · · · · · · · · · · · · ·	D5		
	PROVIDE DETAILED TECHNICAL CALCULATIONS TO SUPPORT ALL EMISSION, CONTROL, AND REGULATORY					
	DEMONSTRATIONS MADE IN THIS APPLICATION. INCLUDE A COMPREHENSIVE PROCESS FLOW DIAGRAM AS NECESSARY TO SUPPORT AND CLARIFY CALCULATIONS AND ASSUMPTIONS. ADDRESS THE					
	FOLLOWING SPECIFIC ISSUES ON SEPARATE PAGES:					
			rough B9) - SHOW CALCULATIONS USED, INCLUDING EMISSION			
			HE POLLUTANT EMISSION RATES IN THIS APPLICATION WERE DE AFTER CONTROLS. CLEARLY STATE ANY ASSUMPTIONS MADE A			
		RENCES AS NEEDED TO SUPPORT MATERIAL BALANCE				
_						
			E V ONLY) - PROVIDE AN ANALYSIS OF ANY REGULATIONS APPLI JSSION OUTING METHODS (e.g. FOR TESTING AND/OR MONITORI			
			CULARLY THOSE REGULATIONS LIMITING EMISSIONS BASED ON			
			CATION FOR AVOIDANCE OF ANY FEDERAL REGULATIONS	505		
			DRMANCE STANDARDS (NSPS), NATIONAL EMISSION STANDARDS IS FROM THE FEDERAL REGULATIONS WHICH WOULD OTHERWIS			
	APPLICABLE TO THI	S FACILITY. SUBMIT ANY REQUIRED INFORMATION TO D	OCUMENT COMPLIANCE WITH ANY REGULATIONS. INCLUDE EM			
	RATES CALCULATE	D IN ITEM "A" ABOVE, DATES OF MANUFACTURE, CONTRO	DL EQUIPMENT, ETC. TO SUPPORT THESE CALCULATIONS.			
с		NALYSIS (FORM C and C1 through C9) - PROVIDE A TECH	INICAL EVALUATION WITH SUPPORTING REFERENCES FOR ANY			
			CE EMISSION RATES IN CALCULATIONS UNDER ITEM "A" ABOVE.	INCLUDE		
			FACTURING RECOMMENDATIONS, AND PARAMETERS AS APPLIE E CONTROL DEVICES). INCLUDE AND LIMITATIONS OR MALFUNC			
			S FACILITY. DETAIL PROCEDURES FOR ASSURING PROPER OPE			
	OF THE CONTROL D	EVICE INCLUDING MONITORING SYSTEMS AND MAINTEN	ANCE TO BE PERFORMED.			
		•	<b>ONLY)</b> - SHOWING HOW COMPLIANCE WILL BE ACHIEVED WHEN E. REFER TO COMPLIANCE REQUIREMENTS IN THE REGULATORY			
	'	,	RAMETERS THAT CAN BE MONITORED AND REPORTED TO			
	DEMONSTRATE COM	MPLIANCE WITH THE APPLICABLE REGULATIONS.				
Е	PROFESSIONAL EN		112 "APPLICATION REQUIRING A PROFESSIONAL ENGINEERING	SEAL "		
-			REQUIRED TO SEAL TECHNICAL PORTIONS OF THIS APPLICATION	,		
	NEW SOURCES AND	MODIFICATIONS OF EXISTING SOURCES. (SEE INSTRU	CTIONS FOR FURTHER APPLICABILITY).			
	,	Thomas O. Pritcher attest that this applica	tion for Duke Energy Carolinas LLC - Buck Combined Cycle Faci	114.7		
	<i>I</i> ,		accurate, complete and consistent with the information supplied	iity		
	in the engineering pla		best of my knowledge. I further attest that to the best of my knowledge	e the		
			gulations. Although certain portions of this submittal package may have			
			s that I have reviewed this material and have judged it to be consistent 5.6A and 143-215.6B, any person who knowingly makes any false state			
			eanor which may include a fine not to exceed \$10,000 as well as civil pe			
	up to \$25,000 per viol	lation.				
	(PLEASE USE BLUE	INK TO COMPLETE THE FOLLOWING)	PLACE NORTH CAROLINA SEAL HERE			
	NAME:					
	DATE:					
	COMPANY:	Environmental Consulting & Technology of North Ca				
	ADDRESS:	7208 Falls of Neuse Road, Suite 102, Raleigh, NC				
	TELEPHONE:	919-861-8888				
	SIGNATURE:					
	PAGES CERTIFIED:	Appendix A & Appendix B				
	(IC	DENTIFY ABOVE EACH PERMIT FORM AND ATTACHMENT				
		THAT IS BEING CERTIFIED BY THIS SEAL)				

### NORTH CAROLINA MODELING PROTOCOL CHECKLIST (2 Pages)

REVISED 09/22/16

### NCDEQ/Division of Air Quality - Application for Air Permit to Construct/Operate

D6-1

The North Carolina Modeling Protocol Checklist may be used in lieu of developing the traditional written modeling plan for North Carolina toxics and criteria pollutant modeling. The protocol checklist is designed to provide the same level of information as requested in a modeling protocol as discussed in Chapter 2 of the *Guideline for Evaluating the Air Quality Impacts of Toxic Pollutants in North Carolina*. The modeling protocol checklist is submitted with the modeling analysis. The above referenced *Guideline* can be found at the following web link:

https://ncdenr.s3.amazonaws.com/s3fs-public/Air%20Quality/permits/mets/Guidance.pdf

Although most of the information requested in the modeling protocol checklist is self-explanatory, additional comments are provided, where applicable, and are discussed in greater detail in the toxics modeling *Guideline* referenced above. References to sections, tables, figures, appendices, etc., in the protocol checklist are found in the toxics modeling *Guideline*.

**INSTRUCTIONS:** The modeling report supporting the compliance demonstration should include most of the information listed below. As appropriate, answer the following questions or indicate by check mark the information provided or action taken is reflected in your report.

	FACI	LITY INFORMATIO	N
Facility Name:	Buck Combined Cycle Facility	Consultant (if app	blicable):
		Environme	ntal Consulting & Technology of North Carolina, PLLC
Facility ID:	8000004		
Address:	1385 Dukeville Road	7208 Falls	Of Neuse Road
	Salisbury, NC, 28146	Suite 102	
		Raleigh, N	C 27615
Contact Name:	Dan Markley	Contact Name:	Thomas Pritcher
Phone Number:	(704)-382-0696	Phone Number:	919-861-8888
Email Address:	dan.markley@duke-energy.com	Email Address:	tpritcher@ectinc.com

GENERAL INFORMATION			
<b>Description of New Source or Source/Process Modification: P</b> rovide a short description of the new or modified source(s) and a brief discussion of how this change affects facility production or process operation.		Included N/A	
Source/Pollutant Identification: Provide a table of the affected pollutants, by source, which identifies the source type (point, area, or volume), maximum pollutant emission rates over the applicable averaging period(s), and, for point sources, indicate if the stack is capped or non-vertical (C/N).	7	Included	
Pollutant Emission Rate Calculations: Indicate how the pollutant emission rates were derived (e.g. AP-42 emission factors, mass balance, etc.) and where applicable, provide the calculations		Included N/A	
Site/Facility Diagram: Provide a diagram or drawing showing the location of all existing and proposed emission sources, buildings or structures, public right-of-ways, and the facility property (toxics)/fence line (criteria pollutants) boundaries. The diagram should also include a scale, true north indicator, and the UTM or latitude/longitude of at least one point.	7	Included	
Certified Plat or Signed Survey: a certified plat (map) from the County Register of Deeds or a signed survey must be submitted to validate property boundaries modeled.	7	Included	
<b>Topographic Map:</b> a topographic map covering approximately 5 km around the facility must be submitted. The facility boundaries should be annotated on the map as accurately as possible.		Included N/A	
Cavity Impact Analysis: no cavity analysis is required if using AERMOD. See Section 4.2		Included N/A	
Background Concentrations (criteria Pollutant analyses only): Background concentrations must be determined for each pollutant for each averaging period evaluated. The averaged background value used (e.g. high, high-second-high, high-third-high, etc.) is based on the		Included	
pollutant and averaging period evaluated. The background concentrations are added to the modeled concentrations, which are then compared to the applicable air quality standard to determine compliance.	4	N/A	
Offsite Source Inventories (criteria pollutant analyses only): Offsite source inventories must be developed and modeled for all pollutants for which onsite source emissions are modeled in excess of the specific pollutant significant impact levels (SILs) as defined in the PSD New Source Review Workshop Manual. The DAQ AQAB must approve the inventories. An initial working inventory can be requested from the		Included	
AQAB.	7	N/A	
Attach Additional Sheets as Necessary	Pac	e 1 of 2	

SCREEN LEVEL MODELING		D6-2
<b>Model:</b> The latest version of the AERSCREEN model must be used. The use of other screening models should be approved by NCDAQ prior to submitting the modeling report.	AERSCF	REEN Version
Source/Source Emission Parameters: Provide a table listing the sources modeled and the applicable source emission parameters. See NC Form 3 - Appendix A.		NA
Merged Sources: Identify merged sources and show all appropriate calculations. See Section 3.3		NA
GEP Analysis: See Section 3.2 and NC Form 1 - Appendix A		NA
<b>Terrain:</b> Indicate the terrain modeled: simple (Section 4.4), and complex (Section 4.5 and NC Form 4 Appendix A). If complex terrain is within 5 kilometers of the facility, complex terrain must be evaluated. Simple terrain must include terrain elevations if any terrain is greater than the stack base of any source modeled. Mark the appropriate terrain type.		Simple Complex
Meteorology: Refer to Section 4.1 for AERSCREEN inputs.		
<b>Receptors:</b> AERSCREEN - use shortest distance to property boundary for each source modeled and use sufficient range to find maximum [See Section 4.1(i) and (j)]. Terrain above stack base must be evaluated.		NA
Modeling Results: For each affected pollutant, modeling results should be summarized, converted to the applicable averaging period (See	-	NA
Table 3), and presented in tabular format indicating compliance status with the applicable AAL, SIL, or NAAQS. See NC Form S5 - Appendix A.		NA
		Electronic
Modeling Files: Either electronic or hard copies of AERSCREEN output must be submitted.		Hard Copy

REFINED LEVEL MODELING	
<b>Model:</b> The latest version of AERMOD should be used. The use of other refined models must be approved by NCDAQ prior to submitting the modeling report.	AERMOD Version
The latest version of AERMOD may be found at the following web address: <u>http://www.epa.gov/scram001/dispersion_prefrec.htm</u>	16216r
Source/Source Emission Parameters: Provide a table listing the sources modeled and the applicable source emission parameters. See NC Form 3 - Appendix A.	Y
GEP Analysis: Use BPIP-Prime with AERMOD.	
Cavity Impact Analysis: No separate cavity analysis is required when using AERMOD as long as receptors are placed in cavity susceptible areas. See Section 4.2 and 5.2.	NA
<b>Terrain:</b> Use digital elevation data from the USGS NED database. Use of other sources of terrain elevations or the non-regulatory Flat Terrain option will require prior approval from DAQ AQAB.	USGS NED
The USGS NED database can be found at the following web address: <u>http://viewer.nationalmap.gov/launch/</u>	
<b>Coordinate System:</b> Specify the coordinate system used (e.g. NAD27, NAD83, etc.) to identify the source, building, and receptor locations. Note: Be sure to specify in the AERMAP input file the correct base datum (NADA) to be used for identifying source input data locations. Clearly note in both the protocol checklist and the modeling report which datum was used.	Coordinate System: NAD83
Receptors: The receptor grid should be of sufficient size and resolution to identify the maximum pollutant impact. See Section 5.3.	Y
Meteorology: Indicate the AQAB, pre-processed, 5-year data set used in the modeling demonstration: See Section 5.5 and Appendix B)	Data Set Used: Charlotte (surface) / Greensboro (upper)
AERMOD Version:	NA
If processing your own raw meteorology, then pre-approval from AQAB is required. Additional documentation files (e.g. AERMET state processing files) will also be necessary. For NC toxics, the modeling demonstration requires only the last year of the standard 5-year data set (e.g. 2005) provided the maximum impacts are less than 50% of the applicable AAL(s).	NA
<b>Modeling Results:</b> For each affected pollutant and averaging period, modeling results should be summarized and presented in tabular format indicating compliance status with the applicable AAL, SIL, or NAAQS. See NC Form R5 - Appendix A.	Y
Modeling Files: Submit input and output files for AERMOD. Also include BPIP-Prime files, AERMAP files, DEM files, and any AERMET input and output files, including raw meteorological data.	Y
Attack Additional Chapta as Nacasawa	D

Attach Additional Sheets as Necessary

Page 2 of 2

**APPENDIX B** 

SUPPORTING EMISSION CALCULATIONS



#### TOXIC EMISSIONS-Modeling

	Existi	ng Turbine	ES-11	Existi	ng Turbine	ES-12	Existin	ng Auxiliary	Boiler	Existing	Auxiliary E	quipment	S	TAR Facilit	y		Total			TPER		Mode	ling Requi	red?
Pollutants	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr	lb/hr	lb/day	lb/yr
Sulfuric Acid Mist	1.7	40.8		1.7	40.8								1.00E-01	2.40		3.50	84.00		0.025	0.25		YES	YES	
Benzene			220			220			0.206	1.38E-02	3.31E-01	1.38E+00			3.34			444.93			8.1			YES
Formaldehyde	4.46E-01			4.46E-01			0.00368			3.20E-03	7.68E-02	3.20E-01	7.64E-03			0.91			0.04			YES		
Hexane		3.94E+00			3.94E+00			2.1168						2.54			12.54			23.0			NO	
Toluene	1.29E-01	3.10E+01		1.29E-01	3.10E+01		1.64E-04	3.94E-03		4.74E-03	1.14E-01	4.74E-01	1.32E-03	3.17E-02		0.26	62.15		14.4	98.0		NO	NO	
Arsenic			4.47			4.47			0.0196	6.97E-05	1.67E-03	6.97E-03			11.37			20.34			0.053			YES
Beryllium			0.27			0.27			0.00118	5.23E-05	1.25E-03	5.23E-03			2.34			2.89			0.28			YES
Cadmium			24.6			24.6			0.108	5.23E-05	1.25E-03	5.23E-03			2.58			51.89			0.37			YES
Soluble chromate compounds as																								
Chromium VI																								1
equivalent	1.43E-04	3.42E-03	1.25	1.43E-04	3.42E-03	1.25	6.27E-07	1.50E-05	0.00549	5.23E-05	1.25E-03	5.23E-03		4.14E-03			0.012			0.013			NO	
Manganese		2.33E-02			2.33E-02			0.000447		1.05E-04	2.51E-03	1.05E-02		6.70E-02			0.117			0.630			NO	
Mercury		9.86E-03			9.86E-03			0.000305		5.23E-05	1.25E-03	5.23E-03		5.66E-04			0.022			0.013			YES	
Nickel		1.29E-01			1.29E-01			0.00247		5.23E-05	1.25E-03	5.23E-03		4.06E-02			0.302			0.013			YES	

Existing Turbine: Bold values are emission limits listed in Permit 03786T34 condition 2.2-A.1. Values not in bold are from Buck Duct Burner Application 2-15-13, Form B. Existing Auxiliary Boiler: Values are from emission limits listed in Permit 03786T34 condition 2.2-A.1. Values not in bold from Buck Duct Burner Application, Table B-4. Existing Auxiliary Equipment: Includes emissions from existing emergency generators and fire water pump. Emissions from NC Emission Estimation Spreadsheets. Per conversation with Nancy Jones on April 11, 2017 Chromium VI was listed increatly in Permit 03786T34 as Non-specific Chromium VI. Chromium VI. Chromium Steriation Should be considered Soluable Chromate compounds Chromium VI total emission is less than TPER, but to be conservative it is still modeled because the emissions are very close to the threshold.

### Duke Energy Buck Station Facility-wide Emissions Summary - Shortterm

	Worst-	Fly Ash + Case Fuel d Emissions	EHE E	missions	Silo/Dome	Emissions	Pollution C Emis	control Silo sions	Wet Ash Emis		Storage Pile	Emissions	Ash	Basin	Ash H	andling	Haul	Roads	Scre	ener	Cru	sher	Screene		Facility Contr Emis		Facility Perm Emis	
Pollutant	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
PM	4.87		5.36	-	0.05		0.11		7.62E-03	-	4.90E-03		5.07E-01		8.58E-02		1.65E-01		0.02	-	0.01		0.86		12.05	-	12.05	
PM <sub>10</sub>	4.48	-	4.93	-	0.02		0.10		3.61E-03	-	2.45E-03		2.54E-01	-	4.06E-02		4.26E-02		0.01	-	0.004		0.86	-	10.75	-	10.75	-
PM <sub>2.6</sub>	2.58		2.84	-	0.02		0.06		5.46E-04	-	9.81E-04		3.80E-02		6.14E-03		4.26E-03		0.0003		0.001		0.86		6.42	-	6.42	
so.	40.23													-						-			0.80	-	41.03	-	41.03	
NO-	18.22																						12.12		30.34		30.34	-
NO <sub>X</sub>	47.60													-										-				
NO <sub>X</sub>																				-		-	12.12		59.72	-	59.72	
0	22.40			-							-			-									2.61	-	25.01	-	25.01	
VOC	2.24													-						-			0.97		3.21	-	3.21	
GHG (Mass Basis)*											-									-								
GHG (CO <sub>2</sub> e Basis)*		-		-						-		-		-		-				-		-						·
Sulfuric Acid Mist <sup>9</sup>	0.10	-		-						-										-					0.10	-	0.10	
Lead	6.48E-04		6.80E-04	-	6.34E-06				9.68E-07	-	6.23E-07		6.44E-05	-	1.09E-05				1.92E-06	-	1.05E-06				1.41E-03	-	1.41E-03	-
Benzene	1.24E-04		1	-	1				1	-	1		1	-	1		1		-	-	1		2.55E-03		2.68E-03	-	2.68E-03	
Formaldehyde	4.41E-03	-		-						-				-						-		-	3.23E-03	-	7.64E-03	-	7.64E-03	
Hexane	1.06E-01	-		-						-				-						-					1.06E-01	-	1.06E-01	
Toluene	2.00E-04			-						-				-						-			1.12E-03		1.32E-03	-	1.32E-03	
Arsenic	5.89E-04		6.35E-04	-	5.92E-06				9.03E-07	-	5.81E-07		6.01E-05	-	1.02E-05				1.79E-06	-	9.78E-07				1.30E-03	-	1.30E-03	
Beryllium	1.20E-04		1.32E-04	-	1.23E-06				1.87E-07	-	1.20E-07		1.25E-05	-	2.11E-06				3.71E-07	-	2.03E-07				2.69E-04	-	2.69E-04	
Cadmium	1.68E-04		1.13E-04		1.06E-06				1.61E-07		1.04E-07		1.07E-05		1.81E-06				3.20E-07	-	1.75E-07				2.96E-04	-	2.96E-04	
Chromium	7.84E-04		7.71E-04		7.18E-06				1.10E-06		7.06E-07		7.30E-05		1.23E-05				2.18E-06	-	1.19E-06				1.65E-03	-	1.65E-03	
Chromium VI	7.71E-05	-	8.48E-05		7.90E-07				1.21E-07	-	7.76E-08		8.03E-06	-	1.36E-06				2.39E-07	-	1.31E-07				1.73E-04	-	1.73E-04	
Cobalt	2.85E-04		3.08E-04	-	2.87E-06				4.39E-07		2.82E-07		2.92E-05		4.94E-06				8.71E-07	-	4.75E-07	-			6.33E-04	-	6.33E-04	
Manganese	1.26E-03		1.36E-03	-	1.27E-05				1.94E-06		1.25E-06		1.29E-04		2.18E-05				3.84E-06	-	2.10E-06	-			2.79E-03	-	2.79E-03	
Mercury	1.90E-05		4.07E-06		3.79E-08				5.80E-09		3.73E-09		3.86E-07		6.52E-08				1.15E-08	-	6.27E-09			-	2.36E-05	-	2.36E-05	-
Nickel	8.25E-04 1.91E-04	-	7.71E-04 2.09E-04	-	7.18E-06 1.94E-06				1.10E-06 2.97E-07	-	7.06E-07 1.91E-07	-	7.30E-05 1.98E-05	-	1.23E-05 3.34E-06				2.18E-06 5.89E-07	-	1.19E-06 3.21E-07			-	1.69E-03 4.26E-04	-	1.69E-03 4.26E-04	-
Selenium Xvlenes	1.91E-04		2.09E-04	-	1.94E-06				2.97E-07	-	1.91E-07		1.98E-05		3.34E-06				5.89E-07	-	3.21E-07		7.80E-04		4.26E-04 7.80E-04	-	4.26E-04 7.80E-04	-
Aylenes 1.3-Butadiene		-		-						-				-						-			7.80E-04 1.07E-04		7.80E-04 1.07E-04	-	7.80E-04 1.07E-04	-
Acetaldehyde				-						-				-		-		-		-					2.10E-04	-		
Acetaldenyde Acrolein				-						-				-						-			2.10E-03 2.53E-04		2.10E-03 2.53E-04	-	2.10E-03 2.53E-04	-
Total PAH				-		-								-						-			2.53E-04 4.60E-04		4.60E-04		2.53E-04 4.60E-04	
Naphthalene	3.59E-05	-		-		-				-				-						-		-	2.32E-04	-	2.68E-04	-	4.60E-04 2.68E-04	-
Acenaphthalene	3.35E-03	-		-						-				-						-		-	1.38E-05	-	1.38E-05	-	1.38E-05	-
Acenaphthene				-										-				-		-			3.89E-06		3.89E-06	-	3.89E-06	-
Fluorene		-		-						-				-						-		-	7.99E-05	-	7.99E-05	-	7.99E-06	-
Phenanthrene		-	1	-	1				1	-		-	1	-					1	-		-	7.99E-05 8.05E-05		7.99E-05 8.05E-05	-	7.99E-05 8.05E-05	-
Anthracene	-		1	-	1				1	-	1		1	-	1	-	1	-	1	-	1	-	5.12E-06	-	5.12E-06	-	5.12E-06	-
Fluoranthene			1	-	1				1	-			1	-					1	-		-	2.08E-05	-	2.08E-05	-	2.08E-05	-
Pyrene	-		1		1		1		1		1		1	-	1		1		1	-	1		1.31E-05	-	1.31E-05	-	1.31E-05	-
Benzo(a)anthracene			1	-	1				1	-			1	-						-		-	4.60E-06		4.60E-06		4.60E-06	-
Chrysene		-	1	-	1				1	-		-	1	-					1	-			9.66E-07		9.66E-07	-	9.66E-07	-
Benzo(b)fluoranthene			1		1				1				1										2.71E-07		2.71E-07		2.71E-07	
Benzo(k)fluoranthene			1		1				1				1										4.24E-07		4.24E-07		4.24E-07	
Benzo(a)pyrene	1		1		1				1						1		1				1		5.15E-07		5.15E-07		5.15E-07	-
Indeno(1.2.3-cd)pyrene	1	-	1	-	1				1	-		-		-	1		1			-	1		1.03E-06		1.03E-06	-	1.03E-06	-
Dibenz(a,h)anthracene									1				1		1		1			-	1		1.60E-06	-	1.60E-06	-	1.60E-06	
Benzo(a.h.l)pervlene			1	-	1				1				1						1				1.34E-06		1.34E-06	-	1.34E-06	
Maximum HAP				1							1	0			1		1				1				1.04E-00		1.06E-01	·
Total HAP	1																								1.31E-01		1.31E-01	

Total mover Note: Duke Energy expects 6%-15% LOI. LOI will affect throughput. Duke Energy wont go above 400,000 toy. <sup>6</sup> Based on SEFA stack test performed September 2016. Sulfuric Acid Mist was 0.05 lb/hr for contingency ECT doubled the number to 0.1 lb/hr.

#### NC15A NCAC 02Q .0711 EMISSION RATES REQUIRING A PERMIT

		Facility Total trolled Emissi	ons
Pollutant	lb/hr	lb/day	lb/yr
Sulfuric Acid Mist	1.00E-01	2.400	
Benzene			
Formaldehyde	7.64E-03		
Hexane		2.541	
Toluene	1.32E-03	0.032	
Arsenic			
Beryllium			
Cadmium			
Chromium			
Chromium VI		0.004	
Manganese		0.067	
Mercury		0.001	
Nickel		0.041	

### Duke Energy Buck Station Facility-wide Emissions Summary - Annual

	Worst-0	Fly Ash + Case Fuel I Emissions	EHF F	missions	Silo/Dome	e Emissions	Pollution Co Emiss			Receiving	Storage Pi	le Emissions	Ash	Basin	Ash H	landling	Haul	Roads	Sco	eener	Cru	isher		er/Crusher gines	Cont	ty Total rolled ssions	Pern	ity Total mitted ssions
Pollutant	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	ton/vr	lb/hr	
PM		21.34		23.46		0.08		0.49		2.18E-02		2.15E-02		2.22E+00		3.76E-01	-	7.22E-01		1.97E-02		1.51E-03		3.81E-01		49.14		49.14
PM <sub>10</sub>		19.63		21.59		0.04		0.45		1.03E-02	-	1.07E-02		1.11E+00		1.78E-01	-	1.86E-01		6.61E-03		6.78E-04		3.81E-01		43.59		43.59
PM <sub>14</sub>		11.31		12.44		0.04		0.26		1.56E-03		4.30E-03		1.67E-01		2.69E-02	-	1.87E-02		4.47E-04		1.25E-04		3.81E-01		24.64		24.64
80		163.63		16.77		0.04		0.20		1.002.00		4.002 00		1.072 01		LOOL OL		1.072.02		4.472.04		1.202 04		0.35	-	163.98	J	163.98
NO <sub>2</sub>				-										-													<u> </u>	117.66
NUX		112.29									-						-							5.36	-	117.66	<u> </u>	
CO		91.10									-						-							1.16		92.26	<u> </u>	92.26
VOC GHG (Mass Basis)*		9.11 116.401									-			-										0.43		9.54		9.54 116.599
						-						-												198.14				
GHG (CO <sub>2</sub> e Basis)*	-	116,406									-						-						-	198.14		116,604.15		116,604
Sulfuric Acid Mist <sup>9</sup>		0.44									-						-									0.44		0.44
Lead	-	2.84E-03		2.98E-03		9.90E-06				2.77E-06		2.73E-06		2.82E-04		4.77E-05	-			2.50E-06		1.91E-07				6.17E-03		6.17E-03
Benzene		5.41E-04									-		-		-		-							1.13E-03		1.67E-03		1.67E-03
Formaldehyde	-	1.93E-02								1	-					1				1				1.43E-03		2.08E-02	<u> </u>	2.08E-02
Hexane		4.64E-01									-															4.64E-01	<u> </u>	4.64E-01
Toluene		8.76E-04									-		-		-		-							4.95E-04		1.37E-03	<u> </u>	1.37E-03
Arsenic		2.58E-03		2.78E-03		9.24E-06	-			2.58E-06		2.55E-06	-	2.63E-04		4.45E-05				2.33E-06		1.78E-07				5.69E-03		5.69E-03
Beryllium		5.27E-04		5.76E-04		1.91E-06	-			5.35E-07	-	5.27E-07	-	5.45E-05		9.22E-06	-			4.83E-07		3.70E-08				1.17E-03		1.17E-03
Cadmium		7.35E-04		4.97E-04		1.65E-06				4.61E-07	-	4.54E-07		4.70E-05		7.95E-06				4.16E-07		3.19E-08				1.29E-03		1.29E-03
Chromium		3.43E-03		3.38E-03		1.12E-05				3.13E-06		3.09E-06	-	3.20E-04		5.41E-05	-			2.83E-06		2.17E-07			-	7.20E-03	<u> </u>	7.20E-03
Chromium VI		3.38E-04		3.71E-04 1.35E-03		1.23E-06				3.45E-07	-	3.40E-07 1.24E-06	-	3.52E-05	-	5.95E-06 2.16E-05	-			3.11E-07		2.38E-08			-	7.53E-04		7.53E-04 2.76E-03
Cobalt		1.25E-03 5.52E-03		1.35E-03 5.96E-03		4.49E-06 1.98E-05				1.25E-06 5.53E-06		1.24E-06 5.45E-06	-	1.28E-04 5.64E-04		2.16E-05 9.54E-05	-			1.13E-06 4.99E-06		8.67E-08 3.82E-07				2.76E-03 1.22E-02		2.76E-03
Manganese Mercurv		5.52E-03 8.32E-05		1.78E-05		5.92E-05				1.66E-08	-	1.63E-08		1.69E-06		9.54E-05 2.85E-07	-			4.99E-06 1.49E-08		1.14E-09	-	_		1.03E-02	<u> </u>	1.03E-04
Nickel		3.61E-03		3.38E-03		1 12E-05				3.13E-06	-	3.09E-06	-	3.20E-06	-	5.41E-05	-			2.83E-06		2 17E-07	-			7.38E-03	<u> </u>	7.38E-03
Selenium		8.37E-04		9.14E-04		3.03E-06				8.48E-07	-	8.36E-07	-	8.65E-05	-	1.46E-05	-			7.66E-07		5.86E-08				1.86E-03		1.86E-03
Xvlenes		0.371-04	-	8.14L-04		3.032-00				0.402-07	-	0.302-07	-	0.03E-03	-	1.402-00	-			7.002-07	-	3.00L-00	-	3.45E-04		3.45E-04	<u> </u>	3.45E-04
1.3-Butadiene											-						-							4.74E-05		4.74E-05		4.74E-05
Acetaldehvde											-		-		-									9.29E-04		9.29E-04		9.29E-04
Acrolein											-						-							1.12E-04		1 12E-04		1.12E-04
Total PAH											-						-							2.04E-04		2.04E-04		2.04E-04
Naphthalene		1.57E-04									-						-							1.03E-04		2.60E-04		2.60E-04
Acenaphthalene																								6.13E-06		6.13E-06		6.13E-06
Acenaphthene								1		1						1	-	1		1		1		1.72E-06		1.72E-06		1.72E-06
Fluorene											-						-							3.54E-05		3.54E-05		3.54E-05
Phenanthrene																	-							3.56E-05		3.56E-05		3.56E-05
Anthracene	-						-				-		-				-				-			2.27E-06	-	2.27E-06		2.27E-06
Fluoranthene	-										-		-		-		-						-	9.22E-06		9.22E-06		9.22E-06
Pyrene							-		-		-		-		-		-				-		-	5.79E-06		5.79E-06		5.79E-06
Benzo(a)anthracene										1	-					1	-						-	2.04E-06		2.04E-06		2.04E-06
Chrysene	-						-				-				-		-			1			-	4.28E-07		4.28E-07		4.28E-07
Benzo(b)fluoranthene	-						-			1	-		-		-	1	-				-			1.20E-07	-	1.20E-07		1.20E-07
Benzo(k)fluoranthene	-						-			1	-		-		-	1	-				-			1.88E-07	-	1.88E-07		1.88E-07
Benzo(a)pyrene							-				-		-				-							2.28E-07		2.28E-07	<u> </u>	2.28E-07
Indeno(1,2,3-cd)pyrene											-									1				4.54E-07		4.54E-07	<u> </u>	4.54E-07
Dibenz(a,h)anthracene							-			1	-		-			1	-			1				7.06E-07		7.06E-07		7.06E-07
Benzo(g,h,l)perylene	-			1			-			1	-		-	1	-	1	-			1	-			5.92E-07	-	5.92E-07		5.92E-07
Maximum HAP																								-		4.64E-01	<u> </u>	4.64E-01
Total HAP		will affect throug																								5.30E-01	4	5.30E-01

Note: Duke Energy expects 6%-15% LOI. LOI will affect throughput. Duke Energy wont go above 400,000 tpy. <sup>5</sup> Based on SEFA stack test performed September 2016. Sulfuric Acid Mist was 0.05 lb/hr for contingency ECT doubled the number to 0.1 lb/hr.

#### NC15A NCAC 02Q .0711 EMISSION RATES REQUIRING A PERMIT

	Facility Total Controlled Emissions								
Pollutant	lb/hr	lb/day	lb/yr						
Sulfuric Acid Mist	-	-							
Benzene		-	3.342						
Formaldehyde		-							
Hexane		-							
Toluene	-	-							
Arsenic	-	-	11.373						
Beryllium	-	-	2.341						
Cadmium			2.579						
Chromium		-	14.407						
Chromium VI	-	-	1.505						
Manganese	-	-							
Mercury		-							
Nickel	-	-							

#### Natural Gas Emissions

	Emission				Emis	sions	
Pollutant	Factor	Units	Throughput	Units	lb/hr	ton/yr	Reference
PM/PM <sub>10</sub> /PM <sub>2.5</sub>	7.6	lb/MMscf	58,824	scf/hr	0.45	1.96	EPA AP-42, Table 1.4-2 (07/98)
SO <sub>2</sub>	0.6	lb/MMscf	58,824	scf/hr	0.04	0.15	EPA AP-42, Table 1.4-2 (07/98)
NO <sub>X</sub>	140	lb/MMscf	58,824	scf/hr	8.24	36.07	EPA AP-42, Table 1.4-1 (07/98)
со	84	lb/MMscf	58,824	scf/hr	4.94	21.64	EPA AP-42, Table 1.4-1 (07/98)
VOC	5.5	lb/MMscf	58,824	scf/hr	0.32	1.42	EPA AP-42, Table 1.4-2 (07/98)
Lead	0.0005	lb/MMscf	58,824	scf/hr	2.94E-05	1.29E-04	EPA AP-42, Table 1.4-2 (07/98)
Benzene	0.0021	lb/MMscf	58,824	scf/hr	1.24E-04	5.41E-04	EPA AP-42, Table 1.4-3 (07/98)
Formaldehyde	0.075	lb/MMscf	58,824	scf/hr	4.41E-03	1.93E-02	EPA AP-42, Table 1.4-3 (07/98)
Hexane	1.8	lb/MMscf	58,824	scf/hr	1.06E-01	4.64E-01	EPA AP-42, Table 1.4-3 (07/98)
Naphthalene	0.00061	lb/MMscf	58,824	scf/hr	3.59E-05	1.57E-04	EPA AP-42, Table 1.4-3 (07/98)
Toluene	0.0034	lb/MMscf	58,824	scf/hr	2.00E-04	8.76E-04	EPA AP-42, Table 1.4-3 (07/98)
Arsenic	0.0002	lb/MMscf	58,824	scf/hr	1.18E-05	5.15E-05	EPA AP-42, Table 1.4-4 (07/98)
Beryllium	0.000012	lb/MMscf	58,824	scf/hr	7.06E-07	3.09E-06	EPA AP-42, Table 1.4-4 (07/98)
Cadmium	0.0011	lb/MMscf	58,824	scf/hr	6.47E-05	2.83E-04	EPA AP-42, Table 1.4-4 (07/98)
Chromium	0.0014	lb/MMscf	58,824	scf/hr	8.24E-05	3.61E-04	EPA AP-42, Table 1.4-4 (07/98)
Cobalt	0.000084	lb/MMscf	58,824	scf/hr	4.94E-06	2.16E-05	EPA AP-42, Table 1.4-4 (07/98)
Manganese	0.00038	lb/MMscf	58,824	scf/hr	2.24E-05	9.79E-05	EPA AP-42, Table 1.4-4 (07/98)
Mercury	0.00026	lb/MMscf	58,824	scf/hr	1.53E-05	6.70E-05	EPA AP-42, Table 1.4-4 (07/98)
Nickel	0.0021	lb/MMscf	58,824	scf/hr	1.24E-04	5.41E-04	EPA AP-42, Table 1.4-4 (07/98)
Selenium	0.000024	lb/MMscf	58,824	scf/hr	1.41E-06	6.18E-06	EPA AP-42, Table 1.4-4 (07/98)

#### Sample Calculations

Natural Gas Flow =	60 MMBtu	10 <sup>6</sup> Btu	scf Nat. Gas	=	58,824	scf/hr Natural Gas
	hr	MMBtu	1020 Btu			
NO <sub>x</sub> Emissions =	58824 scf	MMscf	140 lb NOx	=	8.24	lb/hr NO <sub>x</sub>
	hr	10 <sup>6</sup> scf	MMscf			
	8.24 lb NO <sub>x</sub>	8760 hr	ton	=	36.07	tpy NO <sub>x</sub>
	hr	yr	2000 lb			
	50004					
CO Emissions =	58824 scf	MMscf	84 lb CO	=	4.94	lb/hr CO
	hr	10 <sup>6</sup> scf	MMscf			
	4.04 11 .00	07001	1			
	4.94 lb CO	8760 hr	ton	=	21.64	tpy CO
	hr	yr	2000 lb			

Annual Natural Gas usage provided by SEFA

#### Propane Emissions

	Emission				Emis	sions		
Pollutant	Factor	Units	Throughput	Units	lb/hr	ton/yr	Reference	
PM/PM <sub>10</sub> /PM <sub>2.5</sub>	0.7	lb/10 <sup>3</sup> gal	663	gal/hr	0.46	2.03	EPA AP-42, Table 1.5-1 (07/08)	
SO <sub>2</sub>	0.018	lb/10 <sup>3</sup> gal	663	gal/hr	0.01	0.05	EPA AP-42, Table 1.5-1 (07/08)	Propane sulfur content 0.18 gr/100 ft3
NO <sub>X</sub>	13	lb/10 <sup>3</sup> gal	663	gal/hr	8.62	37.75	EPA AP-42, Table 1.5-1 (07/08)	
СО	7.5	lb/10 <sup>3</sup> gal	663	gal/hr	4.97	21.78	EPA AP-42, Table 1.5-1 (07/08)	
VOC	1	lb/10 <sup>3</sup> gal	663	gal/hr	0.66	2.90	EPA AP-42, Table 1.5-1 (07/08)	

### Sample Calculations

Propane Flow =	60 MMBtu	10 <sup>6</sup> Btu	gal Propane	=	663	gal/hr Propane
	hr	MMBtu	90,500 Btu			
NO <sub>x</sub> Emissions =	663 gal	10 <sup>3</sup> gal	13 lb NOx	=	8.62	lb/hr NO <sub>x</sub>
	hr	1000 gal	10 <sup>3</sup> gal			
	8.62 lb NO <sub>x</sub>	8760 hr	ton	=	37.75	tpy NO <sub>x</sub>
	hr	yr	2000 lb			
CO Emissions =	663 gal	10 <sup>3</sup> gal	7.5 lb CO	=	4.97	lb/hr CO
	hr	1000 gal	10 <sup>3</sup> gal			
	4.97 lb CO	8760 hr	ton	=	21.78	tpy CO
	hr	yr	2000 lb			

Annual Propane usage provided by SEFA

#### Flyash Emissions

	Emission				Uncontrolle	d Emissions	Controlled	Emissions	
Pollutant	Factor	Units	Throughput	Units	lb/hr	ton/yr	lb/hr	ton/yr	Reference
NO <sub>X</sub>	0.12	lb/MMBtu	140	MMBtu/hr	16.80	73.58	16.80	73.58	Emission Factor based on information provided by The SEFA Group Inc.
NO <sub>x</sub>	0.34	lb/MMBtu	140	MMBtu/hr	47.60	208.49	47.60	208.49	Emission Factor based on information provided by The SEFA Group Inc.
со	0.16	lb/MMBtu	140	MMBtu/hr	22.40	98.11	22.40	98.11	Emission Factor based on information provided by The SEFA Group Inc.
VOC	0.016	lb/MMBtu	140	MMBtu/hr	2.24	9.81	2.24	9.81	Emission Factor based on information provided by The SEFA Group Inc.
Lead	126.99	ppmw			6.19E-04	2.71E-03	6.19E-04	2.71E-03	Duke Energy Average Ash Analysis
Arsenic	118.52	ppmw			5.77E-04	2.53E-03	5.77E-04	2.53E-03	Duke Energy Average Ash Analysis
Beryllium	24.55	ppmw			1.20E-04	5.24E-04	1.20E-04	5.24E-04	Duke Energy Average Ash Analysis
Cadmium	21.16	ppmw			1.03E-04	4.52E-04	1.03E-04	4.52E-04	Duke Energy Average Ash Analysis
Chromium	143.92	ppmw			7.01E-04	3.07E-03	7.01E-04	3.07E-03	Duke Energy Average Ash Analysis
Chromium VI	15.83	ppmw			7.71E-05	3.38E-04	7.71E-05	3.38E-04	Duke Energy Average Ash Analysis
Cobalt	57.57	ppmw			2.81E-04	1.23E-03	2.81E-04	1.23E-03	Duke Energy Average Ash Analysis
Manganese	253.98	ppmw			1.24E-03	5.42E-03	1.24E-03	5.42E-03	Duke Energy Average Ash Analysis
Mercury	0.76	ppmw			3.70E-06	1.62E-05	3.70E-06	1.62E-05	Duke Energy Average Ash Analysis
Nickel	143.92	ppmw			7.01E-04	3.07E-03	7.01E-04	3.07E-03	Duke Energy Average Ash Analysis
Selenium	38.94	ppmw			1.90E-04	8.31E-04	1.90E-04	8.31E-04	Duke Energy Average Ash Analysis

#### Sample Calculations

NO <sub>x</sub> Emissions =	0.12 lb NO <sub>x</sub>	140 N	1MBtu	=	16.80 lb/hr NO <sub>x</sub>
	MMBtu	hc	our		
Arsenic Emissions =	118.52 lb As	4.87 lb PM	=	5.77E-04 lb/	/hr Arsenic
(Uncontrolled)	10 <sup>6</sup> lb	hr			

#### Worst-Case STAR® Reactor Unit Emissions

		-					Worst-C	ctor Fly Ash + ase Fuel	STAR® Re Asl Worst-Ca	n + ase Fuel
Pollutant	Natural Gas	ton/yr	Propane E Ib/hr	ton/yr	lb/hr	Emissions ton/yr	lb/hr	Emissions ton/yr	Permitted lb/hr	ton/yr
PM							4.87		4.87	
PM <sub>10</sub>							4.67		4.67	
PM <sub>2.5</sub>							2.58		2.58	
SO <sub>2</sub>							40.23		40.23	
NO <sub>x</sub>	8.24	36.07	8.62	37.75	16.80	73.58	18.22		18.22	
NO <sub>X</sub>	8.24	36.07	8.62	37.75	47.60	208.49	35.82		47.60	
co	4.94	21.64	4.97	21.78	22.40	98.11	17.77		22.40	
VOC	0.32	1.42	0.66	2.90	2.24	9.81	1.94		2.24	
Lead	2.94E-05	1.29E-04			6.19E-04	2.71E-03	6.48E-04		6.48E-04	
Benzene	1.24E-04	5.41E-04					1.24E-04		1.24E-04	
Formaldehyde	4.41E-03	1.93E-02					4.41E-03		4.41E-03	
Hexane	1.06E-01	4.64E-01					1.06E-01		1.06E-01	
Naphthalene	3.59E-05	1.57E-04					3.59E-05		3.59E-05	
Toluene	2.00E-04	8.76E-04					2.00E-04		2.00E-04	
Arsenic	1.18E-05	5.15E-05			5.77E-04	2.53E-03	5.89E-04		5.89E-04	
Beryllium	7.06E-07	3.09E-06			1.20E-04	5.24E-04	1.20E-04		1.20E-04	
Cadmium	6.47E-05	2.83E-04			1.03E-04	4.52E-04	1.68E-04		1.68E-04	
Chromium	8.24E-05	3.61E-04			7.01E-04	3.07E-03	7.84E-04		7.84E-04	
Chromium VI					7.71E-05	3.38E-04	7.71E-05		7.71E-05	
Cobalt	4.94E-06	2.16E-05			2.81E-04	1.23E-03	2.85E-04		2.85E-04	
Manganese	2.24E-05	9.79E-05			1.24E-03	5.42E-03	1.26E-03		1.26E-03	
Mercury	1.53E-05	6.70E-05			3.70E-06	1.62E-05	1.90E-05		1.90E-05	
Nickel	1.24E-04	5.41E-04			7.01E-04	3.07E-03	8.25E-04		8.25E-04	
Selenium	1.41E-06	6.18E-06			1.90E-04	8.31E-04	1.91E-04		1.91E-04	

#### Natural Gas Emissions

	Emission				Emis	sions	
Pollutant	Factor	Units	Throughput	Units	lb/hr	ton/yr	Reference
PM/PM <sub>10</sub> /PM <sub>2.5</sub>	7.6	lb/MMscf	58,824	scf/hr	0.45	1.96	EPA AP-42, Table 1.4-2 (07/98)
SO <sub>2</sub>	0.6	lb/MMscf	58,824	scf/hr	0.04	0.15	EPA AP-42, Table 1.4-2 (07/98)
NO <sub>X</sub>	140	lb/MMscf	58,824	scf/hr	8.24	36.07	EPA AP-42, Table 1.4-1 (07/98)
со	84	lb/MMscf	58,824	scf/hr	4.94	21.64	EPA AP-42, Table 1.4-1 (07/98)
VOC	5.5	lb/MMscf	58,824	scf/hr	0.32	1.42	EPA AP-42, Table 1.4-2 (07/98)
Lead	0.0005	lb/MMscf	58,824	scf/hr	2.94E-05	1.29E-04	EPA AP-42, Table 1.4-2 (07/98)
Benzene	0.0021	lb/MMscf	58,824	scf/hr	1.24E-04	5.41E-04	EPA AP-42, Table 1.4-3 (07/98)
Formaldehyde	0.075	lb/MMscf	58,824	scf/hr	4.41E-03	1.93E-02	EPA AP-42, Table 1.4-3 (07/98)
Hexane	1.8	lb/MMscf	58,824	scf/hr	1.06E-01	4.64E-01	EPA AP-42, Table 1.4-3 (07/98)
Naphthalene	0.00061	lb/MMscf	58,824	scf/hr	3.59E-05	1.57E-04	EPA AP-42, Table 1.4-3 (07/98)
Toluene	0.0034	lb/MMscf	58,824	scf/hr	2.00E-04	8.76E-04	EPA AP-42, Table 1.4-3 (07/98)
Arsenic	0.0002	lb/MMscf	58,824	scf/hr	1.18E-05	5.15E-05	EPA AP-42, Table 1.4-4 (07/98)
Beryllium	0.000012	lb/MMscf	58,824	scf/hr	7.06E-07	3.09E-06	EPA AP-42, Table 1.4-4 (07/98)
Cadmium	0.0011	lb/MMscf	58,824	scf/hr	6.47E-05	2.83E-04	EPA AP-42, Table 1.4-4 (07/98)
Chromium	0.0014	lb/MMscf	58,824	scf/hr	8.24E-05	3.61E-04	EPA AP-42, Table 1.4-4 (07/98)
Cobalt	0.000084	lb/MMscf	58,824	scf/hr	4.94E-06	2.16E-05	EPA AP-42, Table 1.4-4 (07/98)
Manganese	0.00038	lb/MMscf	58,824	scf/hr	2.24E-05	9.79E-05	EPA AP-42, Table 1.4-4 (07/98)
Mercury	0.00026	lb/MMscf	58,824	scf/hr	1.53E-05	6.70E-05	EPA AP-42, Table 1.4-4 (07/98)
Nickel	0.0021	lb/MMscf	58,824	scf/hr	1.24E-04	5.41E-04	EPA AP-42, Table 1.4-4 (07/98)
Selenium	0.000024	lb/MMscf	58,824	scf/hr	1.41E-06	6.18E-06	EPA AP-42, Table 1.4-4 (07/98)

#### Sample Calculations

Natural Gas Flow =	60 MMBtu	10 <sup>6</sup> Btu	scf Nat. Gas	=	58,824	scf/hr Natural Gas
	hr	MMBtu	1020 Btu			
NO <sub>x</sub> Emissions =	58824 scf	MMscf	140 lb NOx	=	8.24	lb/hr NO <sub>x</sub>
	hr	10 <sup>6</sup> scf	MMscf			
	8.24 lb NO <sub>x</sub>	8760 hr	ton	=	36.07	tpy NO <sub>x</sub>
	hr	yr	2000 lb			
CO Emissions =	58824 scf	MMscf	84 lb CO	=	4.94	lb/hr CO
	hr	10 <sup>6</sup> scf	MMscf			
	4.04 11 .00	07001	1			
	4.94 lb CO	8760 hr	ton	=	21.64	tpy CO
	hr	yr	2000 lb			

Anuual Natural Gas usage provided by SEFA

#### Propane Emissions

	Emission				Emissions			
Pollutant	Factor	Units	Throughput	Units	lb/hr	ton/yr	Reference	
PM/PM <sub>10</sub> /PM <sub>2.5</sub>	0.7	lb/10 <sup>3</sup> gal	663	gal/hr	0.46	2.03	EPA AP-42, Table 1.5-1 (07/08)	
SO <sub>2</sub>	0.018	lb/10 <sup>3</sup> gal	663	gal/hr	0.01	0.05	EPA AP-42, Table 1.5-1 (07/08)	Propane sulfur content 0.18 gr/100 ft3
NO <sub>X</sub>	13	lb/10 <sup>3</sup> gal	663	gal/hr	8.62	37.75	EPA AP-42, Table 1.5-1 (07/08)	1
СО	7.5	lb/10 <sup>3</sup> gal	663	gal/hr	4.97	21.78	EPA AP-42, Table 1.5-1 (07/08)	
VOC	1	lb/10 <sup>3</sup> gal	663	gal/hr	0.66	2.90	EPA AP-42, Table 1.5-1 (07/08)	

### Sample Calculations

Propane Flow =	60 MMBtu	10 <sup>6</sup> Btu	gal Propane	=	663	gal/hr Propane
	hr	MMBtu	90,500 Btu			
NO <sub>x</sub> Emissions =	663 gal	10 <sup>3</sup> gal	13 lb NOx	=	8.62	lb/hr NO <sub>x</sub>
	hr	1000 gal	10 <sup>3</sup> gal			
	8.62 lb NO <sub>x</sub>	8760 hr	ton	=	37.75	tpy NO <sub>x</sub>
	hr	yr	2000 lb			
CO Emissions =	663 gal	10 <sup>3</sup> gal	7.5 lb CO	=	4.97	lb/hr CO
	hr	1000 gal	10 <sup>3</sup> gal			
	4.97 lb CO	8760 hr	ton	=	21.78	tpy CO
	hr	yr	2000 lb			

Anuual Propane usage provided by SEFA

#### Flyash Emissions

	Emission				Uncontrolle	d Emissions	Controlled Emissions		
Pollutant	Factor	Units	Throughput	Units	lb/hr	ton/yr	lb/hr	ton/yr	Reference
NO <sub>x</sub>	0.12	lb/MMBtu	130	MMBtu/hr	15.60	68.33	15.60	68.33	Emission Factor based on information provided by The SEFA Group Inc.
NO <sub>X</sub>	0.34	lb/MMBtu	130	MMBtu/hr	44.20	193.60	44.20	193.60	Emission Factor based on information provided by The SEFA Group Inc.
со	0.16	lb/MMBtu	130	MMBtu/hr	20.80	91.10	20.80	91.10	Emission Factor based on information provided by The SEFA Group Inc.
VOC	0.016	lb/MMBtu	130	MMBtu/hr	2.08	9.11	2.08	9.11	Emission Factor based on information provided by The SEFA Group Inc.
Lead	126.99	ppmw			6.19E-04	2.71E-03	6.19E-04	2.71E-03	Duke Energy Average Ash Analysis
Arsenic	118.52	ppmw			5.77E-04	2.53E-03	5.77E-04	2.53E-03	Duke Energy Average Ash Analysis
Beryllium	24.55	ppmw			1.20E-04	5.24E-04	1.20E-04	5.24E-04	Duke Energy Average Ash Analysis
Cadmium	21.16	ppmw			1.03E-04	4.52E-04	1.03E-04	4.52E-04	Duke Energy Average Ash Analysis
Chromium	143.92	ppmw			7.01E-04	3.07E-03	7.01E-04	3.07E-03	Duke Energy Average Ash Analysis
Chromium VI	15.83	ppmw			7.71E-05	3.38E-04	7.71E-05	3.38E-04	Duke Energy Average Ash Analysis
Cobalt	57.57	ppmw			2.81E-04	1.23E-03	2.81E-04	1.23E-03	Duke Energy Average Ash Analysis
Manganese	253.98	ppmw			1.24E-03	5.42E-03	1.24E-03	5.42E-03	Duke Energy Average Ash Analysis
Mercury	0.76	ppmw			3.70E-06	1.62E-05	3.70E-06	1.62E-05	Duke Energy Average Ash Analysis
Nickel	143.92	ppmw			7.01E-04	3.07E-03	7.01E-04	3.07E-03	Duke Energy Average Ash Analysis
Selenium	38.94	ppmw			1.90E-04	8.31E-04	1.90E-04	8.31E-04	Duke Energy Average Ash Analysis

#### Sample Calculations

NO <sub>x</sub> Emissions =	0.12 lb NO <sub>x</sub>	130 MMBtu		=	15.60 lb/hr NO <sub>x</sub>
	MMBtu	ho	our		
Arsenic Emissions =	118.52 lb As	4.87 lb PM	=	5.77E-04 I	b/hr Arsenic
(Uncontrolled)	10 <sup>6</sup> lb	hr			

#### Worst-Case STAR® Reactor Unit Emissions

	Natural Gas	Emissions	Propane E	missions	Fly Ash E	missions	Worst-C	ctor Fly Ash + ase Fuel Emissions	As Worst-C	eactor Fly h + ase Fuel Emissions
Pollutant	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr	lb/hr	ton/yr
PM								21.34		21.34
PM <sub>10</sub>								19.63		19.63
PM <sub>2.5</sub>								11.31		11.31
SO <sub>2</sub>								163.63		163.63
NO <sub>X</sub>	8.24	36.07	8.62	37.75	15.60	68.33		112.29		112.29
со	4.94	21.64	4.97	21.78	20.80	91.10		70.84		91.10
VOC	0.32	1.42	0.66	2.90	2.08	9.11		7.81		9.11
Lead	2.94E-05	1.29E-04			6.19E-04	2.71E-03		2.84E-03		2.84E-03
Benzene	1.24E-04	5.41E-04						5.41E-04		5.41E-04
Formaldehyde	4.41E-03	1.93E-02						1.93E-02		1.93E-02
Hexane	1.06E-01	4.64E-01						4.64E-01		4.64E-01
Naphthalene	3.59E-05	1.57E-04						1.57E-04		1.57E-04
Toluene	2.00E-04	8.76E-04						8.76E-04		8.76E-04
Arsenic	1.18E-05	5.15E-05			5.77E-04	2.53E-03		2.58E-03		2.58E-03
Beryllium	7.06E-07	3.09E-06			1.20E-04	5.24E-04		5.27E-04		5.27E-04
Cadmium	6.47E-05	2.83E-04			1.03E-04	4.52E-04		7.35E-04		7.35E-04
Chromium	8.24E-05	3.61E-04			7.01E-04	3.07E-03		3.43E-03		3.43E-03
Chromium VI					7.71E-05	3.38E-04		3.38E-04		3.38E-04
Cobalt	4.94E-06	2.16E-05			2.81E-04	1.23E-03		1.25E-03		1.25E-03
Manganese	2.24E-05	9.79E-05			1.24E-03	5.42E-03		5.52E-03		5.52E-03
Mercury	1.53E-05	6.70E-05			3.70E-06	1.62E-05		8.32E-05		8.32E-05
Nickel	1.24E-04	5.41E-04			7.01E-04	3.07E-03		3.61E-03		3.61E-03
Selenium	1.41E-06	6.18E-06			1.90E-04	8.31E-04		8.37E-04		8.37E-04

Est. Gas Flow, acfm		56,846
PM Emission Rate, gr/acf		0.01
Estimated Emissions		
PM (lb/hr)		4.87
PM (TPY)		21.34
		lb/hr
	PM	4.87
	PM <sub>10</sub> (Note 2)	4.48
	PM <sub>2.5</sub> (Note 3)	2.58

Notes:

- 1. PM Emission Factor (grains/acf)
- 2. PM<sub>10</sub> = 3. PM<sub>2.5</sub> =
- 92% 53%

of Total PM (From AP-42 Table 1.1-6 (09/98)) of Total PM (From AP-42 Table 1.1-6 (09/98))

4. TPY = Tons per Year

#### Duke Energy Buck Station STAR<sup>®</sup> Emissions - SO<sub>2</sub> - Shortterm (ES-74)

Process Throughput										
Raw Feed LOI (%)	6.0%	7.0%	8.0%	9.0%	10.0%	11.0%	12.0%	13.0%	14.0%	15.0%
Max Heat Input (MMBtu/hr)	140	140	140	140	140	140	140	140	140	140
Carbon (lb/hr)	9,655	9,655	9,655	9,655	9,655	9,655	9,655	9,655	9,655	9,655
Raw Feed Rate (TPH)	80.46	68.97	60.34	53.64	48.28	43.89	40.23	37.14	34.48	32.18
Feed Ash Sulfur %	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%
Estimated Emissions										
SO <sub>2</sub> (lb/hr) - Uncontrolled - Ash	804.60	689.66	603.45	536.40	482.76	438.87	402.30	371.35	344.83	321.84
SO <sub>2</sub> (lb/hr) - Uncontrolled - NG/Propane	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04	0.04
SO <sub>2</sub> (lb/hr) - Uncontrolled - Total	804.63	689.69	603.48	536.43	482.79	438.91	402.33	371.39	344.86	321.87
SO <sub>2</sub> (lb/hr) - Controlled										
95.00%	40.23	34.48	30.17	26.82	24.14	21.95	20.12	18.57	17.24	16.09

#### Duke Energy Buck Station STAR<sup>®</sup> Emissions - SO<sub>2</sub> - Annual (ES-74)

Process Throughput										
Raw Feed LOI (%)	6.0%	7.0%	8.0%	9.0%	10.0%	11.0%	12.0%	13.0%	14.0%	15.0%
Max Heat Input (MMBtu/hr)	130	130	130	130	130	130	130	130	130	130
Carbon (lb/hr)	8,966	8,966	8,966	8,966	8,966	8,966	8,966	8,966	8,966	8,966
Raw Feed Rate (TPH)	74.71	64.04	56.03	49.81	44.83	40.75	37.36	34.48	32.02	29.89
Feed Ash Sulfur %	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%	0.25%
Estimated Emissions $SO_2$ (lb/hr) - Uncontrolled - Ash	747.13	640.39	560.34	498.08	448.28	407.52	373.56	344.83	320.20	298.85
SO <sub>2</sub> (lb/hr) - Uncontrolled - NG/Propane SO <sub>2</sub> (lb/hr) - Uncontrolled - Total SO <sub>2</sub> (lb/hr) - Controlled	0.04 747.16	0.04 640.43	0.04 560.38	0.04 498.12	0.04 448.31	0.04 407.56	0.04 373.60	0.04 344.86	0.04 320.23	0.04 298.89
95.00%	37.36	32.02	28.02	24.91	22.42	20.38	18.68	17.24	16.01	14.94

#### **Duke Energy Buck Station** EHE Emissions Unit 1 and Unit 2 (ES-77 and ES-78)

Total operation of unit 1 and 2 combined will not exceed 8760 hours per years Therefore annual emission are based on the lb/hr of a single unit \* 8760 hours per year.

	Est. Emissions		
		TPY	
	lb/hr	(Total for	
	(per unit)	both units)	
PM (Note 2)	5.36	23.46	
PM <sub>10</sub> (Note 3)	4.93	21.59	
PM <sub>2.5</sub> (Note 4)	2.84	12.44	

			Emissions		
Pollutant	Emission Factor	Units	lb/hr (per unit)	ton/yr (Total for both units)	Reference
Lead	126.99	ppmw	6.80E-04	2.98E-03	Duke Energy Average Ash Analysis
Arsenic	118.52	ppmw	6.35E-04	2.78E-03	Duke Energy Average Ash Analysis
Beryllium	24.55	ppmw	1.32E-04	5.76E-04	Duke Energy Average Ash Analysis
Cadmium	21.16	ppmw	1.13E-04	4.97E-04	Duke Energy Average Ash Analysis
Chromium	143.92	ppmw	7.71E-04	3.38E-03	Duke Energy Average Ash Analysis
Chromium VI	15.83	ppmw	8.48E-05	3.71E-04	Duke Energy Average Ash Analysis
Cobalt	57.57	ppmw	3.08E-04	1.35E-03	Duke Energy Average Ash Analysis
Manganese	253.98	ppmw	1.36E-03	5.96E-03	Duke Energy Average Ash Analysis
Mercury	0.76	ppmw	4.07E-06	1.78E-05	Duke Energy Average Ash Analysis
Nickel	143.92	ppmw	7.71E-04	3.38E-03	Duke Energy Average Ash Analysis
Selenium	38.94	ppmw	2.09E-04	9.14E-04	Duke Energy Average Ash Analysis

Notes:

1. Exhaust Flow (dSCFM):

25,000 2. PM Emission Factor (grains/dSCF) 0.025

Vendor Guarantee 92% of Total PM (From AP-42 Table 1.1-6 (09/98))

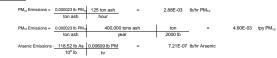
3. PM<sub>10</sub> = 4. PM<sub>2.5</sub> = 53% of Total PM (From AP-42 Table 1.1-6 (09/98))

5. TPY = Tons per Year

#### Duke Energy Buck Station Silos and Dome Emissions

#### Potential Emissions ES-80B Storage Dome ES-73A Feed Silo Filling ES-73B Feed Silo Unloading ES-81A Loadout Silo Chute 1A ES-81B Loadout Silo Chute 1B ES-80A Storage Dome Filling ES-79A Transfer Silo Filling ES-79B Transfer Silo Unloading ES-81 Loadout Silo Unloa (275 tph, 400,000 tpy) Emission (125 tph, 400,000 tpy) (75 tph, 400,000 tpy) (75 tph, 400,000 tpy) (100 tph, 200,000 tpy) (100 tph, 200,000 tpy) (75 tph, 400,000 tpy) (125 tph, 400,000 tpy) (75 tph, 400,000 tpy) Total Silo Emissions lb/hr lb/hr ton/yr Pollutan Units lb/hr lb/hr lb/hr lb/hr lb/hr lb/hr lb/hr lb/hr Factor ton/yr ton/yr ton/yr ton/yr ton/yr ton/yr ton/yr ton/yr ton/yr 0.0000487 lb/ton 6.09E-03 9.74E-03 3.65E-03 9.74E-03 3.65E-03 9.74E-03 4.87E-03 4.87E-03 4.87E-03 4.87E-03 3.65E-03 9.74E-03 1.34E-02 9.74E-03 6.09E-03 9.74E-03 3.65E-03 9.74E-03 4.99E-02 7.79E-02 ΡM PM10 0.000023 lb/ton 2.88E-03 4.60E-03 1.73E-03 4.60E-03 1.73E-03 4.60E-03 2.30E-03 2.30E-03 2.30E-03 2.30E-03 1.73E-03 4.60E-03 6.33E-03 4.60E-03 2.88E-03 4.60E-03 1.73E-03 4.60E-03 2.36E-02 3.68E-02 PM<sub>2.4</sub> 0.000023 lb/ton 2.88E-03 4.60E-03 1.73E-03 4.60E-03 1.73E-03 4.60E-03 2.30E-03 2.30E-03 2.30E-03 2.30E-03 1.73E-03 4.60E-03 6.33E-03 4.60E-03 2.88E-03 4.60E-03 1.73E-03 4.60E-03 2.36E-02 3.68E-02 7.73E-07 4.64E-07 4.64E-07 6.18E-07 6.18E-07 4.64E-07 1.70E-06 1.24E-06 6.34E-06 ead 126.99 ppmw 1.24E-06 1.24E-06 1.24E-06 6.18E-07 6.18E-07 1.24E-06 1.24E-06 7.73E-07 1.24E-06 4.64E-07 9.90E-06 Arsenic 118.52 ppmw 7.21E-07 1.15E-06 4.33E-07 1.15E-06 4.33E-07 1.15E-06 5.77E-07 5.77E-07 5.77E-07 5.77E-07 4.33E-07 1.15E-06 1.59E-06 1.15E-06 7.21E-07 1.15E-06 4.33E-07 1.15E-06 5.92E-06 9.24E-06 Energy Average Ash 24.55 ppmw 1.49E-07 2.39E-07 8.97E-08 2.39E-07 8.97E-08 2.39E-07 1.20E-07 1.20E-07 1.20E-07 1.20E-07 8.97E-08 2.39E-07 3.29E-07 2.39E-07 1.49E-07 2.39E-07 8.97E-08 2.39E-07 1.23E-06 1.91E-06 Beryllium e Energy Average As 21.16 ppmw 1.29E-07 2.06E-07 7.73E-08 2.06E-07 7.73E-08 2.06E-07 1.03E-07 1.03E-07 1.03E-07 1.03E-07 7.73E-08 2.06E-07 2.83E-07 2.06E-07 1.29E-07 2.06E-07 7.73E-08 2.06E-07 1.06E-06 1.65E-06 Cadmium tuke Energy Average Ash Ana 143.92 ppmw 8.76E-07 1.40E-06 5.26E-07 1.40E-06 5.26E-07 1.40E-06 7.01E-07 7.01E-07 7.01E-07 7.01E-07 5.26E-07 1.40E-06 1.93E-06 1.40E-06 8.76E-07 1.40E-06 5.26E-07 1.40E-06 7.18E-06 1.12E-05 hromiun ke Energy Average Ash Anal 5.78E-08 5.78E-08 1.54E-07 7.71E-08 7.71E-08 7.71E-08 5.78E-08 2.12E-07 1.54E-07 9.64E-08 5.78E-08 1.54E-07 7.90E-07 1.23E-06 Chromium VI 15.83 ppmw 9.64E-08 1.54E-07 1.54E-07 7.71E-08 1.54E-07 1.54E-07 e Energy Average Ash Anal 57.57 ppmw 3.50E-07 5.61E-07 2.10E-07 5.61E-07 2.10E-07 5.61E-07 2.80E-07 2.80E-07 2.80E-07 2.80E-07 2.10E-07 5.61E-07 7.71E-07 5.61E-07 3.50E-07 5.61E-07 2.10E-07 5.61E-07 2.87E-06 4.49E-06 Cobalt Energy Average Ash Analysis 253.98 ppmw 1.55E-06 2.47E-06 9.28E-07 2.47E-06 9.28E-07 2.47E-06 1.24E-06 1.24E-06 1.24E-06 1.24E-06 9.28E-07 2.47E-06 3.40E-06 2.47E-06 1.55E-06 2.47E-06 9.28E-07 2.47E-06 1.27E-05 1.98E-05 Manganese ke Energy Average Ash Analysi 0.76 ppmw 4.63E-09 7.40E-09 2.78E-09 7.40E-09 2.78E-09 7.40E-09 3.70E-09 3.70E-09 3.70E-09 3.70E-09 2.78E-09 7.40E-09 1.02E-08 7.40E-09 4.63E-09 7.40E-09 2.78E-09 7.40E-09 3.79E-08 5.92E-08 Nercury e Energy Average Ash Analys Nickel 143.92 ppmw 8.76E-07 1.40E-06 5.26E-07 1.40E-06 5.26E-07 1.40E-06 7.01E-07 7.01E-07 7.01E-07 7.01E-07 5.26E-07 1.40E-06 1.93E-06 1.40E-06 8.76E-07 1.40E-06 5.26E-07 1.40E-06 7.18E-06 1.12E-05 e Energy Average Ash Analys alanium 38.94 ppmw 2.37E-07 3.79E-07 1.42E-07 3 79E-07 1.42E-07 3 79E-07 1 90E-07 1 90E-07 1 90E-07 1 90E-07 1.42E-07 3 79E-07 5 22E-07 3 70E-07 2.37E-07 3 79E-07 1.42E-07 3 79E-07 1.94E-06 3.03E-06

Sample Calculations



# Duke Energy Buck Station Pollution Control Silos

		FGD Absorbent Silo (ES-76)		FGD Byproduc	ct Silo (ES-75)
Est. Gas Flow, acfm		1,300		1,300	
PM loading Rate, gr/acf		0.005		0.005	
Estimated Emissions	Estimated Emissions				
			tpy	lb/hr	tpy
	PM	0.06	0.24	0.06	0.24
	PM <sub>10</sub> (Note 2)	0.05	0.22	0.05	0.22
	PM <sub>2.5</sub> (Note 3)	0.03	0.13	0.03	0.13

Total					
lb/hr	tpy				
0.11	0.49				
0.10	0.45				
0.06	0.26				

Notes:

1. PM Emission Factor (grains/acf)

- 2. PM<sub>10</sub> = 92% 53%
- 3. PM<sub>2.5</sub> =

4. TPY = Tons per Year

of Total PM (From AP-42 Table 1.1-6 (09/98))

of Total PM (From AP-42 Table 1.1-6 (09/98))

#### **Duke Energy Buck Station** Wet Ash Receiving Emissions (F-1 and F-2)

#### Transfer of material to storage shed (F-1)

Section 13.2-4 Aggregate Handling and Storage Piles, Ap-42 Fifth Edition November 2006

E= k*	0.0032 * (((U/5)^1.3)/((	M/2)^1.4))	
E =	lb/ton		
k =	particle size	e multiplier (dimensionless)	
	PM	0.74	
	PM <sub>10</sub>	0.35	
	PM <sub>2.5</sub>	0.053	
U =	mean wind	speed, miles per hour (mph) 3	Average wind speed for 2016 Rowan County airport about 9 miles from the site from weatherunderground.com
M =		isture content 15	15% moisture content is an conservatively low estimate typical moisture is 20%
	70 tph 400,000 tpy	Based on Air Permit info 2-17-	17, Item 9
	lb/hr	tpv	

	lb/hr	tpy
PM	2.54E-03	7.26E-03
PM <sub>10</sub>	1.20E-03	3.43E-03
PM <sub>2.5</sub>	1.82E-04	5.20E-04

Note: assumed 50% control as a result of the shed having three side to enclose pile

			Emissions		
Pollutant	Emission Factor	Units	lb/hr	ton/yr	Reference
Lead	126.99	ppmw	3.23E-07	9.22E-07	Duke Energy Average Ash Analysis
Arsenic	118.52	ppmw	3.01E-07	8.60E-07	Duke Energy Average Ash Analysis
Beryllium	24.55	ppmw	6.24E-08	1.78E-07	Duke Energy Average Ash Analysis
Cadmium	21.16	ppmw	5.38E-08	1.54E-07	Duke Energy Average Ash Analysis
Chromium	143.92	ppmw	3.66E-07	1.04E-06	Duke Energy Average Ash Analysis
Chromium VI	15.83	ppmw	4.02E-08	1.15E-07	Duke Energy Average Ash Analysis
Cobalt	57.57	ppmw	1.46E-07	4.18E-07	Duke Energy Average Ash Analysis
Manganese	253.98	ppmw	6.45E-07	1.84E-06	Duke Energy Average Ash Analysis
Mercury	0.76	ppmw	1.94E-09	5.53E-09	Duke Energy Average Ash Analysis
Nickel	143.92	ppmw	3.66E-07	1.04E-06	Duke Energy Average Ash Analysis
Selenium	38.94	ppmw	9.89E-08	2.83E-07	Duke Energy Average Ash Analysis

#### **Duke Energy Buck Station** Wet Ash Receiving Emissions (F-1 and F-2)

#### Transfer of material to hopper (F-2)

Section 13.2-4 Aggregate Handling and Storage Piles, Ap-42 Fifth Edition November 2006

E= k\*0.0032 \* (((U/5)^1.3)/((M/2)^1.4))

E =	lb/ton					
k =	particle size	particle size multiplier (dimensionless)				
	PM	0.74				
	PM <sub>10</sub>	0.35				
	PM <sub>2.5</sub>	0.053				

U = mean wind speed, miles per hour (mph) 3 material moisture content 15 M =

Average wind speed for 2016 Rowan County airport about 9 miles from the site from weatherunderground.com 15% moisture content is an conservatively low estimate typical moisture is 20%

70 tph Based on Air Permit info 2-17-17, Item 9 400,000 tpy

	lb/hr	tpy
PM	5.08E-03	1.45E-02
PM <sub>10</sub>	2.40E-03	6.87E-03
PM <sub>2.5</sub>	3.64E-04	1.04E-03

			Emissions		
Pollutant	Emission Factor	Units	lb/hr	ton/yr	Reference
Lead	126.99	ppmw	6.45E-07	1.84E-06	Duke Energy Average Ash Analysis
Arsenic	118.52	ppmw	6.02E-07	1.72E-06	Duke Energy Average Ash Analysis
Beryllium	24.55	ppmw	1.25E-07	3.56E-07	Duke Energy Average Ash Analysis
Cadmium	21.16	ppmw	1.08E-07	3.07E-07	Duke Energy Average Ash Analysis
Chromium	143.92	ppmw	7.31E-07	2.09E-06	Duke Energy Average Ash Analysis
Chromium VI	15.83	ppmw	8.04E-08	2.30E-07	Duke Energy Average Ash Analysis
Cobalt	57.57	ppmw	2.93E-07	8.36E-07	Duke Energy Average Ash Analysis
Manganese	253.98	ppmw	1.29E-06	3.69E-06	Duke Energy Average Ash Analysis
Mercury	0.76	ppmw	3.86E-09	1.10E-08	Duke Energy Average Ash Analysis
Nickel	143.92	ppmw	7.31E-07	2.09E-06	Duke Energy Average Ash Analysis
Selenium	38.94	ppmw	1.98E-07	5.65E-07	Duke Energy Average Ash Analysis

### Duke Energy Buck Station Wet Ash Receiving Emissions (F-1 and F-2)

#### **Total Emissions**

Pollutant	lb/hr	tpy
PM	7.62E-03	2.18E-02
PM <sub>10</sub>	3.61E-03	1.03E-02
PM <sub>2.5</sub>	5.46E-04	1.56E-03
Lead	9.68E-07	2.77E-06
Arsenic	9.03E-07	2.58E-06
Beryllium	1.87E-07	5.35E-07
Cadmium	1.61E-07	4.61E-07
Chromium	1.10E-06	3.13E-06
Chromium VI	1.21E-07	3.45E-07
Cobalt	4.39E-07	1.25E-06
Manganese	1.94E-06	5.53E-06
Mercury	5.80E-09	1.66E-08
Nickel	1.10E-06	3.13E-06
Selenium	2.97E-07	8.48E-07

#### Duke Energy Buck Station GHG Emissions

Heating Value of Natural Gas	1,028	btu/scf	Table C-1 to subpart C of 40 CFR Part 98 (natural gas)
Heat Input	15,840	MMBtu/yr	Total Supplemental / Auxiliary Fuel = 12 months x 3 cold starts x 400 MM Btu = 14,400 MM Btu's + 10% = 15,840 MM Btu's per year.
Operation Hours	24 8,760	hrs/day hrs/year	
$\frac{Emission Factors}{CO_2}$ $CH_4$ $N_2O$ $CO_2$ $CH_4$ $N_2O$	53.06 1.00E-03 1.00E-04 2.20462 116.98 2.20E-03 2.20E-04	kg CO <sub>2</sub> /MMBtu kg CH <sub>4</sub> /MMBtu kg N <sub>2</sub> O/MMBtu lb/kg lb/MMBtu lb/MMBtu lb/MMBtu	Table C-1 to subpart C of 40 CFR Part 98 (natural gas) Table C-2 to subpart C of 40 CFR Part 98 ( natural gas) Table C-2 to subpart C of 40 CFR Part 98 ( natural gas) Table A-2 to subpart A of 40 CFR Part 98
<u>Global Warming Potential</u> CO <sub>2</sub> CH <sub>4</sub> N <sub>2</sub> O Emission Rates - GHG (CO <sub>2</sub> e)	1 25 298		Table A-1 to subpart A of 40 CFR Part 98 Table A-1 to subpart A of 40 CFR Part 98 Table A-1 to subpart A of 40 CFR Part 98
CO <sub>2</sub> CH <sub>4</sub> (CO <sub>2</sub> e) N <sub>2</sub> O (CO2e)	<b>lb/yr</b> 1,852,917.85 873.03 1,040.65	<b>tpy</b> 926.46 0.44 0.52	
GHG (CO <sub>2</sub> e)		927.42	
CO <sub>2</sub> CH <sub>4</sub> N <sub>2</sub> O GHG (Mass Basis)	<b>Ib/yr</b> 1,852,917.85 34.92 3.49	tpy 926.46 0.02 0.00 926.48	

#### Duke Energy Buck Station GHG Emissions

Heating Value of Propane	0.091	MMBtu/gal	Table C-1 to subpart C of 40 CFR Part 98 (petroleum products)
Heat Input	15,840	MMBtu/yr	
Emission Factors CO <sub>2</sub>	C4 4C		Table C 4 to subset C of 40 CED Dat 00 (presents - patroleum products)
-	61.46 3.00E-03	kg CO <sub>2</sub> /MMBtu	Table C-1 to subpart C of 40 CFR Part 98 (propane - petroleum products)
CH₄		kg CH₄/MMBtu	Table C-2 to subpart C of 40 CFR Part 98 (petroleum)
N <sub>2</sub> O	6.00E-04	kg N <sub>2</sub> O/MMBtu	Table C-2 to subpart C of 40 CFR Part 98 (petroleum)
	2.20462	lb/kg	Table A-2 to subpart A of 40 CFR Part 98
CO <sub>2</sub>	135.50	lb/MMBtu	
CH <sub>4</sub>	6.61E-03	lb/MMBtu	
N <sub>2</sub> O	1.32E-03	lb/MMBtu	
Global Warming Potential			
CO <sub>2</sub>	1		Table A-1 to subpart A of 40 CFR Part 98
CH <sub>4</sub>	25		Table A-1 to subpart A of 40 CFR Part 98
N <sub>2</sub> O	298		Table A-1 to subpart A of 40 CFR Part 98
Emission Rates - GHG (CO2e)			
	lb/yr	tpy	
CO <sub>2</sub>	2,146,255.77	1,073.13	
CH <sub>4</sub> (CO <sub>2</sub> e)	2,619.09	1.31	
N <sub>2</sub> O (CO2e)	6,243.91	3.12	
GHG (CO <sub>2</sub> e)		1,077.56	
	lb/yr	tpy	
CO <sub>2</sub>	2,146,255.77	1,073.13	
CH <sub>4</sub>	104.76	0.05	
N <sub>2</sub> O	20.95	0.01	
		4 072 40	
GHG (Mass Basis)		1,073.19	
STAR CO <sub>2</sub> Production			
Yearly Feed Rate (TPY)	400,000		
Average Feed LOI	7.80%		
Availability	80.00%		
Avg. Feed Rate (TPH)	57.08		400,000/ (8760*80%)
Avg. Fuel Input (MMBtu/hr)	129.11		57.08*2000*7.80%*14500/1000000
Max. CO <sub>2</sub> Production (TPY)	114,401		57.08*2000*7.80%*3.6667*8760*80%/2000

Note: Duke Energy expects 6%-15% LOI. LOI will affect throughput.

Expected GHG Emission Range $CO_2$	116,400.63
$CH_4 (CO_2e)$	1.75
$N_2O (CO2e)$	3.64
GHG (CO <sub>2</sub> e)	116,406.02
CO <sub>2</sub>	116,400.63
CH <sub>4</sub>	0.07
N <sub>2</sub> O	0.01
GHG (Mass Basis)	116,400.71

#### Duke Energy Buck Station Unloading Pile Windblown Fugitive Dust Emissions (F-3)

Where.	E <sub>1</sub> = E <sub>f</sub> * A E <sub>f</sub> = J * 1.7 * ((sL)/1.5) * ((365-	4
,	E1 = Particulate matter emissio	н
	E <sub>f</sub> = Emission Factor in tons/ad	С
	A = Exposed surface area of s	s
	J = Particulate aerodynamic f	a
	J (TSP) =	1
	J (PM <sub>10</sub> ) =	0.5
	J (PM <sub>2.5</sub> ) =	0.2
	sL = Average silt loading of sto	DI
	P = Average number of days/	y
	I = Percent of time with unob	5
	E <sub>2</sub> = Particulate matter emissio	и
	$E_2 = E_1/8760*2000$	

From Emissions Inventory Guidance, Mineral (Methodology Derived From AP-42, Chapter 1

Silt Loading =	12 %	6
Conservative Days with Precipitation =	120 da	ays
Conservative Windy Hours =	8.3 %	ó
Acreage of Fly Ash Pile =	0.03 a	cres
Control Efficiency (Dust Suppression) =	50 %	ó

Pollutant				Potential En (with Cor	
				(lb/hr)	(ton/yr)
PM				4.90E-03	2.15E-02
PM <sub>10</sub>				2.45E-03	1.07E-02
PM <sub>2.5</sub>				9.81E-04	4.30E-03
	Emission Factor	Units		(lb/hr)	(ton/yr)
Lead	126.99	ppmw		6.23E-07	2.73E-06
Arsenic	118.52	ppmw		5.81E-07	2.55E-06
Beryllium	24.55	ppmw		1.20E-07	5.27E-07
Cadmium	21.16	ppmw		1.04E-07	4.54E-07
Chromium	143.92	ppmw		7.06E-07	3.09E-06
Chromium VI	15.83	ppmw		7.76E-08	3.40E-07
Cobalt	57.57	ppmw		2.82E-07	1.24E-06
Manganese	253.98	ppmw		1.25E-06	5.45E-06
Mercury	0.76	ppmw		3.73E-09	1.63E-08
Nickel	143.92	ppmw		7.06E-07	3.09E-06
Selenium	38.94	ppmw		1.91E-07	8.36E-07
Note: Emission rates may need to adjus	ted for applicable averaging pe	riod when used for modeling	g.		
Variable			Data Source		
Silt Loading AP-42 Section 13.2.4, Table 13.2.4-1 (Misc Fill Materials) Conservative Days with Precipitation AP-42 Section 13.2.2, Figure 13.2.2-1 Conservative Windy Hours Wind data from Charlotte Airport 2011-2015 Acreage of Ash Pile SEFA 2017					
Control	Efficiency (Dust Suppression) =		e wet with up to 20% moisture		

#### Emissions Estimate: Wind Erosion at the Ash Basin (F-4)

Dust may be generated by wind erosion of exposed area within an industrial facility. Section 13.2.5 of the U.S. EPA's AP-42 document was used to estimate emissions from the monofill.

The first step is to calculate a height-to-base ratio to determine if Equation (4) can be used to determine the friction velocity (u\*):

Assuming a square area, this active area yields an approximate length as follows:

520.7	m, Linear Dimension of Active Area
3.3	ft/m, Conversion Factor
1708.4	ft, Linear Dimension of Active Area
15	ft, Approximate Mean Elevation of the Active Area (Above Grade)

Per page 13.2.5-5 of AP-42, if the height to base ratio is less than 0.2 then Equation (4) can be used to calculate the friction velocity (u\*).

0.009 Calculated Height to Base Ratio

Therefore equation (4) from AP-42 13.2.5 can be used for calculation of the friction velocity.

Per the following website: http://www.nc-climate.ncsu.edu/dynamic\_scripts/cronos/query.php (maintained by the North Carolina State Climate Office), the anemometer height for the fastest mile data is:

10 m, Anemometer Height

Since the reported fastest wind speeds are from an anemometer of height 10 m, using equation (5) on page 13.2.5-6 is not necessary:

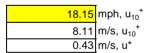
When the calculated friction velocity ( $u^*$ ) exceeds the threshold friction velocity ( $u_t^*$ ), emissions from wind erosion occur. As shown in Equation 3 of AP-42, if  $u^* \le u_t^*$ , emissions are zero.

From Table 13.2.5-1 threshold friction velocity (ut\*) is as follows. The most conservative value presented in AP-42 has been used.

0.43 m/s, ut\* Threshold Friction Velocity

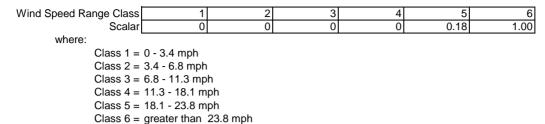
Therefore, in order to generate emissions, the following wind speed must be exceeded.

3,600 sec/hr, Conversion Factor 1,609.3 m/mile, Conversion Factor



#### Emissions Estimate: Wind Erosion at the Ash Basin (F-4)

AERMOD allows users to account for the variability of wind speed when determining offsite impacts. The scalars below are used based on the respective wind speed range. (AERMOD User Guide 3.3.4. Using Variable Emission Rates). There are zero wind based emissions in classes 1 thru 4 because the threshold friction velocity is not exceeded (ut\*). The scalar for Class 5 is determined as the ratio of emission factors for Class 5 and Class 6. Emission factor derivation follows.



The emissions rate (which is dependent on the friction velocity  $(u^*)$ ) varies linearly with wind speed. For Class 5, emissions will increase linearly as wind speed increases. AERMOD does not facilitate the variable emission rates based on wind speed. Therefore, the friction velocity for Class 5 is determined using the upper end wind speed of 23.8 mph. Using Equation (4) on page 13.2.5-5, the equivalent friction velocity  $(u^*)$  may be calculated.

$$u^{*} = 0.053u_{10}^{+}$$
23.8 mph,  $u_{10}^{+}$ 
10.64 m/s,  $u_{10}^{+}$ 
Class 5 0.56 m/s, u\*, Class 5 Wind Speed Range

The friction velocity for Class 6 is determined using the average of the maximum daily wind gusts for each month.

Emission factors for Class 5 and Class 6 are determined using AP-42 Section 13.2.5 Equation (3) which is shown below:

$$PM\left(\frac{g}{m^2}\right) = 58(u^* - u_i^*)^2 + 25(u^* - u_i^*)$$

Equation (3) from AP-42 13.2.5

Where:

 $u^*$  is the friction velocity (m/s)  $u^*_t$  is the threshold friction velocity (m/s)

Class 5	4.39	g/m <sup>2</sup> (of Disturbed Area), Class 5 Wind Speed Range
Class 6	23.84	g/m <sup>2</sup> (of Disturbed Area), Class 6 Wind Speed Range

#### Emissions Estimate: Wind Erosion at the Ash Basin (F-4)

As stated in AP-42, on page 13.2.5-2, emissions generated by wind erosion are also dependent on the frequency of disturbance of the erodible surface because each time that a surface is disturbed, its erosion potential is restored. A disturbance is defined as an action that results in the exposure of fresh surface material. Only a fraction of the active area is disturbed each day. This disturbed area is used to calculate the potential daily emission rate.

10         acres, Working Area           15%         Fraction of Active Area Disturbed Daily           40,468.70         m², Average Area Disturbed Daily	85% Fraction of Inactive Area 230,671.59 m <sup>2</sup> , Average Inactive Area		
453.6 g/lb, Conversion Factor	453.6 g/lb, Conversion Factor		
Class 5 391.4 lb/day Class 6 2127.0 lb/day	Class 5 2231.1 lb/day Class 6 12123.7 lb/day		

The facility will implement mitigation to suppress dust emissions. Control efficiencies are based on engineering judgment and supported by *WRAP Fugitive Dust Handbook, September 7, 2006.* The controlled emission rates for Class 5 and Class 6 emissions are as follows:

	61%	Apply Water every 3.2	hours to disturbed areas	80%	Inherent Moisture and Watering
Class 5**	152.7	lb/day	Class 5	446.2	lb/day
Class 6**	829.5	lb/day	Class 6	2424.7	lb/day

For the purposes of determining potential emissions for permitting, wind data has been applied as shown below.

Total Class 5 Emissions	598.9 lb/day
Total Class 6 Emissions	3254.2 lb/day

Fraction of time in Class 5 0.0116 (approximately 102 hours in Class 5) Fraction of time in Class 6 0.0016 (approximately 14 hours in Class 6)

Time fraction spent in Class 5 and Class 6 determined by analyzing hourly wind speeds for 1992 from DAQ Approved RDU Met Data. 1992

is the worst case modeling year for the 5 year period required to be modeled (1988 - 1992)

Total emissions per day 12.17 lb/day

Emissions from the ash pond will only occur when Class 5 and Class 6 wind speed conditions are met. AERMOD will utilize meteorological data to determine when these conditions occur. For the purposes of the PSD analysis, permitting, and TPER evaluation, it is conservatively assumed that Class 6 condition occur year round.

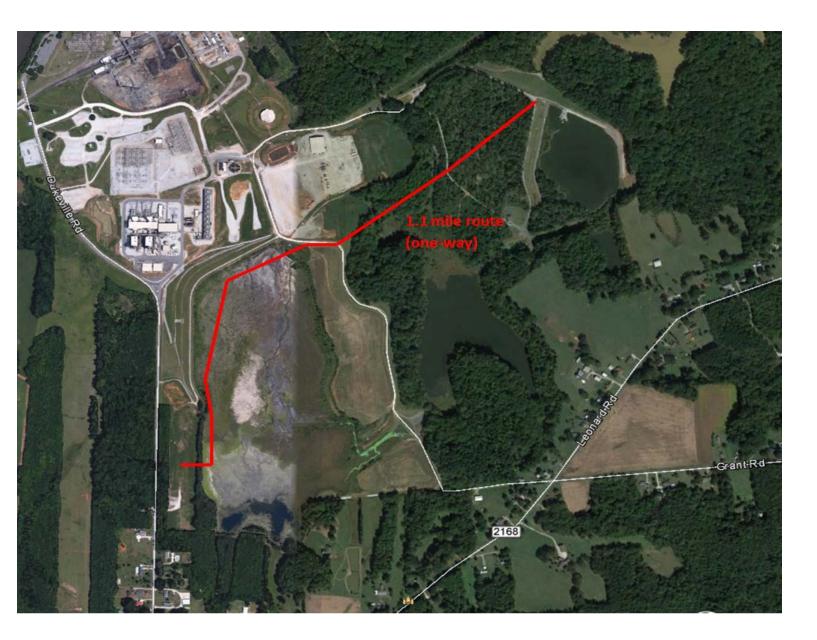
Compound	Avg Ash Analysis (ppm)	Emissions (Ib/hr)	Emissions (Ib/day)	Emissions (Ib/yr)	Emissions (ton/yr)
PM	1.00 **	0.51	12.17	4,443.49	2.22
PM10	0.50 **	0.25	6.09	2,221.74	1.11
PM2.5	0.08 **	0.04	0.91	333.26	0.17
Lead	126.99	6.44E-05	1.55E-03	0.56	2.82E-04
Arsenic	118.52	6.01E-05	1.44E-03	0.53	2.63E-04
Beryllium	24.55	1.25E-05	2.99E-04	0.11	5.45E-05
Cadmium	21.16	1.07E-05	2.58E-04	0.09	4.70E-05
Chromium	143.92	7.30E-05	1.75E-03	0.64	3.20E-04
Chromium VI	15.83	8.03E-06	1.93E-04	0.07	3.52E-05
Cobalt	57.57	2.92E-05	7.01E-04	0.26	1.28E-04
Manganese	253.98	1.29E-04	3.09E-03	1.13	5.64E-04
Mercury	0.76	3.86E-07	9.25E-06	0.00	1.69E-06
Nickel	143.92	7.30E-05	1.75E-03	0.64	3.20E-04
Selenium	38.94	1.98E-05	4.74E-04	0.17	8.65E-05

\*\* PM distribution factors (k value) taken from AP-42 Page 13.2.5-3 All other values in ppm.

### Truck Traffic VMT Estimates

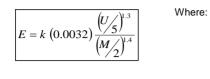
	Ash Trucked Offsite (ton/yr)	Truck Capacity (ton/truck)	Truck Loads/Year	Route Distance (miles)	Total Miles Traveled VMT/yr	Total VMT/yr
Empty Trucks to Loading Area	430,000	25.00	17.200	1.10	18,920.00	37,840.00
Loaded Trucks to Offsite	430,000	23.00	17,200	1.10	18,920.00	57,040.00

Documentation Supporting Haul Road VMT Estimates



#### Emissions Estimate: Ash Handling Operations (F-5)

Section 13.2.4 (Aggregate Handling and Storage Piles) of U.S. EPA's AP-42 document is used to estimate emissions from the handling of material at an industrial site. The "Drop Equation" is shown below:



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E is the emission factor in [lb/ton] K is the particle size multiplier [dimensionless] U is the average wind speed [mph] M is the average moisture content [%]

Constant	PM2.5	PM10	PM
k	0.053	0.35	0.74

7 mph, Average Wind Speed 15 %, Moisture

The HAP and TAP emissions are derived from the PM estimate based on the average trace element analysis: Emissions are calculated assuming a maximum throughput of ash:

	ton/yr, Potential Ash Throughput
8	Number of Drop Points

					Total
AshTrace Element	Average	Emission	Annual	Annual	Annual
Analysis	Concentration	Factor	PTE	PTE	PTE
	(ppm)	(lb/ton)	(lb/yr)	(lb/hr)	(ton/yr)
PM		2.18E-04	751.31	0.09	0.38
PM10		1.03E-04	355.35	0.04	0.18
PM2.5		1.56E-05	53.81	0.01	0.03
Lead	126.99	2.77E-08	0.10	1.09E-05	4.77E-05
Arsenic	118.52	2.59E-08	0.09	1.02E-05	4.45E-05
Beryllium	24.55	5.36E-09	0.02	2.11E-06	9.22E-06
Cadmium	21.16	4.62E-09	0.02	1.81E-06	7.95E-06
Chromium	143.92	3.14E-08	0.11	1.23E-05	5.41E-05
Chromium VI	15.83	3.46E-09	0.01	1.36E-06	5.95E-06
Cobalt	57.57	1.26E-08	0.04	4.94E-06	2.16E-05
Manganese	253.98	5.55E-08	0.19	2.18E-05	9.54E-05
Mercury	0.76	1.66E-10	0.001	6.52E-08	2.85E-07
Nickel	143.92	3.14E-08	0.11	1.23E-05	5.41E-05
Selenium	38.94	8.50E-09	0.03	3.34E-06	1.46E-05

#### Additional Haul Roads Supporting the Movement of Ash Offsite - Loaded Trucks (F-6)

Where:

A portion of the ash will be moved by truck to an offsite location. Particulate emissions are generated from the haul roads from the force of the wheels on the road surface. This force causes pulverization of the surface material. The particles are lifted and dropped from the rolling wheels and the road surface is exposed to strong air currents, which generate airborne particulate emissions.

The methodology presented below is taken from Section 13.2.2 (Unpaved Roads) of the U.S. EPA's AP-42 document and is based on the vehicle miles traveled (VMT) at the site.

$$E = k \left(\frac{s}{12}\right)^a \left(\frac{W}{3}\right)^b$$

Equation 1a of AP-42 Section 13.2.2 for vehicles traveling on unpaved surfaces at industrial sites

Constant	Industrial Roads			
Constant	PM2.5	PM10	PM	
k	0.15	1.5	4.9	
а	0.9	0.9	0.7	
b	0.45	0.45	0.45	

5.1 %, Average Silt Content of Plant Roads at a Coal Mining Site (Table 13.2.2-1) 50 tons, Mean Vehicle Loaded Weight (Fleet Average)

0.25 lb/VMT, Calculated PM2.5 Emission Factor (Road Silt Portion) 2.46 lb/VMT, Calculated PM10 Emission Factor (Road Silt Portion) 9.55 lb/VMT, Calculated PM Emission Factor (Road Silt Portion)

Emissions associated with the exhaust, brake wear, and tire wear must be added to the values calculated above. The values shown below were taken from Table 13.2.2-4.

Particle Size	PM2.5	PM10	PM
lb/VMT "adder"	0.00036	0.00047	0.00047

0.25 lb/VMT, Calculated PM2.5 Emission Factor (Total, No natural mitigation) 2.46 lb/VMT, Calculated PM10 Emission Factor (Total, No natural mitigation) 9.55 lb/VMT, Calculated PM Emission Factor (Total, No natural mitigation)

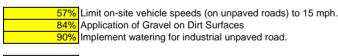
All roads are subject to natural mitigation because of rainfall and other precipitation. The following equation accounts for reductions in the emission factor due to natural mitigation.

$E_{EXT} = E\left[\frac{(365 - P)}{365}\right]$ Where	<ul> <li>E<sub>EXT</sub> is the adjusted emission factor accounting for natural mitigation</li> <li>E is emission factor from Equation 1a</li> <li>P is the number of days per year with at least 0.01 inches of precipitation</li> </ul>
-------------------------------------------------------	-------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------

120 days, Precipitation Greater than 0.01 inches at Plant Location (Figure 13.2.2-1)

0.17 lb/VMT, Calculated PM2.5 Emission Factor (Total, With natural mitigation) 1.65 lb/VMT, Calculated PM10 Emission Factor (Total, With natural mitigation) 6.41 lb/VMT, Calculated PM Emission Factor (Total, With natural mitigation)

In addition to natural mitigation, the following mitigation will be implemented at the site. Control efficiencies taken from the WRAP Fugitive Dust Handbook, September 7, 2006.



0.04 Ib/VMT, Calculated PM Emission Factor (Total, With natural mitigation, and water sprays) 0.01 Ib/VMT, Calculated PM10 Emission Factor (Total, With natural mitigation, and water sprays) 0.001 Ib/VMT, Calculated PM2.5 Emission Factor (Total, With natural mitigation, and water sprays)

18,920 miles/year, "Loaded Truck VMT" 2000 lb/ton, Conversion Factor

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9.52E-02 lb/hr, PM Emissions 2.46E-02 lb/hr, PM10 Emissions 2.46E-03 lb/hr, PM2.5 Emissions

#### Additional Haul Roads Supporting the Movement of Ash Offsite - Unloaded Trucks (F-6)

Where:

A portion of the ash will be trucked to an offsite location. Particulate emissions are generated from the haul roads from the force of the wheels on the road surface. This force causes pulverization of the surface material. The particles are lifted and dropped from the rolling wheels and the road surface is exposed to strong air currents, which generate airborne particulate emissions.

The methodology presented below is taken from Section 13.2.2 (Unpaved Roads) of the U.S. EPA's AP-42 document and is based on the vehicle miles traveled (VMT) at the site.

$$E = k \left(\frac{s}{12}\right)^a \left(\frac{W}{3}\right)^b$$

E is the size-specific emission factor (lb/VMT) s is the surface material silt content (%) W is the mean vehicle weight (tons) k, a, and b are empirical constants

Equation 1a of AP-42 Section 13.2.2 for vehicles traveling on unpaved surfaces at industrial sites

Constant	Industrial Roads			
Constant	PM2.5	PM10	PM	
k	0.15	1.5	4.9	
а	0.9	0.9	0.7	
b	0.45	0.45	0.45	

5.1 %, Average Silt Content of Plant Roads at a Coal Mining Site (Table 13.2.2-1) 25 tons, Mean Vehicle Empty Weight (Fleet Average)

0.18 lb/VMT, Calculated PM2.5 Emission Factor (Road Silt Portion) 1.80 lb/VMT, Calculated PM10 Emission Factor (Road Silt Portion) 6.99 lb/VMT, Calculated PM Emission Factor (Road Silt Portion)

Emissions associated with the exhaust, brake wear, and tire wear must be added to the values calculated above. The values shown below were taken from Table 13.2.2-4.

Particle Size	PM2.5	PM10	PM
lb/VMT "adder"	0.00036	0.00047	0.00047

1.80E-02 lb/hr, PM10 Emissions

1.80E-03 lb/hr, PM2.5 Emissions

0.18 lb/VMT, Calculated PM2.5 Emission Factor (Total, No natural mitigation) 1.80 lb/VMT, Calculated PM10 Emission Factor (Total, No natural mitigation) 6.99 lb/VMT, Calculated PM Emission Factor (Total, No natural mitigation)

All roads are subject to natural mitigation because of rainfall and other precipitation. The following equation accounts for reductions in the emission factor due to natural mitigation.

$E_{EXT} = E \left[ \frac{(365 - P)}{265} \right]$	Where:	E <sub>EXT</sub> is the adjusted emission factor accounting for natural mitigation
$E_{EXT} = E \left[ \frac{1}{365} \right]$		E is emission factor from Equation 1a
		P is the number of days per year with at least 0.01 inches of precipitation

120 days, Precipitation Greater than 0.1 inches at Plant Location (Figure 13.2.2-1)

0.12 lb/VMT, Calculated PM2.5 Emission Factor (Total, With natural mitigation	ı)
1.21 Ib/VMT, Calculated PM10 Emission Factor (Total, With natural mitigation)	)
4.69 Ib/VMT, Calculated PM Emission Factor (Total, With natural mitigation)	

In addition to natural mitigation, the following mitigation will be implemented at the site. Control efficiencies taken from the WRAP Fugitive Dust Handbook, September 7, 2006.

84%	Limit on-site vehicle speeds (on unpaved roads) to 15 mph. Application of Gravel on Dirt Surfaces Implement watering for industrial unpaved road.
0.008	lb/VMT, Calculated PM Emission Factor (Total, With natural mitigation, and water sprays) lb/VMT, Calculated PM10 Emission Factor (Total, With natural mitigation, and water sprays) lb/VMT, Calculated PM2.5 Emission Factor (Total, With natural mitigation, and water sprays)
,	miles/day, One-way Vehicle Distance from Source to Offsite lb/ton, Conversion Factor
7.88E-02	tpy, PM Emissions tpy, PM10 Emissions tpy, PM2.5 Emissions
6.97E-02	lb/hr, PM Emissions

### Duke Energy Buck Station Screener Emissions (ES-82A) Spyder 514TS Double Deck

Capacity, ton/yr	430,000	Duke Energy
Hours of operation, hr/yr	2600	Based on 50/wk M-F
Capacity, ton/hr	165	Duke Energy

Pollutant	Emission Factor <sup>1</sup>	Potential Er	nission Rates
i onutant	lb/ton	(lb/hr)	(tpy)
PM	0.0022	0.015	0.020
PM <sub>10</sub>	0.00074	0.005	0.007
PM <sub>2.5</sub>	0.00005	0.0003	0.0004

Lead	126.99	1.92E-06	2.50E-06	Duke Energy Average Ash Analysis
Arsenic	118.52	1.79E-06	2.33E-06	Duke Energy Average Ash Analysis
Beryllium	24.55	3.71E-07	4.83E-07	Duke Energy Average Ash Analysis
Cadmium	21.16	3.20E-07	4.16E-07	Duke Energy Average Ash Analysis
Chromium	143.92	2.18E-06	2.83E-06	Duke Energy Average Ash Analysis
Chromium VI	15.83	2.39E-07	3.11E-07	Duke Energy Average Ash Analysis
Cobalt	57.57	8.71E-07	1.13E-06	Duke Energy Average Ash Analysis
Manganese	253.98	3.84E-06	4.99E-06	Duke Energy Average Ash Analysis
Mercury	0.76	1.15E-08	1.49E-08	Duke Energy Average Ash Analysis
Nickel	143.92	2.18E-06	2.83E-06	Duke Energy Average Ash Analysis
Selenium	38.94	5.89E-07	7.66E-07	Duke Energy Average Ash Analysis

Notes:

1. Emission Factor for Screening operation from AP-42, Table 11.19.2-2

## Duke Energy Buck Station Crusher Emissions (ES-83A) 4043T Impact Crusher

Capacity, ton/yr	43,000	Duke Energy
Max Hours of operation, hr/day	1	Duke Energy
Hours of operation, hr/yr	365	Based on 1 hr/day 365 days/year
Capacity, ton/day	165	Duke Energy

Pollutant	Emission Factor <sup>1</sup>	Potential Em	ission Rates
ronatant	lb/ton	(lb/hr)	(tpy)
PM	0.0012	0.008	0.002
PM <sub>10</sub>	0.00054	0.004	0.001
PM <sub>2.5</sub>	0.0001	0.001	0.0001

1 1	100.00	1.055.00		
Lead	126.99	1.05E-06	1.91E-07	Duke Energy Average Ash Analysis
Arsenic	118.52	9.78E-07	1.78E-07	Duke Energy Average Ash Analysis
Beryllium	24.55	2.03E-07	3.70E-08	Duke Energy Average Ash Analysis
Cadmium	21.16	1.75E-07	3.19E-08	Duke Energy Average Ash Analysis
Chromium	143.92	1.19E-06	2.17E-07	Duke Energy Average Ash Analysis
Chromium VI	15.83	1.31E-07	2.38E-08	Duke Energy Average Ash Analysis
Cobalt	57.57	4.75E-07	8.67E-08	Duke Energy Average Ash Analysis
Manganese	253.98	2.10E-06	3.82E-07	Duke Energy Average Ash Analysis
Mercury	0.76	6.27E-09	1.14E-09	Duke Energy Average Ash Analysis
Nickel	143.92	1.19E-06	2.17E-07	Duke Energy Average Ash Analysis
Selenium	38.94	3.21E-07	5.86E-08	Duke Energy Average Ash Analysis

Notes:

1. Emission Factor for Crushing operation from AP-42, Table 11.19.2-2

#### Duke Energy Buck Station Screener Engine Emissions (ES-82B)

Pollutant

NOx

CO VOC

SO<sub>2</sub>

PM PM<sub>10</sub>

PM<sub>2.5</sub>

	Engine rating	91		
L	Permitted Hours:	2,600	hrs/yr	
	No. of Engines:	1		Diesel Sulfur Content:
	Heat Input:	0.64	MMBtu/hr (HHV)	Diesel Heat Content:

Emission Factor		actor Potential Emission Rates		HAP Pollutant <sup>1</sup> Emi	Emission Factor	Potential Emission Rates		
	lb/hp-hr	(lb/hr)	(tpy)		(Ib/MMBtu)	(lb/hr)	(tpy)	
	0.031	2.82	3.667	Benzene	9.33E-04	5.94E-04	7.73E-04	
	6.68E-03	0.61	0.790	Toluene	4.09E-04	2.61E-04	3.39E-04	
	2.47E-03	0.22	0.292	Xylenes	2.85E-04	1.82E-04	2.36E-04	
	2.05E-03	0.19	0.243	1,3-Butadiene	3.91E-05	2.49E-05	3.24E-05	
	2.20E-03	0.20	0.260	Formaldehyde	1.18E-03	7.52E-04	9.77E-04	
	2.20E-03	0.20	0.260	Acetaldehyde	7.67E-04	4.89E-04	6.35E-04	
	2.20E-03	0.20	0.260	Acrolein	9.25E-05	5.89E-05	7.66E-05	
				Total PAH	1.68E-04	1.07E-04	1.39E-04	
				Naphthalene	8.48E-05	5.40E-05	7.02E-05	
				Acenaphthalene	5.06E-06	3.22E-06	4.19E-06	
				Acenaphthene	1.42E-06	9.05E-07	1.18E-06	
				Fluorene	2.92E-05	1.86E-05	2.42E-05	
				Phenanthrene	2.94E-05	1.87E-05	2.43E-05	
				Anthracene	1.87E-06	1.19E-06	1.55E-06	
				Fluoranthene	7.61E-06	4.85E-06	6.30E-06	
				Pyrene	4.78E-06	3.04E-06	3.96E-06	
				Benzo(a)anthracene	1.68E-06	1.07E-06	1.39E-06	
				Chrysene	3.53E-07	2.25E-07	2.92E-07	
				Benzo(b)fluoranthene	9.91E-08	6.31E-08	8.21E-08	
				Benzo(k)fluoranthene	1.55E-07	9.87E-08	1.28E-07	
				Benzo(a)pyrene	1.88E-07	1.20E-07	1.56E-07	
				Indeno(1,2,3-cd)pyrene	3.75E-07	2.39E-07	3.11E-07	
				Dibenz(a,h)anthracene	5.83E-07	3.71E-07	4.83E-07	
				Benzo(g,h,l)perylene	4.89E-07	3.11E-07	4.05E-07	

0.0015 weight % 7,000 Btu/hp-hr

#### Summary of GHG Emissions:

		Emissions	Emissions
	Emission Factor	(metric	(US
Pollutant	(kg/MMBtu) <sup>2</sup>	tons/yr) <sup>3</sup>	tons/yr)⁴
CO <sub>2</sub>	73.96	122.5	134.99
CH₄	3.0E-03	0.005	0.005
N <sub>2</sub> O	6.0E-04	0.001	0.001
CO₂e <sup>5</sup>		122.91	135.45

Notes

Assume PM = PM10 = PM2.5

Emission Factor based on Table 3.3 1, EPA AP 42, Chapter 3.3 Gasoline & Diesel Industrial Engines

1. HAPs Emission Factor based on Table 3.3 2, Chapter 3.3 Gasoline & Diesel Industrial Engines. Per 15A NCAC 2Q.0702 (a)(27) these emissions were not included in the TPER analysis. 2. Based on EPA default factors in Subpart C Tables C-1 and C-2 for Distillate Fuel Oil No. 2.

3. Calculated based on the heat input, emission factors, and equations C-1b and C-8b of Subpart C. CO 2 e based on Subpart A Table A-1 factors.

 $CO_2$ ,  $CH_4$ , or  $N_2O$  (metric tpy) = 1E-03 \* Gas (MMBtu/yr) \* Emission Factor (kg/MMBtu)

4. 1 metric ton = 1.102 US ton

5.  $CO_2 e = CO_2$ ,  $CH_4$ , or  $N_2 O$  (tpy) \* Global Warming Potential factor (GWP)

CO <sub>2</sub> GWP	1
CH₄ GWP	25
N₂O GWP	298

Ν	<sub>2</sub> O	GWP	

#### Duke Energy Buck Station **Crusher Engine Emissions (ES-83B)**

Pollutant

NOx

CO VOC

SO<sub>2</sub>

PM

PM<sub>10</sub>

PM<sub>2.5</sub>

Engine rating	300	hp ACERT Diesel Engine Ca	aterpillar C9
Permitted Hours:	365	hrs/yr	
No. of Engines:	1		
Heat Input:	2.10	MMBtu/hr (HHV)	

Emission Factor		Potential Emission Rates		HAP Pollutant <sup>1</sup>	Emission Factor	Potential Emis	Potential Emission Rates		
	lb/hp-hr	(lb/hr)	(tpy)	HAF FOIlutant	(Ib/MMBtu)	(lb/hr)	(tpy)		
	0.031	9.30	1.697	Benzene	9.33E-04	1.96E-03	3.58E-04		
	6.68E-03	2.00	0.366	Toluene	4.09E-04	8.59E-04	1.57E-04		
	2.47E-03	0.74	0.135	Xylenes	2.85E-04	5.99E-04	1.09E-04		
	2.05E-03	0.62	0.112	1,3-Butadiene	3.91E-05	8.21E-05	1.50E-05		
	2.20E-03	0.66	0.120	Formaldehyde	1.18E-03	2.48E-03	4.52E-04		
	2.20E-03	0.66	0.120	Acetaldehyde	7.67E-04	1.61E-03	2.94E-04		
	2.20E-03	0.66	0.120	Acrolein	9.25E-05	1.94E-04	3.55E-05		
				Total PAH	1.68E-04	3.53E-04	6.44E-05		
				Naphthalene	8.48E-05	1.78E-04	3.25E-05		
				Acenaphthalene	5.06E-06	1.06E-05	1.94E-06		
				Acenaphthene	1.42E-06	2.98E-06	5.44E-07		
				Fluorene	2.92E-05	6.13E-05	1.12E-05		
				Phenanthrene	2.94E-05	6.17E-05	1.13E-05		
				Anthracene	1.87E-06	3.93E-06	7.17E-07		
				Fluoranthene	7.61E-06	1.60E-05	2.92E-06		
				Pyrene	4.78E-06	1.00E-05	1.83E-06		
				Benzo(a)anthracene	1.68E-06	3.53E-06	6.44E-07		
				Chrysene	3.53E-07	7.41E-07	1.35E-07		
				Benzo(b)fluoranthene	9.91E-08	2.08E-07	3.80E-08		
				Benzo(k)fluoranthene	1.55E-07	3.26E-07	5.94E-08		
				Benzo(a)pyrene	1.88E-07	3.95E-07	7.21E-08		
				Indeno(1,2,3-cd)pyrene	3.75E-07	7.88E-07	1.44E-07		
				Dibenz(a,h)anthracene	5.83E-07	1.22E-06	2.23E-07		
				Benzo(g,h,l)perylene	4.89E-07	1.03E-06	1.87E-07		

Diesel Sulfur Content:

Diesel Heat Content:

0.0015 weight % 7,000 Btu/hp-hr

#### Summary of GHG Emissions:

		Emissions	Emissions
	Emission Factor	(metric	(US
Pollutant	(kg/MMBtu) <sup>2</sup>	tons/yr) <sup>3</sup>	tons/yr)4
CO <sub>2</sub>	73.96	56.7	62.47
CH₄	3.0E-03	0.002	0.003
N <sub>2</sub> O	6.0E-04	0.0005	0.0005
CO₂e <sup>5</sup>		56.88	62.69

Notes

Assume PM = PM10 = PM2.5

Emission Factor based on Table 3.3 1, EPA AP 42, Chapter 3.3 Gasoline & Diesel Industrial Engines

1. HAPs Emission Factor based on Table 3.3 2, Chapter 3.3 Gasoline & Diesel Industrial Engines. Per 15A NCAC 20.0702 (a)(27) these emissions were not included in the TPER analysis. 2. Based on EPA default factors in Subpart C Tables C-1 and C-2 for Distillate Fuel Oil No. 2.

3. Calculated based on the heat input, emission factors, and equations C-1b and C-8b of Subpart C. CO 2 e based on Subpart A Table A-1 factors.

 $CO_2$ ,  $CH_4$ , or  $N_2O$  (metric tpy) = 1E-03 \* Gas (MMBtu/yr) \* Emission Factor (kg/MMBtu)

4. 1 metric ton = 1.102 US ton

5.  $CO_2 e = CO_2$ ,  $CH_4$ , or  $N_2 O$  (tpy) \* Global Warming Potential factor (GWP)

1
25
298

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## **APPENDIX C**

## PSD NETTING ANALYSIS AND SUPPORT DOCUMENATION



Pollutant	lb/hr	tpy	SER (tpy)	Netting Required
PM	12.05	49.14	25	Yes
PM <sub>10</sub>	10.75	43.59	15	Yes
PM <sub>2.5</sub>	6.42	24.64	10	Yes
SO <sub>2</sub>	41.03	163.98	40	Yes
NO <sub>x</sub> *	30.34	117.66	40	Yes
СО	25.01	92.26	100	No
VOC	3.21	9.54	40	No
Lead	0.001	0.0062	0.6	No
GHG		116,604	75,000	Yes
H <sub>2</sub> SO <sub>4</sub>	0.1	0.44	7	No

## Proposed Project Emissions and Comparison with the respective SERs

\* NOx emissions from STAR unit is based on NOx at 0.12 lb/MMBtu.

#### Duke Buck Station- PSD Netting Analysis

Description of Emissions	NOx	SO <sub>2</sub>	PM	PM <sub>10</sub>	PM <sub>2.5</sub>	CO2e	Unit Operation/Retired date Notes		
Description of Emissions	(TPY)	(TPY)	(TPY)	(TPY)	(TPY)	(TPY)	Unit Operation/Retired date	Notes	
STAR Facility Emissions (Increases)	117.66	163.98	49.14	43.59	24.64	116,604		Emissions Calcs dated 102617 (NOx at 0.12 lb/MMBtu). Application submitted on 4/21/2017.	
PSD Avoidance Cap for ES11 and ES12 (Increases)	599.8		198.90	160.8			Unit 11 began operation - 9/25/2011 Permit No. 03786T34, 2.1-A.6.a (CO, NO <sub>X</sub> , PM, PM <sub>10</sub> ).		
ES11 and ES12 (Increases)		108.52			160.8	2,669,078	and Unit 12 - 10/3/2011 (PSD Avoidance limits)	Application BK Hot gas path mod Table A-4 dated May 7, 2014 $(SO_2)$ . Duct Burner Modification Application Table 3-2 dated Feb 15 2013 (CO2e). PM <sub>25</sub> assumed to equal the PM <sub>10</sub> avoidance cap.	
ES13 - 10 cell cooling tower (Increases)			7	7	7		November 2011 (Potential to Emit)		
ES14 - Auxiliary Boiler, 36.74 MMBtu/hr (Increases)	1.8	0.22	0.40	0.4	0.4		November 2011 (Potential to Emit)	Application Hot gas path mod Table A-7 dated May 7, 2014. PM25	
ES15 - Fuel oil fired emergency generator (1490 hp) (Increases)	0.8	0.0009	0.028	0.023	0.023		November 2011 (Potential to Emit)	assumed to equal PM <sub>10</sub> .	
ES16 - Fuel oil fired fire water pump (237 hp) (Increases)	0.1	0.0001	0.004	0.004	0.004		November 2011 (Potential to Emit)		
ES72 - Chiller cooling tower (Increases)			0.60	0.6	0.6		June 2012 (Potential to Emit)		
Ash Basin Water Management Pump (Increases)	2.5	0.004	0.016	0.016	0.016		Unit added- February 2017 (Potential to Emit)	Letter to DAQ submitted on Feb 2, 2017 for addition of 55 kw diesel fired engine pump along with emissions calculation file.	
ES17 - Fuel Oil fired emergency generator (762 hp) (Increases)	0.513	0.0005	0.003	0.002	0.002		Unit added- February 2015 (Potential to Emit)	Application BK ES-17EmGen Application dated May 18, 2016.	
Total Increases	723.17	272.73	256.09	212.43	193.48	2,785,682			
Contemporaneous Emission Decreases (Unit 5, Blr 8), 2010	447.80	2,833.80	143.13	127.69	109.86			NC DAQ Actual Emissions Inventory 2010 (Unit 5, Blr 8).	
Contemporaneous Emission Decreases (Unit 6, Blr 9), 2010	476.60	2,776.10	156.16	134.61	109.88			NC DAQ Actual Emissions Inventory 2010 (Unit 6, Blr 9).	
Contemporaneous Emission Decreases (Unit 5, Blr 8), 2011	305.80	1,931.50	160.30	140.87	118.54		Units retired - 4/1/2013	NC DAQ Actual Emissions Inventory 2011 (Unit 5, Blr 8).	
Contemporaneous Emission Decreases (Unit 6, Blr 9), 2011	333.20	1,907.50	120.93	112.70	103.39			NC DAQ Actual Emissions Inventory 2011 (Unit 6, Blr 9).	
Contemporaneous Emission Decreases Avg 2010-2011	781.70	4724.45	290.26	257.94	220.84			Average actual emissions from 2010 and 2011.	
PSD SERs	40	40	25	15	10	75,000			
Difference	-58.53	-4451.72	-34.17	-45.50	-27.35	2,785,682			
Significant Modification (Yes/No)	No	No	No	No	No	Yes			

#### Notes:

Emissions from Units 3 and 4 (BIr 5, 6 and 7) are not included for decreases because it does not fall under the 7-year contemporaneous window from the expected start of operation of the current project.

2010-2011, 24 month period is used for the contemporaneous emission decreases.

## **EMISSION INCREASES**

## SECTION 2- SPECIFIC LIMITATIONS AND CONDITIONS

### 2.1- Emission Source(s) Specific Limitations and Conditions

The emission source(s) and associated air pollution control device(s) listed below are subject to the following specific terms, conditions, and limitations, including the monitoring, recordkeeping, and reporting requirements specifically identified herein as applicable requirements:

A. two natural gas-fired combined-cycle combustion turbines (ID Nos. ES-11 and ES-12), each equipped dry low-NOx combustors, a heat recovery steam generator (HRSG) with a natural gas-fired duct burner, and a common steam turbine generator supplied by the two HRSGs; and associated selective catalytic reduction (SCR) (ID Nos. C11A and C12A) and associated CO/VOC oxidation catalyst (ID Nos. C11B and C12B)

The following table provides a summary of limits and standards for the emission source(s) described above:

Regulated Pollutant	Limits/Standards	Applicable Regulation
particulate matter	0.125 lb/mmBtu heat input (applies only when duct burners are firing)	15A NCAC 02D .0503
visible emissions	20 percent opacity	15A NCAC 02D .0521
nitrogen oxides	<ul> <li>15 ppm at 15% O<sub>2</sub> (30-day rolling average)</li> <li>96 ppm at 15% O<sub>2</sub> when operating at less than</li> <li>75 percent of peak load or operating at ambient temperature below 0 °F (30-day rolling average)</li> </ul>	15A NCAC 02D .0524 (40 CFR Part 60, Subpart KKKK)
	Phase II Acid Rain Permit Requirements (see Section 2.3)	15A NCAC 02Q .0402 (40 CFR Part 72)
	2.0 ppmvd at 15% $O_2$ for the first 500 hours of operation and 2.5 ppmvd at 15% $O_2$ after 500 hours (30-day rolling average)	15A NCAC 02D .1418 (RACT)
	Federally-Enforceable Only Cross State Air Pollution Rules See Section 2.1.A.8.	40 CFR Part 97, Subparts AAAAA and BBBBB
sulfur dioxide	0.06 lb/million Btu heat input	15A NCAC 02D .0524 (40 CFR Part 60, Subpart KKKK)
	Phase II Acid Rain Permit Requirements (see Section 2.3)	15A NCAC 02Q .0402 (40 CFR Part 72)
	Federally-Enforceable Only Cross State Air Pollution Rules See Section 2.1.A.8.	40 CFR Part 97, Subpart CCCCC
carbon monoxide nitrogen oxides particulate matter PM-10 sulfuric acid	See Section 2.1.A.4.	15A NCAC 02Q .0317 (PSD avoidance)

Regulated Pollutant	Limits/Standards	Applicable Regulation
volatile organic compounds	Less than 44.7 ton/yr, combined	15A NCAC 02Q .0317 (NSR avoidance)
toxic air pollutants	See Section 2.2 A.1 - State-only requirement	15A NCAC 02D .1100
toxic air pollutants	See Section 2.2 A.2 - State-only requirement	15A NCAC 02Q .0711
nitrogen oxides sulfur dioxide particulate matter PM-10 VOC lead sulfuric acid CO <sub>2</sub> e	See Section 2.1.A.7	15A NCAC 02D .0530(u)

#### 1. 15A NCAC 02D .0503: PARTICULATES FROM FUEL BURNING INDIRECT HEAT EXCHANGERS

Emissions of particulate matter from the combustion of natural gas in these sources (ID Nos. ES-11 and ES-12) that are discharged from these sources into the atmosphere shall not exceed 0.125 pounds per million Btu heat input when the duct burners are in service.

Testing [15A NCAC 02Q .0508(f)]

b. If emissions testing is required, the testing shall be performed in accordance with General Condition JJ. If the results of this test are above the limits given in Section 2.1.A.1.a., above, the Permittee shall be deemed in noncompliance with 15A NCAC 02D .0503.

#### Monitoring/Recordkeeping/Reporting [15A NCAC 02Q .0508(f)]

c. No monitoring/recordkeeping/reporting is required for emissions of particulate matter from the firing of natural gas in these sources (**ID Nos. ES-11 and ES-12**).

#### 2. 15A NCAC 02D .0521: CONTROL OF VISIBLE EMISSIONS

a. Visible emissions from these sources (**ID Nos. ES-11 and ES-12**) shall not be more than 20 percent opacity (except during startup, shutdowns, and malfunctions approved as such according to procedures approved under 15A NCAC 02D .0535) when averaged over a six-minute period. However, six-minute averaging periods may exceed 20 percent not more than once in any hour and not more than four times in any 24-hour period. In no event shall the six-minute average exceed 87 percent opacity.

#### Testing [15A NCAC 02Q .0508(f)]

b. If emissions testing is required, the testing shall be performed in accordance with General Condition JJ. If the results of this test are above the limit given in Section 2.1.A.2.a., above, the Permittee shall be deemed in noncompliance with 15A NCAC 02D .0521.

#### Monitoring [15A NCAC 02Q .0508(f)]

c. No monitoring/recordkeeping/reporting is required for opacity from the firing of natural gas in these sources (**ID Nos. ES-11 and ES-12**).

# 3. 15A NCAC 02D .0524: NEW SOURCE PERFORMANCE STANDARDS (40 CFR PART 60 SUBPART KKKK)

a. The Permittee shall comply with all applicable provisions, including the requirements for emission

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- ii. The SCR shall operate at all times that the turbine is operating except during turbine start-up and shutdown periods to the extent recommended by the manufacturer and operated in a manner so as to minimize ammonia slip.
- iii. During NOX CEM downtimes or CEM malfunctions, the Permittee shall operate at the ammonia injection rates shown in paragraph i above. In the case of a missing hour in conjunction with a Calibration Error Test or a Quarterly Linearity Test, the ammonia injection rate for the hour following the test shall be adjusted to the injection rate shown in paragraph i above until a valid data status has been achieved.

The Permittee shall be deemed in noncompliance with 15A NCAC 02D .1418 if the ammonia injection rate to the SCR system is not continuously measured and recorded or the ammonia injection rate is less than the above injection rates during NOx CEM downtimes or CEM malfunctions.

#### Reporting [15A NCAC 02Q .0508(f)]

- e. The Permittee shall submit reports of excess emissions and monitor downtime as described in Section 2.1.A.3.j. Excess emissions and monitor downtime for NOx for purposes of compliance with the applicable RACT limits are defined in Section 2.1.A.3.j.
- f. The Permittee shall submit a semi-annual summary report, acceptable to the Regional Air Quality Supervisor, of monitoring and record keeping activities postmarked on or before January 30 of each calendar year for the preceding six-month period between July and December, and July 30 of each calendar year for the preceding six-month period between January and June. All instances of deviations from the requirements of this permit must be clearly identified.

#### 6. 15A NCAC 02Q .0317: AVOIDANCE CONDITIONS (Avoidance of 15A NCAC 02D .0530: PREVENTION OF SIGNIFICANT DETERIORATION)

POLLUTANT	EMISSION LIMITS	CONTROL TECHNOLOGY
carbon monoxide	147.0 tons per 12-month rolling average (total both turbines) (PSD avoidance)	oxidation catalyst
nitrogen oxides	599.8 tons per 12-month rolling average (total both turbines) (PSD avoidance)	selective catalytic reduction
particulate matter	198.9 tons per 12-month rolling average (total both turbines) (PSD avoidance)	none
PM-10	160.8 tons per 12-month rolling average (total both turbines) (PSD avoidance)	sulfur content of natural gas shall not exceed 1.7 gr/100 scf
sulfuric acid	18.5 tons per 12-month rolling average (total both turbines) (PSD avoidance)	sulfur content of natural gas shall not exceed 1.7 gr/100 scf

a. In order to avoid applicability of 15A NCAC 02D .0530(g), the following emission limits shall not be exceeded for the combustion turbines (ID Nos. ES-11 and ES-12):

\* Emission limits shall apply at all times except the following: Emissions resulting from start-up, shutdown or malfunction above those given above are permitted provided that optimal operational practices are adhered to and periods of excess emissions are minimized. Periods of excess emissions due to start-up and/or shutdown or operation below 50% load shall not exceed six hours in any 24-hour block period beginning at midnight. Start-up is defined as the period from initial firing to 50% load. Shutdown is defined PM10 emissions from ES-11 or ES-12 (pound/month) =  $(OT_{db})(E_{db}) + (OT_{ndb})(E_{ndb})$ 

 $OT_{db}$  = Operating time (hours per month) when the duct burners are operating.

 $E_{db}$  = PM10 emission factor when the duct burners are operating. (i.e. 16.97 pound/hour)

 $OT_{ndb}$  = Operating time (hours per month) the duct burners not are operating.

 $E_{ndb}$  = PM10 emission factor when the duct burners are not operating. (i.e. 11.53 pound/hour)

Total monthly PM-10 emissions = PM-10 emissions CT ES-11 + PM-10 emissions CT ES-12

g. The sulfur content of the natural gas shall not exceed 1.7 gr/100 scf.

The Permittee shall be deemed in noncompliance with 15A NCAC 02D .0530 if records of the calculations in Paragraphs d. and f. are not maintained, if the records required by Section 2.1.A.3.e. are not maintained, if the catalyst inlet temperature is not monitored, and/or if the calculations or records indicate an exceedance of the limits in Paragraph a., above.

#### Reporting [15A NCAC 02Q .0508(f)]

h. The Permittee shall submit a semi-annual summary report, acceptable to the Regional Air Quality Supervisor, postmarked on or before January 30 of each calendar year for the preceding six-month period between July and December, and July 30 of each calendar year for the preceding six-month period between January and June. The report shall contain the monthly CO emissions from each source (ID Nos. ES-11 and ES-12) and the total monthly CO emissions from both sources for the previous 17 months based on the calculations above. The emissions must be calculated for each of the 12-month periods over the previous 17 months. All instances of deviations from the requirements of this permit must be clearly identified.

#### 7. 15A NCAC 02Q .0317: AVOIDANCE CONDITIONS (Avoidance of 15A NCAC 02D .0531: SOURCES IN NONATTAINMENT AREAS)

a. In order to avoid applicability of 15A NCAC 02D .0531, the following emission limits shall not be exceeded for the combustion turbines (ID Nos. ES-11 and ES-12):

POLLUTANT	EMISSION LIMITS*	CONTROL TECHNOLOGY
volatile organic compounds	44.7 tons per 12-month rolling average (total both turbines) (NSR avoidance)	oxidation catalyst

\* Emission limits shall apply at all times except the following: Emissions resulting from start-up, shutdown or malfunction above those given above are permitted provided that optimal operational practices are adhered to and periods of excess emissions are minimized. Periods of excess emissions due to start-up and/or shutdown or operation below 50% load shall not exceed six hours in any 24-hour block period beginning at midnight. Start-up is defined as the period from initial firing to 50% load. Shutdown is defined as the period from 50% load to flame out.

#### Testing [15A NCAC 02Q .0508(f)]

b. If emissions testing is required, the testing shall be performed in accordance with General Condition JJ. If the results of this test are above the limit given in 2.1.A.7.a above, the Permittee shall be deemed in

Description of	CO <sub>2</sub> e	NO <sub>x</sub>	SO <sub>2</sub>	PM	<b>PM</b> <sub>10</sub>	PM <sub>2.5</sub>	CO	VOC	$H_2SO_4$	Lead
Emissions Increase/Decrease	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)	(ton/yr)
Future Combustion Turbine and Duct Burners Emissions	2,669,078	209.94	127.67	122.29	195.55	195.55	153.38	58.57	14.89	1.12E-02
Current Maximum Potential Combustion Turbine and Duct Burner Emissions	2,323,780	182.78	11.34	98.68	154.30	154.30	112.37	41.94	3.30	9.74E-03
Proposed Project Emissions Increases	345,298	27.16	116.33	23.61	41.25	41.25	41.01	16.63	11.58	1.45E-03
PSD/NNSR Significant Emission Rate <sup>1</sup>	75,000	40.0	40.0	25.0	15.0	10.0	100.0	40.0	7.0	0.60
Netting Required? (Yes/No)	Yes	No	Yes	No	Yes	Yes	No	No	Yes	No
Other Emissions Increases	and Decrea	ses								
Shutdown of Boilers 8 & 9	-879,988	-797	-4,845	-294	-261	-224	-727	-11.8	-6.2	-2.84E-02
GE 7FA Combined Cycle Project December 2011	1,989,090	-538.4	-1,854.8	-74.8	9.0	8.4	70.5	38.0	-2.4	-3.80E-03
Total Net Emission Change	1,454,400	NA	-6,583	NA	-211	-174	NA	NA	3	NA
PSD Threshold	75,000	40	40	25	15	10	100	40	7	0.6
Proposed Project Subject to PSD/NNSR <sup>1</sup> ?	Yes	No	No	No	No	No	No	No	No	No

Table 3-2 Total Annual Project Emissions

(1) Rowan County is designated as moderate nonattainment for the 1997 8-hour ozone standard effective May 31, 2011, and marginal nonattainment for the 2008 8-hour ozone standard effective July 20, 2012. Therefore the NOx and VOC emissions increases are compared to the nonattainment New Source Review significant emission rates.

### 3.5 Toxic air pollutant emissions

The Buck Steam Station has previously demonstrated compliance, as of June 1, 2011, with the NC Toxic Air Pollutants regulations under 15A NCAC 2D.1100 and 2Q.0700, and Section 2.2.B. of the air quality permit for the facility includes source-specific emissions limits based on that demonstration. Any future demonstrations to comply with 15A NCAC 2D.1104 shall only be required on a five-year basis, as stated in the permit.

Duke Power Buck Station - PSD Evaluation 2 GE7FA Combustion Turbine x 1 Steam Turbine Configuration, HRSG with DB

Description of Emissions Increase/Decrease	NO <sub>a</sub> (ton/yr)	SO <sub>2</sub> (ton/yr)	PM (ton/yr)	PM <sub>10</sub> (ton/yr)	CO (ton/yr)	VOC (ton/yr)	H <sub>2</sub> SO <sub>4</sub> (ton/yr)	Lead (ton/yr)
Future Combustion Turbine and Duct Burners Emissions	209.94	108.52	122.29	148.65	127.82	43.92	12.65	1.12E-02
Non turbine emissions (10 cell mechanical draft cooling tower, auxiliary boiler rated at 36.74 MMBtu/hr, diesel-fired emergency generator, diesel-fired fire water pump, Chiller Cooling Towers) <sup>(4)</sup>	2.70	0.22	8.01	8.00	4.50	1.45	0.00	1.80E-05
Total Project Potential Emissions	212.6	108.7	130.3	156.6	132.3	45.38	12.7	1.12E-02
Emission decreases from the March 2008 minor source permit application <sup>(b)</sup>	727.8	1,866.5	181.9	153.8	51.5	6.10	5.7	1.36E-02
PSD/NNSR Significant Emission Rate <sup>(c)</sup>	40.0	40.0	25.0	15.0	100.0	40.0	7.0	6.00E-01
PSD avoidance emission caps for the combustion turbines (emission decreases plus PSD significant emission rate - non-turbine emissions)	765.1	1,906.3	198.9	160.8	147.0	44.65	12.7	0.6
Combustion turbine emissions minus PSD avoidance emissions caps	-557.86	-1,797.98	-84.61	-20.15	-23.68	-2.18	-0.05	

## Table A-4 Revised Project Emissions Increases and Emission Caps

(a) Appendix B, Permit Application Addendum for the Buck Station, March 2008, updated for "as built" emergency engines and auxiliary boiler emissions.

(b) Appendix C, Permit Application Addendum for the Buck Steam Station, March 2008.

(c) Rowan County is designated as moderate nonattainment for the 1997 8-hour ozone standard effective May 31, 2011, and marginal nonattainment for the 2008 8-hour ozone standard effective July 20, 2012. Therefore the NOx and VOC emissions increases are compared to the nonattainment New Source Review significant emission rates.

Enclosure A Buck Steam Station

April 2014 Page A-5

#### **Duke Energy Carolinas, LLC**

Buck Combined Cycle Facility Salisbury, North Carolina Rowan County Facility ID: 8000004 Permit No. 03786T34

#### Estimation of Emissions from Diesel-Fired Engines

1.341 hp/kW

Given Information:

Er	Use	Potential Hours/Year					
Ash Basin Water Management Pump	55	kW	73.8	hp	Non-Emerg	8,760	hr/yr

Conversion Factors:

7,000 Btu/hp-hr, Brake Specific Fuel Consumption

	Emission Factor <sup>1, 2</sup>		Potential Emissions		Incincifi		Does Engine Qualify as	
Compound			55 kW E	Engine		cant Activity d per Engine	an Insignificant Activity?	
NOx	4.70	g/kW-hr	2.50	ton/yr	5	tpy	Yes	
VOC	4.70	g/kW-hr	2.50	ton/yr		tpy	Yes	
CO	5.00	g/kW-hr	2.66	ton/yr		tpy	Yes	
SO2	1.21E-05	lb/hp-hr	0.00	ton/yr	5	tpy	Yes	
PM	3.00E-02	g/kW-hr	0.02	ton/yr	5	tpy	Yes	
PM10	3.00E-02	g/kW-hr	0.02	ton/yr		tpy	Yes	
PM2.5	3.00E-02	g/kW-hr	0.02	ton/yr	5	tpy	Yes	
Benzene	9.33E-04	lb/MMBtu	4.22	lb/yr	1,000	lb/yr	Yes	
Toluene	4.09E-04	lb/MMBtu	1.85	lb/yr	1,000	lb/yr	Yes	
Xylene	2.85E-04	lb/MMBtu	1.29	lb/yr	1,000	lb/yr	Yes	
1,3 Butadiene	3.91E-05	lb/MMBtu	0.18	lb/yr	1,000	lb/yr	Yes	
Formaldehyde	1.18E-03	lb/MMBtu	5.34	lb/yr	1,000	lb/yr	Yes	
Acetaldehyde	7.67E-04	lb/MMBtu	3.47	lb/yr	1,000	lb/yr	Yes	
Acrolein	9.25E-05	lb/MMBtu	0.42	lb/yr	1,000	lb/yr	Yes	
Naphthalene	8.48E-05	lb/MMBtu	0.38	lb/yr	1,000	lb/yr	Yes	
Total PAH	1.68E-04	lb/MMBtu	0.76	lb/yr	1,000	lb/yr	Yes	

1 - SO2 and HAP from Section 3.3 of AP-42 (using 0.0015%S fuel).

2 - NOx, VOC, CO and PM are based on emission limits from Tier 4 standards. Conservatively assumed that 4.7 g/kW-hr applies to both NOx and VOC. Actually, sum of VOC and NOx must be less than 4.7 g/kW-hr.

## FORM B

## SPECIFIC EMISSIONS SOURCE INFORMATION (REQUIRED FOR ALL SOURCES)

REVISED 12/01/01	NCD	EQ/Division	of Air Quality	- Application	for Air Permit	to.Construct	/Operate		В
EMISSION SOURCE DE	SCRIPTION: Diesel-fin	ed emergency	standby gener	ator, 762 BHI			NO: ES-17(Em	Gen)	
OPERATING SCENARIC				DEVICE ID NO					
		_OF1	1		THIONION		K) ID NO(S): E	P-17	
DESCRIBE IN DETAIL T Emergency standby elec	THE EMISSION SOUR( ctric generation in even	CE PROCESS of loss of electronic fields	(ATTACH FLC ctric power on o	DW DIAGRAN old CT demoli	n.	· · · · · ·			
ТҮР	E OF FMISSION SOLIE								
Coal,wood,oil, gas, oth	E OF EMISSION SOUF		and COMPLE		RATE FORM E	31-B9 ON THE	E FOLLOWING	PAGES):	
				•			s/coatings/inks	(Form B7)	
Liquid storage tanks (I	/finishing/printir silos/bins (For			☐ Incineration (Form B8) ☐ Other (Form B9)					
START CONSTRUCTION		OPERATION	N DATE: 5/29/	2015	DATE MANL	JFACTURED:	Aug-0	6	
MANUFACTURER / MOD	EL NO .: CAT C15, DN	8155		EXPECTED	OP. SCHEDU			DAY/WK	MUCOUD
IS THIS SOURCE SUBJE	CT TO? NSPS (SUBP	ART?):_ <u>lili</u>	NESH	AP (SUBPAR			(SUBPART?):		WK/YR
PERCENTAGE ANNUAL	THROUGHPUT (%): D	EC-FEB 25	MAR-M		JUN-AL		SEP-NO		
EXPECTED ANNUAL HO	URS OF OPERATION:	<u>&lt;</u> 100	VISIBLE STA	CK EMISSIO	NS LINDED NO		ATION		
	CRITERIA AI	R POLLUT	ANT EMISS	SIONS INF	ORMATION	FOR THIS	SOURCE	/0 UP	ACITY
			SOURCE OF	EXPECT	ED ACTUAL	1		L EMISSIONS	
			EMISSION	1	TROLS / LIMITS)	(BEFORE CON	NTROLS / LIMITS)	1	
AIR POLLUTANT EMITTI			FACTOR	ib/hr	tons/yr	lb/hr	tons/yr	Ib/hr	TROLS / LIMITS)
PARTICULATE MATTER			Manufacturer	0.06	0.003		tonary	0.06	tons/yr
PARTICULATE MATTER			Manufacturer	0.04	0.002			0.04	0.003
PARTICULATE MATTER			Manufacturer	0.04	0.002			0.04	
SULFUR DIOXIDE (SO2)	15 ppm ultra low S disti	late	Manufacturer	0.01	0.0005			0.04	0.002
NITROGEN OXIDES (NOx)			Manufacturer	10.26	0.513		1	10.26	0.0005
CARBON MONOXIDE (CO)			Manufacturer	1.25	0.0625			1.25	0.0625
OLATILE ORGANIC CON	MPOUNDS (VOC)		Manufacturer	0.03	0.0015			0.03	0.0625
<u>EAD</u>			AP-42 1996	4.80E-05	2.50E-06			4.80E-05	2.50E-06
	HAZADDOUO	10 001 11							2.002-00
	HAZARDOUS A	IH POLLU	TANT EMIS	SIONS INF	ORMATIO	V FOR THIS	S SOURCE		
			SOURCE OF		D ACTUAL		POTENTIAL	EMISSIONS	
			EMISSION	(AFTER CONT	ROLS / LIMITS)	(BEFORE CON	TROLS / LIMITS)	(AFTER CONT	ROLS / LIMITS)
AZARDOUS AIR POLLU			FACTOR	lb/hr	tons/yr	lb/hr	tons/yr	ib/hr	tons/yr
crolein	75070		AP-42 1996	1.30E-04	6.50E-06			1.30E-04	6.50E-06
enzene	107028		AP-42 1996	4.20E-05	2.10E-06			4.20E-05	2.10E-06
oluene	71432		AP-42 1996	4.14E-03	2.07E-04			4.14E-03	2.07E-04
ylene	108883		AP-42 1996	1.50E-03	7.50E-05			1.50E-03	7.50E-05
ropylene	1330207		AP-42 1996	1.00E-03	5.00E-05			1.00E-03	5.00E-05
ormaldehvde			AP-42 1996	0	0			0	0
aphthalene	<u>50000</u> 91203		AP-42 1996	4.20E-04	2.10E-05			4.20E-04	2.10E-05
	91203		AP-42 1996	6.90E-04	1.52E-03			6.90E-04	1.52E-03
	TOXIC AIR P	OLLUTAN	T EMISSIO	VS INFORI	MATION FO	R THIS SO	UBCE		
		EXPECTED	ACTUAL EMIS	SIONS AFTE	R CONTROLS	/ LIMITATION	S		
DXIC AIR POLLUTANT A	ND CAS NO.		EF SOURCE	ib/		lb/d			
enzo-a-pyrene 50328			AP-42 1996					lb/yr	
ryllium metal 7440417			AP-42 1996	1.50		3.36E		1.40E	
achments: (1) emissions calcu	lations and supporting dos								

describe how these are monitored and with what frequency; and (3) describe any monitoring devices, gauges, or test ports for this source.

COMPLETE THIS FORM AND COMPLETE AND ATTACH APPROPRIATE B1 THROUGH B9 FORM FOR EACH SOURCE Attach Additional Sheets As Necessary

## **EMISSION DECREASES**

North Carolina Department of Environment and Natural Resources Division of Air Quality Air Pollutant Point Source Emissions Inventory – Calendar Year 2010								
· • • • •	ES-4 (B8).13A							
Emission Source Group ID 2. Emission Source Description:	Coal/No. 2 fuel oil–fired electric utility boiler (1,440 million Btu per hour maximum heat input, Unit No. 5 – Boiler No. 8)							
3. Operating Scenario ID/Description:	OS – 8/electric utility boiler fired by coal							
4. SCC Number/Description:	10100202 / Bituminous Coal ; Pulverized Coal: Dry Bottom							
<b>5.</b> Throughput/units in 2010: (e.g. production or fuel use):	239798.5 TON/yr							
6. Fuel Information (If fuel is used)	% Sulfur 0.64 % Ash 12.59 Heat Content 11792.4 Btu/lb (Btu/units)							
<ul><li>7. Capture Efficiency</li><li>(% of Emissions from this Process Vented to Control</li></ul>	100							

(% of Emissions from this Process Vented to Control Device or Stack):

## 8. Control Device Information :

Order	CS-ID	CD ID	<b>Control Device Description</b>
		(as listed in permit)	
1	CS-3	CD-3.13A	Hot-side electrostatic precipitator (80,640 square feet of plate area)

## 9. Emission Release Point (ERP) Information: (Sources vented to more than one ERP use additional entry lines):

ERP ID	ERP Type	(in feet)	<b>Diameter</b> Circle (enter #): Rectangle (L x W) (in 0.1 feet)	<b>Temperature</b> (F)	Velocity (Feet/sec)	Volume Flow Rate <sup>(Acfm)</sup>	ERP Description
ES–9 Stack	VERTICAL STACK	216	8	334	92	277465.46	ES–9 Discharge Stack

**10. Operating Schedule**: (Source/Operating Scenario that best characterizes Calendar Year 2010) **Hours per Day** (24) **Days per Week** (7) **Weeks per Year** (52)

11. Typical Start & End Times For Operating Scenario: Start: 0 End: 2359

Jan-Feb + Dec 27% March-May 29%		Sept.–Nov. 2010
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## 13. <u>Actual Emissions per Pollutant Listed :</u>

Attach calculations and documentation of emission factors or other estimation methods used.

GHG Pollutants	CAS	Emissions– GHG Pollutants (Tons/Year)	Emission Estimation Method Code (See Instructions)	Control Efficiency (Net after all controls)	Emission Factor	Ef Control
		2010				
Criteria (NAAQS) Pollutants	Pollutant Code	Emissions– Criteria Pollutants (Tons/Year)	Emission Estimation Method Code (See Instructions)	<b>Control</b> <b>Efficiency</b> (Net after all controls)	Emission Factor	EF Control
		2010				
СО	СО	448.4	08	0		
NOx	NOx	447.8	01	0		
TSP	TSP	142.9	08	99.69		
PM10	PM10	127.5	08	0		
PM2.5	PM2.5	109.7	08	0		
SO2	SO2	2833.8	01	0		
VOC	VOC	7.19	08	0	0.06	AFTER
HAP/TAP Pollutants (In Alphabetical Order)	CAS (see instructions)	Emissions HAP/TAPS (Pounds/Year)	Emission Estimation Method Code (See Instructions)	Control Efficiency (Net after all controls)	Emission Factor	EF Control
		2010				
Acetaldehyde	75-07-0	18.63836	08	0	0.0000777251	
Acrolein	107-02-8	11.06653	08	0	0.0000461493	
Allyl chloride	107-05-1	53.0029	08	0	0.000221031	
Ammonia (as NH3)	7664-41-7	14	08	0		
Arsenic Unlisted Compounds – Specify Compound (Component of ASC)	ASC-Other	20.8	08	0		

Benzene	71-43-2	22.71549	08	0	0.0000947274
Beryllium Metal (unreacted)				0	
(Component of BEC)	7440-41-7	2.9	08	0	
Cadmium Metal, elemental,	7440-43-9	2.1	08	0	
unreacted (Component of CDC)			0.0		0.00002/510
Carbon disulfide	75-15-0	6.40694	08	0	0.000026718
Chromic acid (VI) (Component of SolCR6 CRC)	7738–94–5	5.856	08	0	
Chromium Unlisted Compounds – Specify Compound (Component of CRC)	CRC-Other	42.94	08	0	
Cobalt Unlisted Compounds – Specify Compound (Component of COC)	COC-Other	13.3	08	0	
Cresol, p–	106-44-5	6.40694	08	0	0.000026718
DEHP (Di(2-ethylhexyl)phthalate)	117-81-7	20.96815	08	0	0.0000874407
Dichlorobenzene(p), 1,4-	106-46-7	6.40694	08	0	0.000026718
Dichloropropene, 1,3-	542-75-6	4.19362	08	0	0.0000174881
Dinitrotoluene, 2,4–	121-14-2	1.1649	08	0	0.00000485782
Ethylene dibromide (dibromoethane)	106-93-4	15.14366	08	0	0.0000631516
Fluoranthene (Component of 83329/POMTV)	206-44-0	0.87367	08	0	0.00000364336
Fluorene (Component of 83329/POMTV)	86-73-7	0.81543	08	0	0.00000340047
Formaldehyde	50-00-0	15.14366	08	0	0.0000631516
Furans – Dibenzofurans (group total – CAA – unchlorinated) (Component of 83329/POMTV)	132-64-9	3.37821	08	0	0.0000140877
Hydrogen chloride (hydrochloric acid)	7647-01-0	526958	02	0	
Hydrogen fluoride (hydrofluoric acid as mass of HF) (Component of 16984488/Fluorides)	7664-39-3	35773	02	10	
Isophorone	78-59-1	6.98938	08	0	0.0000291469
Lead Unlisted Compounds – Specify Compound (Component of PBC)	PBC-Other	29.9	08	0	
MIBK (methyl isobutyl ketone)	108-10-1	13.39632	08	0	0.0000558649
Manganese Unlisted Compounds – Specify Compound (Component of	MNC-Other	41	08	0	
MNC)					
Mercury, vapor (Component of HGC)	7439–97–6	36.4	08	24	
Methyl bromide (bromomethane)	74-83-9	5.1838	08	0	0.0000216173
Methyl chloride (chloromethane)	74-87-3	6.40694	08	0	0.000026718
Methyl iodide (iodomethane)	74-88-4	11.64898	08	0	0.0000485782
Methylene chloride	75-09-2	20.96815	08	0	0.0000874407
Naphthalene (Component of 83329/POMTV)	91–20–3	3.61117	08	0	0.0000150592
Nickel metal (Component of NIC)	7440-02-0	42.9	08	0	

Phenanthrene (Component of 83329/POMTV)	85-01-8	2.44628	08	0	0.0000102014
Polycyclic Organic Matter (Inc PAH, dioxins, etc. NC AP 42 historic)	РОМ	12.06834	08	0	0.000050327
Propionaldehyde	123-38-6	11.06653	08	0	0.0000461493
Pyrene (Component of 83329/POMTV)	129-00-0	0.38442	08	0	0.00000160308
Selenium Compounds	SEC	1334.3	08	44	
Sulfuric acid	7664-93-9	2247	08	99	
Vinyl chloride	75-01-4	4.25187	08	0	0.000017731

### North Carolina Department of Environment and Natural Resources **Division of Air Quality** Air Pollutant Point Source Emissions Inventory - Calendar Year 2010 1. Emission Source ID (from permit) or ES-4 (B8).13A **Emission Source Group ID** 2. Emission Source Description: Coal/No. 2 fuel oil-fired electric utility boiler (1,440 million Btu per hour maximum heat input, Unit No. 5 - Boiler No. 8) 3. **Operating Scenario ID/Description:** OS – 9/electric utility boiler fired by No. 2 fuel 10100501 / Distillate Oil (No. 1 2); Normal Firing 4. SCC Number/Description: 5. Throughput/units in 2010: 138839 GAL/yr (e.g. production or fuel use): 6. Fuel Information (If fuel is used) % Sulfur 0.0015 % Ash 0.01 138110 Btu/gallon Heat Content (Btu/units) 7. Capture Efficiency 100

(% of Emissions from this Process Vented to Control Device or Stack):

## 8. Control Device Information :

Order	CS-ID	CD ID	Control Device Description
		(as listed in permit)	
1	CS-3	CD-3.13A	Hot-side electrostatic precipitator (80,640 square feet of plate area)

## 9. Emission Release Point (ERP) Information: (Sources vented to more than one ERP use additional entry lines):

ERP ID	ERP Type	(in feet)	<b>Diameter</b> Circle (enter #): Rectangle (L x W) (in 0.1 feet)	<b>Temperature</b> (F)	Velocity (Feet/sec)	Volume Flow Rate <sup>(Acfm)</sup>	ERP Description
ES–9 Stack	VERTICAL STACK	216	8	334	92	277465.46	ES–9 Discharge Stack

**10. Operating Schedule**: (Source/Operating Scenario that best characterizes Calendar Year 2010) **Hours per Day** (24) **Days per Week** (7) **Weeks per Year** (52)

11. Typical Start & End Times For Operating Scenario: Start: 0 End: 2359

## **12. Seasonal Periods Percent Annual Throughput:**

Jan–Feb + Dec	25%	March–May	25%	June–Aug.	25%	Sept.–Nov.	25%
2010	, ,	2010		2010		2010	

## 13. <u>Actual Emissions per Pollutant Listed :</u>

Attach calculations and documentation of emission factors or other estimation methods used.

GHG Pollutants	CAS	Emissions– GHG Pollutants (Tons/Year) 2010	Emission Estimation Method Code (See Instructions)	<b>Control</b> <b>Efficiency</b> (Net after all controls)	Emission Factor	Ef Control
Criteria (NAAQS) Pollutants	Pollutant Code	Emissions– Criteria Pollutants (Tons/Year)	Emission Estimation Method Code (See Instructions)	<b>Control</b> <b>Efficiency</b> (Net after all controls)	Emission Factor	EF Control
	00	2010	00	0	0.005	
СО	СО	0.35	08	0	0.005	AFTER
TSP	TSP	0.23	08	50		
PM10	PM10	0.19	08	0		
PM2.5	PM2.5	0.16	08	0	0.0002	
VOC	VOC	0.01	08	0	0.0002	AFTER
HAP/TAP Pollutants (In Alphabetical Order)	CAS (see instructions)	<b>Emissions</b> <b>HAP/TAPS</b> (Pounds/Year)	Emission Estimation Method Code (See Instructions)	<b>Control</b> <b>Efficiency</b> (Net after all controls)	Emission Factor	EF Control
		2010				
Arsenic Unlisted Compounds – Specify Compound (Component of ASC)	ASC–Other	0.07719	08	0	5.56E-7	
Beryllium Metal (unreacted) (Component of BEC)	7440-41-7	0.0579	08	0	4.17E–7	
Cadmium Metal, elemental, unreacted (Component of CDC)	7440-43-9	0.0579	08	0	4.17E–7	
Chromic acid (VI) (Component of SolCR6 CRC)	7738–94–5	0.0579	08	0	4.17E–7	
Cobalt Unlisted Compounds – Specify Compound	COC-Other	0.82984	08	0	0.000005977	

(Component of COC)						
Formaldehyde	50-00-0	4.58169	08	0	0.000033	
Lead Unlisted Compounds – Specify Compound (Component of PBC)	PBC–Other	0.17369	08	0	0.000001251	
Manganese Unlisted Compounds – Specify Compound (Component of MNC)	MNC-Other	0.11579	08	0	8.34E-7	
Mercury, vapor (Component of HGC)	7439–97–6	0.0579	08	0	4.17E–7	
Naphthalene (Component of 83329/POMTV)	91-20-3	0.15689	08	0	0.00000113	
Selenium Compounds	SEC	0.28948	08	0	0.000002085	

### North Carolina Department of Environment and Natural Resources **Division of Air Quality** Air Pollutant Point Source Emissions Inventory - Calendar Year 2010 1. Emission Source ID (from permit) or ES-5 (B9).13A **Emission Source Group ID** 2. Emission Source Description: Coal/No. 2 fuel oil-fired electric utility boiler (1,440 million Btu per hour maximum heat input, Unit No. 6 - Boiler No. 9) 3. **Operating Scenario ID/Description:** OS - 10/electric utility boiler fired by coal 10100202 / Bituminous Coal ; Pulverized Coal: Dry Bottom 4. SCC Number/Description: 5. Throughput/units in 2010: 225818.5 TON/yr (e.g. production or fuel use): 6. Fuel Information (If fuel is used) Heat Content % Sulfur 0.64 % Ash 12.54 11830.21 Btu/lb (Btu/units) 7. Capture Efficiency

(% of Emissions from this Process Vented to Control 100 Device or Stack):

## 8. Control Device Information :

Order	CS-ID	<b>CD ID</b> (as listed in permit)	Control Device Description
1	CS-3	CD-3.13A	Hot-side electrostatic precipitator (80,640 square feet of plate area)

## 9. Emission Release Point (ERP) Information: (Sources vented to more than one ERP use additional entry lines):

ERP ID	ERP Type	(in feet)	<b>Diameter</b> Circle (enter #): Rectangle (L x W) (in 0.1 feet)	<b>Temperature</b> (F)	Velocity (Feet/sec)	Volume Flow Rate <sup>(Acfm)</sup>	ERP Description
ES–9 Stack	VERTICAL STACK	216	8	334	92	277465.46	ES–9 Discharge Stack

**10. Operating Schedule**: (Source/Operating Scenario that best characterizes Calendar Year 2010) **Hours per Day** (24) **Days per Week** (7) **Weeks per Year** (52)

11. Typical Start & End Times For Operating Scenario: Start: 0 End: 2359

12. Seasonal Periods Percent Annual Through
---------------------------------------------

Jan–Feb + Dec 21% March–Ma 2010 2010	28%	June–Aug. 2010	41%	Sept.–Nov. 2010	10%
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## 13. <u>Actual Emissions per Pollutant Listed :</u>

Attach calculations and documentation of emission factors or other estimation methods used.

GHG Pollutants	CAS	Emissions– GHG Pollutants (Tons/Year)	Emission Estimation Method Code (See Instructions)	Control Efficiency (Net after all controls)	Emission Factor	Ef Control
		2010				
Criteria (NAAQS) Pollutants	Pollutant Code	Emissions– Criteria Pollutants (Tons/Year)	Emission Estimation Method Code (See Instructions)	<b>Control</b> <b>Efficiency</b> (Net after all controls)	Emission Factor	EF Control
		2010				
СО	СО	427.1	08	0		
NOx	NOx	476.6	01	0		
TSP	TSP	155.9	08	99.54		
PM10	PM10	134.4	08	0		
PM2.5	PM2.5	109.7	08	0		
SO2	SO2	2776.1	01	0		
VOC	VOC	6.9	08	0		
HAP/TAP Pollutants (In Alphabetical Order)	CAS (see instructions)	Emissions HAP/TAPS (Pounds/Year)	Emission Estimation Method Code (See Instructions)	Control Efficiency (Net after all controls)	Emission Factor	EF Control
		2010				
Acetaldehyde	75-07-0	17.55177	08	0	0.0000777251	
Acrolein	107-02-8	10.42137	08	0	0.0000461493	
Allyl chloride	107-05-1	49.91289	08	0	0.000221031	
Ammonia (as NH3)	7664-41-7	18.2	08	0		
Arsenic Unlisted Compounds – Specify Compound (Component of ASC)	ASC-Other	27.7	08	0		

Benzene	71-43-2	21.3912	08	0	0.0000947274
Beryllium Metal (unreacted)				-	
(Component of BEC)	7440–41–7	4.2	08	0	
Cadmium Metal, elemental,	7440-43-9	2.4	08	0	
unreacted (Component of CDC)		2.4	08	0	
Carbon disulfide	75-15-0	6.03342	08	0	0.000026718
Chromic acid (VI) (Component of SolCR6 CRC)	7738–94–5	6.948	08	0	
Chromium Unlisted Compounds – Specify Compound (Component of CRC)	CRC-Other	50.95	08	0	
Cobalt Unlisted Compounds – Specify Compound (Component of COC)	COC-Other	16.5	08	0	
Cresol, p–	106-44-5	6.03342	08	0	0.000026718
DEHP (Di(2-ethylhexyl)phthalate)	117-81-7	19.74573	08	0	0.0000874407
Dichlorobenzene(p), 1,4-	106-46-7	6.03342	08	0	0.000026718
Dichloropropene, 1,3–	542-75-6	3.94914	08	0	0.0000174881
Dinitrotoluene, 2,4–	121-14-2	1.09699	08	0	0.00000485782
Ethylene dibromide (dibromoethane)	106-93-4	14.26044	08	0	0.00006315
Fluoranthene (Component of 83329/POMTV)	206-44-0	0.82274	08	0	0.00000364336
Fluorene (Component of 83329/POMTV)	86-73-7	0.76789	08	0	0.00000340047
Formaldehyde	50-00-0	14.2608	08	0	0.0000631516
Furans – Dibenzofurans (group total – CAA – unchlorinated) (Component of 83329/POMTV)	132-64-9	3.18178	08	0	0.00001409
Hydrogen chloride (hydrochloric acid)	7647-01-0	496721	02	0	
Hydrogen fluoride (hydrofluoric acid as mass of HF) (Component of 16984488/Fluorides)	7664–39–3	33709	02	10	
Isophorone	78-59-1	6.58191	08	0	0.0000291469
Lead Unlisted Compounds – Specify Compound (Component of PBC)	PBC–Other	38.5	08	0	
MIBK (methyl isobutyl ketone)	108-10-1	12.61533	08	0	0.0000558649
Manganese Unlisted Compounds – Specify Compound (Component of MNC)	MNC-Other	62.5	08	0	
Mercury, vapor (Component of HGC)	7439–97–6	34.3	08	24	
Methyl bromide (bromomethane)	74-83-9	4.88159	08	0	0.0000216173
Methyl chloride (chloromethane)	74-87-3	6.03387	08	0	0.00002672
Methyl iodide (iodomethane)	74-88-4	10.96986	08	0	0.0000485782
Methylene chloride	75-09-2	19.74573	08	0	0.0000874407
Naphthalene (Component of 83329/POMTV)	91-20-3	3.40065	08	0	0.0000150592
Nickel metal (Component of NIC)	7440-02-0	49.2	08	0	

Phenanthrene (Component of 83329/POMTV)	85-01-8	2.30366	08	0	0.0000102014	
Polycyclic Organic Matter (Inc PAH, dioxins, etc. NC AP 42 historic)	РОМ	11.36477	08	0	0.000050327	
Propionaldehyde	123-38-6	10.42137	08	0	0.0000461493	
Pyrene (Component of 83329/POMTV)	129-00-0	0.36201	08	0	0.00000160308	
Selenium Compounds	SEC	1257.3	08	44		
Sulfuric acid	7664-93-9	0	08	99.9		
Vinyl chloride	75-01-4	4.00399	08	0	0.000017731	

### North Carolina Department of Environment and Natural Resources **Division of Air Quality** Air Pollutant Point Source Emissions Inventory - Calendar Year 2010 1. Emission Source ID (from permit) or ES-5 (B9).13A **Emission Source Group ID** 2. Emission Source Description: Coal/No. 2 fuel oil-fired electric utility boiler (1,440 million Btu per hour maximum heat input, Unit No. 6 – Boiler No. 9) 3. **Operating Scenario ID/Description:** OS – 11/electric utility boiler fired by No. 2 fuel SCC Number/Description: 10100501 / Distillate Oil (No. 1 2); Normal Firing 4. 5. Throughput/units in 2010: 159835 GAL/yr (e.g. production or fuel use): 6. Fuel Information (If fuel is used) % Sulfur 0.0015 % Ash 0.01 138083 Btu/gallon Heat Content (Btu/units) 7. Capture Efficiency 100

(% of Emissions from this Process Vented to Control Device or Stack):

## 8. Control Device Information :

Order	CS-ID	CD ID	<b>Control Device Description</b>
		(as listed in permit)	
1	CS-3	CD-3.13A	Hot-side electrostatic precipitator (80,640 square feet of plate area)

## 9. Emission Release Point (ERP) Information: (Sources vented to more than one ERP use additional entry lines):

ERP ID	ERP Type	(in feet)	<b>Diameter</b> Circle (enter #): Rectangle (L x W) (in 0.1 feet)	<b>Temperature</b> (F)	Velocity (Feet/sec)	Volume Flow Rate <sup>(Acfm)</sup>	ERP Description
ES–9 Stack	VERTICAL STACK	216	8	334	92	277465.46	ES–9 Discharge Stack

**10. Operating Schedule**: (Source/Operating Scenario that best characterizes Calendar Year 2010) **Hours per Day** (24) **Days per Week** (7) **Weeks per Year** (52)

11. Typical Start & End Times For Operating Scenario: Start: 0 End: 2359

## **12. Seasonal Periods Percent Annual Throughput:**

Jan–Feb + Dec 25%	March–May 2010	25%	June–Aug. 2010	25%	Sept.–Nov. 2010	25%
-010	2010		-010		-010	

## 13. <u>Actual Emissions per Pollutant Listed :</u>

Attach calculations and documentation of emission factors or other estimation methods used.

GHG Pollutants	CAS	Emissions– GHG Pollutants (Tons/Year) 2010	Emission Estimation Method Code (See Instructions)	<b>Control</b> <b>Efficiency</b> (Net after all controls)	Emission Factor	Ef Control
Criteria (NAAQS) Pollutants	Pollutant Code	Emissions– Criteria Pollutants (Tons/Year)	Emission Estimation Method Code (See Instructions)	<b>Control</b> <b>Efficiency</b> (Net after all controls)	Emission Factor	EF Control
	00	2010	00	0	0.005	
СО		0.4	08	0	0.005	AFTER
TSP	TSP DM10	0.26	08	50		
PM10	PM10	0.21	08	0		
PM2.5	PM2.5	0.18	08	0	0.0002	
VOC	VOC	0.02	08	0	0.0002	AFTER
HAP/TAP Pollutants (In Alphabetical Order)	CAS (see instructions)	<b>Emissions</b> <b>HAP/TAPS</b> (Pounds/Year)	Emission Estimation Method Code (See Instructions)	<b>Control</b> <b>Efficiency</b> (Net after all controls)	Emission Factor	EF Control
		2010				
Arsenic Unlisted Compounds – Specify Compound (Component of ASC)	ASC–Other	0.08887	08	0	5.56E-7	
Beryllium Metal (unreacted) (Component of BEC)	7440-41-7	0.06665	08	0	4.17E–7	
Cadmium Metal, elemental, unreacted (Component of CDC)	7440-43-9	0.06665	08	0	4.17E–7	
Chromic acid (VI) (Component of SolCR6 CRC)	7738–94–5	0.06665	08	0	4.17E–7	
Cobalt Unlisted Compounds – Specify Compound	COC-Other	0.95533	08	0	0.000005977	

(Component of COC)						
Formaldehyde	50-00-0	5.27456	08	0	0.000033	
Lead Unlisted Compounds – Specify Compound (Component of PBC)	PBC–Other	0.19995	08	0	0.000001251	
Manganese Unlisted Compounds – Specify Compound (Component of MNC)	MNC-Other	0.1333	08	0	8.34E-7	
Mercury, vapor (Component of HGC)	7439–97–6	0.06665	08	0	4.17E–7	
Naphthalene (Component of 83329/POMTV)	91-20-3	0.18061	08	0	0.00000113	
Nickel metal (Component of NIC)	7440-02-0	0.06665	08	0	4.17E–7	
Selenium Compounds	SEC	0.33326	08	0	0.000002085	

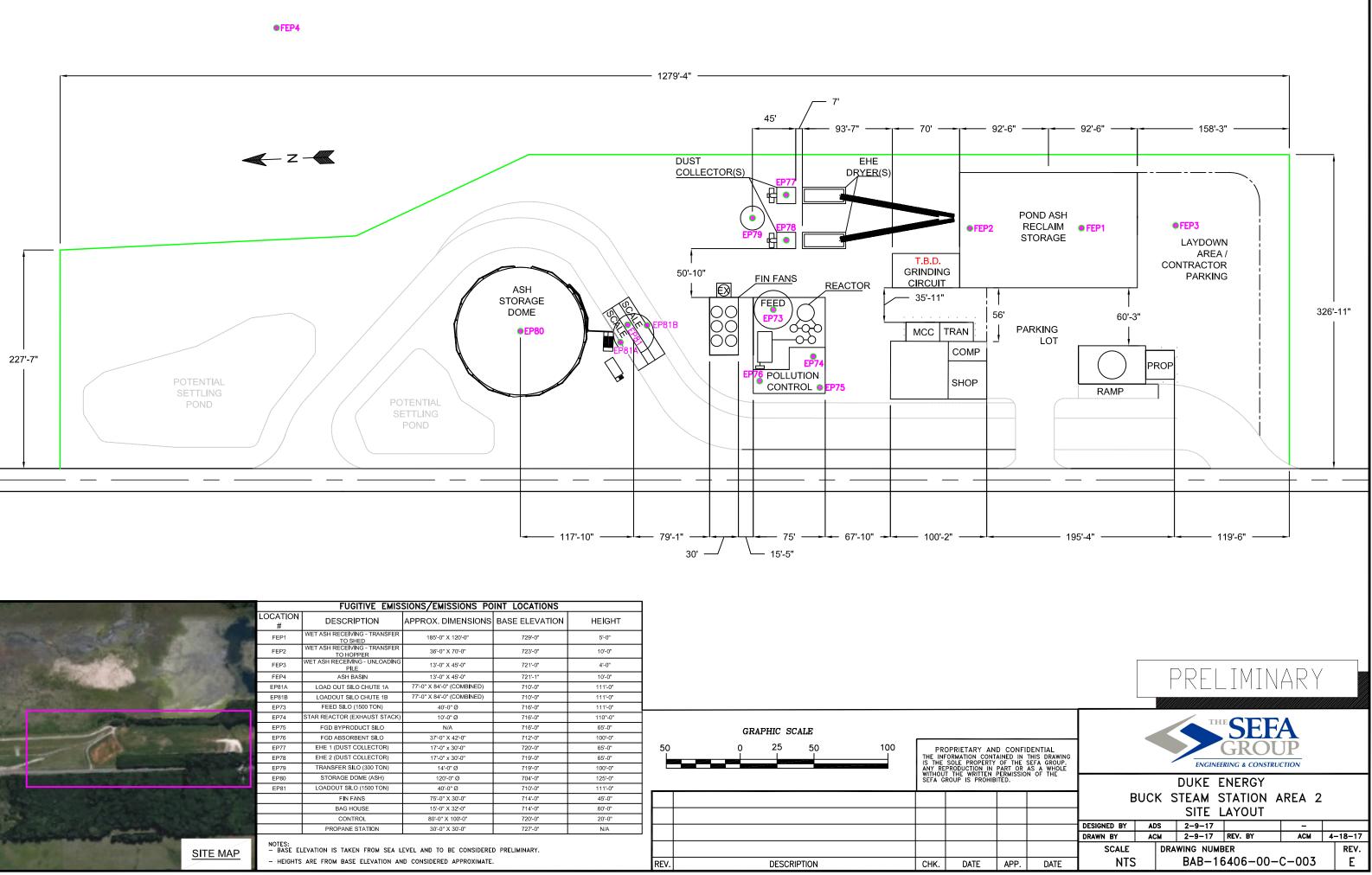
### Buck Total Criteria Emissions Reporting Year: 2011

	Unit 5 Blr. 8 Emissions (tons)	Unit 6 Blr. 9 Emissions (tons)	Unit 7-C Emissions (tons)	Unit 8-C Emissions (tons)	Unit 9-C Emissions (tons)	Unit 10CC Emis. (tons)	Unit 11CC Emis. (tons)	Unit 10-Aux. Emissions (tons)	Total Emissions (tons)
Filterable PM	58.82	24.87	0.00	0.00	0.00	1.25	0.00	0.00	84.94
Filterable PM-10	39.39	16.64	0.00	0.00	0.00	1.25	0.00	0.00	57.28
Filterable PM-2.5	17.06	7.33	0.00	0.00	0.00	0.63	0.00	0.00	25.02
Condensable PM	101.48	96.06	0.01	0.01	0.00	3.10	0.00	0.00	200.66
SO2	1,931.50	1,907.50	0.00	0.00	0.00	0.49	0.00	0.01	3839.5
NOx	305.80	333.20	0.74	0.51	0.00	7.97	0.00	0.00	648.22
VOC	4.41	4.41	0.00	0.00	0.00	1.38	0.00	0.00	10.20
СО	274.68	265.41	0.19	0.13	0.00	5.81	0.00	0.00	546.23
TSP - total	160.30	120.93	0.01	0.01	0.00	4.35	0.00	0.00	285.60
PM-10 - total	140.87	112.70	0.01	0.01	0.00	4.35	0.00	0.00	257.94
PM-2.5 - total	118.54	103.39	0.01	0.01	0.00	3.73	0.00	0.00	225.68

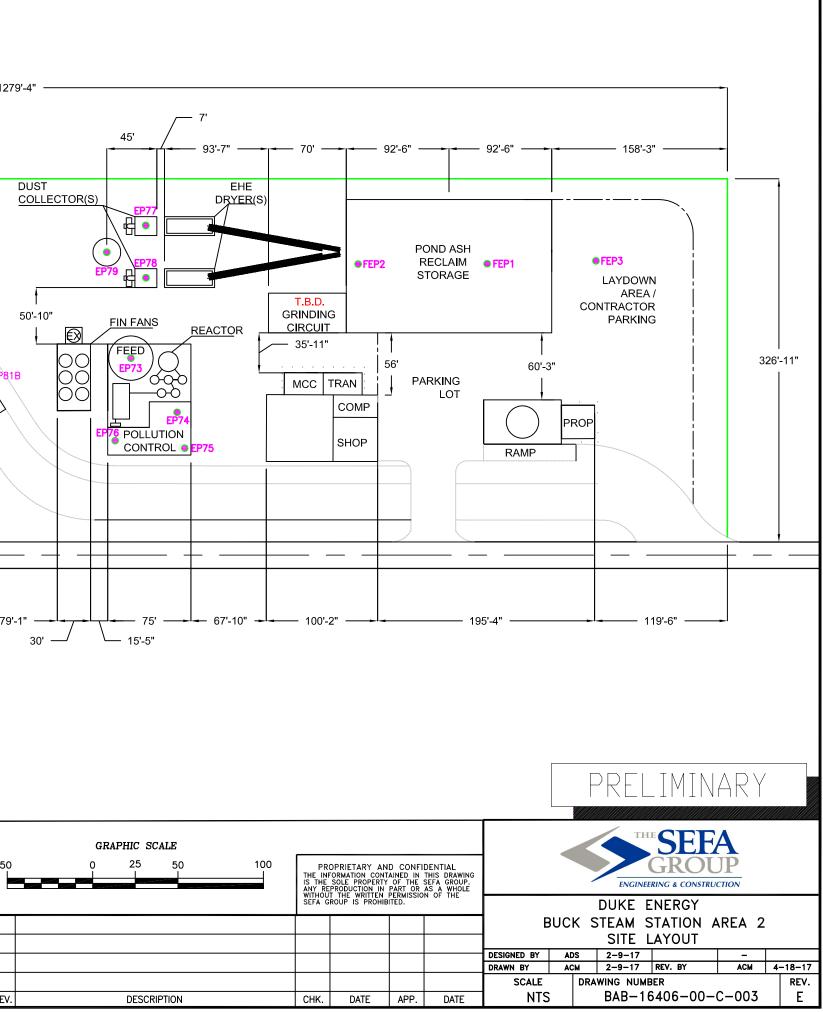
# **APPENDIX D**

# FACILITY DRAWINGS





			SIONS/EMISSIONS PO	INT LOCATIONS		l
and the second	LOCATION #	DESCRIPTION	APPROX. DIMENSIONS	BASE ELEVATION	HEIGHT	
the state of the s	FEP1	WET ASH RECEIVING - TRANSFER TO SHED	185'-0" X 120'-0"	729'-0"	5'-0"	
A DECEMBER OF THE OWNER OWNE	FEP2	WET ASH RECEIVING - TRANSFER TO HOPPER	36'-0" X 70'-0"	723'-0"	10'-0"	
	FEP3	WET ASH RECEIVING - UNLOADING PILE	13'-0" X 45'-0"	721'-0"	4'-0"	l
A REAL PROPERTY OF THE REAL	FEP4	ASH BASIN	13'-0" X 45'-0"	721'-1"	10'-0"	J
A CONTRACTOR OF THE OWNER OWNER OF THE OWNER OWNE	EP81A	LOAD OUT SILO CHUTE 1A	77'-0" X 84'-0" (COMBINED)	710'-0"	111'-0"	l
Section Company of the local section of the	EP81B	LOADOUT SILO CHUTE 1B	77'-0" X 84'-0" (COMBINED)	710'-0"	111'-0"	l
	EP73	FEED SILO (1500 TON)	40'-0" Ø	716'-0"	111'-0"	
State of the second	EP74	STAR REACTOR (EXHAUST STACK)	10'-0" Ø	716'-0"	110"-0"	
	EP75	FGD BYPRODUCT SILO	N/A	716'-0"	65'-0"	
	EP76	FGD ABSORBENT SILO	37'-0" X 42'-0"	712'-0"	100'-0"	
CARD IN AND	EP77	EHE 1 (DUST COLLECTOR)	17'-0" x 30'-0"	720'-0"	65'-0"	
	EP78	EHE 2 (DUST COLLECTOR)	17'-0" x 30'-0"	719'-0"	65'-0"	
The second secon	EP79	TRANSFER SILO (300 TON)	14'-0" Ø	719'-0"	100'-0"	
	EP80	STORAGE DOME (ASH)	120'-0" Ø	704'-0"	125'-0"	
	EP81	LOADOUT SILO (1500 TON)	40'-0" Ø	710'-0"	111'-0"	
		FIN FANS	75'-0" X 30'-0"	714'-0"	45'-0"	
		BAG HOUSE	15'-0" X 32'-0"	714'-0"	60'-0"	
	6	CONTROL	80'-0" X 100'-0"	720'-0"	20'-0"	
	-	PROPANE STATION	30'-0" X 30'-0"	727'-0"	N/A	
SITE MAP	NOTES: - BASE E	LEVATION IS TAKEN FROM SEA L	EVEL AND TO BE CONSIDERE	D PRELIMINARY.		





recommends the independent verification of any information contained on this site by the user. Rowan County makes no warranty or other assertion as to the fitness of the maps for any particular purpose and neither Rowan County nor it's agents or employees shall be liable for any claim alleged to have resulted from any use thereof.

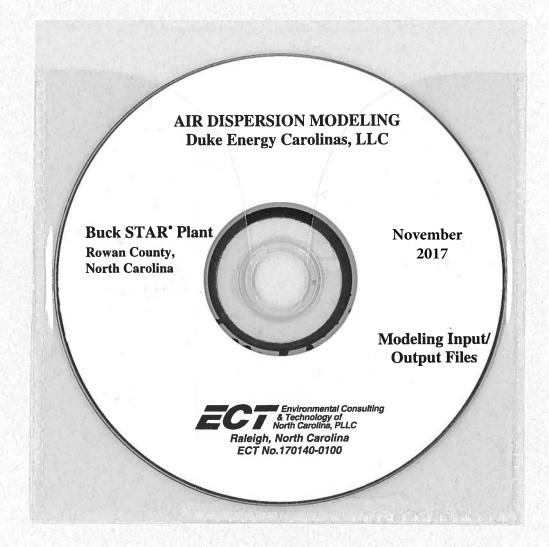
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4/3/2017

**APPENDIX E** 

AIR DISPERSION MODELING







NHSM DETERMINATION





## North Carolina Department of Environment and Natural Resources

Pat McCrory Governor Donald R. van der Vaart Secretary

June 10, 2015

Mr. Jim Clayton The SEFA Group 217 Cedar Road Lexington, SC 29073

## SUBJECT: Applicability Determination No. 2501 The SEFA Group Lexington, SC

Dear Mr. Clayton:

The North Carolina Division of Air Quality (DAQ) received your letter dated September 5, 2014, requesting the DAQ's concurrence with its determination of regulatory status of certain coal combustion residues, when used in its Staged Turbulent Air Reactor (STAR Reactor), in accordance with 40 CFR 241 "Solid Wastes Used As Fuels or Ingredients in Combustion Units" ("Solid Waste Definition Rule" or "Rule" hereinafter).

Specifically, SEFA Group (SEFA) requests the confirmation that coal ash obtained from the following specific sources meets the requirements in §241: flyash received directly from coal-fired power plant's particulate collection infrastructure (i.e., electrostatic precipitator or baghouse), and processed flyash received from landfills and ash ponds.

Unless exempt, combustion of "non-hazardous secondary material (NHSM), as defined in §241.2 would subject the emissions unit (such as STAR reactor) to requirements in 40 CFR 60 Subpart CCCC "Standards of Performance for Commercial and Industrial Solid Waste Incineration Units" or, Subpart DDDD "Emissions Guidelines and Compliance Times for Commercial and Industrial Solid Waste Incineration Units". These regulations are commonly known as CISWI ("Commercial and Industrial Solid Waste Incineration").

The DAQ has determined that the coal ash received directly from the coal-fired power plant's particulate collection infrastructure (i.e., electrostatic precipitator or baghouse) is a NHSM and an "ingredient", as defined in §241.2. DAQ has further determined that this flyash meets the legitimacy criteria included in §241.3(d)(2) and thus, concludes that it is not a solid waste. Therefore, the STAR Reactor is not subject to the requirements in CISWI.

Moreover, the processed flyash received from landfills or ash ponds is a NHSM and an ingredient, and DAQ has determined that this flyash also meets the legitimacy criteria included in 241.3(d)(2), and thus, concludes that it is not a solid waste. Therefore, the STAR Reactor is not subject to the requirements in CISWI.

1641 Mail Service Center, Raleigh, North Carolina 27699-1641 Phone: 919-707-8400 / Internet: www.ncdenr.gov

The following includes discussion on STAR Reactor, and technical and regulatory analysis supporting these conclusions for each of the above types of flyash:

### **STAR Reactor**

The STAR Reactor is a patented technology developed by SEFA for thermal beneficiation / processing of either a low or high-Btu value fine particulate matter, such as the above described flyash [hereinafter "feedstock"], along with other ingredient materials (gas, solids, and liquids) into a variety of commercial products. These products are used not only for application as a partial cement replacement but for many other commercial and industrial applications. There are several products which SEFA is currently capable of producing because of the flexibility embodied in this reactor. For example, STAR<sup>®</sup> RP, Ultrix<sup>®</sup>, Spherix<sup>®</sup>, Fortimix<sup>®</sup>, and Permanix<sup>TM</sup>.

The STAR Reactor process is inherently flexible in that operating parameters can be varied and different ingredients can be added to produce a desired product. The primary component of the STAR Reactor is a cylindrical refractory-lined vessel in which the majority of the process reactions take place. These reactions can include a range of both chemical and physical reactions. Air is required for pneumatic uplift of the solids and for the process reactions enters through the floor of the STAR Reactor as well as through the walls at multiple locations. The raw feedstock and any other ingredients are introduced through the walls of the STAR Reactor. All of the solids and gases exit together at the top of the reactor. The gas/solids mixture enters a hot cyclone where the majority of solids are separated from the gas and recycled back to the STAR Reactor. The very high rate of hot recycle solids increases the operating flexibility of the process. The process reactions can occur through this reactor/hot cyclone loop. Due to the high gas velocity, the multiple injection points, and the recycle solids, there is a significant amount of turbulence created which enhances the mixing of the ingredients and optimizes the reactions. The gas and remaining solids not collected by the hot cyclone are passed over a heat exchanger which can be designed to preheat the process air, used in heat recovery, or to simply cool the gas/solids mixture. Once cooled, the solids are separated from the gas in a fabric filter recovery device. Solids can also exit the STAR Reactor at the bottom or from the recycle loop. These solids can be combined with the solids/gas stream before the heat recovery equipment or, since they have different characteristics as compared to the solids exiting the hot cyclone, they can be processed separately for a particular application. By design the STAR Reactor operates under a wide range of process parameters.

### **Technical and Regulatory Analysis**

Flyash Received Directly from Coal-fired Power Plant's Particulate Collection Infrastructure (i.e., Electrostatic precipitator or Baghouse)

As described above, the STAR Reactor is capable of utilizing flyash, received directly from coal-fired power plant's particulate emissions controls, as its primary ingredient along with other select ingredients in order to produce a variety of products for markets.

§241.2(b)(3) of the rule defines NHSM as "a secondary material that, when discarded, would not be identified as a hazardous waste under Part 261 of this chapter". Further the same section defines secondary material as "any material that is not the primary product of a manufacturing or commercial process, and can include post-consumer material, off-specification commercial chemical products or manufacturing chemical intermediates, post-industrial material, and scrap."

It is indisputable that flyash generated from combustion of coal is not a "primary product of a manufacturing" facility (such as electric generating facility) and this product can be deemed as "post-industrial material". Moreover, coal flyash is not regulated as a hazardous waste as per Part 261 of 40 CFR "Identification and Listing of Hazardous Waste". In fact, EPA has promulgated a rule on April 17, 2015 (80 FR 21302) to regulate disposal of coal combustion residues (fly ash, bottom ash, boiler slag, and flue gas desulfurization materials generated from burning coal for the purpose of generating electricity by electric utilities and independent power producers) [CCR] as solid waste under Subtitle D "State or Regional Solid Waste Plans" of the Resource Conservation Act (RCRA) [administrative regulations included in 40 CFR 257) and not under the Subtitle C of the RCRA "Hazardous Waste Management" [administrative regulations included in 40 CFR 261]. In addition, the beneficial uses (e.g., use of flyash in concrete manufacturing replacing traditional product cement) of CCR is exempt from this regulation.

Based, on the above discussion, it is concluded that the flyash generated from the coal combustion and received directly from coal-fired power plant's particulate emissions control devices, is a NHSM.

§241.3(b)(3) of the Solid Waste Definition Rule provides that NHSMs are not solid waste when "used as an ingredient in a combustion unit that meet the legitimacy criteria specified in paragraph (d)(2) of this section." §241.2 of the Solid Waste Definition Rule defines "ingredient" as "a non-hazardous secondary material that is a component in a compound, process or product." The feedstock is merely one component among a number of variables which are introduced to the STAR Reactor to produce many different products. Therefore, feedstock processed in the STAR Reactor is an ingredient under the Solid Waste Definition Rule.

### Legitimacy Criteria

For a non-hazardous secondary material used as an ingredient to be excluded from the definition of solid waste under 241.3 of the Solid Waste Definition Rule, the material must satisfy the following legitimacy criteria under Subsection (d)(2):

- (i) The non-hazardous secondary material must be managed as a valuable commodity;
- (ii) The non-hazardous secondary material must provide a useful contribution to the production or manufacturing process.
- (iii) The non-hazardous secondary material must be used to produce a valuable product or intermediate.

(iv) The non-hazardous secondary material must result in products that contain contaminants at levels that are comparable in concentration to or lower than those found in traditional products that are manufactured without the non-hazardous secondary material.

## Managed as a Valuable Commodity - §241.3(d)(2)(i)

SEFA stores its feedstock in silos and or covered shelters prior to using it as an ingredient in the STAR Reactor and conveys the material to the process equipment pneumatically. As per 241.3(d)(2)(i), the Solid Waste Definition Rule identifies the following three factors to be considered in determining whether a material is managed as a valuable commodity:

- (A) The storage of the non-hazardous secondary material prior to use must not exceed reasonable time frames;
- (B) Where there is an analogous ingredient, the non-hazardous secondary material must be managed in a manner consistent with the analogous ingredient or otherwise be adequately contained to prevent releases to the environment;
- (C) If there is no analogous ingredient, the non-hazardous secondary material must be adequately contained to prevent releases to the environment;

As per SEFA, in a previously permitted design, the storage capacity of the silos and partially enclosed storage bins for incoming feedstock ranges from 800-2000 tons and could accommodate approximately three to ten days of production when the STAR Reactor is operating on SEFA's normal production schedule. As such, under normal operations, the incoming feedstock is typically stored no more than three days prior to introduction into the STAR Reactor process. However, during shutdown of the STAR Reactor or when off-specification feedstock is received from a supplier, the feedstock may be stored for longer periods of time, but usually no more than sixty days. In the past, as per SEFA, shutdown of the STAR Reactor has generally not exceeded twenty days. With respect to the management of off-specification feedstock, SEFA has indicated that if this off-specification material can be blended with other feedstock at ratios which ensure that processing in the STAR Reactor produces an end product which meets SEFA's quality control standards, it will attempt to do so. Depending on the nature and amount of the material's deviation from SEFA's feedstock specifications, if it cannot be blended, the offspecification feedstock will have to be rejected and returned to the supplier. If it is capable of being blended, the blending process may require storage of the off-specification feedstock for as long as 60 days depending upon the quantity involved. Accordingly, even outside of the normal three-day processing scheduling for incoming feedstock, SEFA's storage of incoming feedstock does not exceed a reasonable time frame.

Additionally, SEFA manages the incoming feedstock as a valuable commodity and takes measures to prevent loss of material during off-loading and storage. In the preamble to the rule, EPA explains that "If on the other hand, a company does not manage the non-hazardous secondary material as it would traditional ingredients, that behavior may indicate that the non-

hazardous secondary material is being discarded." Refer to 76 FR 15543. The material must be "stored in a manner that both adequately prevents releases or other hazards to human health and the environment, considering the nature and toxicity of the non-hazardous secondary material." *Id.* In most cases, this requirement is satisfied if the material is in some manner "contained." *Id.* As noted, SEFA stores its feedstock in enclosed silos or covered and partially enclosed storage bins and therefore meets this criterion. Additionally, at all times prior to processing, SEFA handles the material in a manner consistent with this criterion. Feedstock is transferred from its suppliers (typically, coal-fired power plants) to SEFA either (i) directly by pneumatic conveyor into the silos or (ii) by truck to the SEFA facility. All bin vents within the pneumatic conveyer system are equipped with fabric filter recovery devices to minimize loss of this valuable material. Thus, SEFA believes that it unquestionably manages its feedstock as a valuable commodity.

## Useful Contribution to the Production or Manufacturing Process - §241.3(d)(2)(ii)

SEFA believes that there is no question that the feedstock processed in the STAR Reactor provides a useful contribution to its production of the various end products marketed by SEFA. In the preamble to the Solid Waste Definition Rule, at 76 FR 15543, EPA explains the rationale behind this criterion for legitimacy:

A non-hazardous secondary material used as an ingredient in combustion systems provides a useful contribution if it contributes valuable ingredients to the production/manufacturing process or to the product or intermediate of the production/manufacturing process. This criterion is an essential component in the determination of legitimacy because legitimate use is not occurring if the nonhazardous secondary material doesn't add anything to the process, such that the non-hazardous secondary material is basically being disposed of or discarded. This criterion is intended to prevent the practice of "sham" recycling by adding non-hazardous secondary materials to a manufacturing operation simply as a means of disposing of them.

SEFA states that the feedstock processed in the STAR Reactor is clearly not added to dispose of that material and the processing of the feedstock in the STAR Reactor can in no manner be characterized as "sham" recycling. Additionally, the fact that some of the constituents of the feedstock are not needed or desirable for the STAR Process does not affect the status of the "useful contribution" of the feedstock:

For purposes of satisfying this criterion, not every constituent or component of the non-hazardous secondary material has to make a contribution to the production/manufacturing activity. For example, non-hazardous secondary materials used as ingredients may contain some constituents that are needed in the manufacturing process, such as, for example, zinc in non-hazardous secondary materials that are used to produce zinc-containing micronutrient fertilizers, while other constituents in the non-hazardous secondary material, such as lead, do not provide a useful contribution. Provided the zinc is at levels that provides a useful contribution, we believe the non-hazardous

secondary material would satisfy this criterion, although we would note that the constituents not directly contributing to the manufacturing process could still result in the non-hazardous secondary material not meeting the contaminant part of the legitimacy criteria. The Agency is not quantitatively defining how much of the non-hazardous secondary material needs to provide a useful contribution for this criterion to be met, since we believe that defining such a level would be difficult and is likely to be different, depending on the non-hazardous secondary material. The Agency recognizes that this could be an issue if persons argue that a non-hazardous secondary material is being legitimately used as an ingredient, but in fact, only a small amount or percentage of the non-hazardous secondary material is used.

## 76 FR 15543-44 (emphasis added).

The fact that reactions in the STAR Reactor eliminate certain undesirable constituents of the feedstock material does not preclude a determination that the feedstock meets the legitimacy criteria as an ingredient. As described above, the STAR Reactor has the capability to control the chemical and physical reactions in the process to produce marketable materials with a broad range of characteristics. The constituents and characteristics of each STAR Reactor product are tailored to the intended market and vary depending on the needs of that market. The elimination of certain constituents does not affect the determination that the feedstock is an ingredient which makes a useful contribution to the products produced in the STAR Reactor.

## Produces a Valuable Product or Intermediate - §241.3(d)(2)(iii)

As per SEFA, it is undisputed that feedstock material is used in the STAR Reactor to make valuable products. "The product or intermediate is valuable if it is (i) sold to a third party or (ii) used as an effective substitute for a commercial product or as an ingredient or intermediate in an industrial process." Refer to 76 FR 15544. Also, as discussed above, the STAR Reactor has the capability to process its fly ash and other materials to produce a broad range of products. All of the products currently produced in the STAR Reactor have application as both substitutes for commercial products and as ingredients in an industrial process. Ultrix<sup>®</sup> and STAR RP<sup>®</sup> are sold for use as partial replacement for Portland cement. Fortimix<sup>®</sup> is sold for use as an additive for rubber compounds. Permanix<sup>TM</sup> is designed for use as a broad-spectrum UV blocker. Accordingly, in all respects, SEFA's feedstock processed in the STAR Reactor satisfies this criterion for legitimacy as an ingredient.

## Comparable Contaminants Concentration of End Product - § 241.3(d)(2)(iv)

Again, as discussed above, the STAR Reactor has the capability to process its feedstock to reduce or eliminate some undesirable constituents and to alter the chemical and physical characteristics of others in its various end products. The Solid Waste Definition Rules provides as follows:

> The non-hazardous secondary material must result in products that contain contaminants at levels that are comparable in concentration to or lower than those found in traditional products that are manufactured without the non-hazardous secondary material.

Refer to §241.3(d)(2)(iv).

The preamble to the Rule includes the following:

The assessment of whether the products produced from the use of nonhazardous secondary materials that have contaminants that are comparable to (or lower) in concentration can be made by a comparison of contaminant levels in the ingredients themselves to the traditional ingredients they are replacing, or by comparing the contaminant levels in the product itself with and without the use of the nonhazardous secondary material.

Refer to 76 FR 15544.

As applied to the use of the feedstock as an ingredient in the STAR Reactor, the relevant comparison is a comparison of the various STAR Reactor end products to comparable products in the industries in which each is used. For example, Ultrix<sup>®</sup> and STAR RP<sup>®</sup> are both used as supplementary cementitious materials in concrete, but, due to the unique processing regime of the STAR Reactor, neither has varying quantities of adsorptive unburned carbon, which characterize by-product fly ashes typically used in the marketplace. In fact, the air-entraining characteristics of Ultrix<sup>®</sup> and STAR RP<sup>®</sup> are tailored by STAR Reactor to exactly match the air-entraining characteristics of plain cement concrete.

The preamble to the proposed rule for the Solid Waste Definition Rule explains the rationale for and purpose of the comparison of contaminants in the legitimacy criteria for use of a non-hazardous secondary material as an ingredient:

The Agency recognizes that there may be instances where the contaminant levels in the products manufactured from non-hazardous secondary material ingredients may be somewhat higher than found in the traditional products that are manufactured without the non-hazardous secondary material, but the resulting concentrations would not be an indication of discard and would not pose a risk to human health and the environment.

Refer to 75 FR 31844, 31885 (Jun. 4, 2010).

In addition, EPA has recognized that contaminant levels in the products made from NHSM can have contaminant levels within a "small acceptable range" at 76 FR 15523 (March 21, 2011).

The above discussion clearly provides that it may be allowable under (241.3(d)(2)(iv)) for certain contaminants in the end product made with non-hazardous secondary materials ingredients to be "somewhat higher" or within a "small acceptable range" than those in traditional products. Thus, SEFA's fly ash feedstock satisfies the legitimacy criterion in (241.3(d)(2)(iv)) despite the slightly higher concentrations of arsenic and beryllium in the STAR RP<sup>®</sup> as compared to Portland Cement, as included in Attachment A to the SEFA's September 2014 letter. Also, using additional analytical data received from SEFA<sup>1</sup>, it can be said that the contaminant levels in the SEFA product are within the range of contaminants levels or within a "small acceptable range" for Portland Cement (traditional product).

Additionally, as stated in the preamble to the proposed rule above, the purpose of the contaminant comparison criterion is to demonstrate that the use of the non-hazardous secondary material ingredient is not indicative of discard and does not pose a risk to human health and the environment. Expanding of the "indication of discard" aspect of this component of the legitimacy criteria, EPA further explains:

Based on our assessment of all of the comments, we believe it appropriate to include contaminant levels as a legitimacy criterion. Thus, we do not agree with those commenters that assert that contaminant comparisons are not appropriate to require as part of the legitimacy criteria. The Agency believes the criterion is necessary because non-hazardous secondary materials that contain contaminants that are not comparable in concentration to those contained in traditional fuel products or ingredients would suggest that these contaminants are being combusted as a means of discarding them, and thus the non-hazardous secondary material should be classified as a solid waste. In some cases, this can also be an indicator of sham recycling.

Refer to 75 FR 31871-72 (emphasis added).

As such, the primary purpose of the comparison on contaminants in an end product using the non-hazardous secondary material ingredient to that of traditional products made without the non-hazardous secondary material ingredient is to demonstrate that such use is not a means of discarding the non-hazardous secondary material or indicative of sham recycling.

With respect to the additional industrial uses for products produced by using fly ash feedstock as an ingredient in the STAR Reactor, a direct comparison of SEFA's end product to a traditional product which is manufactured without fly ash feedstock is not feasible for many of the end products produced in the STAR Reactor. However, based on the detailed comparison of the STAR<sup>®</sup> RP to Portland Cement and the various markets for SEFA's other STAR Reactor products as included in the above referenced submittal, it is clear that SEFA is not processing the fly ash feedstock as a means of discarding the fly ash or any of its constituents.

<sup>&</sup>lt;sup>1</sup> Email dated 5/12/2015 from Thomas Pritcher, Environmental Consulting & Technology, Inc., to Rahul Thaker, NCDAQ.

To the extent that the purpose of the contaminant comparison is to demonstrate that these products do not pose a risk to human health and the environment, SEFA has provided additional information as well as copies of the material safety data sheets for these products to demonstrate that no such risk is posed in the various industrial uses of STAR Reactor end products. For example, the material safety data sheets for Spherix<sup>®</sup> and Fortimix<sup>®</sup> included in Attachment B to the SEFA's September 2014 letter. As per SEFA, in many cases, the STAR<sup>®</sup> Reactor end products provide a safe alternative to traditional products which may pose a potential risk to human health and the environment.

### Flyash Received from Landfill or Ash Pond

\$241.3(b)(4) of the rule provides that NHSMs are not solid waste when "fuel or ingredient products that are used in a combustion unit, and that are produced from the processing of discarded non-hazardous secondary materials and that meet the legitimacy criteria specified in paragraph (d)(1) of this section, with respect to fuels, and paragraph (d)(2) of this section, with respect to ingredients."

As discussed above, the coal flyash disposed off in a landfill or an ash pond can be deemed as a NHSM. Prior to being used as an acceptable ingredient (feedstock) in the STAR Reactor, any flyash received from landfills or ash ponds must be "processed," as that term is defined in the rule. As discussed below, any commercial agreement between a supplier and SEFA will specify the acceptable criteria (i.e., specifications) for a feedstock that can be used in the STAR Reactor as a condition for supplying processed flyash to SEFA.

Pursuant to §241.2, "processing" means any operations that transform discarded nonhazardous secondary material into a non-waste fuel or non-waste ingredient product. Processing includes, but is not limited to, operations necessary to: remove or destroy contaminants; significantly improve fuel characteristics of the material, *e.g.* sizing or drying the material in combination with other operations; or chemically improve the as-fired energy content. Minimal operations that result only in modifying the size of the material by shredding do not constitute processing for purposes of this definition. Under the same section of the Rule, "Secondary material" is defined as any material that is not the primary product of a manufacturing or commercial process, and can include post-consumer material, off-specification commercial chemical products or manufacturing chemical intermediates, post-industrial material, and scrap.

While it is recognized that coal flyash which was initially placed into a landfill may be considered to have been "previously discarded" by custom and practice, coal-fired utilities also collect this coal ash in permitted wastewater treatment ponds. This coal ash has not historically been considered "discarded" as it was merely solids settling within a permitted wastewater unit. SEFA believes that the processing of these materials as required to satisfy SEFA's specifications for its feedstock would meet the requirements for processing of "previously discarded" materials under the Solid Waste Definition Rule as applied to CISWI. As such, the requisite processing of materials to be used as feedstock in the STAR Reactor would be sufficient to transform them to an ingredient.

The Solid Waste Definition Rule provides that a previously discarded material may be processed to transform the waste to a non-waste ingredient. Specifically, §241.3(b)(4) of the Solid Waste Definition Rule provides as follows:

Fuel or ingredient products that are used in a combustion unit, and are produced from the processing of discarded non-hazardous secondary materials and that meet the legitimacy criteria specified in paragraph (d)(1) of this section, with respect to fuels, and paragraph (d)(2) of this section, with respect to ingredients. The legitimacy criteria apply after the non-hazardous secondary material is processed to produce a fuel or ingredient product. Until the discarded nonhazardous secondary material is processed to produce a non-waste fuel or ingredient, the discarded non-hazardous secondary material is considered a solid waste and would be subject to all appropriate federal, state, and local requirements.

As per SEFA, any processing of materials from landfills or from ash ponds to meet SEFA's feedstock specifications will be undertaken under the control of the supplier prior to being received by SEFA for use an ingredient in its STAR Reactor. Accordingly, this feedstock when received by SEFA or used in the STAR Reactor would meet the legitimacy criteria for direct use as an ingredient and therefore would not be a solid waste under the Solid Waste Definition Rule. All feedstock shipped to SEFA for use as an ingredient in the STAR Reactor will first be required to undergo processing by the supplier to be:

- A. Free of all, but minimal contaminants (e.g., organic debris, slag);
- B. Finely-divided and free-flowing,
- C. Have consistent moisture content of  $\leq 25\%$ ; and
- D. Have a consistent chemical composition, including organic content as measured by loss on ignition.

The above are SEFA specifications for acceptance of any coal flyash (discarded in landfills or ash ponds).

As per SEFA, the specific processing steps that may be needed to meet the SEFA specifications (as described above) and produce a suitable feedstock for the STAR Reactor will vary depend upon the specific characteristics of each source of coal flyash. Generally speaking, one or more of the following four processing steps will be necessary to produce a suitable feedstock for the STAR Reactor:

- 1) Dewatering,
- 2) Screening/Separation,
- 3) Milling, and
- 4) Blending.

For use as a feedstock in the STAR Reactor, coal ash from an ash pond having higher moisture content will likely need to be processed using most, if not all, of these steps. Coal ash

from a landfill may not require every step. For example, it may be unnecessary to dewater coal ash from landfills if the material has consistent and acceptable moisture content.

Depending on the source of the ash, the general steps described above can require sub processes. For example, feedstock appropriate for the STAR Reactor, it may be necessary to remove larger particles or other materials found with the ash. In addition, to meet SEFA's specifications, some coal ash may require further processing through a separate loop that includes equipment (e.g., roll crusher) needed to produce a more finely-divided, free-flowing feedstock. For others, it may be necessary to utilize a magnetic separator to remove metal constituents. Also, materials such as coal, pyrites, or other more coarse materials may need to be screened. The Screening/Separation step will occur routinely to produce a free-flowing, finely-divided feedstock suitable for the STAR Reactor. Depending on the source of coal ash, milling may not be necessary to achieve a finely-divided and free-flowing material.

As emphasized by SEFA, the specific processing steps and the specific processing equipment cited above are typical examples for how these materials might be processed to produce a suitable feedstock. Those performing the actual work (i.e., suppliers) will elect to use different techniques and/or equipment. SEFA states that as long as the processed coal ash conforms to SEFA's general specifications outlined above, the coal flyash received from landfills or ash ponds will have been sufficiently "processed" and will be a suitable feedstock as an ingredient in the STAR Reactor.

It needs to be noted here that the EPA has recognized similar processing steps (similar to SEFA suggested processing steps as above to meet the SEFA specifications) are "likely to meet our definition of processing, as it appears that these processes in fact remove contaminants and improve the ingredient characteristics of these recovered CCRs (i.e., ash from ponds and landfills)". Refer to 76 FR 15518, March 21, 2011 (emphasis added).

With respect to the requirement for meeting the legitimacy criteria in §241.3(d)(2), pursuant to §241.3(b)(4), for flyash received from landfill or ash pond, SEFA emphasizes that after completion of "processing", it will become similar to the flyash received directly from coal-fired plant's particulate collection infrastructure (i.e., Electrostatic precipitator or Baghouse), and thus, will meet all legitimacy criteria as discussed above for it.

Finally, with respect to the particular criterion for comparable contaminants concentration of end product (traditional products) in 241.3(d)(2)(iv), SEFA analyzed each of these materials for semi-volatile organic compounds, organo-chlorine pesticides, PCBs, chlorides, metals and sulfur content, during engineering studies to assess the suitability of coal ash previously placed in water treatment ponds (pond ash) or previously placed in landfills (landfill ash). A comparison of the constituents in dry source feedstock, pond ash and landfill ash from SCE&G's<sup>2</sup> Wateree facility is provided in Attachment C to the SEFA's September 2014 submittal. In comparison to the dry collection feedstock, the landfill ash is comparable with slightly higher results for a few constituents. The sampling results on pond ash indicate that all constituents detected were lower

<sup>&</sup>lt;sup>2</sup> www.sceg.com

than those for the dry collection feedstock and the landfill ash. Despite certain variables in the manner in which coal ash were previously placed in ponds or landfills, as per SEFA, these sampling results are sufficient to demonstrate that contaminants in coal flyash previously placed in ponds and landfills are comparable to or lower than those in dry collection coal flyash processed as feedstock (that is, flyash received directly from the coal-fired power plant's particulate emissions control) for the STAR Reactor. Furthermore, the metals and sulfur levels of the landfill ash are comparable to those of the dry collection feedstock, and the metals and sulfur levels of the pond ash are significantly lower than those of the dry collection feedstock. Finally, more recent sampling data (March-April 2015) for dry ash and pond ash, provided by SEFA, indicates that the contaminants in pond ash as are lower than the dry ash received directly from electric utility plant.<sup>3</sup> Therefore, SEFA concludes that there will be no increase in emissions as a result of the use of pond ash and landfill ash as a feedstock for the STAR Reactor.

### Conclusions

In summary, the DAQ has determined that the fly ash received directly from the coalfired power plant's particulate collection infrastructure (i.e., electrostatic precipitator or baghouse) is a NHSM and an "ingredient", as defined in §241.2. DAQ has further determined that this flyash meets the legitimacy criteria included in §241.3(d)(2). Thus, it concludes that it is not a solid waste and therefore, STAR Reactor is not subject to the requirements in CISWI.

Moreover, the processed flyash received from ash landfills or ash ponds meets the definition of "processing" in §241.2, and is also a NHSM and an ingredient. DAQ has further determined that this flyash also meets the legitimacy criteria included in §241.3(d)(2). Thus, it concludes that it is not a solid waste and therefore, STAR Reactor is not subject to the requirements in CISWI.

It needs to be emphasized here that this letter includes only the "non-waste" determination, which is specific to the materials discussed herein. Further, the determination does not give any permission to SEFA to burn or process flyash in the STAR Reactor. SEFA will need to evaluate and submit a permit application for an air permit, as needed, for burning / processing flyash, as discussed herein, in the STAR Reactor at any location in NC.

If you have any questions regarding this determination, please contact Rahul P. Thaker, P.E., QEP, at (919) 707-8470.

<sup>&</sup>lt;sup>3</sup> Email dated 5/12/2015 from Thomas Pritcher, Environmental Consulting & Technology, Inc., to Rahul Thaker, NCDAQ.

Sincerely,

With With \_\_\_\_

William D. Willets, P.E., Chief, Permitting Section Division of Air Quality, NCDENR

c: Central Files

**APPENDIX G** 

**RACT ANALYSIS** 



# <u>REASONABLY AVAILABLE CONTROL TECHNOLOGY (RACT) ANALYSIS FOR</u> <u>STAR<sup>®</sup> UNIT</u>

Duke Energy Carolinas, LLC (Duke Energy) is currently permitted (Air Permit No. 03786T34) to operate the Buck Steam Station located in Rowan County, North Carolina. Duke Energy is proposing to install and operate a fly ash processing facility consisting of a Staged Turbulent Air Reactor (STAR<sup>®</sup>) plant and associated ash handling activities. The proposed STAR<sup>®</sup> unit will be a source of nitrogen oxides (NO<sub>x</sub>) and does not meet the definition of a boiler, indirect-fired process heater, stationary combustion turbine, or stationary internal combustion engine. However, the source is located at a facility that has the potential to emit 100 tons per year or more of NO<sub>x</sub> or 560 pounds per calendar day or more from May 1 through September 30. As a result, the proposed emission unit is subject to the NO<sub>x</sub> RACT requirements listed in 15A 02D.1413 – Sources Not Otherwise Listed in this Section.

The NO<sub>x</sub> RACT analysis was performed in accordance with EPA's top-down method. The first step in the top-down RACT procedure is identification of available control technologies. Following identification of available control technologies, the next step in the analysis is to determine which technologies may be technically infeasible. The third step in the top-down RACT process is the ranking of the remaining technically feasible control technologies from high to low in order of control effectiveness. And fourth step is to evaluate the most suitable technology.

The fifth and final step is the selection of a RACT emissions limitation or a design, equipment, work practice, operational standard, or combination thereof corresponding to a reasonable, technically feasible control technology that was not eliminated based on adverse energy, environmental, or economic grounds.

## **RACT ANALYSIS FOR NOx**

## Step 1—Potential Control Technologies

Available technologies for controlling NO<sub>x</sub> emissions from STAR reactor include the following:

- Selective catalytic reduction (SCR).
- Selective non-catalytic reduction (SNCR).

- o Staging of Air.
- o Water Injection.

A description of each of the listed control technologies is provided in the following subsections.

#### **Selective Catalytic Reduction**

SCR reduces  $NO_x$  emissions by reacting ammonia or urea with exhaust gas  $NO_x$  to yield nitrogen and water vapor in the presence of a catalyst. Ammonia is injected upstream of the catalyst bed where the following primary reactions take place:

$$4NH_3 + 4NO + O_2 \rightarrow 4N_2 + 6H_2O \tag{1}$$

$$4NH_3 + 2NO_2 + O_2 \rightarrow 3N_2 + 6H_2O \tag{2}$$

The catalyst serves to lower the activation energy of these reactions, which allows  $NO_x$  conversions to take place at a lower temperature than the exhaust gas. The optimum temperatures range from as low as 350°F to as high as 1,100°F (typically 600 to 750°F), depending on the catalyst. Typical SCR catalysts include metal oxides (titanium oxide and vanadium), noble metals (combinations of platinum and rhodium), zeolite (alumino-silicates), and ceramics.

Factors affecting SCR performance include space velocity (volume per hour of flue gas divided by the volume of the catalyst bed), ammonia/NO<sub>x</sub> molar ratio, and catalyst bed temperature. Space velocity is a function of catalyst bed depth. Decreasing the space velocity (increasing catalyst bed depth) will improve NO<sub>x</sub> removal efficiency by increasing residence time but will also cause an increase in catalyst bed pressure drop. The reaction of NO<sub>x</sub> with ammonia theoretically requires a one-to-one molar ratio. Ammonia/NO<sub>x</sub> molar ratios greater than one-to-one are necessary to achieve high NO<sub>x</sub> removal efficiencies due to imperfect mixing and other reaction limitations. Reaction temperature is critical for proper SCR operation. Below this critical temperature range, reduction reactions (1) and (2) will not proceed. At temperatures exceeding the optimal range, oxidation of ammonia will take place resulting in an increase in NO<sub>x</sub> emissions. NO<sub>x</sub> removal efficiencies for SCR systems typically range from 80 to 90 percent.

#### **Selective Noncatalytic Reduction**

The SNCR process involves the gas phase reaction, in the absence of a catalyst, of NO<sub>x</sub> in the exhaust gas stream with injected ammonia or urea to yield nitrogen and water vapor. The two commercial applications of SNCR include the Electric Power Research Institute's NO<sub>x</sub>OUT<sup>TM</sup> and Exxon's Thermal DeNO<sub>x</sub><sup>TM</sup> processes. The two processes are similar in that either ammonia (Thermal DeNO<sub>x</sub><sup>TM</sup>) or urea (NO<sub>x</sub>OUT<sup>TM</sup>) is injected into a hot exhaust gas stream at a location specifically chosen to achieve the optimum reaction temperature and residence time. Simplified chemical reactions for the Thermal DeNO<sub>x</sub><sup>TM</sup> process are as follows:

$$4NO + 4NH_3 + O_2 \rightarrow 4N_2 + 6 H_2O \tag{3}$$

$$4 \text{ NH}_3 + 5 \text{ O}_2 \rightarrow 4\text{NO} + 6 \text{ H}_2\text{O} \tag{4}$$

The NO<sub>x</sub>OUT<sup>TM</sup> process is similar with the exception that urea is used in place of ammonia. The critical design parameter for both SNCR processes is the reaction temperature. At temperatures below 1,600 degrees Fahrenheit (°F), rates for both reactions decrease allowing unreacted ammonia to exit with the exhaust stream. Temperatures between 1,600 and 2,000°F will favor reaction (3), resulting in a reduction in NO<sub>x</sub> emissions. Reaction (4) will dominate at temperatures above approximately 2,000°F, causing an increase in NO<sub>x</sub> emissions. Due to reaction temperature considerations, the SNCR injection system must be located at a point in the exhaust duct where temperatures are consistently between 1,600 and 2,000°F.

#### **Staging of Air and Water Injection**

Staging of air and injection of water into the primary combustion reduces formation of thermal  $NO_x$  by decreasing the peak combustion temperature and reduces the residence time at the peak temperature. Water injection decreases the peak flame temperature by diluting the combustion gas stream and acting as a heat sink by absorbing heat necessary to vaporize the water (latent heat of vaporization) and raise the vaporized water temperature to the combustion temperature. A lower peak temperature occurs at stoichiometric ratios where  $NO_x$  formation is less likely to occur. A smaller residence time at the peak temperature reduces the amount of nitrogen that can become ionized and therefore reduces the formation of  $NO_x$ .

#### Step 2—Technical Feasibility

**SCR** uses either ammonia or urea as a reagent along with a catalyst to reduce  $NO_x$  into molecular nitrogen and water vapor. The optimum temperature for SCR varies based on the catalyst used and the composition of the flue gas, but typically occurs between 480°F and 800°F. Due to this requirement, the application point would need to occur before the product baghouse which would expose the SCR to 100% of the product ash loading. This would result in severe erosion of the pollution control equipment. In addition, any ammonia slip from the SCR would result in product contamination.

**SNCR** uses either ammonia or urea as a reagent to reduce  $NO_x$  into molecular nitrogen and water vapor. The optimum temperature for SNCR varies based on the composition of the flue gas, but typically occurs between 1650°F and 2000°F. These temperature requirements are above the normal operating regime for the STAR reactor. In addition, since this application point occurs before the product baghouse, ammonia slip would result in product contamination.

## **Staging of Air and Water Injection:**

As discussed above in Step 1, Staging of air and Water injection reduces the peak temperature within the reactor, and reduces the residence time at the peak temperature which reduces the formation of  $NO_x$ . Staging of air and water injection in the STAR<sup>®</sup> unit already occur since air and water are part of the ingredients added to the reactor to create the final ash product. Therefore, both methods can be easily used to suppress  $NO_x$  formation.

## **Step 3—Ranking of Controls**

Due to the risk of product contamination from SCR and SNCR processes, use of both air staging and water injection is the only feasible control measure; therefore, no ranking of the potential control approaches is necessary.

## Step 4—Evaluation of Most Effective Controls

As stated previously, use of a combination of air staging and water injection is the only feasible control measure available to the STAR process.

## Step 5—Selection of RACT

Due to the risk of product contamination from SCR and SNCR processes, a combination of air staging and water injection are the best methods to control  $NO_x$  formation in the STAR<sup>®</sup> unit. There are three permitted STAR<sup>®</sup> units (two in South Carolina and one in Maryland), and none were subject to a control technology review analysis. Duke Energy is proposing a  $NO_x$  emissions limit of 0.12 lb/MMBtu for the STAR<sup>®</sup> unit. The proposed limit is based on:

- Review of the other permitted STAR<sup>®</sup> units that have permit limits ranging from 0.34 lb NO<sub>x</sub>/MMBtu to 0.05 lb NO<sub>x</sub>/MMBtu. Please note that the 0.05 lb NO<sub>x</sub>/MMBtu permit limit is associated with a STAR<sup>®</sup> unit that is not currently permitted to process ash from ponds and/or landfills.
- Review of 2016 NO<sub>x</sub> stack test data for the Winyah STAR<sup>®</sup> unit that showed values ranging from 0.05 lb NO<sub>x</sub>/MMBtu to 0.08 lb NO<sub>x</sub>/MMBtu
- Consideration of the potential variability and inconsistency in the proposed ash pond feedstock, which can create variability in NO<sub>x</sub> emission rates.
- Consideration of a reasonable limit for a technology/process that is still developing.

## **Proposed Demonstration of Compliance**

Duke Energy proposes to demonstrate compliance with the proposed NO<sub>x</sub> RACT limit through an initial performance test and subsequent performance testing on an annual basis. Duke Energy also proposes that if two consecutive annual source tests show compliance, then the frequency of testing be reduced to once every five years. If after the frequency of testing is reduced, a source test shows that the proposed emission limit is exceeded, the STAR<sup>®</sup> unit will be tested annually until two consecutive annual tests show compliance.

**APPENDIX H** 

CAM PLAN



## COMPLIANCE ASSURANCE MONITORING PLAN

for

Sulfur Dioxide (SO<sub>2</sub>) Emissions from STAR® Unit

Duke Energy Carolinas, LLC - Buck Combined Cycle Facility

Salisbury, Rowan County, North Carolina

## I. Background

A.	Emissions Unit and C	Control Device
	EU ID:	ES-74
	Description:	STAR® (Staged Turbulent Air Reactor) system with a 140 million Btu/hour total heat rate input that processes feed-stock (fly ash and other ingredient materials) into a variety of commercial products
	Control Device	Dry Flue Gas Desulfurization (FGD) scrubber and bagfilter for SO <sub>2</sub> emissions control
-		

B. Applicable Emissions Limits and Monitoring Practices

*Emissions Limits:* SO<sub>2</sub> :

2.3 pounds of sulfur dioxide per million BTU input per 15A NCAC 02D .0516 Sulfur Dioxide Emission From Combustion

Compliance Demonstration Requirements: SO<sub>2</sub> Initial performance tests

Initial performance tests will be conducted.

Lime-to-Sulfur Ratio XXX establish compliance demonstration procedures for parametric monitoring systems.

Baghouse  $\Delta P$  XXX establish compliance demonstration procedures for parametric monitoring systems.

Periodic Monitoring Requirements:

**TBD** 

 $SO_2$ 

Lime-to-Sulfur Ratio TBD

Baghouse  $\Delta P$  TBD

## C. Control Technology

Dry FGD scrubber and bagfilter for SO<sub>2</sub> emissions control

## D. Potential Emission Rates

Pre-control SO<sub>2</sub>: XXX tons/year Post-control SO<sub>2</sub>: XXX tons/year (assumes 95% control)

## II. Monitoring Approach

## A. Background

For emissions of sulfur dioxide (SO<sub>2</sub>) from the STAR® system, Duke Energy is subject to Compliance Assurance Monitoring (CAM) requirements for the state SO<sub>2</sub> standard, i.e., 2.3 lb/MMBtu per 15A NCAC 02D .0516.

Duke Energy selected Lime-to-Sulfur Ratio and Pressure drop across the baghouse (Baghouse  $\Delta P$ ) as indicators for the CAM Plan for SO<sub>2</sub> emissions from the STAR® system. Duke Energy conducted testing for SO<sub>2</sub> emissions to derive a relationship between the Lime-to-Sulfur Ratio and SO<sub>2</sub> emissions of the STAR® system. This relationship was then used to determine a Lime-to-Sulfur Ratio value for the applicable SO<sub>2</sub> limit, such that as long as the Lime-to-Sulfur Ratio is at or above the value during normal operation, there is a reasonable assurance that the STAR® system will also comply with the respective applicable SO<sub>2</sub> emission limit. This relationship was used to determine appropriate Lime-to-Sulfur Ratio value for the state standard of 2.3 lb/mmBtu. In addition, Duke Energy established an appropriate Baghouse  $\Delta P$  range based on manufacturer's specifications and recommendations. It is assumed as long as the Baghouse  $\Delta P$  is within the established range during normal operation, there is a reasonable assurance that the dry FGD baghouse is operating as designed and the STAR® system will also comply with the respective applicable SO<sub>2</sub> emission limit.

## B. <u>CAM SO<sub>2</sub> Testing</u>

SO<sub>2</sub> testing was conducted to derive a relationship between the Lime-to-Sulfur Ratio and SO<sub>2</sub> emissions of the STAR® system. The SO<sub>2</sub> testing was conducted for operating conditions of the dry FGD system resulting in High-Ash Sulfur Content, Mid- Ash Sulfur Content and Low- Ash Sulfur Content.

The table below provides a summary of the test results for CAM testing completed on XXXX. Each test consisted of at least three runs using USEPA Test Method XXX for XXX. For the operating conditions tested, all SO<sub>2</sub> emission test results were less than XX percent of the applicable state SO<sub>2</sub> emission limitation (2.3 lb/mmBtu).

## Insert Table of Results

Baghouse  $\Delta P$  was monitored and recorded during the testing to verify that the operating range of ..... is appropriate for the baghouse

## C. <u>CAM Averaging Period</u>

The CAM Rule does not provide specific averaging periods to be used in the development of monitoring approaches. However, 40 CFR 64.3(d)(3)(i) implies that the appropriate averaging period is the averaging period of the underlying emissions standard. Since emissions testing for SO<sub>2</sub> includes at least three test runs, each nominally one-hour in duration, this indicates that a three-hour averaging period is an appropriate averaging time for purposes of CAM for the state rule.

## D. <u>CAM Excursion</u>

During "normal operation", (i.e., periods other than startup, shutdown or malfunction), an excursion is a rolling three-hour period Lime-to-Sulfur Ratio is less than the establish value during testing. Each excursion must be investigated by the source to determine the monitoring status and operating conditions responsible for the excursion.

## E. <u>CAM Excursion Corrective Action</u>

Upon detecting an excursion, Duke Energy will implement corrective action to restore the indicator to the appropriate indicator range. Corrective action should begin with an evaluation of the monitoring system to determine if the excursion is related to the monitoring system or the control device. Individual unit process and control device operating parameters will be reviewed to determine the cause of the excursion. To the extent possible, any corrective action should reduce the potential of similar excursions from recurring.

## F. <u>CAM Reporting Requirements</u>

All excursions must be reported in the facility's semi-annual report. As required by the CAM Rule, the Permittee shall include summary information on the number, duration and cause of excursions and the corrective actions taken. It is not necessary to report SO<sub>2</sub> control equipment malfunctions that do not cause an excursion. Duke Energy will also include summary information on the number, duration, and cause of monitor downtime incidents.

## G. <u>Summary of Proposed CAM for SO2</u>

Continuous monitoring of Lime-to-Sulfur Ratio is required. If the Lime-to-Sulfur Ratio does not fall below the level established during initial compliance testing and the Baghouse  $\Delta P$  is within the established range provided by manufacturer's specifications and recommendations, then compliance will be reasonably assured. The minimum Lime-to-Sulfur Ratio will not apply during periods of startup, shutdown, or malfunction. A summary of the CAM plan is provided in Table 1.

## Table 1 SO<sub>2</sub> CAM Plan Summary – Buck Combined Cycle Facility

STAR® Unit (ES-74)

A. Indicator	Lime-to-Sulfur Ratio and Baghouse ΔP
Measurement Approach	XXXX
B. Indicator Range	An excursion is defined as
	The Lime-to-Sulfur Ratio to be determined during the initial performance testing will provide reasonable assurance of compliance with limits to be contained in the Title V air permit. Excursions will trigger an inspection of the Lime injection system to determine the cause and necessary corrective action. If the Lime-to-Sulfur Ratio falls below acceptable levels (e.g. an excursion) for more than XX consecutive unit operating hours, a test will be performed to re-establish the SO <sub>2</sub> emission rate and lime injection correlation for the ash sulfur content range. Baghouse $\Delta P \dots$
<b>C. Performance Criteria</b> 1. Data Representativeness	TBD
2. Verification of Operational	TBD
Status	
<ol> <li>QA/QC Practices and Criteria</li> <li>Monitoring Frequency</li> </ol>	TBD TBD
<ol> <li>Data Averaging Period</li> </ol>	TBD
6. Data Collection	Automated data acquisition system (DAHS)

## III. Monitoring Approach Justification

A. <u>Explanation of Applicability</u>Justification will be added based on final vendor design data

B. <u>Rationale for Selection of Indicator Ranges</u> To be determined...

NC DEQ will be provided copies of test results from all required tests.

C. <u>Rationale for Selection of Corrective Actions</u> To be determined...



**APPENDIX I** 

# ZONING COMMISSION DOCUMENTATION

